



Predicting Biomass Char Yield from High Heating Rate Devolatilization using Chemometrics

Leth-Espensen, Anna; Glarborg, Peter; Jensen, Peter Arendt

Published in:
Energy and Fuels

Link to article, DOI:
[10.1021/acs.energyfuels.8b02073](https://doi.org/10.1021/acs.energyfuels.8b02073)

Publication date:
2018

Document Version
Peer reviewed version

[Link back to DTU Orbit](#)

Citation (APA):
Leth-Espensen, A., Glarborg, P., & Jensen, P. A. (2018). Predicting Biomass Char Yield from High Heating Rate Devolatilization using Chemometrics. *Energy and Fuels*, 32(9), 9572-9580.
<https://doi.org/10.1021/acs.energyfuels.8b02073>

General rights

Copyright and moral rights for the publications made accessible in the public portal are retained by the authors and/or other copyright owners and it is a condition of accessing publications that users recognise and abide by the legal requirements associated with these rights.

- Users may download and print one copy of any publication from the public portal for the purpose of private study or research.
- You may not further distribute the material or use it for any profit-making activity or commercial gain
- You may freely distribute the URL identifying the publication in the public portal

If you believe that this document breaches copyright please contact us providing details, and we will remove access to the work immediately and investigate your claim.

Predicting Biomass Char Yield from High Heating Rate Devolatilization using Chemometrics

Anna Leth-Espensen, Peter Glarborg, and Peter Arendt Jensen

Energy Fuels, **Just Accepted Manuscript** • DOI: 10.1021/acs.energyfuels.8b02073 • Publication Date (Web): 09 Aug 2018

Downloaded from <http://pubs.acs.org> on August 13, 2018

Just Accepted

“Just Accepted” manuscripts have been peer-reviewed and accepted for publication. They are posted online prior to technical editing, formatting for publication and author proofing. The American Chemical Society provides “Just Accepted” as a service to the research community to expedite the dissemination of scientific material as soon as possible after acceptance. “Just Accepted” manuscripts appear in full in PDF format accompanied by an HTML abstract. “Just Accepted” manuscripts have been fully peer reviewed, but should not be considered the official version of record. They are citable by the Digital Object Identifier (DOI®). “Just Accepted” is an optional service offered to authors. Therefore, the “Just Accepted” Web site may not include all articles that will be published in the journal. After a manuscript is technically edited and formatted, it will be removed from the “Just Accepted” Web site and published as an ASAP article. Note that technical editing may introduce minor changes to the manuscript text and/or graphics which could affect content, and all legal disclaimers and ethical guidelines that apply to the journal pertain. ACS cannot be held responsible for errors or consequences arising from the use of information contained in these “Just Accepted” manuscripts.

Predicting Biomass Char Yield from High Heating Rate Devolatilization using Chemometrics

Anna Leth-Espensen, Peter Glarborg, and Peter Arendt Jensen*

*Technical University of Denmark, Department of Chemical and Biochemical Engineering,
Søltofts Plads 229, 2800 Kgs. Lyngby, Denmark*

E-mail: paj@kt.dtu.dk

Abstract

This study provides a simple model for biomass char yield obtained under conditions relevant for suspension firing. Using the multivariate data analysis methods, principal component analysis (PCA) and partial least squares regression (PLS regression), an equation is presented, which predict the char yield for wood and herbaceous biomass. The model parameters are heating rate ($0.1\text{-}12 \cdot 10^3$ K/s), average particle size (0.13-0.93 mm), maximum temperature (873-1673 K), potassium content (from 0.02 wt% db and upwards), and char yield (1-15 wt% daf). The model is developed based on wood biomass data and subsequently expanded to include straw and other herbaceous biomass. It is validated against experimental data from the literature and in general it exhibits the same characteristics. Independent data sets of wood are predicted with an average error (RMSEP) of 0.9 wt%point daf, and straw with an RMSEP = 0.9 wt% daf for the model, when a slope/intercept correction is applied, or RMSEP = 1.1 wt% daf otherwise. To include herbaceous biomass, the model introduces a potassium cut off level at 0.53wt%db, because the catalytic effect of potassium on the devolatilization

1
2
3 process levels off above this concentration. The model consists of one equation, making
4 implementation into CFD and devolatilization models possible without adding to the
5 computational costs.
6
7
8
9

10 11 **1 Introduction** 12 13

14 The increased awareness of climate change has resulted in a demand for a more sustainable
15 power and heat production. One possible option is suspension firing of biomass, which is
16 often economically advantageous, because biomass particles can be utilized in existing boil-
17 ers originally constructed for coal combustion. Combustion of single particles, regardless of
18 whether it is coal or biomass, in suspension fired boilers includes devolatilization followed by
19 volatile and char combustion. The combustion of the released volatiles happens relatively
20 fast within the visual flame, while the char combustion is a more time consuming process.^{1,2}
21 Consequently, it is important to know the fractions of volatiles and char for prediction of the
22 burnout of the fuel. The volatile and char fractions are also often used as input parameters
23 in combustion models.³⁻⁵ Differences between coal and biomass particles include e.g. particle
24 size, chemical composition, and volatile fraction;⁶ which influence the obtainable char yield.
25 Since so many parameters influence the process, char yield fractions are often determined
26 experimentally for each individual fuel batch, but this is time-consuming and laborious un-
27 der suspension firing conditions.
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43

44 Several experimental studies⁷⁻¹² have investigated how typical suspension fired conditions
45 influence the char yield of different types of biomass. Typical condition for suspension firing
46 include high heating rates (> 1000 K/s), high final temperatures (> 1000 K), and small par-
47 ticles (< 3 mm). For fully devolatilized wood particles char yields in the range 1-15 wt% dry
48 ash free basis (daf) have been observed.^{7,8} Experimental results obtained under suspension
49 firing conditions have shown that particle size,⁷⁻⁹ final temperature,^{7,8,10,11} heating rate,⁸
50 and alkali content^{7,8,12} influence the obtained char yield. Higher values for both particle size
51
52
53
54
55
56
57
58
59
60

1
2
3 and potassium content result in a higher char yield for suspension firing conditions. For an
4 increase in particle size the tendency is weak,⁸ whereas the potassium content shows a strong
5 correlation to char yield up to approximately 0.5 wt% db of the biomass.⁸ Values above 0.5
6 wt% db seem not to change the char yield further. An increase in final temperature and/or
7 heating rate yields an exponentially decreasing correlation with char yield.⁸
8
9
10
11
12
13
14

15 In this study, the influence of different experimental and material parameters on biomass
16 char yield has been examined through multivariate data analysis. The use of multivariate
17 data analysis to determine biomass thermal conversion properties is limited, but a few ex-
18 amples have been found in literature. Acquah et al.¹³ have made a chemometric analysis for
19 predicting the results of thermogravimetric analysis (TGA) experiments, Kim et al.¹⁴ used
20 principal component analysis (PCA) to study biomass properties after exposure to CO₂, and
21 wood pellet properties have been studied using PCA by both Toscano et al.¹⁵ and Mancini
22 et al.¹⁶ To the knowledge of the authors, no papers predicting the char yield of high heating
23 rate experiments with the help of multivariate data analysis have been published. Neves et
24 al.¹⁷ made an empirical model for char yield obtained from devolatilization at final temper-
25 atures up to 1273 K and heating rates in the order 1-100 K/s. Trubetskaya et al.¹⁸ made a
26 one dimensional kinetic model of the char yield, fitting a set of differential equations.
27
28
29
30
31
32
33
34
35
36
37
38
39
40

