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Lowering district heating temperatures - Impact to system performance in current and future Danish energy scenarios

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Abstract

Combined heat and power (CHP) production in connection with district heating (DH) systems has previously demonstrated a significant reduction in primary energy consumption. With extended installation of intermittent sustainable sources, such as eg. wind turbines rather than thermal units, the changed distribution of generation technologies may suggest a reconsideration of optimum for DH network temperatures, in order to achieve low cost and minimize carbon emissions. A mixed integer linear optimisation model was used to investigate the changed operation based on changed network characteristics. Utility plants and demand curves corresponded to the current and future scenarios for the DH system of Greater Copenhagen. Performance curves from typical CHP-plant technologies were used to represent the changed operation of power and heat production for changed DH temperatures. The results show that primary fuel consumption is reduced approximately 5-7 % at DH design temperatures of 60 - 70 °C. Further reduction in DH temperatures resulted in opposing tendencies, as hot tap water requires electricity to reach the required temperatures. The results are network-specific, as they represent the given network and production units, but similar trends can be expected for other large networks.

Keywords: Heat pumps, District heating, Combined heat and power, Optimisation.

1 1 Introduction

² Combined heat and power (CHP) production in connection with district heating (DH) systems has resulted

in significant reduction in primary energy consumption in Denmark [1]. With power production investments
 moving from thermal units to intermittent renewable sources, such as eg. wind turbines or solar photovoltaics

⁵ technology [2], the excess heat co-generated with power is decreased.

6 The changed distribution between thermal and intermittent technologies for electricity suggest changes to the

7 corresponding technologies for supplying heat to the DH network. As investment in new utility technologies

 $_{\circ}~$ is required, it is suggested also to consider the influence of DH network temperatures for a complete system

⁹ optimization. The choice of temperatures does not only affect network heat losses, but also impacts network

¹⁰ capacities, and changes the possible benefit of different technologies. Thus it is likely that two different

choices in network temperatures will result in two significantly different optimal technology distributions, and vice versa.

¹³ In Denmark, the investment in future utility production units is constrained to renewable technologies due to

political zero carbon emission ambitions (eg. Danish Government [3]). Such ambitions are also represented

¹⁵ in the local communities. The city council of Copenhagen agreed in 2013 on a climate plan attempting to

¹⁶ make Copenhagen the first CO_2 neutral capital in 2025 [4]. Carbon neutral heating and power production

 $_{17}$ $\,$ is naturally key focuses to achieve such goals. As the DH network supplies 98% of the heat demand in the

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Nomencla	ture		
\dot{C}	cost rate, €/h	F	forward
C	constant	f,g,h,i,j	index
k	opening degree, -	in	inlet
\dot{m}	massflow, kg/s	out	outlet
p	pressure, Pa	R	return
T	temperature, °C	$_{\rm sink}$	sink reservoir
		source	source reservoir
Greek symbo	ols	T	turbine
α	flow characteristic	t	hours
β	power loss factor for heat extraction	total	total utilisation
Δ	variation or glide		
ρ	density, kg/m ³	Abbreviations	
		CC	Combined Cycle
Subscripts		CHP	Combined Heat and Power
C	consumer	COP	Coefficient Of Performance
cond	condensation	DH	District Heating
E	exiting consumer	Gen	Generator
evap	evaporation	HP(s)	Heat $Pump(s)$
elec	electric		

¹⁸ Copenhagen municipality, these utility production units are of main concern. The climate plan proposes

to convert central CHP units to biomass and integrating central, large-scale heat pumps (HPs) in the DH networks as two feasible measures.

²¹ A series of previously published reports named "Heat Plan Greater Copenhagen" (in Danish "Varmeplan

²² Hovedstaden"), of which the newest at the time of writing is number 3, concludes that a limited share (300

²³ MW installed capacity) of central heat pumps, may provide small reductions in heat cost after 2030-35

²⁴ [5]. According to their calculations, the use of sustainable biomass is the major driver for cost and carbon

²⁵ reductions in the future system. With one highly dominant fuel type, the system may, however, experience

²⁶ a significant reduction in security of supply.

Four explanations are conceivable for the expected poor penetration of heat pumps in the future technology
 composition for DH:

²⁹ 1 The extraction CHP plant technology provides highly efficient conversion of electricity to heat (typ-³⁰ ically approx. ratio: 7-11:1 [6]) according to the power loss factors by heat extraction [7]. This is a ³¹ performance advantage in the order of a factor of 3 compared to the HP technology [8].

Low coefficient of performance (COP) from integrating HPs to supply heat in the transmission network at 90 °C or above [9]. With low COP the HP utilises large quantities of electricity, which in addition to the cost of electricity also carries significant network losses and taxes. Heat can be co-supplied at lower temperatures to increase COP (e.g. to the return stream of the network) but such integration schemes increase the operational constraints of the system, and the HPs can in this case not be utilised as a stand alone technology.

- 3 Taxation for HPs reaches above 50 % of the levelized cost for heat [10] considering the Danish taxation
 scheme [11].
- 40 4 Insufficient heat sources with high temperature, which are located within or close to the DH net-41 work perimeter [5, 12]. In case the heat sources are not co-located with the large DH-streams, the 42 investments for HPs are increased significantly.

Item 2 and 3 are addressed by lowering DH temperatures, in this way increasing the COP of the HP unit.
As taxation is based on the consumption of electricity for heat production, increasing COP will lower the
quantity of the heat cost that originate from taxes.

⁴⁶ When the temperature in the DH network is changed, all of the existing types of utility technologies will

⁴⁷ experience performance changes. In order to fully evaluate the improved performance of the HPs at changed

⁴⁸ DH temperatures, the performance estimates for existing technologies should also correspond to the changed
 ⁴⁹ temperatures.

⁵⁰ In this paper, the effects of changing DH temperatures are evaluated in terms of the total cost for heat and ⁵¹ electricity for the consumers, carbon emissions and primary fuel consumption. Performance curves from

52 typical CHP-plant technologies are used to represent the changed operation of power and heat production.

As large changes are expected for the current network within a limited time-frame, two cases are considered

⁵⁴ in order to evaluate the implications of changing DH temperatures for the current and future network and ⁵⁵ utility units. The current energy scenario is assessed by utilising a validated layout for 2011 where steam-

⁵⁵ utility units. The current energy scenario is assessed by utilising a validated layout for 2011 where steam-⁵⁶ based DH networks are utilised in central areas of the network [13]. The future scenario (2025) corresponds

⁵⁷ closely to that considered in "Heat Plan Greater Copenhagen 2" [14]. Neither of the two scenarios utilises

central HPs in DH networks. In the paper two corresponding scenarios are included considering a significant

⁵⁹ integration (200 MW capacity) of HPs.

 $_{\rm 60}$ $\,$ To assess the changes to the network capacity corresponding to the current and future design, a DH network

⁶¹ model is included, where the changed capacity at changed temperature levels is considered. This allows

⁶² an analysis of the possibilities for changing network temperatures without further investment in the large

⁶³ transmission and distribution lines of Greater Copenhagen.

⁶⁴ The developed model thus represents an existing system as a case, but it is intended to be an illustration of

⁶⁵ current and future energy systems in cities with high penetration of CHP-based district heating and thus

high-efficient heat supply. The study shows the possibilities for optimal integration of intermittent renew ables when accounting for the performance of different technologies under different operating temperature

68 conditions.

69 2 Method

Thermodynamic models of representative technologies were used in order to analyse the change in performance of the individual units with changes in temperature of the DH network. The models were programmed in Engineering Equation Solver [15]. These models are further described in section 2.1, 2.2 and 2.3.

⁷² A detailed mixed integer linear optimisation model was used to investigate the new operation based on

the changed parameters. The model was programmed in Matlab and GAMS using the CPLEX solver [16, 17, 18]. The model was designed and used for the case study of the production technologies and

network characteristics of Greater Copenhagen [13], but the implementation of energy system equipment
 in the model is generic and easy to change to other systems. The heat and power system model is further
 described in section 2.5 and appendix A.

79 2.1 Temperature of current and future DH networks, network capacities and DH heat losses

⁸⁰ Generally, the temperatures for a district heating network are kept as low as possible in order to reduce heat

⁸¹ losses and increase efficiency of electricity co-production. The lower limit for traditional DH forward temper-

atures is reached when the required temperature of certain constituents of the demand (often approximately

⁸³ 55 °C due to hot tap water) is no longer met.

In a Danish context the forward temperature $(T_{\text{DH,forward}})$ varies from 70 °C to 120 °C [19, 20]. The corresponding network return temperatures $(T_{\text{DH,return}})$ range from 35 °C to 55 °C. The design temperatures

of the current DH network and utility units are 100 °C, with temperature variations of 95-110 °C to account

for network capacity constraints in cold periods and energy savings in the summer.

⁸⁸ In Lund et al. [21] further reduction in temperatures is proposed, with a lower limit of DH design temper-

⁸⁹ atures reaching as low as 40 °C, which is the limit allowed by modern space heating technology (4GDH).

⁹⁰ In this case electric heaters or booster HP units are required for production of hot tap water [22, 23, 24].

The performance of booster HP units is further addressed in section 2.4. In table 1 both current and future proposals for temperature in DH networks are presented.

⁹³ Based on the considered temperature sets, the return and forward temperatures were interpolated linearly ⁹⁴ for the range of $T_{\text{DH,forward}} = 40\text{-}110$ °C and $T_{\text{DH,return}} = 20\text{-}55$ °C as shown in Fig 1.



Figure 1: Temperature spans applied of the modelled DH networks.

- ⁹⁵ The temperature levels do not only influence the production technologies, but also the volume flow of
- 96 DH fluid is significantly changed for a constant amount of transferred heat. As the pressure losses become
- ⁹⁷ significant for increasing flow rates in the network [25, 26, 27], the various transmission lines were constrained
- 98 to a maximal volume flow. The maximal flow rates for the two scenarios were based on a data from a
- ⁹⁹ corresponding network model for 2012 and 2025 [5, 12]. Only transmission lines and capacity constraints for
- ¹⁰⁰ large distribution lines were included in the model. The capacity of the individual transmission lines was

¹⁰¹ varied according to the changed temperatures in the model.

