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Graphical abstract



1 Life cycle assessment as development and decision

2 support tool for wastewater resource recovery

3 technology

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8 Keywords

9 Resource recovery, life cycle assessment, technology development, wastewater treatment, enhanced

10 biological phosphorus removal, algal cultivation

11 Abstract

12 Life cycle assessment (LCA) has been increasingly used in the field of wastewater treatment where the focus 13 has been to identify environmental trade-offs of current technologies. In a novel approach, we use LCA to 14 support early stage research and development of a biochemical system for wastewater resource recovery. The 15 freshwater and nutrient content of wastewater are recognized as potential valuable resources that can be 16 recovered for beneficial reuse. Both recovery and reuse are intended to address existing environmental 17 concerns, for example water scarcity and use of non-renewable phosphorus. However, the resource recovery 18 may come at the cost of unintended environmental impacts. One promising recovery system, referred to as 19 TRENS, consists of an enhanced biological phosphorus removal and recovery system (EBP2R) connected to 20 a photobioreactor. Based on a simulation of a full-scale nutrient and water recovery system in its potential 21 operating environment, we assess the potential environmental impacts of such a system using the 22 EASETECH model. In the simulation, recovered water and nutrients are used in scenarios of agricultural

23 irrigation-fertilization and aquifer recharge. In these scenarios, TRENS reduces global warming up to 15% 24 and marine eutrophication impacts up to 9% compared to conventional treatment. This is due to the recovery and reuse of nutrient resources, primarily nitrogen. The key environmental concerns obtained through the 25 26 LCA are linked to increased human toxicity impacts from the chosen end use of wastewater recovery 27 products. The toxicity impacts are from both heavy metals release associated with land application of 28 recovered nutrients and production of AlCl₃, which is required for advanced wastewater treatment prior to 29 aquifer recharge. Perturbation analysis of the LCA pinpointed nutrient substitution and heavy metals content 30 of algae biofertilizer as critical areas for further research if the performance of nutrient recovery systems 31 such as TRENS is to be better characterized. Our study provides valuable feedback to the TRENS developers 32 and identified the importance of system expansion to include impacts outside the immediate nutrient 33 recovery system itself. The study also showed for the first time the successful evaluation of urban-to-34 agricultural water systems in EASETECH.

35 1. Introduction

36 Sustainability in the urban water cycle is increasingly at the forefront of discussions on new treatment 37 technologies due changes in climate, population, and regulation (Guest et al., 2009). Wastewater resource 38 recovery and reuse is one area where technology is responding to the need for pollution prevention and 39 resource efficiency. Wastewater (also referred to as used water – Verstraete et al., 2009) technology 40 development has traditionally been compliance-driven, designed to meet safety and discharge regulations. 41 During conventional treatment, nutrients – notably nitrogen and phosphorus – are biologically and physical-42 chemically converted and removed from the water. Increasingly, the freshwater and nutrient content of 43 wastewater are recognized as resources that can be recovered to address existing environmental concerns (e.g. 44 water scarcity, use of non-renewable phosphorus) (Guest et al., 2009). However, resource recovery may 45 come at the cost of increased treatment intensity and there is a need to assess treatment systems from a 46 holistic systems perspective so that the quest for sustainability in the water cycle does not overshadow other 47 environmental concerns (Mo & Zhang, 2013, Batstone et al., 2014).

48 TRENS is a wastewater resources recovery technology currently under development (Valverde-Pérez et al., 49 2015b), which combines an enhanced biological phosphorous removal and recovery (EBP2R) system 50 (Valverde-Pérez et al., 2015) with a downstream photobioreactor (PBR) to cultivate green microalgae under 51 optimal growth conditions. The system recovers both water and nutrient resources from wastewater, with the 52 nutrients being taken up and encapsulated by the algal biomass. This water and algae suspension can then be 53 used together (for combined irrigation and fertilization, otherwise referred to as fertigation) or individually if 54 the algae are harvested through solid-liquid separation. The coupled system is a completely biological process that is less chemical and energy intensive than conventional physical-chemical phosphorus removal 55 processes - e.g. struvite precipitation, ultrafiltration (Valverde-Pérez et al., 2015), thereby reducing the water 56 57 and energy demand of traditional algae cultivation (Clarens et al., 2010). In recent years, Life Cycle Assessment (LCA) has been used in environmental assessment of urban water 58 59 systems (Loubet et al., 2014), including wastewater specific studies (Corominas et al., 2013, Zang et al., 60 2015). Moreover, LCA has been used in understanding environmental trade-offs in optimizing specific 61 treatment technologies such as ozonation (Rodríguez et al. 2012). Recent wastewater related LCA studies for 62 technology development include coupled wastewater treatment for microalgae biofuel production 63 (Rothermel et al., 2013) and nutrient removal and recovery from anaerobic digestion supernatant (Rodriguez-Garcia et al., 2014). Both of these studies report the need to expand the system boundaries to include the 64 wastewater treatment plant (WWTP) when evaluating wastewater technologies and emphasize the need to 65 consider options at a plant level rather than at a unit process level. One of the challenges of LCA is 66 delineating the system boundary since they vary widely, with some studies limited to the WWTP and others 67 encompassing the entire urban water system (Corominas et al., 2013, Zang et al., 2015). The environmental 68 performance of WWTPs is largely dependent on effluent discharge and sludge application on land (Hospido 69 70 et al., 2004, 2012, Foley et al., 2010), although plant performance can be affected by influent composition, 71 plant size, and local climate (Lorenzo-Toja et al., 2015). Furthermore, the sludge and solids stream of 72 wastewater treatment accumulates beneficial and problematic compounds (e.g. phosphorus and heavy 73 metals) that need to be included in LCA (Yoshida et al., 2013). Therefore, any environmental assessment of

a novel wastewater technology needs to include life cycle boundaries that encompass the end use of waterand nutrients.

