Mechanisms of sulfur dioxide and sulfuric acid neutralization in lube oil for marine diesel engines

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Mechanisms of sulfur dioxide and sulfuric acid neutralization in lube oil for marine diesel engines

PhD Thesis
by
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May 2019
Preface and acknowledgments

This thesis is the summary of three years of research, from October 2015 to December 2018, and is submitted in partial fulfillment of the requirements for the PhD degree. Besides the research, the requirements for completion of the PhD degree also include: taking courses, teaching, dissemination, and the public defense of this thesis. The work was conducted at the Technical University of Denmark (DTU) at the Department of Chemical and Biochemical Engineering in the research center Combustion and Harmful Emission Control (CHEC).

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Thank you,
Kasper Hartvig Lejre
Abstract

The maritime sector has seen notable changes in recent years, the most important being sailing at reduced speeds to save fuel, which has been possible due to the abundance of large vessels. This, combined with new engine designs and tunings for further fuel savings, has resulted in increased water and acid condensation onto the cylinder liner, promoting a combination of corrosion and wear, significantly reducing the liner lifetime. The condensing sulfuric acid (H$_2$SO$_4$) originates from the fuel bound sulfur. To counteract corrosion, the lubrication (lube) oil is formulated with additives (CaCO$_3$-based reverse micelles).

Nowadays, further engine improvements for better fuel efficiencies are desired, however, the effects on corrosive wear are difficult to predict. In addition, switching fuels frequently is being introduced driven by availability, price, and stricter regulations on emissions. To cope with legislation, either sulfur-poor fuel can be combusted or sulfur-rich fuel with subsequent treatment with an exhaust after-treatment technology. These improvements/changes put additional demand on lubricating the engine optimally because defective lubrication has severe consequences. To understand how to optimally lubricate the engines, knowledge on what happens to the sulfur-related species (SO$_2$ and H$_2$SO$_4$) in the lube oil film is required.

The work presented in this thesis is an investigation of the neutralization of SO$_2$(g) and H$_2$SO$_4$(aq) by reaction with CaCO$_3$(s) reverse micelles in a fully formulated lube oil. The reactions are studied individually and by experiments and mathematical modeling.

The first part of the thesis investigates experimentally the reaction between H$_2$SO$_4$ and CaCO$_3$ in lube oil in a mixed flow reactor (MFR) setup by varying the Ca/S molar ratio, H$_2$SO$_4$(aq) inlet concentration, residence time, and stirrer speed. The analysis methods applied were Fourier Transform Infrared (FTIR) spectroscopy and a titration method to quantify the conversion of CaCO$_3$ and H$_2$SO$_4$ at specific conditions. The results revealed that the first step of the reaction was emulsification of the H$_2$SO$_4$ into the lube oil followed by reaction between the solubilized H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles. For the residence times investigated, it was observed that the reaction between H$_2$SO$_4$ and CaCO$_3$ was significantly reduced when reaching a critically low Ca/S molar ratio. A certain degree of stirring was found to initiate and maintain the reaction. Also, no apparent effect of varying the residence time was observed. Diluting the inlet H$_2$SO$_4$
concentration led to a decreased conversion of CaCO₃, probably due to the introduction of a large amount of water, leading to poor solubilization of the H₂SO₄ droplets.

The second part of the thesis concerns mathematical modeling of the experimental MFR data for the reaction between H₂SO₄ droplets and CaCO₃ reverse micelles. It was difficult to identify conclusively the limiting step of the neutralization reaction, however, a quantitative description of the reaction rate and its temperature-dependency was determined. The validated mathematical model was used to predict conversion of H₂SO₄ in a lube oil for conditions relevant for a full-scale application. The calculations show that H₂SO₄ may interact with the cylinder liner surface regardless of how well-wetted the surface is.