41 This paper has two main purposes. First, it presents an exploratory investigation into
42 data from devolatilization of biomass under suspension firing conditions using the key in-
43 put parameters; particle size, final temperature, heating rate, and potassium content. This
44 investigation is conducted through a principal component analysis (PCA). Subsequently, a
45 model using aforementioned data to predict char yield is presented. The prediction model is
46 calculated using partial least squares regression (PLS). The model is interpreted; evaluating
47 the importance of the input parameters in a quantifiable way. The prediction model is sim-
48 ple, so it can be implemented into more complicated models and CFD simulations without
49
50
51
52
53
54
55
56
57
58
59
60

1
2
3 adding substantial computational time.
4
5
6

7 **2 Method**

8
9

10 Chemometrics is the subject of extracting information from chemical measurements with a
11 statistical approach. Commonly used methods within chemometrics are PCA and PLS.^{19–21}
12 In depth descriptions of PCA and PLS is beyond the scope of this paper, but can be found
13 in the literature.^{19–24} The PCA and PLS models presented here are made in PLS Toolbox
14 version 8.1.1, Matlab version 9.3.0 (R2017b). The data have been extracted from the relevant
15 papers using WebPlotDigitizer version 4.1.
16
17
18
19
20
21
22
23

24 **2.1 Definitions of Parameters used for Model Development**

25
26

27 The input parameters to the models are particle size, final temperature, heating rate, and
28 potassium content, as they affect char yield from high heating rate biomass devolatiliza-
29 tion.^{8,17} In the scope of this paper **particle size** is defined as the average between the upper
30 and the lower sieve sizes used for determination of biomass particle size. The sieve size
31 average is used because it is frequently available and for simplicity. As biomass can vary
32 in size and shape, more complicated measures exist.²⁵ **Final temperature** is the final or
33 maximum temperature of the applied reactor. **Heating rate** can be obtained, e.g., via a
34 thermocouple in a wire mesh reactor. Otherwise the heating rate is estimated as described in
35 supplementary material. The **potassium content** is here defined as the potassium content
36 in wt% dry basis (db) of the original biomass. In papers where the potassium content is not
37 published it is estimated as described in the supplementary material. The **Char yield** is
38 defined as the percentage of ash free char from a dry ash free biomass sample.
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

2.2 Selection of Data Applicable for Model Development

The interest of this study is the final char yield after suspension firing, hence only data for fully devolatilized particles have been used both for model development and model evaluation. The data set used for developing the model is obtained in a wire mesh reactor (WMR) and a drop tube reactor (DTR), originates from Trubetskaya et al.^{8,10} and will be referred to as the calibration set. Any data, which fulfills the requirements indicated below will be used for independent validation of the model, and is referred to as the validation set. The papers used for validation are given in table 2. The data have been obtained in EFRs and DTRs as noted in the table. Particles were considered to have obtained full devolatilization if a paper showed consistent results for particle yield fractions over time and/or the residence time was long compared to the particle size.⁸ Data which describe the char yield for fully devolatilized particles are scarce in literature, and papers,²⁶⁻³² which do not provide data on fully devolatilized particles have been omitted from the study. Likewise, papers,^{33,34} where the experimental conditions are outside the parameter intervals for the calibration data set, are also omitted from this study. The parameter intervals are given in table 1 for woody biomasses. Furthermore, char yield data^{35,36} obtained from reactor types (e.g. fluid bed reactors), where particle and operating conditions are vastly different from suspension firing conditions, may not be comparable and have been disregarded.

As the amount of published data describing char yield for non-wood biomass is limited, the presented model is developed based on wood biomass only. Considerations regarding expansion of the model to include herbaceous biomass char yield is presented in section 3.5 and 3.6. The parameter spans valid for the herbaceous char yield model are identical to the ones presented in table 1, except the potassium content, which has no upper limit for the herbaceous model.

Table 1: Parameter span for which the model for wood biomass is made. The full data set containing 37 data points from Trubetskaya et al.^{8,10} can be seen in the supplementary material. The herbaceous biomass model use the same parameter spans except for the potassium content, where there is no upper limit; see section 3.6. * Estimated value as described in the supplementary material.

Parameter	min	max
Size [mm]	0.13	0.93
Final Temperature [K]	873	1673
Heating rate [10^3 K/s]	0.10	12*
K content [wt% db]	0.02	0.37

Table 2: Data used for model evaluation. Only data for fully devolatilized particles are taken from the cited papers. Data above the dashed line are from wood biomass experiments. Data below the dashed line are from herbaceous material. * Estimated value as described in supplementary material. HR = Heating rate. # = Number of data points. EFR = Entrained flow reactor. DTR = Drop tube reactor. Potassium levels in herbaceous material is accounted for in section 3.6. Typical potassium levels in *Cynara Cardunculus* (used by Jiménez et al.³⁷) is studied by Solano et al.³⁸ and the potassium content is taken from the latter.

Paper	Reactor	Part. size	Final Temp.	HR	K content	#
	[mm]	[K]	[10^3 K/s]	[wt%db]		
A Chen et al. ³⁹	DTR	0.35	1073	2.4*	0.05*	1
B Dall’Ora et al. ⁷	EFR	0.30	1273-1573	4.6-11*	0.03-0.1	4
C Septien et al. ⁹	DTR	0.36-0.82	1273-1673	1.2-8.1*	0.08 - 0.09	6
D Zhang et al. ¹¹	DTR	0.25	1273	12*	0.03*	1
E Jiménez et al. ³⁷	EFR	0.35	1073-1448	10	>0.53*	4

2.3 Preprocessing

Preprocessing is performed to develop a robust model. The parameters have been preprocessed individually to ensure linearity between parameters and char yield, as PLS is a linear regression method. The reader is referred to figure 2-4+6 in the paper⁸ where the calibration set is originally presented for documentation of the correlations between the four independent parameters and char yield. For **particle size** the correlation seems linear, so no individual preprocessing method is applied here. **Final temperature** and **heating rate** show an exponentially decreasing correlation to char yield. It is, however, possible that it

1
2
3 can be approximated by a linear correlation in the parameter span relevant for suspension
4 firing. Both a logarithmic and no individual preprocessing (linear correlation) are tested
5 as possibilities. The **potassium content** seems to have a linear correlation to char yield
6 until approximate 0.5 wt% db,⁸ above which the effect of the potassium levels off. As the
7 latter is only relevant for non-woody biomass, since no woody samples had potassium levels
8 above 0.5 wt% db, no preprocessing of the potassium content parameter has been tested.
9 An overview of the combinations in which the preprocessings have been tested is presented
10 in table 3. The data is collected in two matrices; **X** containing values for the independent
11 variables, and **Y** containing the dependent char yield values.
12
13
14
15
16
17
18
19
20
21
22

23 All parameters in the presented model have additionally been scaled to account for unit
24 variance, to ensure that parameters contribute numerically equal regardless of the unit in
25 which they have been measured.
26
27
28
29
30

31 2.4 Cross Validation

32
33 The cross validation performed in this study is based on the random subset method, be-
34 cause the information, regarding duplicates and chronology of experiments in the papers^{8,10}
35 containing the data used for the calibration set, is scarce. The random subset method is
36 described by Dubitzky et al.⁴⁰ and ensures that the entire parameter span is used for cross
37 validation. In this paper the cross validation is made with six splits and six iterations, i.e.
38 each subset consists of approximately 17 % of the data set. The cross validation is per-
39 formed at least ten times for all models described in table 3. The explained variances in **Y**
40 and RMSECV values are averages of the performed cross validations. The calibration set
41 contains two different types of woody biomass, pine and beech. A common cross validation
42 approach is to remove one type of biomass to see if the remaining biomass type would give
43 similar results. In this case, however, it could lead to dubious results, due to the differences
44 in char yield values. In other words, as the two biomass types are primarily producing two
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

1
2
3 different ranges of char yield values, using one type to predict the other would require an
4 extrapolation of the model, which is undesirable.
5
6
7