76 This is the first study related to LCA-supported technology development that accounts not only for the 77 WWTP, but also the larger system, which includes the urban-rural water connection and end-use of 78 recovered water and nutrients. This broader system boundary is particularly necessary in view of the 79 development objectives of TRENS, which is to provide an efficient resource recovery technology. An LCA 80 carried out in the early development phase of TRENS provides a diagnostic opportunity: a chance to identify 81 environmental impacts that may be roadblocks to developing and marketing a sustainability-focused 82 technology. Moreover, the LCA results become documentation for sustainability that can iteratively follow 83 TRENS throughout its development, optimization, and ultimately implementation. The study objectives are (1) to demonstrate the use of LCA in the early research and development phase of a 84 new wastewater process by quantifying its environmental performance using accepted impact categories; (2) 85 to provide a first assessment of the environmental impacts of the TRENS system and (3) to use LCA results 86 87 to provide feedback for additional research by identifying further areas of interest and data needs. The

- 88 TRENS performance is assessed in three scenarios based on the Lynetten WWTP in Copenhagen. The
- 89 scenarios were chosen to ensure an evaluation that captures the necessary infrastructure additions,
- 90 operational changes, and reuse options.
- 91 2. Materials and Methods

92 **2.1. Framing a context for water and nutrient recovery**

93 Copenhagen and its surrounding municipalities are supplied entirely by groundwater. HOFOR, the local 94 water utility, supplies approximately 50 million m³ annually to 1 million residents in the area. A high 95 percentage of Danish households (>85%) are connected to the sewers, meaning a large portion of the 96 distributed water resource can be recaptured (Hochstrat et al., 2005). The Lynetten WWTP serves a 97 catchment area of 76 km² of the central and North-East sections of Copenhagen (Flores-Alsina et al., 2014)

and treated 59.3 million m³ in 2012 (Lynettefællesskabet I/S). In the existing Lynetten WWTP, the effluent 98 99 is discharged and mixed into the sea water of Øresund. Through the treatment process, nitrogen resources in 100 the wastewater are converted to free nitrogen gas and lost to the atmosphere, while phosphorus is lost to the 101 sludge and subsequently incinerated. In the WWTP, excess phosphorus that is not taken up in the biologically process is removed through chemical precipitation using iron (III) chloride (FeC13). 102 The groundwater resource surrounding Copenhagen is over-exploited due to abstraction for drinking water. 103 104 Henriksen et al. (2008) reported an estimated deficit of 77 million m³/year for the Northern-Zealand area, 105 which encompasses Copenhagen. However, the refinement in spatial resolution can change results of water 106 stress evaluations by 10-53% (Hybel et al., 2015). In this context, wastewater reuse presents a valid 107 opportunity to ameliorate the local groundwater resource deficit related to the Northern-Zealand area. In 108 particular, there is an opportunity to collect water from the high-use urban area and return it to the rural 109 groundwater abstraction areas.

Regulatory standards of treated wastewater reuse for irrigation or aquifer recharge are not specifically addressed by existing European Union (EU) policies, although there is an on-going effort to identify appropriate policies and encourage reuse (EC, 2012). Treated wastewater is most commonly reused for nonpotable purposes such as irrigation of non-food crops or crops requiring further processing (Bixio et al., 2006). This restricted use is due partly to the public's perceived risks from wastewater and partly to the lack of formal regulatory frameworks (Bixio et al., 2005, Chen et al., 2012). The implications of water quality, and therefore treatment needs, for scenario design is presented in Section 2.3.

117 2.2. TRENS process addition to existing WWTP

The TRENS system was included in this study as a side-stream process, where a portion of the influent wastewater at the Lynetten WWTP was diverted, while the remainder passed through existing conventional treatment (**Fig. 1**). The new side-stream system was designed to treat 10% of WWTP influent flow, which is approximately 5.9 million m³/yr or 16247 m³/d. This flow rate is in excess of the reported local agricultural demands for irrigation water (2.1 and 0.93 million m³/yr for Zealand and the Capital Region, respectively,

covering 2561 km² in total). However, it is possible that irrigation values are underestimated since the total is
based on self-reported water use from only 22% of the farms surveyed, in addition to inferred values from
the non-responders (EC, 2010). It was also assumed that crop selection and irrigation practices may increase
to take advantage of the available supply of reuse water. The TRENS system was designed to produce a
nitrogen to phosphorus ratio (N-to-P ratio) of 16 optimal for microalgae cultivation in the PBR (ValverdePérez et al, 2015b). The nutrient concentration in the TRENS water is 47 mg/L N and 6.5 mg/L P, thereby
recovering 9 and 8% respectively of the nitrogen and phosphorus load to the Lynetten WWTP.

130 **2.3. Scenario construction**

131 Although many reuse options exist for reclaimed water (i.e. reuse in urban cleaning, industrial applications, 132 control of salt water intrusion), this study focuses on two reuse scenarios that were considered most 133 applicable to the TRENS system and the Danish context (Table 1). First, agriculture is the second largest water use sector after urban use and would therefore be a logical recipient of TRENS effluent which contains 134 both nutrients and water. Second, as groundwater is the main freshwater supply in Denmark, aquifer 135 recharge is an obvious method to augment freshwater sources. In addition, both agricultural irrigation and 136 137 aquifer recharge are common and well-documented options for wastewater reuse (Bixio et al., 2006, EEA, 2010). Although the two scenarios are modeled separately in this study, it is possible to consider them as 138 complementary where fertigation and aquifer recharge could be used at the same time with various flow 139 140 ratios or individually at different times of the year. These use combinations were not modeled in order to 141 minimize the scenario complexity. Additionally, the two scenarios represent two extreme cases for nutrient 142 reuse, one where the nutrients are recovered continuously and the other where no nutrients are recovered.

For the agricultural fertigation scenario it is assumed that the nutrients and water must be used together. If TRENS is used to supply a crop with 300 mm/year of irrigation water, the average nutrient load would be approximately 140 kg/ha for N and 20 kg/ha for P, similar to the nutrient needs for common Danish crops such as winter wheat (Olesen et al., 2009). Since the water and nutrients are used together, either the water demand or the nutrient demand will be met first depending on numerous factors such as crop type, farming

practices, and local climate. In reality, fertilizer and water requirements may have large variations seasonally and across crop types and this complexity is not captured in the scenario. This scenario makes a simplifying assumption that fertilizer and water needs are constant throughout the year and TRENS operation continues uninterrupted. In this scenario, TRENS water is not further treated for pathogen removal since irrigation is not targeted at any specific crop and the potential need for further treatment would vary by crop (e.g. less strict for biofuel production than for tomato production).