- Similar constraints were found for sensible heat storages, where the energy content of a volume of stored
 water changes with changed DH temperature.
- ¹⁰⁴ The relative variation of the two technologies is presented in Fig. 4d, where 100 °C forward design temper-
- ¹⁰⁵ ature is used as the base. As seen from the figure, the relative differences of stored heat per volume and
- ¹⁰⁶ capacity of DH network are coinciding.

¹⁰⁷ The temperatures of the DH network forward and return streams were defined to be at the location of the ¹⁰⁸ utility unit (T_f and T_r) in Fig. 2. In the considered network, the heat is supplied from the utility plant to ¹⁰⁹ a transmission network, which transfers the heat to smaller distribution grids.

The heat losses for transmission and distribution were determined individually for 2011 as 2 % and 15 % respectively [19, 20]. By assuming that the losses correspond to transmission network operation at 100 °C and 50 °C for forward and return temperatures, the combined heat transfer characteristics of each individual heat network to the ground was found [28, 29]. Using this assumption, it was possible to estimate the heat losses, as well as the consumer temperature T_C for variations in DH temperatures corresponding to Fig. 1.

- The temperature of the soil was estimated as the average of yearly temperature variation for the area (8.8
- 116 °C).

115

Network typeMediaDH forward
temperatureDH return
temperatureTransmission H_2O $110^{\circ}C$ $55^{\circ}C$ Old distribution H_2O $90^{\circ}C$ $45^{\circ}C$

 H_2O

H₂O

New distribution

4GDH (low limit)

 $70^{\circ}C$

 $40^{\circ}C$

35°C

 $20^{\circ}C$

Table 1: Current and future temperature sets for DH networks



Figure 2: Schematic diagram of DH system with transmission and distribution networks.

117 2.2 Performance of CHP units at changed DH temperatures

¹¹⁸ In order to evaluate the effects of changing DH network temperatures, three separate models of CHP plants ¹¹⁹ was programmed in EES. The developed models are:

- Extraction: Extraction type steam turbine (Rankine) cycle.
- Back-pressure: Back-pressure steam turbine (Rankine) cycle.
- Combined cycle: Gas turbine (open Brayton) and steam turbine (Rankine) cycle.

Schematic diagrams of the three considered CHP technologies are presented in Fig. 3. The layout of the three units was modelled to represent specific units in the current utility production.

Besides energy, entropy and mass balances, different, representative expressions were used to establish the impulse balances in different parts of the systems.

For each section of the modelled turbines, a turbine constant accounts for the swallowing capacity of a specific unit:

$$C_T = \frac{\dot{m} \cdot \sqrt{T_{\rm in}}}{\sqrt{p_{\rm in}^2 - p_{\rm out}^2}} \tag{1}$$

where the massflow of working fluid \dot{m} , the temperature of entering fluid $T_{\rm in}$ and pressures at inlet $p_{\rm in}$ and outlet $p_{\rm out}$ are used. Once installed, the swallowing capacity should be considered constant throughout the lifetime of the unit. The constant is required to calculate the off-design operation of such units.

132 2.2.1 Extraction CHP

In the current energy scenario based on todays Eastern Danish energy system, the Nordpool DK2 area [30], four central extraction CHP units are operated (five in case the reserve unit at Asnæsværket (ASV5) is included), of which three are located within the DH network. The same units are expected to be operating in 2025, although two of the units (which are identical) require overhaul and conversion to biomass fuel.

¹³⁷ The model for extraction type steam turbine (Rankine) cycles represent one of these units (AVV1 or AMV3).

¹³⁸ The model follows the instructions of the proposal for simulator contest of ECOS 2003 [31, 6], where

¹³⁹ specific information about the temperatures, isentropic efficiencies, temperature differences, auxiliary power

¹⁴⁰ consumption and pressure losses are defined. The model used for this analysis corresponded closely to the



Figure 3: Schematic diagram of the three considered combined heat and power plants.

one used in Ommen et al. [9]. The steam enters the intermediate and low pressure part of the turbine train
after expansion in the preceding turbine, IP1, and may be used for power generation or to supply district
heating. The output of each product is controlled by adjusting the valves before the low pressure turbines
and the district heating heat exchangers.

¹⁴⁵ For each of the values, a flow characteristic was fixed, in order to account for the pressure losses when the

valve is operated between fully open and fully closed. The constant is required to calculate the off-design

¹⁴⁷ operation of such units.

$$\dot{V} = \alpha_{\text{valve}} \cdot k \cdot \sqrt{\frac{\Delta p_{\text{valve}}}{\rho_{\text{in}}}},\tag{2}$$

where α is the flow characteristic, k is the opening degree of the valve and Δp_{valve} is the pressure loss over the valve.

¹⁵⁰ Considering DH temperatures of 100 °C and 50 °C for forward and return temperatures, the model represents ¹⁵¹ a plant with an electric efficiency of 42.0 % at full boiler load and in condensing mode and 34.9 % at full

¹⁵² back-pressure mode, respectively. In full back-pressure mode the total energy utilization is 91.5 %.

153 2.2.2 Back-pressure CHP

Back-Pressure CHP units are extensively used in Copenhagen today and in future scenarios (see section
2.6). The units are typically fuelled by biomass, or used for waste incineration. A few of the units allow the
steam to bypass the turbine, in order to be utilised directly for heat production.

The back-pressure CHP unit was modelled to represent the Amagerværket unit 1 (AMV1), which is a biomass-fuelled unit located centrally in Copenhagen. The component details corresponded to those used

for the extraction plant. In the current energy scenario, only a high pressure turbine is installed, as the unit
 supplies steam to a central network. When the steam network has been phased out (expected before 2025)
 a low-pressure turbine will be added to the unit.

Considering DH temperatures of 100 °C and 50 °C for forward and return temperatures, the model represents a plant with an electric efficiency of 29.5 % and total energy utilization of 92 %.

164 2.2.3 Combined cycle CHP

The combined cycle CHP plant corresponds to the two combined cycle units at Avedøreværket unit 2. For the Rankine cycle, the component details correspond to those used for the extraction plant. Combined cycle units represent a small fraction of the current electricity and heat production, and are expected to play an even smaller role in the system of 2025. Out of the four current units, two will be retired as they are used for the steam network, and the two at AVV2 will be utilised exclusively as electricity reserve measures.

For DH forward and return temperatures of 100 °C and 50 °C respectively, the model represents a plant with an electric efficiency of 51 % and total energy utilization of 85 %.

172 2.2.4 Performance improvement of CHP technologies from reduction in temperatures of DH network

The individual models of CHP units were varied according to the district heating temperature levels presented in Fig. 1. In this way, the potential improvements for the individual plants were determined. By assuming, that the models are representative for the individual CHP-plant types, the influence from DH temperatures are found for all considered units in the current and future energy scenarios. The changed performance parameters are presented in Fig. 4a, 4b and 4c for extraction, back-pressure and combined cycle CHP, respectively.

For extraction CHP units, the temperature variations contributed to significant modifications to the electricity efficiency and to the power loss factor by heat extraction β . For back-pressure units the electricity efficiency was significantly changed. For both extraction and back-pressure CHP units, minor impact was experienced for the total energy utilization of the unit.

¹⁸³ For the combined cycle technology, the electric efficiency has changed with variation of DH temperature.

¹⁸⁴ Opposed to the above-mentioned technologies, the alteration of DH temperature affects the total efficiency

¹⁸⁵ significantly, although less than the corresponding change in electrical efficiency.



Figure 4: Changed performance parameters of three CHP types, HP and changed temperatures in DH network when design conditions (100 °C forward temperature) are altered to off-design operation.

186 2.3 Heat pumps in DH

¹⁸⁷ In Ommen et al. [9] five possible heat pump configurations in DH networks are analysed. The operational ¹⁸⁸ performance of the configurations are investigated based on four key performance factors, which are the ¹⁹⁹ coefficient of performance, the coefficient of system performance, the volumetric heating capacity and the ¹⁹⁰ cost of fuel.

The SF configuration was utilised for the present analysis. In this configuration the sink DH stream is heated from the temperature of the return line to that of the forward stream. The main advantage of the SF configuration is that this configuration allows operation independently of other technologies. A schematic diagram of a single stage vapour compression heat pump is presented in Fig. 5.

¹⁹⁵ The performance of the HP was evaluated based on four variables and fixed temperature differences for both ¹⁹⁶ evaporator and condenser. The utilised variables were: the temperature of the sink process stream leaving ¹⁹⁷ the condenser T_{sink} , the temperature of the source T_{source} and the process stream temperature variation ¹⁹⁸ from inlet to outlet in both heat exchangers (ΔT_{sink} and ΔT_{source}). Both the sink temperature, and the ¹⁹⁹ variation of the sink was determined for a SF configuration HP as the forward temperature of DH, or the ²⁰⁰ difference between DH forward and return in Fig. 1, respectively.

The temperature of the source is dictated by the type and location of the installation [32]. By using a DH network, large installations can be located near heat sources of elevated temperatures (compared to ambient conditions), such as sewage water, industrial waste heat, power plant stack gasses etc. Most of these heat sources tend to have a low yearly temperature variation and a finite heat capacity rate of the stream. In some cases the heat source can also be ocean or lakes where yearly variation in temperature would be expected.

The performance of the considered heat pump was calculated using constant efficiencies for compressor and electrical motor, as well as fixed temperature differences in the heat exchangers. The used values for heat

²⁰⁸ source and performance of equipment are presented in Table 2.

²⁰⁹ For DH forward and return temperatures of 100 °C and 50 °C respectively, the HP model represents a



Figure 5: Schematic diagram of a single stage heat pump system for DH (configuration SF)

Table 2: Operational parameters for SF configuration HP

	Value	Unit	Designation
Type	R134a	-	Working fluid
Efficiency	0.8	-	Compressor isentropic efficiency
	0.95	-	Electric motor efficiency
Temperature	20	°C	Temperature of heat source
	10	Κ	Temperature variation of heat source
	5	Κ	Evaporator superheat
	5	Κ	Minimum pinch point in heat exchangers

unit with a COP of 2.97 (-) including electric motor efficiency (3.12 (-), if only the thermodynamic cycle is considered).