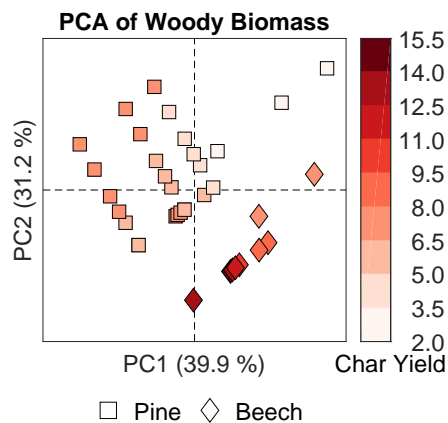
8 9 **3 Results**

10 11 12 **3.1 Principal Component Analysis**

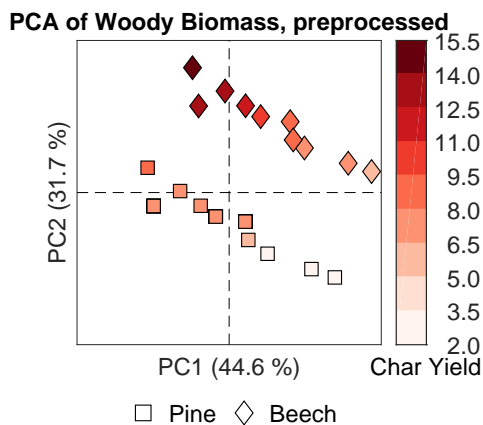
13
14
15
16 A PCA reveals systematic behavior in a data set. Ideally the data should be normally
17 distribution, but even when this is not the case PCA can reveal some systematic behavior
18 in a data set. In this case only the first two principal components (PCs) are deemed of
19 interest, so only these are shown in figure 1. The loading plots for figure 1 can be seen in
20 supplementary material. In the direction of the first PC there is a separation of the data
21 points into biomass type. Within each biomass type there is also a correlation to char yield
22 in the direction of the first PC. In the direction of the second PC the scattering due to
23 differences in char yield is more pronounced. Since the data show systematic behavior with
24 respect to char yield in the PCA, a PLS model is developed.
25
26
27
28
29
30
31
32
33
34

35 36 **3.2 Partial Least Squares Regression Model**

37
38 The PLS model is developed to be able to predict the char yield of woody biomasses and
39 thereby also the volatile yields. The preprocessing methods described in section 2.3 have
40 been tested in different combinations reported in table 3.
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60



(a) Original variables.



(b) Preprocessed variables corresponding to model 10 presented in table 3. Some of the pine samples are located identically, which means not all are visible in this plot.

46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

Figure 1: PCA plot for the 37 biomass data points from Trubetskaya et al.^{8,10} given in supplementary material colored by char yield [wt%daf]. Explained variances in PC1 and PC2 are given in the parentheses on the axes. Loading plots can be seen in supplementary material.

Table 3: Overview of tested PLS models for wood biomass. All models are made with one PLS component. ExpVarY and RMSECV are average values of at least ten cross validation runs. ExpVarY = Explained variance in \mathbf{Y} , FT = final temperature, HR = heating rate, KC = potassium content, CY = char yield. x = parameter is included. - = parameter not included directly as input parameter.

Model #	Size	FT	HR	KC	CY	ExpVarY [%]	RMSECV [wt%points daf]
1	x	x	x	x	x	72.9	1.6
2	x	x	log(x)	x	x	81.8	1.3
3	x	log(x)	log(x)	x	x	81.7	1.4
4	x	x	log(x)	x	log(x)	81.5	1.1
5	x	log(x)	log(x)	x	log(x)	81.3	1.1
6	-	x	x	x	x	77.6	1.5
7	-	x	log(x)	x	x	88.6	1.1
8	-	x	x	x	log(x)	80.5	1.4
9	-	x	log(x)	x	log(x)	86.5	1.0
10	-	log(x)	log(x)	x	log(x)	86.5	1.0
11	-	log(x)	log(x)	x	x	88.8	1.1

Based on the RMSECV and explained variance in \mathbf{Y} , the most well-performing models are number 7, 9, 10, and 11. As previously noted a logarithmic correlation is likely between the final temperature and the char yield, hence model 10 and 11 are preferred over model 7 and 9. All graphs presented in the paper have been inspected for both model 10 and 11, but as they are qualitatively similar; only one set will be presented. Since the RMSECV (and RMSEP given in section 3.4) are lower for model 10 it will be preferred. As stated in table 3 the size parameter is not included in model 10, and in general when the size parameter is included the regression models seem to predict the char yield less accurately than when it is omitted. This will be discussed in the subsequent section 4. One PLS component is used for prediction in all the PLS models reported here. Various plots were inspected for outlier detection, but none have been found. An example of hotelling T^2 vs Q residuals is presented in the supplementary material.

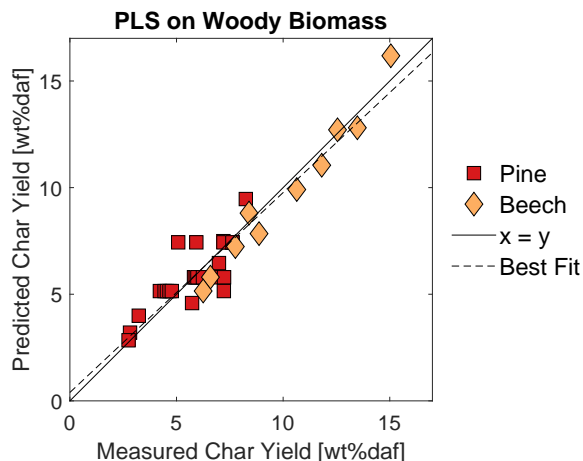


Figure 2: PLS plot of model 10 for the wood biomass calibration set.

In figure 2 the cross validated predicted char yields have been plotted as a function of the measured char yield for model 10. The figure shows good agreement between the two, and the model has $\text{RMSECV} = 1.0 \text{ wt}\% \text{point}$ and $r^2 = 0.87$. The model is condensed to a regression vector, which is given both for the preprocessed data and for the raw data in table 4.

Table 4: Regression vectors for model 10.

Parameter	Reg. vec. (Preprocessed)	Reg. vec. (Raw data)
Intercept	0	3.4370
$\log(\text{FT})$	-0.4521	-0.6598
$\log(\text{HR})$	-0.6850	-0.2130
K content	0.5713	0.6852

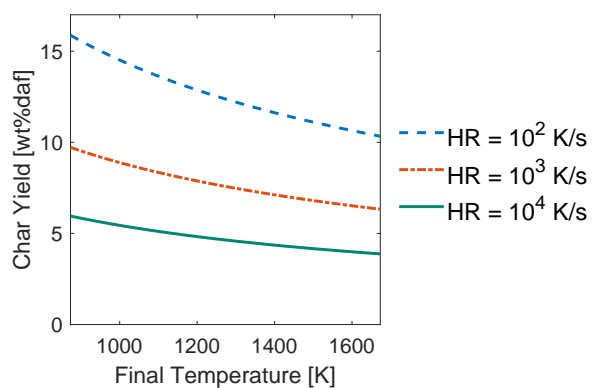
The char yield can be predicted for new data, by converting the regression vector values back to the values, they would have without the preprocessing. Thus the char yield from wood devolatilization can be predicted for new data from equation (1).

$$CY_{wood} = 10^{3.4370 + 0.6852 \cdot KC - 0.6598 \cdot \log(\text{FT}) - 0.2130 \cdot \log(\text{HR})} \quad (1)$$

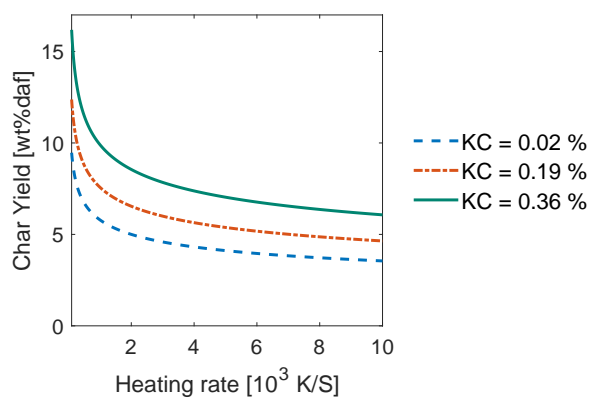
Here CY_{wood} is the char yield in $\text{wt}\% \text{daf}$, KC is the potassium content in $\text{wt}\% \text{db}$, FT is the final temperature in K, and HR is the heating rate in K/s.