154 In the aquifer recharge scenario, the microalgae component is separated out and ultimately incinerated.

155 Although the nutrients are an integral portion of the TRENS system, the intention of this scenario is to

156 explore the water recovery and reuse aspect independent of the nutrients. Excluding nutrient recovery also

157 results in a more conservative outcome since there are no environmental benefits from nutrient reuse. Due to

158 the lack of EU-specific policies on water quality for aquifer recharge, the technology-based Californian Title

159 22 regulation was used to define additional treatment processes including: coagulation/flocculation,

160 sedimentation, filtration, and UV disinfection (Bixio et al., 2006).

161 From a TRENS perspective, the aquifer recharge scenario is possibly the least optimal way to operate the 162 system since the nutrients are not utilized. Together with fertigation, which is possibly the most optimal way 163 TRENS can be operated, these two scenarios form the operational "envelope" for a potential TRENS system. 164 Neither scenario is completely realistic, but gives a simplified view of possibilities.

165 **2.4. LCA Methodology**

The LCA is performed using EASETECH (DTU, Denmark), a model that allows handling of heterogeneous materials and tracking of flows at the substance level essential for evaluation of environmental technologies (Clavreul et al., 2014). Although initially developed for waste management systems, EASETECH's ability to handle mass and individual substance flows allows for detailed modelling of wastewater treatment systems (Yoshida et al., 2014a). The study follows the four-phased, iterative approach defined by ISO (2006) consisting of (1) goal and scope definition, (2) inventory analysis, (3) impact assessment, and (4) results interpretation.

173 **2.4.1.** LCA - goal and scope

174 The goal of the LCA is to quantify the environmental impacts of wastewater resource recovery and reuse in 175 agricultural crops production and in aquifer recharge associated with the operation of Lynetten WWTP, 176 located southeast of Copenhagen, Denmark. To that end, the boundaries of this study are defined as starting 177 from the influent of the WWTP, and extend to cover the WWTP itself, the TRENS side-stream process, 178 transportation of the treated water in a pressurized pipeline, and final end use (including any additional 179 advanced treatment required). Construction and operating phases are included in the scope. However, end-180 of-life phases for the WWTP and TRENS system are not included. Studies related to WWTPs (Foley et al, 181 2010) and water reuse (Ortiz et al., 2007, Tangsubkul et al., 2005) have reported that end-of-life phases 182 contribute relatively little to overall impacts compared to the construction and operation phases. Within the 183 operating phase, both direct emissions (e.g. gas and treated water effluent) and indirect emissions (e.g. 184 derived from production of chemicals and power generation) are included. The functional unit is defined as 1 m³ of influent wastewater with the same composition as reported by Lynettefællesskabet I/S (2012), as the 185 186 primary function of the WWTP system – with or without TRENS sidestream – is to maintain public health 187 and environmental water quality, with fertigation and aquifer recharge as secondary benefits.

188

2.4.2. Life cycle inventory

189 Life cycling inventory (LCI) data was collected from operating reports for existing processes, databases, and 190 model results. Background inventory data was obtained through the Ecoinvent LCA database that contains 191 unit process data valid mainly for Swiss and European markets (Frischknecht et al., 2005). Where TRENS 192 water is used for crop irrigation, the nutrients N and P contained in the microalgae are assumed to offset 193 mineral fertilizer application and production. In this study, both N and P substitutability is assumed as 100% 194 based on algae fertilizer performance on seedlings as reported in Mulbry et al. (2005). It is further assumed 195 that microalgal fertilizer would result in zero runoff and leaching, and would perform similarly to mineral fertilizer in terms of ammonia volatilization, and soil mineralization. This assumption is analyzed in section 196 3.2.6 as it is known to be an oversimplification from other applications of biomass to land (Yoshida, 2014c). 197 198 Although promising, the use of algae as fertilizer is still under investigation, as the influence of algae

harvesting and application methods on fertilizer stability, availability, and performance is still poorly
documented in literature (Shilton et al. 2012). Additionally, the substitution of organic mineral fertilizer
depends on factors such as soil property and application technique (Lundin et al., 2000).

202 An analysis was made regarding nutrient leaching from algae fertilizer on environmental performance by increasing leaching of applied nutrient N and P to groundwater in the model from 0 to 10%. This study 203 initially assumed an optimal PBR operation where all the nutrients would be encapsulated in algae biomass. 204 205 Thus, the model was run with zero nutrient leaching to groundwater. This meant, there was no adverse 206 environmental impact and this process could not be identified during contribution analysis. However, this 207 process is important to investigate because one of the key benefits of algae fertilizer is its expected reduction 208 of nutrient mobility. The leaching could occur if the nutrients sent to the PBR were not completely taken up 209 by the algae and some remained in the water phase when it is sent to the irrigation systems.

Electricity production was based on consumption of Danish specific electricity mix, which is predominantly fossil-based and uses coal (46.6%), natural gas (24.4%), wind (12.4%) and heavy fuel oil (10.2%) as the main sources (EC-JRC, 2002).

213

2.4.3. Impact assessment

214 This study uses the LCIA method recommended by the International Reference Life Cycle Data System 215 (ILCD) (EC-JRC, 2010), commonly referred to as ILCD 2011. This method was selected as it consists of 216 fourteen impact categories based on existing best practice. Human toxicity related impacts were assessed 217 using USETox, which is included in ILCD 2011 as best-of-the-field. Nevertheless, USETox results, 218 particularly for metals, should be interpreted with caution since there are still many uncertainties related to 219 the characterization factors (e.g. degradation rate, exposure routes). Results are normalized using 220 normalization factors from Blok et al. (2013) and presented in milli-person equivalents (mPE), where 1 mPE 221 represents one thousandths of an average European person's annual impact.