The third and last part of this thesis describes a study of the mechanism underlying the reaction between gaseous SO₂ and CaCO₃ reverse micelles in lube oil in a pressurized stirred batch reactor setup. The first step of the mechanism is the absorption of gaseous SO₂ into the lube oil emulsion, followed by reaction with CaCO₃ reverse micelles. The reaction shows a dependence on the initial water concentration due to increased SO₂ absorption in the lube oil emulsion. The overall temperature dependence on the reaction was observed to be weak because the absorption of SO₂ decreases at increased temperature. It was also observed that CaSO₃ was initially formed, followed by formation of CaSO₄ at extended residence times and increased temperature. A mathematical model was derived and kinetic parameters were determined by fitting of the model to experimental data. The batch reactor model was used to predict the CaCO₃ conversion in a lube oil emulsion from SO₂ for worst-case conditions relevant for a full-scale application. The simulations revealed that consumption of CaCO₃ by SO₂ is insignificant in a two-stroke marine diesel engine application; the H₂SO₄-CaCO₃ reaction is much faster than the SO₂-CaCO₃ reaction.

The work contributes with insight on how H₂SO₄ is neutralized by CaCO₃ reverse micelles in the lube oil film and that SO₂ is not a concern with respect to CaCO₃ consumption. The tools developed can be used in models of complete two-stroke marine diesel engines, including estimation of the condensation rate of H₂SO₄ and the corrosion rate of the cylinder liner surface by unreacted H₂SO₄ in the lube oil emulsion, with the aim of determining optimal lubrication strategies.
Dansk Resumé

Den maritime sektor har gennemgået betydelige ændringer i de seneste år, hvoraf en af de vigtigste er at sejle med reducerede hastigheder for at spare brændstof, hvilket har kunnet lade sig gøre grundet overfloden af store containerskibe. Dette, kombineret med nye motordesign og justeringer for at spare yderligere brændstof, har resulteret i stigende kondenserings af vand og syre på cylinderføringerne i motorerne, hvilket har fremmet en kombination af korrosion og slid. Dette har nedbragt levetiden af foringerne betydeligt. Den kondenserende svovlsyre (H₂SO₄) stammer fra svovlen som er bundet i brændslet. Derfor, for at modvirke korrosion, formuleres smøreolien med additiver (CaCO₃-baserede omvendte miceller).

Nu til dags ønskes endnu flere motorforbedringer for at øge brændselseffektiviteten yderligere, men indvirkningerne af disse på korrosivt slid, er vanskelige at forudsige. Derudover, drevet af tilgængelighed, pris og strengere udledningsreguleringer, udskiftes det anvendte brændsel ofte i motoren. For at overholde lovgivningen, kan enten svovlfattige eller svøvlrige brændsler forbrændes i motoren med efterfølgende behandling af udstødningsgassen. Disse ændringer/forbedringer sætter yderligere krav til optimal smøring af motoren, fordi en ufuldstændig smøring har alvorlige konsekvenser. Derfor, for at forstå hvordan motoren smøres optimalt, kræves der yderligere viden omkring, hvad der sker med de svovlrelaterede arter (SO₂ og H₂SO₄) i smøreoliefilmen.

Denne afhandling er en undersøgelse af neutraliseringen af SO₂(g) og H₂SO₄(aq) ved reaktion med CaCO₃(s) omvendte miceller i en fuldt formuleret smøreolie. Reaktionerne blev studeret individuelt ved forsøg og matematisk modellering.

Første del af afhandlingen er en eksperimental undersøgelse af reaktionen mellem H₂SO₄ og CaCO₃ i smøreolie i en velomrørt reaktoropstilling ved at variere Ca/S molforholdet, indgangskoncentrationen af H₂SO₄(aq), opholdstiden samt omrøringshastigheden. De anvendte analysemetoder var Fourier Transform Infrarød (FTIR) spektroskopi og titreringsmetode til at kvantificere omdannelsen af CaCO₃ og H₂SO₄ under specifikke forsøgsforhold. Resultaterne viste, at det første trin i reaktionen var emulgering af H₂SO₄ i smøreolien efterfulgt af reaktion mellem de emulgerede H₂SO₄ dråber og CaCO₃ omvendte miceller. For de undersøgte opholdstider blev det observeret, at reaktionen mellem H₂SO₄ og CaCO₃ var betydeligt reduceret, når et kritisk lavt Ca/S molforhold blev anvendt. Der blev ikke observeret nogen tilsyneladende
virkning af at variere opholdstiden. En vis grad af omrøring viste sig at igangsætte og opretholde reaktionen. Fortynding af indgangskoncentrationen af H₂SO₄ førte til reduceret omdannelse af CaCO₃, sandsynligvis på grund af tilsætningen af en stor mængde vand, hvilket resulterede i nedsat emulgering af H₂SO₄ dråberne.