3.3 General Tendencies

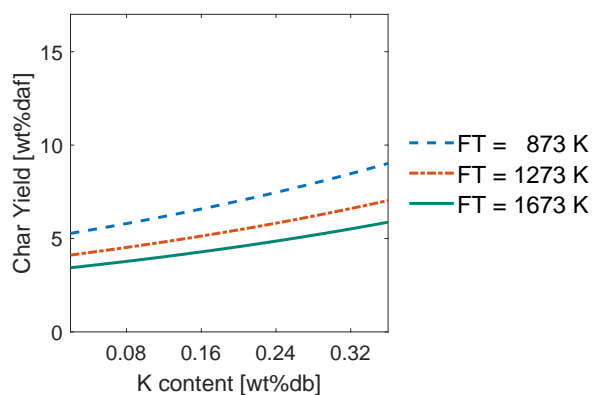
The general tendencies predicted by the model can be seen in figure 3a through 3c. In figure 3a it can be seen that the char yield decreases for increasing final temperature. In figure 3b it can be seen that the char yield decreases rapidly with increasing heating rate in the lower end of the heating rate range and that the changes are leveling out for higher values of the heating rate. Both figure 3a and 3b show an exponential correlation between heating rate, final temperature, and char yield. Figure 3c shows that the char yield increases as a function of increasing potassium concentrations in the biomass. All these findings are in good agreement with the experimental observations made by Dall'Ora et al.,⁷ Trubetskaya et al.,⁸ and Septien et al.⁹



(a) K content = 0.19 wt%db.



(b) Final Temperature = 1273 K.



(c) Heating rate = 5000 K/s.

Figure 3: Model predictions for different parameters. HR = Heating rate, KC = potassium content in [wt%db], FT = Final temperature.

3.4 Model Validation with External Data

The model has been validated with data from external experimental studies given in table 2.

The predicted and measured char yield values for the external data is depicted in figure 4.

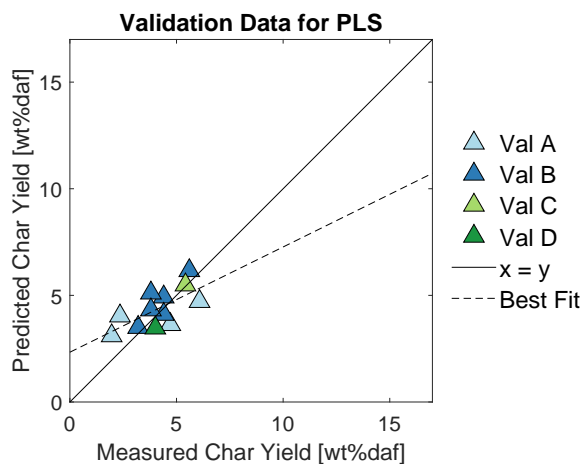


Figure 4: PLS plot for model 10 for the validation data given in supplementary material. Best fit line is for the validation data. Val A from Dall’Ora et al.,⁷ Val B from Septien et al.,⁹ val C from Chen et al.,³⁹ and Val D from Zhang et al.¹¹ The validation data are only in the lower end of the char yield range. The axes values are the same as in figure 2 for comparability.

The figure shows predicted vs. measured char yield for the validation data. There are limited data available for external validation, but in general the data are predicted well. More data, especially in the upper char yield range, would be preferable in order to evaluate this part of the model as well. The root mean squared error of prediction (RMSEP) is 0.9 wt%points for the external data. I.e., the average error for predicted biomass char yield for the completely independent data sets is ± 0.9 wt% points which is low and similar to the RMSECV value of 1.0 wt%points, indicating that the model is robust.

3.5 Predicting Char Yield of Straw

Straw is also a commonly used biomass fuel in suspension fired boilers. Trubetskaya et al.^{8,10} have conducted experiments with wheat straw, but no additional wheat straw data obtained under suspension firing conditions applicable as validation data have been found.

Consequently, a model for straw char yield has been developed by making a slope/intercept correction to the wood biomass model. An advantage of this approach is that the model is modified to give the best possible fit for the data, so biomass samples which are very similar are predicted well. Another advantage is that the slope/intercept is unbiased in determining the communal importance of the input parameters. A disadvantage of the slope/intercept is that it is not applicable for data which is different from the data used to modify the model. The following model is hence only valid for straw/herbaceous material which have the same characteristics as the wheat straw given in supplementary material. The predicted vs. measured wheat straw char yield can be seen in figure 5. It can be seen that the data are approximately linear, which strengthens the validity of expanding the model by a slope/intercept correction. Slope/intercept corrections are a standard procedure described both in academia⁴¹ and industry.⁴² A more generally applicable model is presented in section 3.6.

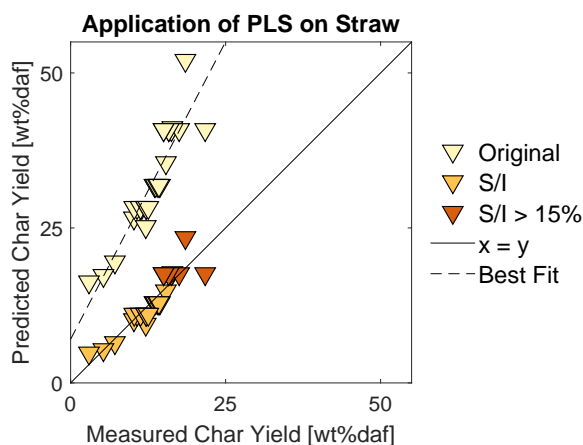


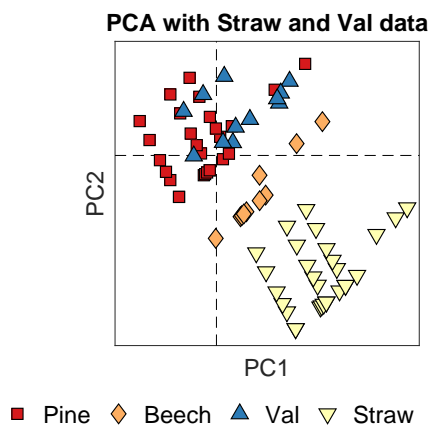
Figure 5: Predicted vs. measured char yield for model 10 in [wt%daf] for straw data by Trubetskaya et al.^{8,10} both for the original and the slope/intercept corrected model. The measured char yield data above 15 wt% daf are colored a darker orange to indicate which predicted values are found by extrapolation of the model. S/I = slope/intercept corrected model. The dashed best fit line is for the original model. The slope intercept corrected model has been corrected to have the best fit as the $y=x$ line. Straw data is given in the supplementary material.