222 **2.4.4.** Contribution and perturbation analysis

The approach recommended by Clavreul (2013) for uncertainty and sensitivity assessment is used as the basis for the contribution and perturbation analysis. The goal is to systematically identify potential sources of uncertainty, while operating under data scarcity and limited resources to evaluate the large number of inputs in the LCA model. This approach takes advantage of the iterative nature of LCA and uses the initial results from LCIA. The following steps were performed:

- 1. The contribution analysis identified any process (e.g. WWTP operation or biogas collection) that
- contributed more than 5% to any impact category. Then, the key parameters that collectively contribute

230 to >90% of the process impacts were identified (e.g. N₂O emission during WWTP operation). The cut-

- off is arbitrary and assigned to constrain the number of parameters so that they can be evaluated in a
- limited time frame.
- 2. A perturbation analysis was performed whereby the parameters identified in step 1 were varied one at a
 time by 10% to gauge the sensitivity of the model output to the parameter input following the example of
 Yoshida et al. (2014a) and Clavreul et al. (2012). Parameter sensitivity was then evaluated using a
 sensitivity ratio (SR):

$$SR = \frac{\frac{\Delta results}{initial result}}{\frac{\Delta parameter}{initial parameter}}$$

3. The results were discussed to highlight the sensitive parameters. The limitation of the assessment is that
it does not take into account the actual uncertainty of the parameters, only how sensitive the model is to
these parameters. The benefit of this method is it allows refinement the number of parameters needed for
further data collection when ultimately conducting an uncertainty analysis.

241 **3. Results and discussion**

3.1. Inventory

A summary of the life cycle inventory results is presented in Table 2. More detail is available in the
Supporting Information.

245 **3.2. Impact assessment**

246 **3.2.1. Scenario A Status quo**

In the life cycle impacts of the existing Lynetten WWTP, the two impact categories of ecotoxicity (ETox) 247 248 and marine eutrophication (ME) are the highest at 3.1 and 1.0 mPE, respectively (Fig. 2). This is primarily 249 due to the discharge of treated effluent to the sea (Fig. 3). Nitrate-nitrogen in the effluent contribute most to the ME category, while the heavy metals in the effluent (mainly zinc and copper) contribute to the ETox 250 category. Global warming at 7.8×10^{-2} mPE (GWP) is the third highest category. The largest contributor to 251 this impact is energy consumption during WWTP operation (67%), followed by emissions of N_2O to air 252 253 during treatment (18%), emissions during incineration (11%), and leakage of methane during biogas 254 collection from the anaerobic digester (4%). Biogas combustion and subsequent use for district heating, 255 results in an offset GWP of -4.5%.

256 The emissions related to sludge incineration and biogas combustion are also major contributors to several impact categories, such as acidification (AC), terrestrial eutrophication (TE), and photochemical oxidant 257 formation (POF). Nitrogen oxides (NO_x) and sulfur-dioxide are the main compounds responsible in these 258 categories. Deposition of nitrogen and sulfur from the atmosphere contributes to acidification. In addition to 259 260 the acidifying effect, atmospheric deposition of nitrogen also contributes to terrestrial eutrophication 261 (Jaworski et al., 1997, Jeffries and Marron, 1997). Both NOx and sulfur dioxide contribute to POF since they 262 form ozone when exposed to sunlight, which ultimately contributes to urban smog (Derwent et al., 1998). The results suggest that the status quo model provides a reasonable representation of a large, centralized 263

264 WWTP consistent with other wastewater LCA studies. The WWTP electricity consumption is one of the

main contributors to global warming and fossil resource depletion as reported in Corominas et al. (2013). 265 266 Our study also finds that discharge to sea (primarily nitrate-nitrogen) is another main source of impacts, 267 consistent with results from Hospido et al. (2004). All impact categories except one are within the same order of magnitude as values obtained in an LCA study of the Avedøre WWTP in Copenhagen (Yoshida et 268 269 al., 2014a). The exception is for ETox where our result is more than twenty times higher than the median 270 value given by Yoshida et al. 2014a. One possible reason for the higher ETox value at Lynetten WWTP is that it discharged eight times the copper per 1 m³ of influent than Avedøre WWTP (Spildevandscenter 271 Avedøre I/S, 2012, Lynettefællesskabet I/S, 2012). 272

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3.2.2. Scenario B Agricultural fertigation

275 Implementation of Scenario B has predicted environmental impacts that are on the order of 0 to 0.2 mPE/ m³ 276 less than Scenario A. The small changes are partly due to the design of the side-stream system. Since only 10% of the influent water passes through the TRENS system, the impacts are dominated by the effects of 277 90% of the flow passing through the WWTP. In the fertigation scenario, the main WWTP processes (e.g. 278 discharge to sea and WWTP operation) continue to contribute to the impacts (Fig. 3b and c compared to Fig. 279 280 **3a**). However, the use-on-land process now plays a large part in the toxicity impacts (ETox, HTc, and HTnc). 281 Fig. 4a shows that the largest changes, both positive and negative, occur in the ME, ETox, HTc and HTnc 282 categories. Overall, the reduced impacts are a result of two main processes (Fig. 4b): (1) reduced flow 283 through WWTP secondary treatment leading to less N₂O emissions, and (2) offset mineral fertilizer 284 production. Increases in environmental impacts are mainly due to four processes: (1) land application of 285 algae suspension, (2) energy consumption of the TRENS system, (3) energy consumption of the pipeline, and (4) emissions from increased biogas combustion. 286

The largest change from the baseline (+0.19 mPE, +290%) is in the human toxicity, non-cancer effects
category (HTnc). This is almost entirely a result of heavy metals - primarily zinc and mercury - application
to soil from the treated effluent. The other toxicity categories (ETox and HTc) are similarly affected by the

heavy metals. The avoided production and application of mineral fertilizer (shown in Fig. 4 as fertilizer

substitution) results in some savings in toxicity related impacts. This is because mining of commercial
fertilizer ingredients such as phosphate rock brings with it the naturally occurring heavy metals, notably
cadmium (Wilsenach et al., 2003). These metals then end up in the soil once the fertilizer is applied. The
avoided mineral fertilizer production is also responsible for 1%-24% savings in other impact categories
(GWP, AC, TE, POF and PM), since there is lower production and therefore lower emissions from the
associated industrial processes. However, land application of the effluent results in a net toxicity increase.
There is a decrease in marine eutrophication from the baseline (-9.2e-2 mPE, -9%), which is almost entirely

(98%) due to the avoided discharge of nitrate-nitrogen to the sea. The TRENS side-stream diverted flow that would otherwise have entered the recipient water body (Øresund). In addition, during the TRENS process, soluble nitrogen, which has the potential to contribute to surface runoff and leaching, is taken up and stored in algal biomass prior to land application. Global warming impacts are reduced by 15% (1.2e-2 mPE) due to lower emissions of N₂O from the WWTP since the water diverted to TRENS does not undergo ammonia oxidation and denitrification, the main pathways for N₂O production (Kampschreur et al., 2009).