Anden del af afhandlingen omhandler matematisk modellering af de eksperimentelle data fra den velomrørte reaktor for reaktionen mellem H₂SO₄ dråber og CaCO₃ omvendte miceller. Det var vanskeligt at bestemme det begrænsende trin i neutraliseringsreaktionen, dog blev den temperaturafhængige reaktionshastighed bestemt kvantitativt. Den validerede matematiske model blev brugt til at forudsige omdannelse af H₂SO₄ i en smøreolie under betingelser, der er relevante for en fuldskalaapplikation. Beregningerne viste, at H₂SO₄ muligvis interagerer med cylinderforingsoverfladen, uafhængigt af hvor godt befugtet overfladen er.


Dette arbejde bidrager med indsigt i, hvordan H₂SO₄ neutraliseres af CaCO₃ omvendte miceller i smøreoliefilmen og at SO₂ ikke er et problem med hensyn til forbrug af CaCO₃. De udviklede værktøjer kan anvendes i modeller, som beskriver en komplet totakts dieselmotor, herunder estimation af kondensationshastigheden af H₂SO₄ og korrosionshastigheden af cylinderforingsoverfladen af det ikke-omsatte H₂SO₄ i smøreolieemulsionen med det formål at bestemme optimale smøringsstrategier.
Conference contribution and publications

Oral conference contribution


Peer-reviewed article published in conference proceedings


Peer-reviewed article published in journal


Article in preparation

Kasper H. Lejre, Peter Glarborg, Henrik Christensen, Stefan Mayer, Søren Kiil, ”Experimental investigation and mathematical modeling of the reaction between SO₂(g) and CaCO₃(s)-containing micelles in lube oil for large two-stroke marine diesel engines”, To be submitted 2019.
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Introduction

Approximately 90% of the world trade is transported by the international shipping industry\(^1\) and the dominant propulsion technology in the modern ship propulsion market is the large, low-speed two-stroke diesel engine.\(^2,3\)

In the latter part of the 2000s, high oil prices and the global economic recession forced ship operators to dramatically reduce operating costs, especially the fuel oil consumption, which constitutes the main expense of the ship operation.\(^4\) The easiest way of reducing the fuel cost was to reduce the speed of the ships, also known as slow steaming.\(^5\) By operating large container ships at 60-70% of their design speeds, reduction of up to 70% of the daily fuel consumption was achieved.\(^6\) The enablement for the introduction of the slow steaming principle was overcapacity in the shipping market at that time due to a downturn in trade and delivery of newly build ships ordered before the economic crisis.\(^6\) The total economic profit of increasing the slow steaming vessel fleet to maintain the vessel frequency is difficult to exactly assess, as it depends on many factors.\(^5\) Addition of a vessel that would otherwise have been idle allowed carriers to reduce the overcapacity because the lower speeds add to the voyage time.\(^6,7\)

Along with the introduction of the slow steaming principle, the ship manufactures further optimized fuel efficiency in the low load range by introducing new engine designs and tunings.\(^8\) The overall effect of slow steaming and engine modifications/improvements led to increased operating cylinder pressures and lower cylinder liner surface temperatures.\(^8\) These changes in operating conditions resulted in increased water and acid condensation onto the cylinder liners and promoted a combination of abnormal corrosion and wear (called cold corrosion) of the cylinder liners and piston rings.\(^8,13\) The condensing acid responsible for the observed cold corrosion is thought to be sulfuric acid (H\(_2\)SO\(_4\)), which originates from the preferred fuel used, heavy fuel oil (HFO).\(^14\) The HFO is of very low quality and is basically a waste product from the oil refineries, containing a considerable amount of sulfur.\(^15\) Because cold corrosion can develop within hours\(^16\) and result in a high material loss rate (thereby significantly reducing the lifetime of the components),\(^8,13\) it is crucial to mitigate the phenomenon. To hamper corrosion of the cylinder liners and piston rings, cylinder lubricants are fed to the engine, providing an oil film between piston rings and cylinder liners. The cylinder lubricant (lube) oils contain alkaline additives, for the purpose of mitigating the harmful effects from the combustion products, mainly condensing H\(_2\)SO\(_4\).\(^14,17-20\) The general, but rather obvious, recommendation is to limit cold corrosion by supplying sufficient alkaline additives to the cylinder liner (the amount of alkalinity is defined by the base number, BN: mg KOH per g oil), see Figure 1.1.
In reality, the way of lubricating the engine optimally is a difficult task. Under-lubricating the cylinder liners lead to cold corrosion, whereas too much lube oil is expensive and may have severe, irreversible consequences, such as scuffing (direct metal to metal contact). Actually, a controllable degree of corrosion (denoted “low wear” in Figure 1.1) is beneficial to maintain a sufficiently rough surface for better supporting an oil film. Adding to the complexity of determining the optimal lubrication strategy is the newly and future actions related to emission legislation taken by the International Maritime Organization (IMO), which has defined regulations regarding overseas emission of sulfur oxides, see Figure 1.2.