The slope/intercept correction is further supported by the results in figure 6a and 6b,

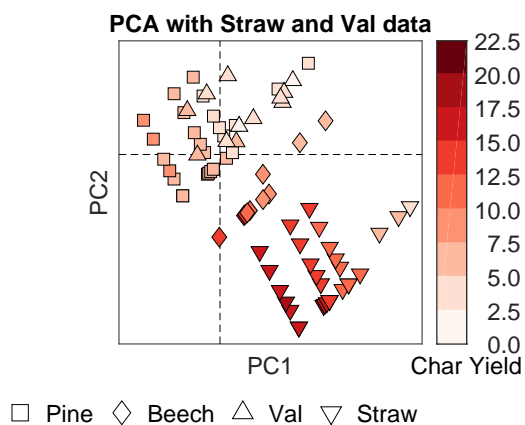
1
2
3 which show PCA plots for the original calibration set together with validation data and
4 straw data. Since the validation data for wood are occupying the same space in the PCA
5 vector space as the calibration set, it is plausible that the prediction model is applicable also
6 for the validation set, which is in good agreement with the results observed in section 3.4.
7
8 The straw data are located away from the calibration set in the PCA plot, so applying the
9 char yield model for wood directly as presented in equation (1) is not likely to yield useful
10 results. The differences in locations in the PCA plots are primarily attributable to the
11 potassium content being higher for straw. However, it is worth noticing that the tendency
12 with respect to char yield in the PCA vector space is the same for straw and woody data,
13 so a slope/intercept corrected model is appropriate. Since some of the char yields for the
14 straw exceed the maximum char yield in the calibration set, these data points have been
15 excluded before making the slope/intercept correction. They are removed because having to
16 extrapolate a PLS model is generally not advisable. As can be seen in figure 5 the removed
17 straw data are approximately located on a straight line with the same slope as the remaining
18 straw data, so the changes obtained by removing them are minor. A comparison of the model
19 statistics with and without char yield data above 15 wt% daf and the original straw data
20 can be seen in table 5. The expression for straw char yield can be seen in equation (2).
21
22 The equation has not been validated against an external validation set and should thus be
23 used more cautiously than the model for wood biomass, especially if the potassium content
24 is vastly different in the sample one wants to predict the char yield of.
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43

$$44 \quad CY_{Straw} = \frac{10^{(3.4370+0.6852 \cdot KC - 0.6598 \cdot \log(FT) - 0.2130 \cdot \log(HR))} - 10.6603}{45 \quad 1.4963} \quad (2)$$

46
47
48 Here CY_{straw} is the char yield in wt%daf, KC is the potassium content in wt%db, FT is the
49 final temperature in K, and HR is the heating rate in K/s.
50
51
52
53
54
55
56
57
58
59
60



24
25
26
27 (a) Colored by biomass type.



43 (b) Colored by char yield. NB. Colorbar is in a
44 different scale than the one presented previously.
45

46 Figure 6: The validation data and straw data incorporated into the PCA first introduced in
47 figure 1a.
48
49
50
51
52
53
54
55
56
57
58
59
60

Table 5: Model statistics for the PLS model for the cross validated calibration set for woody biomass, the validation data for woody biomass, and the straw data. The original straw model (Model 10) has been reported as well as slope/intercept corrected data with and without char yield data above 15 wt%daf. * RMSECV. ** RMSEP.

Included Data	RMSE [wt%points daf]	r ²
Woody cross validated calibration Data, Model 10	1.0*	0.87
Woody validation Data, Model 10	0.9**	0.45
Straw, Model 10	19.8**	0.82
Straw, Model 10 (S/I)	1.8**	0.82
Straw, Model 10 (S/I), yield < 15 wt% daf	0.9**	0.93

3.6 Predicting Char Yield of Herbaceous Material

Straw is not the only herbaceous material used for suspension firing and a more broadly applicable char yield model would be advantageous. A possible way of modifying the model for wood presented in equation (1) in order to include additional biomass species is to determine the potassium concentration at which the catalytic effect of this compound levels off. An advantage of this approach is a more versatile model, but it comes at the cost of lower model accuracy. The cut off level for the effect of potassium is here determined from the wheat straw experimental data by Trubetskaya et al.,^{8,10} and the cut off level is then tested for other herbaceous material experimental data by Trubetskaya et al.^{8,10} and independent data by Jiménez et al.³⁷

As previously mentioned, the linear correlation observed in the experimental data between char yield and potassium content levels off around 0.5 wt%db, so the 1.1 wt%db reported for the straw in the experiments used for model generation will likely cause an overshoot in the prediction of the char yield, if the wood model were used. However, if the wood model is used with a correction in potassium content, some of the differences between wood and herbaceous biomass can be highlighted. To determine the concentration, where the effect of potassium levels off, the RMSEP for the straw is used as an optimization parameter;

the lower the RMSEP, the better. For the given straw data the potassium content, which yields the lowest squared error (RMSEP) between measured and predicted straw char yield, is 0.53wt%db. So for biomass with a potassium content above 0.53 wt%db the input to the model in equation (1) should be fixed at 0.53 wt%db. Figure 7 depicts the predicted vs. measured straw char yield, if one uses the wood biomass model with the real straw potassium content and with a potassium content of maximum 0.53 wt%db. This indicates that the major differences in biomass char yield for wood and straw is due to the catalytic effects of potassium in the devolatilization process. This is further strengthened when the cut off value of 0.53 wt%db is used for other herbaceous biomass, as shown in figure 8. Using the same cut off value of 0.53 wt%db on different herbaceous biomass types shows that the change in potassium content accounts for the majority of the difference in char yield between wood and herbaceous material in general, but the potassium content cut off value of 0.53 wt%db is not equally good for all biomass types. RMSEP values and r^2 values for the herbaceous biomass can be seen in table 6.

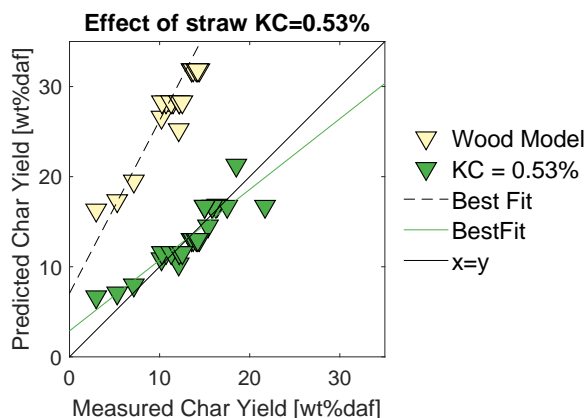


Figure 7: Predicted vs. measured char yield for model 10 in [wt%daf] for the original straw data by Trubetskaya et al.^{8,10} and for the wood model with a cut off value of $KC = 0.53$ wt%db. KC = potassium content.

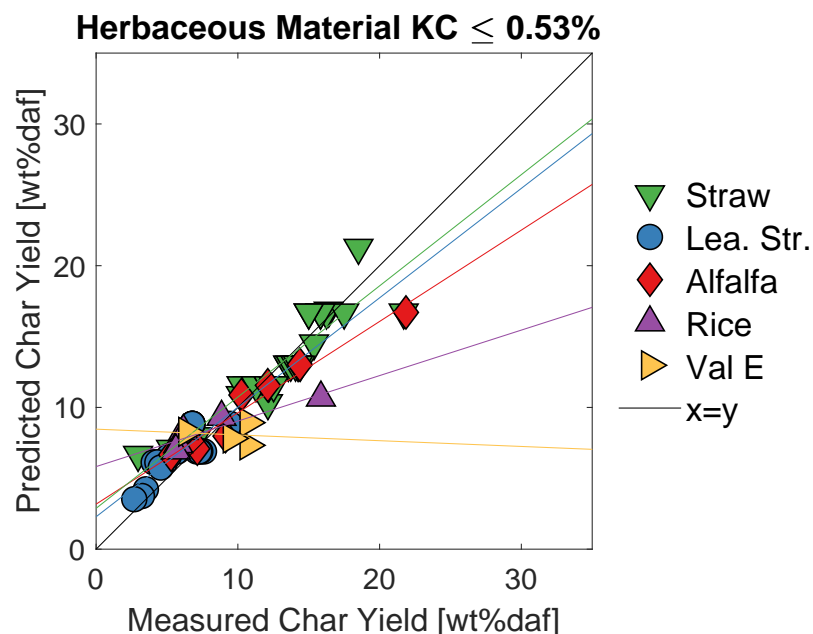


Figure 8: Predicted vs. measured char yield for model 10 in [wt%daf] for leached wheat straw, rice husk, alfalfa, and wheat straw. The two latter have a cut off value of $KC = 0.53$ wt%db. The leached wheat straw has $KC = 0.13$ wt%db. Rice husk $KC = 0.25$ wt% db. Val E = validation data from Jiménez et al.³⁷ from *Cynara Cardunculus* thistle with a cut off value of $KC=0.53$ wt%db. KC = potassium content. Best fitted lines for all biomass types can be seen in their respective colors.