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3.2.3. Scenario C Aquifer recharge

The overall environmental performance of the aquifer recharge scenario is similar to that of the baseline,
 Scenario A (Fig. 5). Scenario C has reduced WWTP energy consumption, but increased in TRENS-related
 energy consumption resulting in a very minor net change in total energy use.

The ME impact category decreased 8.6e-2 mPE (9%) from the baseline as a result of avoided nitrate-nitrogen discharge due to diversion of the TRENS sidestream. The category with the largest percent increase is HTc (26%, 3.6e-3 mPE) as a result of pre-infiltration treatment, specifically due to production of aluminum chlorite (AlCl₃) used in the flocculation step of the pre-infiltration treatment to separate algae from the water. The production phase produces emissions of hexavalent chromium, Cr (VI), and arsenic, both of which are highly toxic. Niero et al. (2014) noted in a WWTP study that AlCl₃ production was one of the main processes contributing to ecotoxicity. Separation of the algae and water could also be achieved through

315 centrifugation or direct filtration, although these methods are associated with their own negative 316 environmental impacts related to high energy demand (Rothermel et al. 2013). All other impact categories 317 show changes of less than 5% from the baseline. In terms of the processes involved, biogas combustion is a 318 major contributor to increases in terrestrial eutrophication (TE) and photochemical oxidant formation (POF) 319 impact categories. This was a result of increased sludge, and associated biogas, production from the TRENS 320 system, thereby increasing biogas combustion and combustion-source pollutants (e.g. NOx). When compared to Scenario B (fertigation), the lack of nutrient recovery for agricultural reuse in this scenario meant higher 321 GWP (12%), AC (18%), TE (23%), and POF (12%). However, HTc and HTnc were 45% and 290% lower 322 323 than in the fertigation scenario, which shows the difference in diverting the nutrient water suspension to land, 324 versus just water.

325 Scenario C explored a reuse option that was at the extreme end for TRENS, since only the water is reused 326 and none of the recovered nutrients are reused. Although the environmental benefits are less pronounced 327 than in the fertigation scenario, there are still benefits in terms of the ME impact category. TRENS may be a 328 valid option in situations where there is interest in both water reuse and reducing nitrate-nitrogen discharge.

329 **3.2.4.** Relative importance of construction versus operation of the overall life cycle

The WWTP related impacts (**Fig. 6a**) are dominated by the operating phase, while the TRENS (**Fig. 6b**) and pipeline (**Fig. 6c**) impacts were more equally shared between the construction and operating life cycle phases. Furthermore, several impacts categories (TE, ME, POF, ETox, HTc, and RD) which are dominated by the operating phase for the WWTP, are instead dominated by the construction phase for TRENS and the pipeline. These differences were due to the higher use of plastic materials, specifically LDPE and HDPE plastics, in construction of the PBR and pipeline. In addition, the shorter service life of the PBR (15 years compared to 30 years for the WWTP) meant the construction phase impacts are more prominent.

The results are consistent with reports from Machado et al. (2007) and Pasqualino et al. (2010) who
considered the WWTP construction phase insignificant compared to the operating phase. In studies which
reported the opposite, Corominas et al. (2013) noted that those were for low-tech, non-energy intensive

processes which are not comparable to the Lynetten WWTP. In terms of PBR construction, Rothermel et al. 340 341 (2013) reported that LDPE plastic production contributed to increased eutrophication, as was observed in this 342 study. Silva et al. (2013) also found that the choice of construction material (in their case PVC plastic) 343 caused the majority of PBR construction impacts. Both sources recommended optimizing the use of plastics 344 in PBR construction as a way to reduce environmental impacts. It should be noted that this study's choice to 345 use LDPE, as a representative material for PBR construction, was based on Rothermel et al. (2013) and this choice explains that LDPE production contributes a large portion of the overall TRENS impacts. These 346 347 results illustrate the variability of life cycle phase contributions to environmental impacts. The construction phase was not important when dealing with the WWTP. However, this assumption should not be 348 349 extrapolated to apply to other systems such as the PBR and the pipeline, and the construction phase should 350 always be considered as supported by other piped network studies for both drinking water (Sanjuan-Delmás 351 et al., 2014) and sewers (Petit-Boix et al., 2014).

352 Other implications for technology developers and future implementation of TRENS are: i) for the TRENS 353 system, addressing both the construction and operating life cycle phases could have environmental benefits 354 since both phases contribute nearly equally to the environmental impacts; and ii) in Scenarios B and C, 355 TRENS (construction and operation) caused 4.4% and 3.5% of the overall environmental impacts. This was 356 for a side-stream TRENS system treating 10% of the total influent wastewater and this contribution should increase as the proportion of side-stream flow increases. These results are technology specific. Impact results 357 would change if the algae production takes place in an open pond system, which has lower energy 358 359 requirements, but also has drawbacks like high land use and lower productivity (Jorquera et al., 2010).

360

3.2.5. Contribution analysis

The contribution analysis shows that 10 of the 14 processes included in this study had a greater than 5% contribution to one or more impact categories (**Fig. 7**). In some cases, the process was mainly controlled by one parameter, while others were governed by multiple parameters. In all, 18 parameters were identified that govern the important processes (**Fig. 8**) out of the 100s of input parameters. For example, the process

365 "biogas collection" is a contributor to the GWP impact category and the key parameter responsible is the 366 percentage of methane leakage during collection. Another example is the "WWTP operation" process; its 367 impacts to GWP are governed by WWTP energy use, FeCl₂ use, and NaOH use, which collectively 368 contribute to more than 90% of the impacts. The implication for technology developers is that, in addition to 369 reducing the number of relevant processes and parameters, the contribution analysis reveals specific areas 370 where a system like TRENS may be competitive (i.e. FeCl₂ use can be reduced by switching from chemical 371 precipitation to TRENS for phosphorous removal and recovery).