212 2.4 DH booster heat pump

For supply of hot tap water, two constraints are to be respected, considering the Danish DH case. The requirements of the Danish building standard must be met [33], where hot tap water is utilised at two temperature levels 45 °C and 40 °C, respectively. Additionally, a main concern is the issues related to the Legionella bacterium. To avoid bacteria growth, the hot tap water must either exceed a predefined temperature limit, where the bacteria can no longer exist when stored, or the tap water is not to be stored after being heated.

Two HP booster integration schemes were identified, corresponding to the schemes presented in Fig. 6a and 6b. In Ommen and Elmegaard [23] various specific configurations are investigated and compared based on their exergy efficiency. It is found that a heat pump on the primary side of the hot tap water heat exchanger, is superior in terms of COP and exergy efficency at almost all temperature configurations of low temperature DH. The considered configuration is presented in Fig. 6c.

²²⁴ In case the temperature of the DH network at the location of the consumer (in Fig. 2) is lower than 55 °C, it

²²⁵ is assumed that the hot tap water constitutes a fixed share of DH heat demand. The share was determined





(a) Heat pump on primary side of the tap water heat exchanger

(b) Heat pump on secondary side of the tap water heat exchanger



Figure 6: Two DH booster HP integration schemes.

by assessing the heat demand of the individual area (without heat losses) during the periods of the year where space heating is not needed. The remaining part of the supplied heat is utilised for space heating, and it was assumed that this fraction did not require boosting of the temperature.

²²⁹ For district heating consumer forward temperature of 40 °C and return temperature of 22 °C, the model

 $_{\rm 230}$ $\,$ represents a unit with a COP of 5.6 (-) and a power consumption of 0.066 kWh per kWh of hot tap water.

²³¹ For a forward temperature approaching 55 °C, the heat load is reduced and the COP of the unit increases.

 $_{232}$ $\,$ Thus at 55 °C the electricity consumption for boosting tap water temperatures becomes zero.

233 2.5 Heat and power system model

A detailed system model was developed for calculation of the economic and environmental impact of integrating heat pumps in an energy system with a high share of CHP-plants and intermittent electricity production from renewable technologies, e.g. wind turbines. The result was a validated heat and power system model, which features detailed representation of CHP technology as well as detailed representation of different heat pump technologies and integration possibilities [13].

The optimal production cost for the combined system can be achieved by minimisation of consumer cost for electricity and heat in daily auctions on hourly basis [34]. The optimal daily market clearances are then added for the duration of the year. When considering a system where capital cost can be considered as sunk cost, the objective function can be written as 3.

$$\min\left[\sum_{t\in\mathcal{T}} \left(\sum_{i\in\mathcal{I}} (\dot{C}_{i,t}^{\text{CHP}}) + \sum_{h\in\mathcal{H}} (\dot{C}_{h,t}^{\text{boiler}}) + \sum_{g\in\mathcal{G}} (\dot{C}_{g,t}^{\text{HP}}) + \sum_{f\in\mathcal{F}} (\dot{C}_{f,t}^{\text{Other}}) + \sum_{j\in\mathcal{J}} (\dot{C}_{j,t}^{\text{import}} - \dot{C}_{j,t}^{\text{export}})\right)\right]$$
(3)

²⁴³ Where \dot{C} is the total cost rate of production at the individual plant. The CHP units in the system are ²⁴⁴ indexed by \mathcal{I} , boilers by \mathcal{H} , heat pumps by \mathcal{G} and other heat and/or electricity production by \mathcal{F} . The ²⁴⁵ neighbouring energy markets are indexed by \mathcal{J} . It was assumed, that electricity and heat production of small-scale decentralized CHP-plants and intermittent
 electricity production from wind turbines are independent of the electricity cost in the individual hour. Using
 this assumption, the production profile of such units can be obtained from historical data.

The objective function shown in Eq. 3 was subject to a number of economic and technical constraints, of which the most important ones are presented and explained in appendix A. The economic constraints related to taxation are autonomous for each country, and are thus not presented in detail here. We refer to [13] for further information. The cost rates include all costs associated with utility production (e.g. fuel, taxes and subsidies) at the specific plant. In order to ensure the competitive conditions for import and export of electricity across taxation borders, the taxes for electricity are placed on the consumption. This is opposite to taxation for fuel, which is closely linked to the production.

²⁵⁶ The detailed representation of the CHP units includes various features which are briefly mentioned below:

- Four types of power plant units possible: Back-pressure, extraction, gas turbines/combined cycle or condensation.
- Limitation for hourly ramp rates and minimum technical production limits.
- Reduction in electricity production efficiency at part-load operation, which is specified individually for each unit.
- Startup and shutdown costs corresponding to size and type of unit
- Extraction technology represented by two power loss factors by heat extraction (β^1, β^2) depending on production above or below the "no-loss" point [7].
- Production at specific units can be prioritised, e.g. waste incineration.
- Availability (to market) is set individually for all units. For validation these data were obtained from urgent market messages from Nord Pool Spot [35].
- Different Danish taxation schemes for heat production are preprogrammed for each unit.
- Steam bypass of turbine possible for back-pressure CHP-units.
- Minimum available manual and frequency reserves are included for the total system, and technical limitations of reserves may be specified individually for each unit.
- Specific units may produce at higher capacity than their rating (overload) at reduced efficiency.

273 2.6 Current and future energy scenarios for Copenhagen

For each of the thermal CHP units in the current and planned utility system, specific information regarding capacity and efficiency, cost of fuels and maintenance, as well as capacities and consumption of the network were available online from various sources [36, 37, 38, 39, 40, 14].

In this way it was possible to derive the plant characteristics for current (Table 3a) and future (2025) energy scenario (Table 3b). Most of the data in the table is referring directly to the operational parameters of the individual units, but the table also includes fuel cost for 2011 and 2025 using historical prices or prognoses [38]. It should be noted that both electric efficiency and energy utilization were calculated for the plant in back-pressure operation mode.

The capacity and demand profiles, as well as planned changes, of DH networks in 2012 and 2025 were based

²⁸³ on information from CTR, HOFOR and VEKS [14]. Changes to the demand, capacity of decentral CHP,

on- and offshore wind turbines, photovoltaics and spot-prices for electricity in 2025 were available from Energinet.dk [38].

- ²⁸⁶ As the process of converting old steam networks to water-based networks is ongoing, the heat demand for
- ²⁸⁷ water-based networks increases its demand faster than that which can be related to the heat demand from
- 288 new areas. In the current scenario a number of units produces heat for the steam network, and is thus not

	(a) Current (2011) energy scenario														
	Fuel	Cost	Type	Pri-	Turb.	$\eta_{\rm elec}$	η_{total}	β^1	β^2	Ramp	Min.	Man.	Freq.	$\eta_{\rm elec}$	Boiler
	$_{\mathrm{type}}$	fuel		ority	byp.					rate	load	reserve	reserve	reduction	capacity
		(\in/GJ)				(-)	(-)	(-)	(-)	(-)	(-)	(-)	(-)	(%)	(MW)
AMV1	bio/straw	9.4	Backp.		Х	0.20	0.92			0.25	0.50		0.05	0.08	350
AMV3	coal	3.3	Extr.			0.35	0.89	0.14	0.10	0.25	0.50		0.05	0.08	595 (+75)
HCV4	nat. gas	5.9	Backp.		Х	0.11	0.82			0.25	0.45	0.03	0.05	0.08	157
HCV7	nat. gas	5.9	Backp.		Х	0.26	0.89			0.25	0.45	0.03	0.05	0.08	285
HCV8	nat. gas	5.9	CC			0.20	0.89			1.00	0.55	0.05	0.10	0.16	127
SVM7	nat. gas	5.9	CC			0.23	0.92			1.00	0.50	0.05	0.10	0.16	275
AMF1	waste	4.0	Backp.	Х	Х	0.21	0.83			0.25	0.70			0.08	132
AVV1	coal	3.3	Extr.			0.35	0.89	0.14	0.10	0.25	0.50	0.03	0.05	0.08	595 (+75)
$AVV2_{B1}$	bio	9.9	Extr.			0.36	0.92	0.18	0.12	0.25	0.45	0.03	0.05	0.08	805
$AVV2_{B2}$	straw	8.0	Extr.			0.34	0.91	0.16	0.12	0.25	0.45			0.08	100
$AVV2_{cc1}$	nat. gas	5.9	CC			0.51	0.85	0.11	0.11	1.00	0.55	0.05	0.10	0.16	135
$AVV2_{cc2}$	nat. gas	5.9	CC			0.51	0.85	0.11	0.11	1.00	0.55	0.05	0.10	0.16	135
KARA5	waste	4.0	Backp.	Х	Х	0.17	0.80			0.25	0.70			0.08	65
VF5	waste	4.0	Backp.	Х		0.13	0.82			0.25	0.70			0.08	90
VF6	waste	4.0	Backp.	Х		0.19	0.82			0.25	0.70			0.08	105
ASV2	coal	3.3	Extr.			0.31	0.88	0.18	0.15	0.25	0.20	0.03	0.05	0.08	368
ASV5	coal	3.3	Extr.			0.26	0.88	0.18	0.15	0.25	0.40	0.03	0.05	0.08	1750
KYB1	oil	11.9	Elec. only			0.33	0.33			0.60	0.48	0.03	0.05	0.08	790
KYB2	oil	11.9	Elec. only			0.33	0.33			0.60	0.48	0.03	0.05	0.08	790

Table 3: Thermal power plant unit characteristics for central power plants and waste inceneration plants in DK2 bidding area.