Table 6: Model statistics for herbaceous biomass with a cut off value for potassium of 0.53wt%db in model 10. The cut off value for potassium has been determined by determining the minimal possible RMSEP for the straw data, all data points included. Validation data are below dashed line.

Biomass Type	RMSEP [wt%points daf]	r^2
Wheat Straw	1.6	0.82
Wheat Straw, yield < 15 wt% daf	1.1	0.93
Leached Wheat Straw	1.4	0.70
Alfalfa	2.2	0.95
Rice husk	2.7	0.86
Thistle (Val E)	2.3	0.01

4 Discussion

The model is generally good at predicting char yield from woody biomass from both the calibration data set and from externally sourced data with $RMSECV = 1.0$ wt%point and $RMSEP = 0.9$ wt%point, respectively. Model validity is further supported by the PCA, which shows that the char yield is correlated to one or more parameters in the data set. Expansion of the model to include wheat straw, by a slope/intercept correction, also yields good modeled results; $RMSEP = 0.9$ wt%point for straw with a char yield below 15 wt%daf. The model is further expanded to include different herbaceous biomass of higher potassium contents. For the versatile model, the $RMSEP = 1.1$ wt%daf for straw with a char yield below 15 wt%daf.

An advantage of developing a model using chemometrics is the prevention of bias in the selection of which parameters should have the most influence in the model, namely false assumptions about how the parameters influence the char yield and which physical phenomena are more important. Parameters are only excluded from the developed model if they do not enhance the prediction accuracy of the desired dependent parameter, specifically the char yield.

In this study, the particle size is excluded as input parameter to the model in the development process, because inclusion decreases the model accuracy. This can be observed by comparing the model statistics for models 1-5 with the ones for models 6-11 in table 3, where the $RMSECV$ and the explained variance in \mathbf{Y} both increase when the size is excluded. It is possible that the reduction to a simple mean sieve size is too crude an estimate for a biomass particle distribution, as biomass particle sizes are generally difficult to determine.²⁵ Even when the size parameter is omitted it is still implicit in the model as the size affects the wood particle heating rate.

1
2
3 The heating rate can be difficult to determine accurately. In a WMR, which was used
4 to generate most of the calibration set data,⁸ the heating rate can be controlled, but in other
5 reactor types it must be estimated, as seen in the supplementary material. In the present
6 work, a simple model is utilized to estimate particle heating rates, based on the assumption
7 that the calculated heating rate for an isothermal particle is a reasonable approximation of
8 the heating rate in the real particle. The larger the particle, the worse the assumption with
9 respect to isothermicity. The assumption is justifiable, because the model yields consistent
10 results both through the cross and external validation.
11
12
13
14
15
16
17
18
19
20

21 The potassium cut off value of 0.53 wt%db for biomass is useful in expanding the model
22 to include more biomass types. It is, however, also an additional parameter, which has been
23 fitted, and which requires validation. The cut off value results in RMSEP = 2.2 wt%daf for
24 alfalfa and RMSEP = 2.3 wt%daf for thistle, which is comparable to the RMSEP values
25 for the herbaceous biomass with lower potassium levels. The accuracy of the model should
26 be considered taking into account that the char yield is usually otherwise determined by
27 proximate analysis, which overestimates the char yield for suspension firing conditions more
28 than is the case for the model presented here.
29
30
31
32
33
34
35
36
37
38

39 For all models presented in this paper there is a tendency that the char yield is slightly
40 overpredicted for low char yields and underpredicted for high char yields as indicated by the
41 best fit lines in figures 2, 4, 7, and 8. This indicates that the model does not account for
42 extreme values very well and that the PLS models do not account for all variations in the
43 data sets. One possibility of enhancing prediction would be to develop PLS models with
44 a higher number of input parameters, which would also allow for a higher number of PLS
45 components in the model development phase. A disadvantage in using more input param-
46 eters is that usefulness of the model diminishes if complicated measurements are necessary
47 to determine the char yield. For the purpose of presenting a simple model for biomass char
48
49
50
51
52
53
54
55
56
57
58
59
60

1
2
3 yield as an input parameter to more complicated devolatilization models/CFD, the current
4
5 compromise between complexity and accuracy has been deemed sufficient.
6
7

8
9 The model is limited by the uncertainties related to measurements in the original data, which
10
11 was reported to have a measurement error of ± 5 wt% within a 90 % confidence interval. For
12
13 a char yield of 10 wt%daf, this corresponds to a char yield of 10 ± 0.5 wt%daf. This should
14
15 be compared to an RMSEP = 0.9 wt%points. The average error made by the prediction
16
17 model is just shy of twice the error reported for the calibration set data, which is considered
18
19 as being reasonable taking the number of parameters and data points into account. Espe-
20
21 cially considering the difficulty of determining uncertainties in high heating rate experiments.
22
23

24
25 It is possible to increase the quality of the model by conducting additional devolatiliza-
26
27 tion experiments in EFRs and WMRs. This should be done primarily to explore the design
28
29 space more systematically, but also to increase the amount of experimental data. In the
30
31 design space covered by the experiments for the calibration set, the input parameters are
32
33 correlated to the degree seen in the correlation coefficient chart in figure 9. The chart
34
35 gives the correlation (negative or positive) between the input parameter values chosen in
36
37 the experiments. The higher the absolute value in the coefficient chart, the more the two
38
39 parameters are correlated in the conducted experiments. It is advantageous not to have a
40
41 high correlation between parameters in order to be able to determine the effects of the indi-
42
43 vidual parameters. Despite being generally good, the chart still suggests that variations in
44
45 the particle size have not been tested equally for the two wood types, which would have been
46
47 optimal. The correlation between heating rate and final temperature might be more difficult
48
49 to separate as they are physically linked, but more WMR experiments could decouple these
50
51 two parameters.
52
53
54
55
56
57
58
59
60

	HR	FT	KC	Size	log(HR)	log(FT)
HR		0.46	0.14	-0.04	0.85	0.41
FT	0.46		0.14	-0.03	0.32	0.995
KC	0.14	0.14		-0.38	0.06	0.14
Size	-0.04	-0.03	-0.38		0.10	-0.05
log(HR)	0.85	0.32	0.06	0.10		0.28
log(FT)	0.41	0.995	0.14	-0.05	0.28	

Figure 9: Correlation coefficient chart for the parameters used to obtain the calibration set of wood biomass data.

5 Conclusion

Often a proximate analysis is used to determine the char yield for a biomass sample, however, for suspension firing combustion conditions with high heating rates and high final temperatures the char yields are lower. The models presented in this paper can be used to more accurate estimations of char yield under suspension firing conditions.