372 **3.**

3.2.6. Perturbation analysis

The results of the perturbation analysis are plotted as SR for each impact category (**Fig. 9**), where a higher absolute value of SR means that the impacts category is more sensitive to that parameter. The results show that some parameters have impacts across a number of categories (e.g. WWTP energy use and sludge water content), while others are important only to certain categories (e.g. Zn discharge to sea in the Etox impact category).

Nitrogen and phosphorus can both lead to eutrophication of waterways – nitrogen primarily affects marine 378 waters while phosphorus affects freshwater - resulting in phytoplankton blooms and subsequent depletion of 379 380 dissolved oxygen necessary for other aquatic life (Stoate et al., 2001). When leaching of nitrogen to the 381 groundwater was increased from 0 to 10% in the fertigation scenario, marine eutrophication increased by 382 5.5%, with no change in all other categories. Increasing phosphorus leaching in the same scenario from 0 to 383 10% increased freshwater eutrophication by 3.5%, with less than 0.2% change in all other categories. In 384 reality, the concern lies with nitrogen leaching since phosphorus has limited mobility in soil (Stoate et al., 385 2001). These impact changes due to leaching are significant because algae fertilizer performance is still poorly documented (Shilton et al., 2012). The fertigation scenario showed a 9% decrease in marine 386 387 eutrophication under the assumption that nutrients are not lost from the farmland. This benefit may be lost if nutrient leaching is increased. 388

389

3.3. The use of LCA results to support technology research and development

The results of the base scenario, and the fertigation and aquifer recharge scenarios, show how crucial it is to assess new technologies in a holistic systems perspective. In the base scenario, most of the impacts of the full system are due to the WWTP, except for the impact categories ME and ETox. Conversely, in the fertigation scenario, most of the impacts take place outside the WWTP, with direct WWTP impacts playing a role in half of the impact categories. If the focus had been limited to the TRENS technology, which is the natural focus of technology developers, these impacts would not have been recognized.

396

397 For the fertigation scenario, increased toxicity appears to overwhelm the environmental benefits. The 398 impacts on eco- and human toxicity were primarily related to heavy metals application to soil, and 399 specifically to zinc and mercury carried in the TRENS effluent. Hospido et al. (2004) also found these metals 400 to be the main culprits of increased toxicity when wastewater sludge was applied to land. Tangsubkul et al. 401 (2005) noted that increased impacts on terrestrial environments might be inevitable when selecting a 402 technology that optimizes recycling of wastewater nutrients, due to the potentially higher metals loading 403 associated with higher nutrient recovery and reuse. The same findings do not seem to apply for the aquifer 404 recharge scenario. During aquifer recharge the metals are partitioned to the WWTP discharge and incinerator ashes where the toxic impact is lower. This highlights that the form and environmental compartment in 405 406 which metals are found are crucial. Heavy metals in soil (e.g. zinc) are largely immobile as they are retained 407 by sorption, thereby reducing the leaching and related toxic effects to ground- and freshwater bodies (Anderson and Christensen, 1998, Christensen et al., 2000). This suggests that a better understanding of fate 408 409 and toxicity of metals in soil is needed in the toxicity impact assessment methods. The LCA thus also 410 supports that future research should address the heavy metals removal efficiency and reduction strategies in 411 the TRENS technology, to ensure sustainable wastewater recovery.

Using the perturbation analysis, and knowledge of how TRENS may be applied in full-scale, it is possible to
identify parameters which are both sensitive (large absolute value of SR) and subject to large epistemic
uncertainty. Some examples include (Fig. 9): i) "N fertilizer substitution" has a larger absolute SR than "P

415 fertilizer substitution" in multiple impact categories (GWP, AC, TE) and both are related to how much 416 mineral fertilizer is offset through application of algae fertilizer. The higher SR for "N fertilizer substitution" 417 reflects the fact that average nitrogen fertilizer use emits more GHGs (fossil based CO₂, N₂O) than 418 phosphorus fertilizer production (Stoate et al., 2001), suggesting that providing a well-defined N substitution 419 value is more critical than for P substitution. The substitution value is influenced by local soil type and 420 application methods (Lundin et al., 2000), and is likely to have high uncertainty. ii) "N₂O emissions to air" is 421 a sensitive parameter for GWP impact category associated with high uncertainty because it is influenced by 422 many factors such as internal recycle rates, aeration efficiency, temperature, influent nitrogen loading, and 423 sampling challenges (Yoshida et al., 2014b). More critically for TRENS, the interest would be to 424 characterize emissions during PBR operation since studies have shown N₂O production during algae 425 cultivation (Guieysse et al., 2013). These results identified "N fertilizer substitution" and "N₂O emissions" as 426 priority parameters for the future development of TRENS and similar nutrient recovery processes in terms of 427 data collection, laboratory testing, and modeling work.

428 **4.** Conclusion

Our study has shown the beneficial use of applying a mass and substance centered LCA model, EASETECH,
in the early stage development of a new wastewater resource recovery technology. The main conclusions are:

Assessing the true performance potential requires considering the consequences of a full-scale
 system placed into a specific local geographical context, water demand, and existing WWTP
 operations. Relative to status quo, TRENS was shown to reduce impacts by up to 15% for global
 warming and 9% for marine eutrophication. High environmental impacts were associated with eco and human toxicity categories as a result of the selected end uses of TRENS products, emphasizing
 the need for system expansion beyond the water and resource recovery technology itself.
 TRENS primarily improves WWTP performance by reducing nitrogen species in the effluent and

 $\label{eq:438} 438 \qquad \qquad \text{direct nitrogen N_2O emissions in the nitrification-denitrification process.}$

- The TRENS system benefits are restricted by the limited need for freshwater substitution and
 fertilizer needs in the model area, but would increase proportionally with increased demand for
 resource substitution.
- The LCA identifies both construction and operation life cycle impacts as areas for improvement,
 particularly in PBR design, contrary to the operation life cycle focus assumed for conventional
 WWTPs.
- Finally, the LCA results provided feedback to technology developers and specifically TRENS
 developers by highlighting subcomponents that warrant better characterization (e.g. N₂O emissions
 during PBR operation) or evaluation of technology options (e.g. algae cultivation using closed PBR
 or open ponds).
- Ongoing development is focused on laboratory studies and modeling of the biological treatment system.
 However, decision-making and implementation benefits from a broader perspective even in the initial
 stages of development.