(b) Future	(2025)	energy	scenario	
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	Fuel	Cost	Type	Pri-	Turb.	$\eta_{\rm elec}$	$\eta_{\rm total}$	β^1	β^2	Ramp	Min.	Man.	Freq.	$\eta_{ m elec}$	Boiler
	type	fuel		ority	byp.					rate	load	reserve	reserve	reduction	capacity
		(€/GJ)				(-)	(-)	(-)	(-)	(-)	(-)	(-)	(-)	(%)	(MW)
AMV1	bio/straw	8.9	Backp.		Х	0.30	0.92			0.25	0.50		0.05	0.08	350
AMV3	bio	9.9	Extr.			0.34	0.89	0.14	0.10	0.25	0.50		0.05	0.08	640
AMF1	waste	4.0	Backp.	Х	Х	0.21	0.99			0.25	0.70			0.08	203
FLIS1	bio	9.9	Backp.		Х	0.20	0.99			0.25	0.45			0.08	150
AVV1	bio	9.9	Extr.			0.34	0.89	0.14	0.10	0.25	0.50	0.03	0.05	0.08	640
AVV2	bio	9.9	Extr.			0.36	0.92	0.18	0.12	0.25	0.45	0.03	0.05	0.08	960
AVV3	straw	5.7	Extr.			0.34	0.91	0.16	0.12	0.25	0.45			0.08	125
KARA5	waste	4.0	Backp.	Х	Х	0.17	0.80			0.25	0.70			0.08	65
KARA6	waste	4.0	Backp.	Х	Х	0.22	0.99			0.25	0.70			0.08	82
VF5	waste	4.0	Backp.	Х		0.12	0.99			0.25	0.70			0.08	90
VF6	waste	4.0	Backp.	Х		0.18	0.99			0.25	0.70			0.08	105
VF7	waste	4.0	Backp.	Х		0.27	0.99			0.25	0.70			0.08	102
KKV7	bio	9.9	Backp.		Х	0.18	0.90			0.25	0.45			0.08	45
KKV8	bio	9.9	Backp.		Х	0.25	0.90			0.25	0.45			0.08	55
ASV2	coal	3.2	Extr.	Х		0.31	0.88	0.18	0.15	0.25	0.20	0.03	0.05	0.08	368
KYB1	oil	16.0	Elec. only			0.33	0.33			0.60	0.48	0.03	0.05	0.08	790
KYB2	oil	16.0	Elec. only			0.33	0.33			0.60	0.48	0.03	0.05	0.08	790

12

Table 4: Four different cases for analysis of impact to system performance from lowering DH temperatures

	Energy	Capacity dependent on
	scenario	temperature of DH
Case $\#1$	2011	no
Case $#2$	2011	yes
Case $#3$	2025	no
Case $#4$	2025	yes

effected by changes to the network temperature for water based DH systems. The units are AMV1, HCV4-8 and SMV7.

 $_{291}$ The scenarios were named as four different cases, Case #1-4. The details of the cases are presented in table

4. The difference between case #1 and #2 as well as case #3 and #4 is the use of temperature dependency

²⁹³ for capacity constraints in the DH network, as well as temperature dependency for storage systems. The

 $_{294}$ objective of including case #2 and #4 was to show the effects of the temperature dependency in the specific

²⁹⁵ case that no further investments were made to the transmission network or to the storage facilities. This

²⁹⁶ can be seen as a conservative estimate.

The objective of case #1 and #3 was to analyse the effects of lowering temperature, with similar capacity constraints as proposed for the traditional temperature levels. This assumption reflects that some critical network and storage capacity constraints in the transmission network can be low cost changes, compared to the magnitude of investments for the remaining system. Such investments would further imply additional work to DH pumps, due to increased volume flow, which is not included for the analysis. This may thus be

³⁰² seen as a high estimate.

The four energy system cases were further expanded by introduction of a significant capacity of central SF 303 configuration heat pumps (as presented in section 2.3). For each of the four cases the system was analysed 304 without introduction of HP capacity, as well as a case with 200 MW capacity installed in the transmission 305 network of the DH system (denoted "W/HP" for cases with HP installed). The installed capacity was 306 divided equally at two locations, namely the location of Amagerværket (AMV) and Avedøreværket (AVV). 307 Carbon emissions for heat and electricity production in CHP plants were calculated based on the 125 %308 method for heat, assuming that heat is produced at 125 % efficiency, whereas the remaining part correspond 309 to electricity production [41]. Other methods are also utilised for splitting contributions, such as 200 %, 310 energy basis or quality (exergy) of content. Carbon emissions from combustion of fuel correspond to the 311 Danish Energy Agency [40] 312

313 **3 Results**

³¹⁴ The various energy system scenarios were compared based on six different parameters. The parameters were:

 $_{315}$ Combined system cost, CO₂-emissions from heat and electricity individually, primary energy consumption,

net imported electricity and the production ratio between electricity and heat in the extraction CHP units.

³¹⁷ The calculated results represent the entire bidding area, except for carbon emissions of heat, where the

³¹⁸ results represent the emissions in the Greater Copenhagen DH area.

³¹⁹ The results of the analysis were calculated as relative differences, compared to the energy scenario base case

- either state of the art (2011) or compared to the future scenario (2025) as presented in [14]. This implies,

that the results of a specific calculation (e.g. Case #1 at 60 °C) correspond to the relevant scenario (2011)

at DH network design temperature of 100 °C. Each of the six calculated system parameters are presented in table 5 for both current and future energy scenario.

Although only separated by 14 years, the two energy system scenarios are quite different in terms of cost and

carbon emissions. The main reason for the reductions in primary energy use and net import of electricity in 2025 was the significant increase in intermittent electricity production.

The reason for the discrepancy between the calculated emissions and the previously mentioned zero carbon

³²⁷ The reason for the discrepancy between the calculated emissions and the previously mentioned zero carbon ³²⁸ emission goal, was the difference in imposition for carbon expenditure for waste as a fuel. In *Heat plan*

Table 5: Results of energy scenarios base case (100 °C) for six system parameters

Parameter	Unit	2011	2025
		scenario	scenario
Total system cost	$10^{8} \in$	5.16	5.95
Heat CO_2 -emission	kg/MWh	0.13	0.05
Electricity CO ₂ -emission	kg/MWh	0.36	0.15
Primary energy use	$10^7 { m GJ}$	8.42	7.38
Net. Imported Electricity	10^6 MWh	2.09	1.10
Extr. CHP prod. ratio	%	0.00	-2.20

³²⁹ Greater Copenhagen a significant effort is placed for recycling the carbon constituents from waste [14], ³³⁰ whereas the performed calculations in this paper assume similar carbon composition as that of today.

 $_{331}$ The influence to CO_2 -emission for exported electricity corresponds to the overall emissions from electricity,

which thus influences not only the specific bidding area, but also to a limited extent the emissions of neighbouring transmission networks.

334 3.1 Current energy scenario

The results for case #1 and #2 are presented in Fig. 7 relative to the 2011 scenario. For case #1, system cost and CO₂-emissions are presented in Fig. 7a, whereas primary energy use, net imported electricity and extraction CHP production ratio are presented in Fig. 7b. For case #2, similar parameters are presented in Fig. 7c and 7d respectively. The results of DH temperature variations for the base case (without HPs) is presented in black color, whereas results representing configurations with the additional installed heat pump

340 capacity, are presented in gray.

 $_{341}$ By reducing DH temperatures for Case #1 (Fig. 7a), the consumer cost were reduced up to approximately

 $_{242}$ 2.8 %, and emissions by approximately 1 % and 6.4 % for electricity and heat respectively. The performance

³⁴³ improvements were consequences of the increased electricity production efficiency at CHP plants, as well as ³⁴⁴ reduction in heat losses from the network.

Both system cost and carbon emissions from electricity reached a minimum at 60 °C, whereas the minimum emissions for heat were found for forward temperatures of 50 °C. The minimum can be explained by the utilisation of additional electricity to increase the temperature of the hot tap water, when the consumer temperature decreases below the set value of 55 °C.

The electricity and heat demands are similar for all results corresponding to a specific energy scenario, and thus also the interdependency for the specific CO2 emissions for the overall emissions.

By integration of the considered central HP capacity the cost was further reduced. For the reference 351 temperature level (100 °C) a reduction in system cost of 1.2 % was possible, with a corresponding reduction 352 in emissions for heat of 3.6 %. CO₂ emissions for electricity was reduced slightly. The trend for system 353 cost for a system with HPs resembles that of the base case, but with an offset in favour of the HP case of 354 approximately 2 percentage-points. The combination of reduction in DH temperatures and integration of 355 central HP capacity in the network resulted in large reductions of CO_2 emissions for heat. The maximal 356 reduction was 19 %, which was found for DH forward temperature of 40 °C. For forward temperatures below 357 80 °C the CO₂ emissions for electricity was increased compared to the system without HP capacity (up to 358

 $_{359}$ 2 % increase).

It was found that both primary fuel usage and import of electricity decreased when decreasing DH temperatures for case #1 (Fig. 7b). For the case with HP integration, the primary energy usage decreased further, whereas the net import of electricity increased significantly. Such results suggest that the constrained production of CHP units was reduced by integrating HPs. This presumption was further supported

₃₆₄ by increased electricity production ratio of extraction CHP plants in the case with HPs compared to case

#1, and correspond to the increased CO₂ emissions for electricity, as less heat was produced from thermal

units, which shifts carbon emissions from the consumed fuel towards electricity. The increased production



Figure 7: Impact to key parameters for lowering DH network temperature for Case #1 and #2 and with integration of 200 MW central HP capacity

ratio of extraction CHP plants in case #1 (without HP) may be explained by the increase in back-pressure
 efficiency from reduction in DH temperatures.

For case #2 (capacity and storage constraints according to change in DH temperature levels) the obtained 369 results resemble those presented above. Comparing Fig. 7a and 7b with 7c and 7d respectively, it was found 370 that trends are similar at high DH temperatures, whereas the performance improvements at low DH forward 371 temperatures were reduced. The impact was increasingly significant at forward temperatures below 60 °C. 372 The potential benefits at the temperature levels of maximal reductions from case #1 were reduced, but 373 even with capacity constraints in place, the benefit was significant. As an example, the combined system 374 cost reduction was changed from 2.8~% to 2.1~% for the system without HP integration, and reductions in 375 carbon emissions for the system with HPs integrated are even slightly increased. A significant difference 376 was found for the production ratio of extraction CHP plants, which at low forward temperatures increased 377 approximately 5 % for the system without HP, and 6 % for the system with integration of HPs. The 378 difference was particularly large for DH temperatures of 40-60 °C. This could suggest that the production 379 ratio was changed due to limited network capacity at periods with high heat consumption. 380



Figure 8: Comparison of key parameters for current and future energy system scenarios

381 3.2 Comparison of the two energy scenarios

The two reference scenarios (2011 and 2025) are compared in Fig. 8. The results of both scenarios were calculated on the basis of the 2011 scenario (in table 5). Variations from the investigated parameters are presented in black colour for case #1, and by gray curves for case #3.