Through PCA and PLS experimental char yield data from woody biomass particles have been used to develop a simple model for predicting the char yield of woody biomass with an $RMSECV = 1.0 \text{ wt}\%daf$. The input parameters for the model are final temperature, heating rate, and potassium content. Validation of the model has been carried out using experimental data from four different studies, which gave an $RMSEP = 0.9 \text{ wt}\%daf$. The model has been expanded to include wheat straw by applying a slope/intercept correction, which yielded an $RMSEP = 0.9 \text{ wt}\%daf$. At a slight cost in model accuracy the model is

1
2
3 further expanded to include all herbaceous biomass. This gives RMSEP = 1.1 wt% daf for
4 straw, and slightly higher RMSEP values for other herbaceous biomass. The expansion is
5 conducted by determining the potassium content, where the catalytic effects of potassium
6 on the devolatilization process levels off. The value is determined to be 0.53 wt%db. Thus
7 the char yield of biomass can be determined from equation (1) repeated below.
8
9
10
11
12

$$CY_{biomass} = 10^{3.4370+0.6852 \cdot KC - 0.6598 \cdot \log(FT) - 0.2130 \cdot \log(HR)}$$

13
14
15
16
17
18 Here $CY_{biomass}$ is the char yield in wt%daf, FT is the final temperature in K, HR is the
19 heating rate in K/s, KC is the potassium content in wt%db, if $KC > 0.53$ wt%db then
20 $KC = 0.53$ in the above equation. The model is relevant for suspension firing conditions.
21
22
23
24
25

26 27 Acknowledgement

28
29
30 The authors gratefully acknowledge the financial and advisory support received from Ørsted
31 A/S, Burmeister and Wain Scandinavian Contractors A/S, and Rambøll A/S. We also thank
32 the Nordic Five Tech (N5T) alliance for financial support.
33
34
35
36
37

38 39 Supporting Information Available

40
41 The following files are available free of charge.

- 42
43
44 • Supplementary Material: Raw data for chemometric analysis, supplementary plots
45 from the analysis and a model for estimating missing parameters in char yield data.
46
47
48
49

50 51 Nomenclature

52 53 54 55 Abbreviations

1	
2	
3	CFD Computational Fluid Dynamics
4	
5	CY Char Yield
6	
7	daf dry ash free base
8	
9	db dry base
10	
11	DTF Drop Tube Furnace
12	
13	FT Final Temperature
14	
15	HR Heating Rate
16	
17	KC Potassium content
18	
19	LV Latent Variables
20	
21	PC Principal Component
22	
23	PCA Principal Component Analysis
24	
25	PLS Partial Least Squares regression
26	
27	RMSE Root Mean Squared Error
28	
29	TGA Thermogravimetric Analysis
30	
31	WMR Wire Mesh Reactor
32	
33	wt weight
34	
35	

Greek Characters

36		
37		
38	ϵ	emissivity coefficient [-]
39		
40	μ	dynamic viscosity [Pa·s]
41		
42	ρ	density [kg/m ³]
43		
44	σ	Stefan-Boltzmann constant [J/(s·m ² ·K ⁴)]
45		
46		

Roman Characters

47		
48		
49	C_p	specific heat capacity [J/(kg·K)]
50		
51	D	diameter [m]
52		
53	g	gravity acceleration constant [m ² /s]
54		
55	h	convective heat transfer coefficient [J/(s·m ² ·K)]
56		
57		
58		
59		
60		

1			
2			
3	k	thermal conductivity	[J/(s·m·K)]
4			
5	n	number of datapoints	
6			
7	Nu	Nusselt Number	
8			
9	Pr	Prandtl Number	
10			
11	Re	Reynolds Number	
12			
13	T	Temperature	[K]
14			
15	v	velocity	[m/s]
16			
17	y	measured char yield value for experiment i	[wt%]
18			
19	\hat{y}	predicted char yield value for experiment i	[wt%]
20			
21	X	Matrix of independent parameters	
22			
23	Y	Matrix of dependent parameters	
24			
25			

Sub- and Superscripts

26			
27			
28	p	particle	
29			
30	CV	Cross Validation	
31			
32	end	final or maximum value of e.g. the temperature	
33			
34	g	gas	
35			
36	i	index number	
37			
38	ini	initial value	
39			
40	P	Prediction	
41			
42			
43			
44			
45			

References

- (1) Lu, Z.; Jian, J.; Jensen, P. A.; Wu, H.; Glarborg, P. Influence of Torrefaction on Single Particle Combustion of Wood. *Energy Fuels* **2016**, *30*, 5772–5778.
- (2) Lu, Z.; Jian, J.; Jensen, P. A.; Wu, H.; Glarborg, P. Impact of KCl impregnation on single particle combustion of wood and torrefied wood. *Fuel* **2017**, *206*, 684–689.

- 1
2
3 (3) Ström, H.; Thunman, H. CFD simulations of biofuel bed conversion: A submodel for the
4 drying and devolatilization of thermally thick wood particles. *Combust. Flame* **2013**,
5 *160*, 417–431.
6
7
8
9
- 10 (4) Johansen, J. M.; Jensen, P. A.; Glarborg, P.; Mancini, M.; Weber, R.; Mitchell, R. E.
11 Extension of apparent devolatilization kinetics from thermally thin to thermally thick
12 particles in zero dimensions for woody biomass. *Energy* **2016**, *95*, 279 – 290.
13
14
15
- 16 (5) ANSYS Fluent 17.2 Theory Guide. [https://www.sharcnet.ca/Software/Ansys/17.](https://www.sharcnet.ca/Software/Ansys/17.2/en-us/help/flu_th/flu_th_sec_disp_law4.html)
17 [2/en-us/help/flu_th/flu_th_sec_disp_law4.html](https://www.sharcnet.ca/Software/Ansys/17.2/en-us/help/flu_th/flu_th_sec_disp_law4.html), 2016; Accessed: 2018-02-21.
18
19
20
- 21 (6) Priyanto, D. E.; Ueno, S.; Hashida, K.; Kasai, H. Energy-efficient milling method for
22 woody biomass. *Adv. Powder Technol.* **2017**, *28*, 1660 – 1667.
23
24
25
- 26 (7) Dall’Ora, M.; Jensen, P. A.; Jensen, A. D. Suspension Combustion of Wood: Influence
27 of Pyrolysis Conditions on Char Yield, Morphology, and Reactivity. *Energy Fuels* **2008**,
28 *22*, 2955–2962.
29
30
31
32
- 33 (8) Trubetskaya, A.; Jensen, P. A.; Jensen, A. D.; Steibel, M.; Spliethoff, H.; Glarborg, P.
34 Influence of fast pyrolysis conditions on yield and structural transformation of biomass
35 chars. *Fuel Process. Technol.* **2015**, *140*, 205–214.
36
37
38
39
- 40 (9) Septien, S.; Valin, S.; Dupont, C.; Peyrot, M.; Salvador, S. Effect of particle size and
41 temperature on woody biomass fast pyrolysis at high temperature (1000 - 1400 °C).
42 *Fuel* **2012**, *97*, 202–210.
43
44
45
46
- 47 (10) Trubetskaya, A.; Jensen, P. A.; Jensen, A. D.; Llamas, A. D. G.; Umeki, K.; Glar-
48 borg, P. Effect of fast pyrolysis conditions on biomass solid residues at high tempera-
49 tures. *Fuel Process. Technol.* **2016**, *143*, 118–129.
50
51
52
53
- 54 (11) Zhang, Y.; Kajitani, S.; Ashizawa, M.; Miura, K. Peculiarities of Rapid Pyrolysis of
55
56
57
58
59
60