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647 **Table and Figure captions**

- 648 **Table 1**: Operational scenarios for TRENS implementation in the Copenhagen area, Denmark
- 649 **Table 2**: LCI sources and results summary. X denotes where operation and construction is included.
- 650 Complete datasets are available in the Supporting Information.
- **Figure 1**: Flow diagram of TRENS system (EBP2R and downstream PBR) implemented as sidestream
- process to the existing Lynetten WWTP. Figure created from TRENS (Valverde-Pérez et al., 2014;
- 653 Valverde-Pérez et al., 2015) and Lynetten process flow diagrams (Lynettefællesskabet I/S, 2012). Solid lines
- show flow of water, dotted lines show sludge or solids flow.
- **Figure 2**: Normalized LCIA impact results are dominated by marine eutrophication and ecotoxicity. Impact
- 656 categories abbreviations: Global warming potential (GWP), terrestrial acidification (AC), terrestrial
- 657 eutrophication (TE), marine eutrophication (ME), ecotoxicity (ETox), human toxicity cancer effects (HTc),
- human toxicity non-cancer effects (HTnc), particulate matter (PM), resource depletion fossil (RD).
- Figure 3: Percent contribution of individual processes each impact category for the three operating scenarios
 (a) status quo, (b) fertigation, and (c) aquifer recharge. The life cycle phases of construction and operation
 are shown separately for the WWTP, but combined for other processes (e.g. TRENS, pipeline). Refer to Fig.
 2 for abbreviations.
- **Figure 4**: Environmental performance of fertigation with TRENS relative to baseline scenario (a) and the individual processes that contribute to the change (b). The left plot provides the magnitude of change, while the right plot provides the reasons for that change. The percentage contribution plot is scaled such that the sum of all processes is 100%. Refer to Fig. 2 for abbreviations.
- Figure 5: Environmental performance of aquifer recharge with TRENS relative to baseline scenario (left)
 and the individual processes that contribute to the change (right). Refer to Fig. 2 for abbreviations.

- 669 **Figure 6**: Relative contributions of construction and operation phase impacts in the B: fertigation scenario
- 670 results for (a) the WWTP, (b) TRENS system and (c) pipeline. WWTP impacts are dominated by operation
- 671 energy consumption, while TRENS and pipeline are more influenced by materials (plastics) used in the
- 672 construction phase. Refer to Fig. 2 for abbreviations.
- 673 **Figure 7**: Contribution of processes to individual impact categories. Any process with a colored block
- 674 indicates it contributes >5% to an impact category.
- 675 **Figure 8**: Key parameters identified from contribution analysis
- 676 **Figure 9**: Sensitivity ratios showing the change in model output relative to change in parameter input.
- 677 Negative SR indicates that model output responds in the opposite direction as parameter change (i.e. increase
- 678 in parameter means decrease in model output).
- 679

1 **Table 1**: Operational scenarios for TRENS implementation in Copenhagen

A.	Scenario of existing conventional system in Copenhagen, where wastewater is collected and treated at
Status quo	a centralized WWTP for organic carbon and nutrient (N and P) removal.
В.	Scenario directly utilizes the TRENS system outputs (algal suspension) for fertigation. This scenario
Agricultural	involves diverting 10% of the influent WWTP to the TRENS system and requires additional
fertigation	infrastructure and energy consumption. The remaining 90% of the WWTP influent is treated in the
	conventional system. Modified WWTP experiences increased sludge and biogas production due to
	lower solids retention time (SRT) in the EBP2R system. Following the TRENS process, the water is
	pumped to the end user through a 25 km pipeline. There is no treatment downstream of the PBR prior
	to use in fertigation. The nutrients contained in the algae acts as a substitute for synthetic fertilizer.
С.	Scenario requires the same modifications to the WWTP as in the agricultural reuse application. Algal
Aquifer	suspension downstream of the PBR is sent to tertiary treatment to separate the microalgae and water,
recharge	so that the water goes on to aquifer recharge basins and the algae biomass is sent to the WWTP for
-	dewatering, drying, and incineration.



3

4 Table 2: LCI sources and results summary. X marks where operation and construction is included. Complete

5 datasets are available in Supporting Information.

Process	Scenario		Opera -tion	Construc- tion
WWTP		Site-specific data for the Lynetten WWTP was based on available public reports from the local utility for the year 2012 (Lynettefællesskabet I/S, 2012). WWTP infrastructure inventory estimated proportional to flow rate using Foley et al. (2010).		
	A, B, C	The WWTP is a 59.3 million m ³ /year facility, including primary and secondary treatment (BNR and phosphorus precipitation), anaerobic digestion, and incineration. Energy consumption of 0.51 kWh/m ³ . Anaerobic digester operated with yield of 70% anaerobically degradable carbon to produce biogas with 60% methane. Bulk of biogas sent to combustion for heat generation (89%), some lost in leaks (3%), and remainder flared (8%). Assumed lifetime is 30 years.	Х	Х
TRENS	B, C	 Well-established activated sludge models (ASM) were used for process design and optimization (Henze et al., 2000). ASM-2d (Flores-Alsina et al., 2012) and ASM-A (Valverde-Pérez et al., 2014) models used to simulate growth of activated sludge bacteria in the EBP2R process and green micro-algae in the PBR, respectively. Reactor sizing and operating of the EBP2R were based on scenario analysis optimization as carried out in Valverde-Pérez et al. (2015), while the PBR was designed according to Wágner et al. (2015). Energy usage for EBP2R due to aeration, pumping and mixing was evaluated using the Benchmark Simulation Model no. 2 (BSM2) guidelines (Gernaey et al., 2014). The PBR construction impacts are represented by calculating the mass of lowdensity polyethelene (LDPE) plastic needed to construct the horizontal reactor panels (Rothermel et al., 2013). PBR operational energy was taken from literature for closed, flat-panel PBRs (Jorquera et al., 2010). Two anaerobic tanks (680 m³ each), one aerobic tank (3150 m³) and a settler were constructed. WWTP infrastructure inventory increased by 2.6% proportional to increase in reactor volumes. Energy use of WWTP increases by 0.12 kWh/m³ due to EBP2R side-stream aeration, pumping, and mixing. Sludge production increased by 13% due to lower solids retention time. Biogas production increased proportionally to sludge production. PBR reactor of 20,000 m³ requiring 0.015 kg LDPE/m³ and 0.14 kWh/m³ influent. This system has an 80% phosphorus recovery (combined for the EBP2R and PBR) and produces effluent N-to-P ratio of 17 which is encapsulated in the algae. 	X	X