The case #1 data for cost and CO₂-emissions in Fig. 8a, as well as primary fuel usage and import in Fig. 8b,

are similar data as those presented in Fig. 7a and 7b, respectively. Compared to case #1, case #3 presented

 $_{387}$ significantly increased system cost (typically around 14-15 % increase) but at the same time significantly $_{388}$ reduced heat and electricity CO₂ emissions. The reductions in emissions were minimum 52 % for heat and

389 58 % for electricity.

From Fig. 8b it is found, that case #3 implied a significantly lower net import of electricity (between 40 and 50 %), and lower consumption of primary energy (approximately a reduction of 14 %). The reduction was due to a large increases of intermittent electricity in the future scenario. This was obtained without significantly affecting the production ratio of the extraction plants compared to todays operation.

The impact of changing DH temperatures on the performance of the two cases was shown to be equal in magnitude and experience similar trends at various temperature levels.

396 3.3 2025 energy scenario

Results for future scenario cases #3 and #4 are presented in Fig. 9. The reference data (black) of Fig. 9a and 9b, corresponds to the gray curves presented in Fig. 8a and 8b, respectively.

The maximal reduction in system cost, by decreasing the DH temperatures, was 3.2 % for case #3, and a reduction of 6 % when the considered additional HP capacity was integrated. For both cases this was marginally higher savings, than those presented for case #1. For case #3 with HP, the savings at forward temperatures of 50 °C was similar to that of 60 °C. The gain from integrating HP technology in low temperature DH in terms of cost was larger in 2025 low temperature scenarios, compared to 2011. For the case of 50 °C, the gain of central HP units were at a magnitude, where the technology compensates for the

⁴⁰⁵ additional electricity consumption at the consumer booster HP.

The gain in terms of CO_2 emissions of lowering DH temperatures for case #3 were small, considering systems with or without central HP integration. The maximal reduction was for heat, which was 5.8 and

7.2% respectively, but as the base scenario was already significantly reduced, the actual reductions were

low. From Fig. 9b it was found that net imported electricity was significantly reduced, with a minimum at

410 -24 to -28 % for 60 - 70 °C depending on whether or not HP capacity was included.



Figure 9: Impact to key parameters for lowering DH network temperature for Case #3 and #4 and with integration of 200 MW central HP capacity

As for the similarities between case #1 and #2, corresponding characteristics were found for the differences between case #3 and #4. The effects of DH temperature capacity constraints were large at DH temperature

 $_{413}$ levels below 60 °C. A difference for the future scenario was that a reduction in carbon emissions was not

achieved for case #4 at DH temperatures between 70 and 110 °C.

415 3.4 Parametric analysis

A detailed parametric analysis is presented for four significant input parameters, and analysed for three of the six presented parameters, as well as HP operation hours for the two units. The parametric analysis was performed for the 2025 energy scenario, case #4 w/HP, and is presented in Fig. 10 with variations of \pm 20 % of the individual input parameters. The results were calculated as relative to DH network temperatures of 100 °C for 2025 scenario.

⁴²¹ The four considered input parameters are presented below:

• Mean spot price for bidding area. Capacity of interconnections remain as specified by Energinet.dk [38].

• Biomass fuel cost.

• Production of electricity from residual technologies. This parameter is for both intermittent sources as well as decentral CHP units.

• The COP of the considered HP.

In Fig. 10a the influence of the four input parameters is presented for the combined system cost. It was found that the spot price, biomass fuel cost and the changes in production of residual electricity technologies affected the results with similar magnitude: approximately 5 to 7 % changed cost for a 20 % change in input parameter. Changes to HP COP influenced the cost of the system to a minor degree.

For carbon emissions from electricity, the chosen input parameter of biomass fuel cost was highly sensitive. 432 A reduction of 14 % on carbon emissions for 20 % reduction in fuel cost was experienced, according to Fig. 433 10b. The influence was not as significant if the fuel cost was increased. Minimal changes were found for 434 changes to CO_2 emissions from heat (Fig. 10c), where the fuel cost of biomass again was the most sensitive. 435 In Fig. 10d heat pump operation hours were presented. It was shown, that one unit (the one located at 436 Avedøreværket) experienced significantly less operation hours than the sibling (located at Amagerværket). 43 This was included to show that for case #4 w/HP, at 70 °C, the DH network capacity constraints were 438 a significant limitation to the considered technologies, especially for the marginal cost unit of the network 439 capacity. 440

441 4 Discussion

⁴⁴² In the analysis, the influence of varying DH temperatures for several different utility technologies was exam-⁴⁴³ ined. This was done in order to establish the potential for reductions in cost and primary fuel consumption.

⁴⁴⁴ In such large systems with many cooperating units, minor misrepresentation for individual technologies

can have affected the production distribution, but not significantly influenced the total consumer cost, car-

bon emissions or total primary fuel use. The litterature study revealed no similar studies or analysis, and

447 comparison with relevant literature was thus not possible.

The energy system model which was utilised for the analysis has been validated against historical data of

⁴⁴⁹ 2011. The scenario of the current energy system was based directly on the validated calculation. The future ⁴⁵⁰ energy scenario was based on a prognosis of demand and planned energy system changes such as design data ⁴⁵¹ for new units [38, 14].

The impact of lowering temperatures for utility technologies in the network were calculated based on a series of thermodynamic models. Due to lack of data, only the model for the extraction CHP plant was validated (against Elmegaard and Houbak [6]), but the remaining models was verified for operation within the considered temperature span for DH. The model for the DH booster HP configuration was previously published and the technology is currently close to commercially available [42]

⁴⁵⁶ published and the technology is currently close to commercially available [42].
⁴⁵⁷ Several of the findings (e.g. Fig. 7 and 9) suggested choosing temperatures at 60 °C, as this technically
⁴⁵⁸ is the optimal temperature for achieving low operation cost. In the analysis, the investment cost related
⁴⁵⁹ to changes in the system were not included, which likely would change recommendation towards higher

temperatures. Additionally, at 60 °C forward temperatures, the consumer temperature was below 55 °C, which thus required DH booster HP units in all dwellings. As the reduction in terms of cost and emissions

 $_{462}$ $\,$ were low from utilising temperatures above this investment limit, forward temperatures of e.g. 70 $^{\circ}\mathrm{C}$ would

463 likely result in increased relevance for the consumer.

The presented results may be seen as case specific, as they represent the specific generation technologies,

demand curves and capacity constraints of the Greater Copenhagen network. But, as shown in the analysis, the two energy scenario cases result in quite similar trends for development in terms of cost, carbon emissions

and primary fuel consumption. Thus, it is expected that similar trends would be representative for other

468 large networks.

⁴⁶⁹ The transmission network was included in the calculation, due to the impact of such constraints to cost

⁴⁷⁰ reductions or energy efficiency in the current system. By changing the DH network temperatures further

471 capacity constraints may occur, e.g. in the distribution network. Such information was not available, and



Figure 10: Parametric analysis of the results from case #4 w/HP at forward temperatures of 70 °C

would require significant changes to the utilised models. On the other hand, the constraints of network capacities in distribution networks could be assessed individually, as transmission network flow profiles can

473 capacities in distribution networks could be assessed indiv
474 be supplied as an input, based on the presented study.

475 5 Conclusion

The influence of DH network temperatures to the performance of utility production in Greater Copenhagen was investigated for forward temperatures between 40 to 110 °C. Two energy scenarios were considered, one current, which was validated model for 2011, and a future scenario, as proposed by energy planners for 2025, where reductions in carbon emissions for heat were of major interest. As neither of the two scenarios utilise central HPs for DH production, two additional scenarios were created to investigate if changed DH temperatures influenced the performance of this technology.

- 482 Compared to the current, the future scenario resulted in increased cost for consumers by approximately 15
- $_{483}$ $\,$ %, but also carbon reductions above 50 % on both electricity and heat. The two scenarios showed similar
- trends for cost and emissions for reduced DH temperatures. Reduction in consumer cost were possible, with increasing magnitude with reductions in DH temperatures, until the point where electricity was needed to
- 486 boost the temperatures of hot tap water in the individual dwellings.

⁴⁸⁷ Integration of central HPs became increasingly beneficial with reductions in DH temperatures. In a current ⁴⁸⁸ scenario with central HPs installed, cost reductions of approximately 4-5 % were achieved, which further

reduces carbon emissions from DH by more than 15 %. For future scenarios, cost reductions were further increased, but further reduction in carbon emissions for 2025 were barely possible with the considered HP

⁴⁹⁰ increased, but further reduction in carbon emissions for 2025 were barely possible with the considered HP ⁴⁹¹ technology. For both cases the maximal reduction of consumer cost was found for 60 °C forward temperature.

⁴⁹² Based on the results, the authors recommend the use of 65-70 °C as the optimal forward temperature for

⁴⁹³ DH networks, since lower temperatures require high investment, among others DH booster HP units in

each dwelling. The difference between 60 and 70 °C forward temperatures corresponds to a difference of

 $_{495}$ approximately 1.5-2 % on consumer costs for the future scenario.

 $_{496}$ The results were network specific, as they represent the specific generation technologies and demand curves

and network capacities, but similar trends were found for the two different scenarios, and similar effects may
 thus also be expected for other large DH networks.

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Nomenclature	e		
\dot{C}	cost rate, €/h	Subscripts	
с	cost factor, \in /MWh or \in	f	other technologies
\dot{H}	flow rate of enthalpy, MWh/h	g	heat pumps
0	binary operation variable, -	h	boilers
P	power, MW	i	CHP plants
Q	quantity of heat in storage, MWh	$_{j}$	energy markets
ò	heat production. MJ/s	k	thermal unit sites
r	ratio	l	transmission notes
UMM	availability input parameter	m	transmission networks
v	binary design input parameter	n	distribution networks
-		t	hours
Greek symbols			
β	power loss factor by heat extraction	Abbreviations	
Δ	reduction. MJ/s	CHP	Combined Heat and Power
n	efficiency	COP	Coefficient of Performance
		HP(s)	Heat Pump(s)
Superscripts		HS	Heat storage
1	below the "no-loss" point	O&M	operation and maintenance
2	above the "no-loss" point	TL	transmission losses
elec	electric		
ex.	extraction		
max	maximum		
min	minimum		
rel	relative to maximum		

Appendices

602 603 604 605 606	Α	Energy system 1 A.1 Structure . A.2 Economic con A.3 Electricity an A.4 Technology c	nodel formulation straints	· · · · ·	· · · ·	 	 	 	· · · ·	· · · ·	· · · ·	· · · · · ·	· · · · ·	23 24 24 25 27
607 608 609	в	A.5 System reserveEnergy system nB.1 Environments	es and operational on the second seco	nts 	· · · ·	· ·	· · · ·	· · · ·	· · ·	· · · ·		· · ·		30 30 . 31

610 A Energy system model formulation

⁶¹¹ In this appendix, the key technical and economical constraints of the detailed system model are presented. ⁶¹² As the economic constraints related to taxation are autonomous for each country, the reader is referred to ⁶¹³ [13] for further information on this specific topic for Danish conditions.