The sulfur cap defined by IMO depends on whether a ship is operated within or outside a specific Emission Control Area (ECA) depicted in Figure 1.2. When operated within an ECA, a maximum of 0.1 wt.% sulfur is allowed in the burned fuel. A significant reduction in sulfur emission is enforced in 2020 by reducing the global sulfur cap from 3.5 to 0.5 wt.%. However, it is allowed to operate with higher sulfur content in the fuel if using an exhaust cleaning technology capable of reducing the emissions to an equivalent level to that of burning low-sulfur fuel. Depending on price and availability, it may therefore be cost-effective to combust high sulfur fuels in the future, and even burning fuels with a sulfur content higher than today’s limit of 3.5 wt.%. Based on the global 0.5 wt.% sulfur cap enforced in 2020, MAN Energy Solutions expects that the high sulfur fuels will remain a significant part of the fuels burned after 2020; the price may probably be sufficiently low to support installation and operation of exhaust gas cleaning technologies. Against this background, it may be profitable to change the fuel type with respect to sulfur content frequently. As a consequence, the lube oil dosing has to conform to maintain its performance with respect to low wear rates, outlined in Figure 1.3.
1.1 SULCOR – SULfuric acid CORrosion in large marine diesel engines

Figure 1.3. Liner wear as a function of cylinder lube oil feed rate for different sulfur-containing fuels. If the engines are not lubricated by an optimal feed rate of lube oil, scuffing or cold corrosion may occur giving high wear rates of the cylinder liners.16

Figure 1.3 only considers the interaction between sulfur content in the fuel, the lube oil feed rate, and wear rate. However, differences in operational conditions, ambient conditions, and engine configuration add to the complexity of setting up general recommendations for optimal lubrication dosage. Especially when trying to further optimize the performance of the engines for better fuel efficiencies, it is presently impossible to predict the exact effect on the sulfur chemistry in the hostile cylinder environment and how to best mitigate the harmful effects. What needs further investigation is a detailed physical and chemical understanding of the processes in the combustion chamber that govern the cold corrosion phenomenon, that is the formation of SO₃ and H₂SO₄, the simultaneous heat transfer and phase change of combustion gases in the turbulent boundary layer close to cooled combustion chamber walls, the diffusion of acid into the oil film, and the chemical reactions that takes place within the oil film and on the cylinder surfaces. With improved knowledge in these areas, it will be possible to guide the design process towards engine concepts with even lower fuel consumption without sacrifices to component lifetime and reliability. To gain a deeper understanding of the underlying processes occurring in the large two-stroke marine diesel engine with respect to sulfur corrosion, the research project SULCOR was initiated.

1.1 SULCOR – SULfuric acid CORrosion in large marine diesel engines

The overall objective of the SULCOR project was to identify the mechanisms and rate-limiting steps, as well as the impact of process parameters, on the sulfur-induced corrosion in marine diesel engines. By developing experimentally verified mathematical tools, sulfur corrosion was to be quantified. The hope was that this would allow MAN Energy Solutions to develop efficient tools for mitigating the corrosion problem and improve engine efficiency. The anticipated modeling tools in SULCOR included a multi-zone model to calculate the amount of H₂SO₄ condensing on the cylinder liner, a heat and mass transfer model for the turbulent boundary layer near the wall, a model for the physical/chemical neutralization of H₂SO₄ in the lube oil film, and a corrosive wear model of the cylinder liner wall. The anticipated result of the project was hoped to be a significant improvement of the ability to predict corrosion in large diesel engines for ship propulsion. These improvements will lead to faster development of these engines in the efforts to meet stricter regulations on fuels, fuel consumption, and emissions. The project was a collaboration between research groups at DTU Mechanical Engineering (2 PhD and 2 Postdoc) and DTU Chemical Engineering (2
1 Introduction

PhD), together with MAN Energy Solutions. In addition, three international universities were involved in SULCOR, namely University of Southampton, Rostock University, and Lund University.