- 1
2
3 Biomass Covering Medium- and High-Temperature Ranges. *Energy Fuels* **2006**, *20*,
4 2705–2712.
5
6
7
8 (12) NikAzar, M.; Hajaligol, M. R.; Sohrabi, M.; Dabir, B. Mineral matter effects in rapid
9 pyrolysis of beech wood. *Fuel Process. Technol.* **1997**, *51*, 7 – 17.
10
11
12 (13) Acquah, G. E.; Via, B. K.; Fasina, O. O.; Adhikari, S.; Billor, N.; Eckhardt, L. G.
13 Chemometric modeling of thermogravimetric data for the compositional analysis of
14 forest biomass. *PLoS ONE* **2017**, *12*, 1–15.
15
16
17 (14) Kim, K.; Labbé, N.; Warren, J. M.; Elder, T.; Rials, T. G. Chemical and anatomical
18 changes in *Liquidambar styraciflua* L. xylem after long term exposure to elevated CO₂.
19 *Environ. Pollut.* **2015**, *198*, 179 – 185.
20
21
22 (15) Toscano, G.; Rinnan, Å.; Pizzi, A.; Mancini, M. The Use of Near-Infrared (NIR) Spec-
23 troscopy and Principal Component Analysis (PCA) to Discriminate Bark and Wood of
24 the Most Common Species of the Pellet Sector. *Energy Fuels* **2017**, *31*, 2814–2821.
25
26
27 (16) Mancini, M.; Rinnan, Å.; Pizzi, A.; Mengarelli, C.; Rossini, G.; Duca, D.; Toscano, G.
28 Near infrared spectroscopy for the discrimination between different residues of the wood
29 processing industry in the pellet sector. *Fuel* **2018**, *217*, 650–655.
30
31
32 (17) Neves, D.; Thunman, H.; Matos, A.; Tarelho, L.; Gómez-Barea, A. Characterization
33 and prediction of biomass pyrolysis products. *Prog. Energy Combust. Sci.* **2011**, *37*,
34 611–630.
35
36
37 (18) Trubetskaya, A.; Surup, G.; Shapiro, A.; Bates, R. B. Modeling the influence of potas-
38 sium content and heating rate on biomass pyrolysis. *App. Energy* **2017**, *194*, 199–211.
39
40
41 (19) Wold, S.; Esbensen, K.; Geladi, P. Principal Component Analysis. *Chemom. Intell.*
42 *Lab. syst.* **1987**, *2*, 37–52.
43
44
45 (20) Jackson, J. E. *A user's guide to principal components*; John Wiley & Sons, Inc., 1991.
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

- 1
2
3 (21) Eriksson, L.; Johansson, E.; Kettaneh-Wold, N.; Wold, S. *Multi- and Megavariate Data*
4 *Analysis. Principles and Applications*, page 71; Umetrics Academy, 2003; Vol. 1.
5
6
7
8 (22) Kjeldahl, K.; Bro, R. Some common misunderstandings in chemometrics. *J. Chemom.*
9 **2010**, *24*, 558–564.
10
11
12 (23) Bro, R.; Smilde, A. K. Principal component analysis. *Anal. Methods* **2014**, *6*, 2812–
13 2831.
14
15
16
17 (24) Zachariassen, C. B. Process Analytical Chemistry and Technology in Pectin Production.
18 Ph.D. thesis, Department of Food Science, University of Copenhagen, 2007.
19
20
21 (25) Trubetskaya, A. Fast pyrolysis of biomass at high temperatures. Ph.D. thesis, Depart-
22 ment og Chemical and Biochemical Engineering, DTU, 2016.
23
24
25
26 (26) Dupont, C.; Commandré, J.-M.; Gauthier, P.; Boissonnet, G.; Salvador, S.; Schwe-
27 ich, D. Biomass pyrolysis experiments in an analytical entrained flow reactor between
28 1073 K and 1273 K. *Fuel* **2008**, *87*, 1155–1164.
29
30
31
32 (27) Lewis, A. D.; Fletcher, T. H. Prediction of Sawdust Pyrolysis Yields from a Flat-Flame
33 Burner Using the CPD Model. *Energy Fuels* **2013**, *27*, 942–953.
34
35
36
37 (28) Niemelä, N. P.; Tolvanen, H.; Saarinen, T.; Leppänen, A.; Joronen, T. CFD based
38 reactivity parameter determination for biomass particles of multiple size ranges in high
39 heating rate devolatilization. *Energy* **2017**, *128*, 676–687.
40
41
42
43 (29) Nunn, T. R.; Howard, J. B.; Longwell, J. P.; Peters, W. A. Product Compositions and
44 Kinetics in the Rapid Pyrolysis of Sweet Gum Hardwood. *Ind. Eng. Chem. Process*
45 *Des. Dev.* **1985**, *24*, 836–844.
46
47
48
49 (30) Umeki, K.; Kirtania, K.; Chen, L.; Bhattacharya, S. Fuel Particle Conversion of Pul-
50 verized Biomass during Pyrolysis in an Entrained Flow Reactor. *Ind. Eng. Chem. Res.*
51 **2012**, *51*, 13973–13979.
52
53
54
55
56
57
58
59
60

- 1
2
3 (31) Zanzi, R.; Sjöström, K.; Björnbom, E. Rapid high-temperature pyrolysis of biomass in
4 a free-fall reactor. *Fuel* **1996**, *75*, 545–550.
5
6
7
8 (32) Zanzi, R.; Sjöström, K.; Björnbom, E. Rapid pyrolysis of agricultural residues at high
9 temperature. *Biomass Bioenergy* **2002**, *23*, 357–366.
10
11
12 (33) Johansen, J. M.; Gadsbøll, R.; Thomsen, J.; Jensen, P. A.; Glarborg, P.; Ek, P.; De Mar-
13 tini, N.; Mancini, M.; Weber, R.; Mitchell, R. E. Devolatilization kinetics of woody
14 biomass at short residence times and high heating rates and peak temperatures. *App.*
15 *Energy* **2016**, *162*, 245–256.
16
17
18
19 (34) Johansen, J. M. Power Plant Burners for Bio-Dust Combustion. Ph.D. thesis, Depart-
20 ment og Chemical and Biochemical Engineering, DTU, 2015.
21
22
23 (35) Anastasakis, K.; Kitsiou, I.; de Jong, W. Fast devolatilization characteristics of 'low
24 cost' biomass fuels, wood and reed. Potential feedstock for gasification. *Fuel Process.*
25 *Technol.* **2016**, *142*, 157–166.
26
27
28 (36) Asadullah, M.; Zhang, S.; Li, C.-Z. Evaluation of structural features of chars from
29 pyrolysis of biomass of different particle sizes. *Fuel Process. Technol.* **2010**, *91*, 877–
30 881.
31
32
33 (37) Jiménez, S.; Remacha, P.; Ballesteros, J. C.; Giménez, A.; Ballester, J. Kinetics of
34 devolatilization and oxidation of a pulverized biomass in an entrained flow reactor
35 under realistic combustion conditions. *Combust. Flame* **2008**, *152*, 588–603.
36
37
38 (38) Solano, M. L.; Manzanedo, E.; Concheso, R.; Curt, M. D.; Sanz, M.; Ferna, J. Potassium
39 fertilisation and the thermal behaviour of *Cynara cardunculus* L. *Biomass Bioenergy*
40 **2010**, *4*, 1487–1494.
41
42
43 (39) Chen, L.; Dupont, C.; Salvador, S.; Grateau, M.; Boissonnet, G.; Schweich, D. Experi-
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

1
2
3 mental study on fast pyrolysis of free-falling millimetric biomass particles between 800
4 °C and 1000 °C. *Fuel* **2013**, *106*, 61 – 66.
5
6
7

8 (40) Dubitzky, W.; Granzow, M.; Berrar, D. P. *Fundamentals of Data Mining in Genomics*
9 *and Proteomics*, page 178; Springer US, 2007.
10
11

12 (41) Eskildsen, C. E.; Hansen, P. W.; Skov, T.; Marini, F.; Nørgaard, L. Evaluation of Mul-
13 tivariate Calibration Models Transferred between Spectroscopic Instruments: Applied
14 to near Infrared Measurements of Flour Samples. *J. Near Infrared Spectrosc.* **2016**, *24*,
15 151–156.
16
17
18
19
20

21 (42) Winning, H. Standardization of FT-IR instruments. *White Paper from Foss A/S* **2014**,
22 *1*, 1–7.
23
24
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60