The model was implemented in General Algebraic Modelling System [17] using the mixed integer linear optimisation algorithm CPLEX [18]. External data processing is handled by Matlab, using the interface gdxmrw [16]. The implementation of energy system layout (eg. CHP-units, heat pumps or transmission capacity) is generic and easy to change from one case to another.

A.1 Structure 618

The problem was considered over a period of time $\mathcal{T} = 1, \ldots, t$, which corresponds to the operation of 619 the spot market. For each time periods, data for power plant load and the amount of stored heat at the 620 termination of the period is passed on to the beginning of the subsequent period. 621

The heat and electricity demands, as well as the electricity produced at decentral CHP plants and by wind 622 turbines in the region, were supplied as input to each of the time periods. 623

For the case where capital cost are considered as sunk cost, the objective function for minimisation of each 624 time period was calculated as presented in Eq. 3 and further explained in section 2.5. 625

Several locations are used in the analysis. Traditional production areas for thermal units are indexed by \mathcal{K} . 626

District heating transmission points (collection of streams) are indexed by \mathcal{L} . Transmission networks are 627 indexed by \mathcal{M} and the distribution networks by \mathcal{N} . 628

A.2 Economic constraints 629

For most of the assessed technologies, the cost of utility production at an individual unit depends on the 630 unit type, its efficiency, operation and maintenance cost and the type of fuel. Apart from direct fuel cost, 631 the individual fuel types may further be affected by different taxation or subsidy schemes or by additional 632 transportation and handling cost. The operation and maintenance cost included in the model correspond 633 to the variable contribution. 634

In the following sections, the economic constraints are listed for individual unit types. Note that the 635 description of power plants represents several types: extraction CHP, back pressure CHP and condensing 636 power plants. 637

A.2.1 Power plants 638

The total cost rate of production at the individual plant was calculated based on various components. The 639 method for calculation of the individual components was similar for most of the contributions. The total 640 cost rate was calculated according to eq. A.1. 641

$$\dot{C}_{i,t}^{\text{CHP}} = \dot{C}_{i,t}^{\text{fuel}} + \dot{C}_{i,t}^{\text{taxes}} - \dot{C}_{i,t}^{\text{subsidy}} + \dot{C}_{i,t}^{\text{VAT}} + \dot{C}_{i,t}^{\text{startup/shutdown}} , i \in \mathcal{I}, t \in \mathcal{T}.$$
(A.1)

The individual components of the total cost rate are dependent on the consumption of fuel and/or the 642 production of electricity and heat. All of the individual contributions to the total cost rate for CHP units 643 are required to be positive. In the case of fuel cost $\dot{C}_{i,t}^{\text{fuel}}$ the contributions are included in eq. A.2.

$$\dot{C}_{i,t}^{\text{fuel}} = c_i^{\text{fuel}} \cdot \dot{H}_{i,t} + c_i^{\text{O&M}} \cdot P_{i,t} \qquad , i \in \mathcal{I}, t \in \mathcal{T}.$$
(A.2)

where \dot{H} is the flow rate of enthalpy for combustion, and P is the produced electricity. The individual fuel 645 cost factor c_i^{fuel} for the plants were calculated based on fuel type and transportation and handling cost [40]. 646 The cost factor for operation and maintenance c_i^{fuel} corresponds to the variable cost for utility production. 647 A similar approach has been used to calculate the contribution from subsidised fuels $\dot{C}_{it}^{\text{subsidy}}$. 648 The cost rates for startup and shutdown were calculated as presented in eq. A.3. 649

$$\dot{C}_{i,t}^{\text{startup/shutdown}} = c_i^{\text{startup}} \cdot o_{i,t}^{\text{startup}} + c_i^{\text{shutdown}} \cdot o_{i,t}^{\text{shutdown}} \\ , o_{i,t}^{\text{startup}}, o_{i,t}^{\text{shutdown}} \in \{0,1\}, i \in \mathcal{I}, t \in \mathcal{T}.$$
(A.3)

The cost c_i^{startup} and c_i^{shutdown} represent the variable cost of changing the operation between on and off. The binary variables $o_{i,t}^{\text{startup}}$ and $o_{i,t}^{\text{shutdown}}$ are controlled by the optimisation algorithm, and further described 650 651 in section A.4. 652

653 A.2.2 Heat boilers

The employed method for calculation of the heat boilers was similar to the approach utilised for section A.2.1. The calculation of the total cost rate is presented in eq. A.4.

$$\dot{C}_{h,t}^{\text{boiler}} = \dot{C}_{h,t}^{\text{fuel}} + \dot{C}_{h,t}^{\text{taxes}} + \dot{C}_{h,t}^{\text{VAT}} \qquad , h \in \mathcal{H}, t \in \mathcal{T}.$$
(A.4)

All of the individual contributions to the total cost rate for boilers are required to be positive. The fuel cost was calculated based on fuel consumption and the production-dependent element of the operation and maintenance cost, which corresponds to the produced heat.

$$\dot{C}_{h,t}^{\text{fuel}} = c_h^{\text{fuel}} \cdot \dot{H}_{h,t} + c_h^{\text{O&M}} \cdot \dot{Q}_{h,t} \qquad , h \in \mathcal{H}, t \in \mathcal{T}.$$
(A.5)

A similar approach was used to calculate the cost rates for the remaining elements of eq. A.4.

660 A.2.3 Electricity-driven heat pumps

⁶⁶¹ In the case of electricity-driven heat pumps, the total cost rate does not include the cost of consumed ⁶⁶² electricity, as the electricity is covered by other elements of the objective function eq. 3 and by the energy ⁶⁶³ balances in section A.3. The remaining elements are presented in Eq. A.6.

$$\dot{C}_{g,t}^{\text{HP}} = \dot{C}_{g,t}^{\text{O\&M}} + \dot{C}_{g,t}^{\text{taxes}} + \dot{C}_{g,t}^{\text{VAT}} \qquad , g \in \mathcal{G}, t \in \mathcal{T}.$$
(A.6)

All of the individual contributions to the total cost rate for HP units are required to be positive. The contribution from O&M corresponds to the variable expenses of operating a heat pump. For the case where the heat pump uses electricity supplied from the distribution grid, a network tariff is used, in order to take the distribution losses of such networks into account.

$$\dot{C}_{q,t}^{O\&M} = c_q^{O\&M} \cdot \dot{Q}_{g,t} + c_q^{\text{networktariff}} \cdot P_{g,t} \qquad , g \in \mathcal{G}, t \in \mathcal{T}.$$
(A.7)

668 A.3 Electricity and heat balances

⁶⁶⁹ In modern energy systems, significant effort is put on balancing of the production and demand at correct ⁶⁷⁰ location and time. The electricity transmission grid within the bidding area was modelled as one uniform ⁶⁷¹ network without bottlenecks for either of the utility units or consumers.

The electricity demand P_t^{consumer} including distribution losses was used for the analysis in the electricity balance eq. A.8.

$$P_t^{\text{transmission}} - \sum_{g \in \mathcal{G}} P_{g,t} - \sum_{j \in \mathcal{J}} P_{j,t}^{\text{export}} = P_t^{\text{consumer}} \qquad , t \in \mathcal{T}.$$
(A.8)

where $P_t^{\text{transmission}}$ is the flow of electricity from the transmission network, $P_{g,t}$ is the consumed electricity from a specific heat pump, and $P_{j,t}^{\text{export}}$ is the export of electricity to a specific area.

The transmission is supplied by thermal units, other units such as wind turbines and decentral CHP units, and import of electricity.

$$\sum_{i \in \mathcal{I}} P_{i,t} + \sum_{f \in \mathcal{F}} P_{f,t}^{\text{other}} + \sum_{j \in \mathcal{J}} P_{j,t}^{\text{import}} = P_t^{\text{transmission}} / (1 - \eta_{\text{TL}}) \qquad , t \in \mathcal{T}.$$
(A.9)

In this way all electricity flows into the network are subject to losses. The magnitude of transmission losses (η_{TL}) was determined based on historical data following a similar procedure. Both import and export of

electricity are further constrained by the interconnection capacity of the two bidding areas. All of the variables in eq. A.8 and A.9 are required to be positive.

The heat balances used in the analysis followed a similar setup. The transmission network for heat is split into several areas, with detailed knowledge of the transmission capacity between each area. Opposite to the electricity demand, the heat demand is split into appropriate locations, according to the detailed data from the transmission operators. For all of the considered areas, energy balances ensure logic distribution and prevent accumulation in areas without storage options.

Two examples of heat balances are presented for introduction of units in transmission and distribution networks in eq. A.10 and eq. A.11.

$$\sum_{i\in\mathcal{I}}\dot{Q}_{i,k,t} + \sum_{h\in\mathcal{H}}\dot{Q}_{h,k,t} + \sum_{g\in\mathcal{G}}\dot{Q}_{g,k,t} = \sum_{l\in\mathcal{L}}\dot{Q}_{l,k,t} \qquad ,k\in\mathcal{K},t\in\mathcal{T}.$$
(A.10)

where $\dot{Q}_{l,k,t}$ is the transferred heat from production area k to the transmission point l. An example of the capacity limitations of the transmission network is addressed in eq. A.12. In the heat distribution network, heat is transformed from a transmission area m to the distribution network a using the variable \dot{Q}

heat is transferred from a transmission area m to the distribution network n using the variable $Q_{n,m,t}$.

$$\sum_{m \in \mathcal{M}} \dot{Q}_{n,m,t} + \sum_{o \in \mathcal{O}} \dot{Q}_{o,n,t} + \sum_{p \in \mathcal{P}} \dot{Q}_{p,n,t} = \dot{Q}_{n,t} \qquad , n \in \mathcal{N}, t \in \mathcal{T}.$$
(A.11)

where $\dot{Q}_{n,t}$ is the demand for heat in area n at time t. All of the variables in eq. A.10 and A.11 are required to be positive.