1.2 Aims of the present work

This PhD project constitutes a part of the larger SULCOR research project, focusing on the chemical/physical interactions taking place within the lube oil film on the cylinder liner, more specifically investigating the sulfur-related reactions with the alkaline additives in a fully formulated lube oil. The specific aims of this PhD project are summarized below:

- Mapping and quantification of acid generation, transport, and neutralization mechanisms in a fully formulated lube oil, by:
  - Constructing reactors to investigate the reactions between the sulfur-related components (SO₂ and H₂SO₄) and the alkaline additives in the lube oil and to verify the mathematical models derived.
  - Developing mathematical models to extract reaction kinetics of the acid neutralization reactions and to quantify acid conditions (such as acid concentration) in the lube oil at the oil-cylinder wall interphase as a function of various engine relevant input parameters such as temperature, flow of sulfur components to the oil phase, limestone content in the lube oil, and lube oil residence time.

1.3 Scientific hypotheses

Now follows the scientific hypotheses which were established based on an extensive literature study and carrying out preliminary experiments of the reaction between H₂SO₄ and lube oil.

- The neutralization reaction between H₂SO₄ and the alkaline additives (present as micelles) in lube oil is limited by a single rate-limiting step; micelle diffusion, micelle adsorption, chemical reaction, micelle desorption, or macromixing.

- The H₂SO₄ droplets get into the bulk of the lube oil film, eventually reaching the cylinder liner surface, by either:
  - Diffusion, or
  - Mixing by the piston rings

- The specific engine conditions will have a significant impact on the conversion rate of the acidic sulfur components.

- Different experimental setups can be used to individually investigate the sub-processes happening in a lube oil film.
• The SO₂ reacts with the alkaline additives in the lube oil in an engine due to the high partial pressure of SO₂ prevailing in the combustion chamber.

• Different analysis equipment can be used to accurately measure the BN and determine the reaction products in the lube oil.

• Modeling results can be used to estimate the acid concentration on the cylinder liner surface, which can be used in a model concerning the corrosive wear of the surface material.

1.4 Outline of this thesis

Each of the following chapters can be read separately. The experimental chapters (Chapters 3, 4, and 5) are manuscripts that are either published or prepared for submission and they are therefore introduced by a short literature section, resulting in some inevitable overlap. The content of each chapter is summarized below:

• **Chapter 2** is a literature review on the general concepts of a two-stroke marine diesel engine, the acid’s way from fuel sulfur to condensing H₂SO₄ that corrodes the cylinder liners, the role of SO₂ on corrosive wear, and how corrosion is mitigated.

• **Chapter 3** consists of a published peer-reviewed conference article with the title “Reaction of sulfuric acid in lube oil: Implications for large two-stroke diesel engines”, where the neutralization of H₂SO₄ in a fully formulated lube oil was investigated experimentally by use of a mixed flow reactor.

• **Chapter 4** is based on a published article with the title “Mixed flow reactor experiments and modeling of sulfuric acid neutralization in lube oil for large two-stroke diesel engines”. The experimental work of this chapter expands the work and conclusions presented in Chapter 3. A mathematical model was also derived to extract kinetics for the neutralization mechanism and used to predict H₂SO₄ conversions at conditions relevant for a two-stroke marine diesel engine.

• **Chapter 5** consists of an article in preparation for submission with the title “Experimental investigation and mathematical modeling of the reaction between SO₂(g) and CaCO₃(s)-containing micelles in lube oil for large two-stroke marine diesel engines”, where the reaction between SO₂ and the alkaline additives contained in the lube oil was investigated in a batch reactor setup at elevated pressures and temperatures. A mathematical model was derived and used to extract kinetics of the reaction. The model was finally used to determine the significance of SO₂ consuming alkaline additives at conditions relevant for a two-stroke marine diesel engine.

• **Chapter 6** revisits the scientific hypotheses in order to clarify whether each of the hypotheses was true or false.