		A		
		Assumed metime is 15 years. Operating energy calculated using Hazen-Williams headloss equation with pipe coefficient of 140. The distribution pipeline construction inventory considered in this study is based on Venkatesh et al. (2009).		
Pipeline	B, C	25 km pipeline constructed consisting of two parallel pipes 0.579 m in diameter and 30 m elevation increase. Infrastructure inventory based on 2292 tons high- density polyethylene (HDPE) required for pipe production and diesel fuel consumption during construction (45 L/m). Operating energy consumption of 0.025 kWh/m ³ . Assumed lifetime is 30 years.	X	Х
Irrigation	В	Existing equipment at farms is assumed used for irrigation, thus no additional infrastructure is included. Energy consumption for TRENS water irrigation is assumed comparable to existing groundwater-based system and small relative to energy required for long-distance distribution pumping. Nutrient content for fertilizer substitution is 4.6 mg P/L and 33 mg N/L.	-	-
Pre- infiltration treatment	С	Pre-treatment and algae harvesting prior to aquifer recharge scenario is based on tertiary treatment data from Pasqualino et al. (2010), which includes coagulation/flocculation, filtration, disinfection (UV and chlorination). Energy consumption is 0.021 kWh/m ³ .	X	-
Infiltration basin	С	$110\ 000\ m^2$ open basin design based on long-term average infiltration rate of 55 m/yr (Københavns Energi, 2001) with water depth of 0.5 m. Basin construction represented by excavation of 78,320 m ³ by hydraulic digger. Infiltration is by gravity, so energy consumption is assumed negligible compared to other processes. Assumed lifetime is 30 years.	-	X



1

- 2 Figure 1: Flow diagram of TRENS system (EBP2R and downstream PBR) implemented as sidestream
- 3 process to the existing Lynetten WWTP. Figure created from TRENS (Valverde-Pérezet al., 2014; Valverde-
- 4 Pérezet al., 2015) and Lynetten process flow diagrams (Lynettefællesskabet I/S, 2012). Solid lines show flow
- 5 of water, dotted lines show sludge or solids flow.

CER MAR





7

8 Figure 2: Normalized LCIA impact results are dominated by marine eutrophication and ecotoxicity. Impact

9 categories abbreviations: Global warming potential (GWP), terrestrial acidification (AC), terrestrial

10 eutrophication (TE), marine eutrophication (ME), ecotoxicity (ETox), human toxicity - cancer effects (HTc),

11 human toxicity - non-cancer effects (HTnc), particulate matter (PM), resource depletion - fossil (RD).





Status quo - Percent contribution

14



- 16 (a) status quo, (b) fertigation, and (c) aquifer recharge. The life cycle phases of construction and operation
- are shown separately for the WWTP, but combined for other processes (e.g. TRENS, pipeline). Refer to Fig.
- 18 2 for abbreviations.





- 22 **Figure 4**: Environmental performance of fertigation with TRENS relative to baseline scenario (a) and the
- 23 individual processes that contribute to the change (b). The left plot provides the magnitude of change, while
- 24 the right plot provides the reasons for that change. The percentage contribution plot is scaled such that the
- sum of all processes is 100%. Refer to Fig. 2 for abbreviations.



- 28 Figure 5: Environmental performance of aquifer recharge with TRENS relative to baseline scenario (a) and
- 29 the individual processes that contribute to the change (b). Refer to Fig. 2 for abbreviations.

30







33 **Figure 6**: Relative contributions of construction and operation phase impacts in the B: fertigation scenario

- 34 results for (a) the WWTP, (b) TRENS system and (c) pipeline. WWTP impacts are dominated by operation
- 35 energy consumption, while TRENS and pipeline are more influenced by materials (plastics) used in the
- 36 construction phase. Refer to Fig. 2 for abbreviations.
- 37

2	0
э	0

Processes exist in	Processes	GWP	AC	TE	ME	POF	ETox	HTc	HTnc	PM	RD
	WWTP construction										
	✓ WWTP operation										
	✓ Discharge to sea										
Scenarios A, B, and C	✓ Sludge incineration										
	✓ Emissions to air										
	✓ Biogas collection										
	✓ Biogas combustion										
	Combustion in flare										
B and C	✓ TRENS (EBP2R + PBR)										
	Pipeline 25km										
В	✓ Fertilizer substitution										
	✓ Use-on-land										
С	✓ Pre-inf treatment										
	Groundwater recharge										

39 \checkmark - Further investigated to identify key parameters

40 **Figure 7**: Contribution of processes to individual impact categories. Any process with a colouredblock

41 indicates it contributes >5% to an impact category.

42



Figure 8: Key parameters identified from contribution analysis.



- 48 Figure 9: Sensitivity ratios showing the change in model output relative to change in parameter input.
- Negative SR indicates that model output responds in the opposite direction as parameter change (i.e. increase
 in parameter means decrease in model output).
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Highlights

- Development of wastewater biotechnology for resource recovery and reuse
- Recovery via low-SRT EBP2R combined with photobioreactor
- Water and nutrient reuse in irrigation-fertilisation combined with aquifer recharge
- Potential environmental impacts assessed using Life Cycle Assessment
- Key environmental risks linked to heavy metals co-recovered with nutrients

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