⁶⁹⁴ The limitations in transmission capacity, as well as in other connections of the DH network, is introduced ⁶⁹⁵ as presented in eq. A.12.

$$\sum_{l \in \mathcal{L}} \dot{Q}_{l,k,t} \leq \dot{Q}_{l,k}^{\max} \qquad , k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.12)

where $\dot{Q}_{l,k}^{\text{max}}$ is the maximal allowed transmission capacity in (MJ/s)

697 A.3.1 Heat storages

Heat storages may be located at any position in the network, but according to the actual locations in the energy system case, the storages was only introduced in the transmission networks. Besides the integration in the network, five equations govern the operation of the storage. The overall heat balance for the unit is presented in eq. A.13.

$$Q_{m,t} + Q_{m,t}^{\text{in}} - Q_{m,t}^{\text{out}} - Q_{m,t}^{\text{heatloss}} = Q_{m,t+1} \qquad , m \in \mathcal{M}, t \in \mathcal{T}.$$
(A.13)

where $Q_{m,t}$ denotes the heat available in the storage at time t, and $Q_{m,t+1}$ in the subsequent time step. All five elements are required to be positive in the optimisation. The heat losses related to heat storage was calculated according to eq. A.14. Low heat losses for short time heat storage are expected due to mixing of stratified layers and temperature differences to the ambient.

$$Q_{m,t}^{out} \cdot (1 - \eta_{\rm HS}) = Q_{m,t}^{\rm heatloss} , m \in \mathcal{M}, t \in \mathcal{T}.$$
(A.14)

Three additional constraints were set to represent the physical dimensions and design of the heat storage.

The constraints are presented in eq. A.15 to A.17. Eq. A.15 describes the installed capacity, where $Q_{m,t}^{\max,\text{size}}$

is the maximal allowed stored heat in (MWh). Eq. A.16 and A.17 limit the charge and discharge of the storage, where $Q_{m,t}^{\max,\text{rate}}$ is the maximal allowed rate per hour.

$Q_{m,t} \leq Q_{m,t}^{\max,\text{size}}$	$,m\in\mathcal{M},t\in\mathcal{T}.$	(A.15)
$Q_{m,t}^{\mathrm{in}} \leq Q_{m,t}^{\mathrm{max,rate}}$	$, m \in \mathcal{M}, t \in \mathcal{T}.$	(A.16)

 $Q_{m,t}^{\text{out}} \leq Q_{m,t}^{\text{max,rate}} , m \in \mathcal{M}, t \in \mathcal{T}.$ (A.17)

710 A.4 Technology constraints

The considered technologies are common utility units which are utilised in many large district heating networks. A large fraction of the utilized technology constraints are presented for each of the individual

⁷¹³ technologies.

- ⁷¹⁴ In the following sections, the constraints are listed for the individual unit types.
- 715 A.4.1 Power plants

The technical constraints for the power plants were defined in order to represent several types. In this way it
is possible to include extraction CHP, back pressure CHP and condensing power plants using few equations.
The maximum and minimum technical load in terms of fuel consumption for a power plant unit was described
according to Eq A.18 and Eq. A.19. The operation of the unit is dependent on a binary operation variable

 $_{720}$ $o_{i,t}$ and its availability UMM_{i,t} according to availability data (historical data for validation).

721 For the specific fuel load, the electricity production in full back pressure was calculated according to Eq.

A.21. A reduction in electric efficiency was modelled assuming a constant contribution at full load. The trend of the derived model is presented in Fig. A.1. The high reduction scheme fits well with the results of the AVV1 model within the typical load range.

⁷²⁵ A constant boiler efficiency was assumed for the full range of applicable loads. The heat production in ⁷²⁶ back pressure operation was evaluated as the residual of the total utilisation of fuel and the back pressure ⁷²⁷ electricity production according to Eq. A.22, where the thermal efficiency η_i^{total} corresponds to the lower ⁷²⁸ heating value of the utilised fuel.

The produced electricity of the unit was calculated according to Eq. A.23. A reduction in heat production 729 of an extraction CHP plant $(\Delta \dot{Q}_{i,k,t}^1 + \Delta \dot{Q}_{i,k,t}^2)$ leads to increased power production according to power loss factors by heat extraction β^1, β^2 [-] [43]. β^1 corresponds to heat extraction below the "no-loss" point, 730 731 β^2 for heat extraction above this operational limit. The binary input parameter $v_i^{\text{ex.}}$ is used to distinguish 732 between units with extraction points and units with only one production scheme (e.g. electricity only or 733 back pressure units). Some of the investigated back pressure units allow the operator to bypass the turbine, 734 in order to utilise the steam for boosting the heat production. The binary input parameter v_i^{bypass} is used 735 to distinguish such units from the remaining. The reduction in electricity from bypassing the turbine is 736 denoted $P_{i,k,t}^{\text{bypass}}$. 737

⁷³⁸ By use of eq A.24 and A.25 it was ensured that the change from one power loss factor to the other corresponds

⁷³⁹ to the physical requirement of the extraction CHP plant. If the binary variable $o_{i,t}^{\text{no-loss}}$ is 1, β^2 should be ⁷⁴⁰ used, otherwise β^1 . The no-loss point was located as the ratio $r_i^{\text{no-loss}}$ between heat extracted above and ⁷⁴¹ below the no loss point. The binary variable $o_{i,t}^{\text{no-loss}}$ was further used in Eq. A.26 and A.27 to determine ⁷⁴² the heat extraction.

The resulting heat from the extraction plant is determined by the Eq. A.28 to A.30. Eq. A.31 ensures that steam bypass corresponds to the bypassed amount of electricity.

For the case where power plants are constrained by rapid ramping of the boiler load, the model includes constraints designed to describe this operation restriction. The constraints were modelled as a limiting difference in load $\dot{H}_{i,k,t}^{\text{rel}}$ of the boiler from one hour to the next. As in Eq. A.32 and A.33 the constraints for startup and shutdown were included in these constraints, and correspond to the additional cost described in A.3. The constraints of Eq. A.34 and A.35 ensure that startup and shutdown only occurs in case of changed production commitment. Technical and operational power plant constraints:

$$\dot{H}_{i,k}^{\max} \cdot o_{i,t} \cdot \text{UMM}_{i,t} \ge \dot{H}_{i,k,t} \qquad , o_{i,t} \in \{0,1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.18)
$$\dot{H}_{i,k}^{\min} \cdot o_{i,t} < \dot{H}_{i,k,t} \qquad , o_{i,t} \in \{0,1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.19)

$$\eta_{i,k}^{\text{backp.}} = \eta_i^{\text{elec}} + \eta_i^{\text{reduc.}} \qquad , i \in \mathcal{I}.$$
(A.20)

$$P_{i,k,t}^{\text{backp.}} = \dot{H}_{i,k,t} \cdot \eta_i^{\text{backp.}} - \dot{H}_{i,k}^{\text{max}} \cdot \eta_i^{\text{reduc.}} \cdot o_{i,t} \qquad , o_{i,t} \in \{0,1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$

$$\dot{Q}_{i,k,t}^{\text{backp.}} = \dot{H}_{i,k,t} \cdot \eta_i^{\text{total}} - P_{i,k,t}^{\text{backp.}} \qquad , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$

$$(A.21)$$

$$\begin{aligned} & \stackrel{i,k,t}{=} = \Pi_{i,k,t} \cdot \eta_{i} \quad - \Gamma_{i,k,t} & , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{I}. \end{aligned}$$

$$\begin{aligned} & P_{i,k,t} = P_{i,k,t}^{\text{backp.}} + \beta_{i}^{1} \cdot \Delta \dot{Q}_{i,k,t}^{1} \cdot v_{i}^{\text{ex.}} + \beta_{i}^{2} \cdot \Delta \dot{Q}_{i,k,t}^{2} \cdot v_{i}^{\text{ex.}} \\ & - P_{i,k,t}^{\text{bypass}} \cdot v_{i}^{\text{bypass}} & , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}. \end{aligned}$$

$$(A.22)$$

$$v_i^{\text{bypass}}$$
, $i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}$. (A.23)

$$\begin{split} \Delta \dot{Q}_{i,k,t}^{1} - \dot{H}_{i,k}^{\max} \cdot o_{i,t}^{\operatorname{no-loss}} \leq \dot{H}_{i,k}^{\max} \cdot r_{i}^{\operatorname{no-loss}} \cdot (\eta_{i}^{\operatorname{total}} - \eta_{i}^{\operatorname{elec}}) \cdot v_{i}^{\operatorname{ex.}} &, o_{i,t}^{\operatorname{no-loss}} \in \{0.1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}. \end{split}$$
(A.24)
$$\Delta \dot{Q}_{i,k,t}^{1} + \dot{H}_{i,k}^{\max} \cdot (1 - o_{i,t}^{\operatorname{no-loss}}) \geq \dot{H}_{i,k}^{\max} \cdot r_{i}^{\operatorname{no-loss}} \cdot (\eta_{i}^{\operatorname{total}} - \eta_{i}^{\operatorname{elec}}) \cdot v_{i}^{\operatorname{ex.}} &, o_{i,t}^{\operatorname{no-loss}} \in \{0.1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}. \end{cases}$$
(A.25)
$$\Delta \dot{Q}_{i,k,t}^{1} \leq \dot{H}_{i,k}^{\max} \cdot r_{i}^{\operatorname{no-loss}} \cdot (\eta_{i}^{\operatorname{total}} - \eta_{i}^{\operatorname{elec}}) \cdot v_{i}^{\operatorname{ex.}} &, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}. \end{cases}$$
(A.26)
$$\Delta \dot{Q}_{i,k,t}^{2} \leq \dot{H}_{i,k}^{\max} \cdot (1 - r_{i}^{\operatorname{no-loss}}) &, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}. \end{cases}$$
(A.27)

$$\dot{Q}_{i,k,t}^{\text{backp.}} - \dot{Q}_{i,k,t}^{1} = \Delta \dot{Q}_{i,k,t}^{1} \cdot v_{i}^{\text{ex.}} \qquad , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.28)