• **Chapter 7** presents conclusions and suggestions for future work.
• **Appendix A** describes shortly preliminary lube oil investigations to determine the kind of alkaline additives formulated in the lube oil used for the experimental work of this thesis. Analysis methods include Fourier Transform Infrared Spectroscopy (FTIR), titration, gas analysis, Energy Dispersive X-Ray Fluorescence (ED-XRF), and Thermogravimetric Analysis (TGA).

• **Appendix B** is a short description of some preliminary computational fluid dynamics (CFD) simulation results that were carried out during this PhD.

• **Appendix C and D** contains supporting information for Chapter 4.

• **Appendix E** contains supporting information for Chapter 5.

References


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(4) Bejger, A.; Drzewieniecki, J. Analysis of Tribological Processes Occurring in Precision Pairs Based on Example of Fuel Injection Pumps of Marine Diesel Engines. 2015, 41 (113), 9–16.


(15) Cordtz, R. The Influence of Fuel Sulfur on the Operation of Large Two-Stroke Marine Diesel


2 | Background

This chapter serves the purpose of introducing the reader to the two-stroke engine principle and the hostile environment prevailing in a cylinder liner with the focus on the sulfur chemistry from burning sulfur-containing fuels. This includes the formation of the corrosive acid species in the gas phase, condensation, neutralization mechanisms, wear mechanisms, and how to mitigate corrosive wear by use of lube oil.

2.1 The two-stroke engine principle

A central part of the reciprocating engine is the cylinder liner that forms the cylindrical inner part of the engine block in which the piston travels. The two-stroke principle is characterized by taking two piston strokes to complete each combustion cycle (converting the energy in the fuel to work). This means that the piston moves one time up and one time down the cylinder liner for each cycle and therefore the crankshaft must revolve once. The two-stroke cycle is illustrated in Figure 2.1 and consists of four major events: 1) compression, 2) injection, 3) combustion, and 4) scavenging.

![Figure 2.1](image_url)

*Figure 2.1.* The two-stroke cycle illustrated by four still images: 1) compression, 2) fuel injection, 3) combustion, and 4) scavenging.¹
The four major events occurring during a cycle are briefly described in the following:\footnote{1}

1) **Compression:** As the piston is moved upwards, the volume of the combustion chamber is decreased and the pressure and temperature increases. This happens after the closing of the exhaust valve and scavenging ports, which means that the combustion chamber is filled mainly with fresh air, but also with some residual combustion gas from the previous combustion cycle.

2) **Fuel injection:** Just before the piston reaches the top of the cylinder (known as top dead center, TDC), fuel injection starts. The fuel breaks into droplets which evaporate and mixes with the air followed by self-ignition and combustion of the fuel.

3) **Combustion:** Due to the occurring combustion, high pressure and temperature are evolved in the combustion chamber which forces the piston downwards (expansion stroke). The force of the downward movement of the piston is transferred into kinetic energy by rotation of the crankshaft.

4) **Scavenging:** Before reaching the bottom of the cylinder (known as bottom dead center, BDC), the exhaust valves open and the combustion gas begins to leave the cylinder. Shortly after, the piston uncovers the scavenge ports from which fresh, pressurized air enters the cylinder environment. The exhaust valves are still open and the fresh intake air therefore pushes the remaining combustion gas out of the combustion chamber. This is called ‘scavenging’. The piston then reaches BDC and begins to approach TDC once again. During the upward stroke, the scavenge ports are covered by the piston, closing off for the intake air and shortly after the exhaust valves also closes. The combustion chamber now mostly consists of fresh intake air and the compression stroke begins.

The two-stroke cycle illustrated in Figure 2.1 can also be presented as a function of the crank angle degree (CAD) in a timing diagram, see Figure 2.2. The combustion cycle consists of two strokes (up and down) and thereby one complete revolution of the crankshaft (360 degrees), i.e., TDC is located at 0 CAD and BDC is located at 180 CAD.

\begin{figure}[h]
\centering
\includegraphics[width=0.5\textwidth]{figure22.png}
\caption{The two-stroke cycle as a function of the crank angle degree (CAD). The placement of the different events in the cycle is described relative to the top dead center position: after top dead center (ATDC) or before top dead center (BTDC).\footnote{2}}
\end{figure}
Figure 2.2 shows that the fuel is injected around 10-20 CAD BTDC followed by combustion and expansion of the combustion gas. Around 110-120 CAD ATDC, the combustion gas is exhausted and the scavenging ports open at around 130-150 CAD ATDC and close at around 130-150 CAD BTDC. Shortly after, at 110-150 CAD BTDC, the exhaust valves are closed and the compression stroke proceeds. The period from injection of the fuel to the exhaust valves open is the available timeframe for the acidic sulfur species to be formed and reach the lube oil film. After the opening of the exhaust valves, the combustion gas is ventilated and this removes the sulfur species formed from the gas phase. The acidic species are then present in the lube oil film as a minimum for the remaining part of the cycle, where they can react with the alkaline additives in the lube oil film or with the cylinder liner wall.