$$\dot{Q}_{i,k,t}^{1} - \dot{Q}_{i,k,t}^{2} = \Delta \dot{Q}_{i,k,t}^{2} \cdot v_{i}^{\text{ex.}} , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$

$$\dot{Q}_{i,k,t} = \dot{Q}_{i,k,t}^{2} + \dot{Q}_{i,k,t}^{\text{bypass}} \cdot v_{i}^{\text{bypass}} , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.29)
$$\dot{Q}_{i,k,t} = \dot{Q}_{i,k,t}^{2} + \dot{Q}_{i,k,t}^{\text{bypass}} \cdot v_{i}^{\text{bypass}} .$$
(A.30)

$$\dot{Q}_{i,k,t}^{\text{bypass}} = P_{i,k,t}^{\text{bypass}} \cdot v_i^{\text{bypass}} \qquad , i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.31)

$$0 \leq \dot{Q}_{i,k,t}, \dot{Q}_{i,k,t}^{1}, \dot{Q}_{i,k,t}^{2}, \dot{Q}_{i,k,t}^{\text{bypass}}, \dot{Q}_{i,k,t}^{\text{backp.}}, \Delta \dot{Q}_{i,k,t}^{1}, \Delta \dot{Q}_{i,k,t}^{2}$$
$$0 \leq P_{i,k,t}, P_{i,k,t}^{\text{bypass}}, P_{i,k,t}^{\text{backp.}}, \dot{H}_{i,k,t}$$



Figure A.1: Estimated reduction of electric efficiency at low unit loads

$$\dot{H}_{i,k,t+1}^{\text{rel}} - \dot{H}_{i,k,t}^{\text{rel}} \leq \dot{H}_{i,k}^{\text{rel},\max} \cdot (1 - o_{i,t+1}^{\text{startup}}) + \dot{H}_{i,k}^{\text{rel},\text{startup}} \cdot o_{i,t+1}^{\text{startup}} \\, o_{i,t}^{\text{startup}} \in \{0,1\}, i \in \mathcal{I}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.32)

$$\dot{H}_{i,k,t}^{\text{rel}} - \dot{H}_{i,k,t+1}^{\text{rel}} \leq \dot{H}_{i,k}^{\text{rel},\max} \cdot (1 - o_{i,t+1}^{\text{shutdown}}) + \dot{H}_{i,k}^{\text{rel},\text{shutdown}} \cdot o_{i,t+1}^{\text{shutdown}}$$

$$o_{i,t+1}^{\text{shutdown}} \in \{0, 1\} \ i \in \mathcal{T} \ k \in \mathcal{K} \ t \in \mathcal{T}$$
(A.33)

$$o_{i,t}^{\text{startup}} \ge o_{i,t}^{\text{CHP}} - o_{i,t-1}^{\text{CHP}}$$

$$(1.55)$$

$$, o_{i,t}^{\text{CHP}}, o_{i,t}^{\text{startup}} \in \{0, 1\}, i \in \mathcal{I}, t \in \mathcal{T}.$$

$$(A.34)$$

$$tdown > CHP \qquad CHP$$

$$\begin{array}{l}
o_{i,t}^{\text{shutdown}} \geq o_{i,t}^{\text{CHP}} - o_{i,t+1}^{\text{CHP}} \\
, o_{i,t}^{\text{CHP}}, o_{i,t}^{\text{shutdown}} \in \{0,1\}, i \in \mathcal{I}, t \in \mathcal{T}.
\end{array}$$
(A.35)

751 A.4.2 Heat boilers

Two sets of heat boiler constraints were included in the model, one for each location type (central vs. decentral). In this section the constraints of the central installations are presented. The maximum technical load in terms of fuel consumption for a boiler unit was described according to Eq A.36.

The resulting heat production was described according to Eq. A.37, where the thermal efficiency η_h^{total} corresponds to the lower heating value of the utilised fuel.

$$\dot{H}_{h,k}^{\max} \ge \dot{H}_{h,k,t} \qquad , h \in \mathcal{H}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.36)

$$\dot{Q}_{h,k,t} = \dot{H}_{h,k,t} \cdot \eta_h^{\text{total}} \qquad , h \in \mathcal{H}, k \in \mathcal{K}, t \in \mathcal{T}$$
(A.37)

757 A.4.3 Heat pumps

Two sets of heat pump constraints were included in the model, one for each location type (central vs. decentral). In this section the constraints of the central installations are presented. The produced heat of

For certain types of installations, operation of the heat pump unit will depend on external factors, such as operation at a specific power plant or facility. For other types, the unit capacity and COP may vary according to ambient temperatures or heat source flow rates. In order to address such cases, the coefficient of performance $COP_{g,t}$ and the capacity constraint $\dot{Q}_{g,k,t}^{max}$ of the heat pump units were split at hourly basis,

the unit was calculated using a coefficient of performance, and the consumed electricity, as presented in Eq.
 A.38.

and a binary operation variable $o_{g,t}^{\text{HP}}$ was introduced. The capacity of such systems were calculated according to Eq. A.39.

$$Q_{g,k,t} = COP_{g,t} \cdot P_{g,k,t} \qquad , g \in \mathcal{G}, k \in \mathcal{K}, t \in \mathcal{T}.$$
(A.38)

$$\circ o_{g,t}^{\mathrm{HP}} \ge COP_{g,t} \cdot P_{g,k,t}$$
 $, o_{g,t}^{\mathrm{HP}} \in \{0,1\}, g \in \mathcal{G}, k \in \mathcal{K}, t \in \mathcal{T}$ (A.39)

768 A.5 System reserves and operational constraints

 $\dot{Q}_{g,k,t}^{\max}$

In order for the model to correspond to the operation of a specific energy system, additional constraints are needed to fully describe for cooperation of units and the different types of system reserves required. Many of the constraints are specified in publications from the system operator [44] [45]. For both manual and frequency reserve capacity the available reserve from a power plant unit was calculated according to Eq. A.40 and A.41 for the individual units. The individual reserve types were further constrained by minimum and maximum constributions from each unit.

$$P_{i,t}^{\text{reserve}} \leq \sum_{k \in \mathcal{K}} (\dot{H}_{i,k}) \cdot o_{i,t} \cdot \eta_i^{\text{elec}} \cdot \dot{H}_i^{\text{rel,reserve}} + \sum_{k \in \mathcal{K}} (\dot{H}_{i,k}) \cdot o_{i,t} \cdot (\eta_i^{\text{total}} - \eta_i^{\text{elec}}) \cdot \dot{H}_i^{\text{rel,reserve}} \cdot (\beta_i^1 + \beta_i^2)/2 , o_{i,t} \in \{0,1\}, i \in \mathcal{I}, t \in \mathcal{T}.$$
(A.40)

$$P_{i,t}^{\text{reserve}} \leq \sum_{k \in \mathcal{K}} (\dot{H}_{i,k}) \cdot o_{i,t} \cdot UMM_i \cdot \eta_i^{\text{elec}} \cdot \dot{H}_i^{\text{rel,reserve}} + \sum_{k \in \mathcal{K}} (\Delta \dot{Q}_{i,k,t}^1) \cdot \beta_i^1 + \sum_{k \in \mathcal{K}} (\Delta \dot{Q}_{i,k,t}^2) \cdot \beta_i^2 - \sum_{k \in \mathcal{K}} (P_{i,k,t}) , o_{i,t} \in \{0,1\}, i \in \mathcal{I}, t \in \mathcal{T}.$$
(A.41)

⁷⁷⁵ The sum of the individual reserves were required to exceed a predefined value for both types of reserves.

776 Additional operational constraints exist, e.g. considerations for operating the steam network, as well as 777 multifuel units with mutual steam turbines and/or gas turbines.

Ensuring short-circuit power, reactive reserves and voltage control was addressed by ensuring 3 large power plants ($P \ge 150$ MW) to be committed at all time.

780 B Energy system model validation

The system model has been validated against a number of data series from various sources with different time resolutions. The comparison with one of the data sources is presented in this appendix. Further results of the validation may be found in [13].

A number of assumptions are used for performance of the individual plants, heat network capacities and
 fuel costs. Historical data are used where available. Both technology and cost data are presented in Table

8a. Such data are considered constant throughout the year, although the efficiency of many units will vary
 according to DH temperatures.

⁷⁸⁷ according to DH temperatures.

By examination of the accuracy and detail of representative segments, it is shown that the model presents good agreement with the historical data. Thus the model is considered applicable to investigate the interac-

tion between several production technologies in a system where both heat and electricity costs are optimized
 for each hour.



Figure B.2: Comparison of produced electricity according to environmental reports 2011 and the model. Results correspond to entire power stations, except for AVV1 and AVV2 units.

792 B.1 Environmental reports

⁷⁹³ Based on data for environmental reports for 2011 from the companies [36, 37] and municipal cooperatives

⁷⁹⁴ [46, 47, 48] operating the considered thermal power plant, it is possible to compare the real production of ⁷⁹⁵ the actual units, with the calculated production, for a given year (2011). The two comparisons are presented

 $_{\rm 796}~$ in Fig. B.2a and B.2b for electricity and heat, respectively.

For most of the considered power plants, data is available for the entire power station, which may represent between 1 (eg. KARA) and 5 (Kyndby power station - KYB) units. For Avedøre power station, the data is available for unit 1 and unit 2 individually, where unit 2 represents a steam turbine with two boilers and two gas turbines in cooperation. The presented data series show close matches for both electricity and heat

for the individual power plants.

⁸⁰² In the case of KYB (peak load and backup unit), a very small separate district heating network exists, which

was not included in the model. For the remaining power stations the difference between actual and modelled

 $_{\tt 804}$ $\,$ production is between 0-2 %, except for SVM where deviation of electricity production is approximately 3 %

which in absolute value is only approximately 4 GWh. For ASV the considered heat demand of Kalundborg

(Asnæs) and the corresponding data from the environmental report differs approximately 2 % or 16 GWh.

⁸⁰⁷ All together, the considered power plants produce a marginally higher amount of electricity and heat in the

 $_{808}$ model compared to the operation data from 2011. This corresponds to approximately 31 GWh electricity

and 29 GWh heat.