2.2 Sulfur chemistry in the gas phase

The main sulfur products from the combustion of sulfur-containing fuels are SO$_2$, SO$_3$, and H$_2$SO$_4$ according to the overall reactions shown below:

\[
\text{Fuel-S}_2(s) + O_2(g) \rightarrow SO_2(g) \quad (2.1)
\]

\[
SO_2(g) + \frac{1}{2}O_2(g) \rightarrow SO_3(g) \quad (2.2)
\]

\[
SO_3(g) + H_2O(g) \rightarrow H_2SO_4(g) \quad (2.3)
\]

\[
H_2SO_4(g) \rightarrow H_2SO_4(aq/l) \quad (2.4)
\]

The first step is oxidation of the sulfur in the fuel according to Eq. (2.1). For excess air combustion, as is valid for an engine application, the reaction is fast and the fuel sulfur is predominantly oxidized to SO$_2$ because local temperatures reach more than 2500 K. A fraction of the SO$_2$ is then oxidized to SO$_3$, primarily in the temperature range from 1300 K to 2000 K during the expansion stroke, up to 10% depending on species concentrations (SO$_2$, O$_2$, SO$_3$), temperature, and pressure (which are determined by the specific operating conditions of the engine such as load, sulfur content in fuel, and ambient conditions). The SO$_3$ reaction mechanism at combustion conditions has been investigated comprehensively over the years and a detailed reaction mechanism has been proposed. Formation of gaseous H$_2$SO$_4$ from Eq. (2.3) is favored when the temperature decreases further. This happens very close to the cylinder wall, where a high temperature difference is present between the cylinder temperature and the cylinder liner temperature. It is also in this narrow segment that H$_2$SO$_4$ condenses either as concentrated acid or diluted acid in water.

Because it is impossible to track the formation rate of SO$_3$ and H$_2$SO$_4$ practically during an expansion stroke, due to for instance the moving piston, the short residence time, etc., various models have been developed to describe this. However, SO$_2$ to SO$_3$ conversion degrees have been measured experimentally in the exhaust. Investigation of formation of gaseous SO$_3$ and H$_2$SO$_4$ in the combustion chamber under large, two-stroke marine diesel engine conditions is scanty in the literature. Van Helden et al. modeled corrosive wear due to H$_2$SO$_4$ on the liners, however, they assumed that all fuel sulfur was initially present as SO$_2$ and that 5% of the SO$_2$ was immediately converted to SO$_3$, i.e., no realistic evolution of the sulfur species was considered during the expansion stroke. Further, the developed model completely neglects condensation of H$_2$SO$_4$. The first numerical model considering the realistic formation of SO$_3$ and H$_2$SO$_4$ during cylinder
expansion under large two-stroke marine diesel engine conditions was developed by Cordtz et al.\(^6,7,12\) They derived a 0D multizone model which was able to predict realistic SO\(_2\) to SO\(_3\) conversion degrees. However, detailed information about temperature and combustion product distributions was absent. To provide a more detailed insight into the in-cylinder events happening during the expansion stroke, Pang et al. recently performed 3D Computational Fluid Dynamics (CFD) simulations.\(^5\) They developed a skeletal hydrocarbon/sulfur reaction mechanism, reducing the SO\(_x\) mechanism from 18 species and 98 reactions\(^8\) down to 4 species and 5 reactions. Kinetics of the H\(_2\)SO\(_4\) formation reaction, Eq. (2.3), was taken from Reiner and Arnold.\(^{13}\) The simulations were based on the conditions and dimensions of the MAN Energy Solutions 4T50ME-X research engine. The simulated SO\(_2\) to SO\(_3\) conversions under low load conditions were compared with measurements from engine tests and acceptable agreement was found. The CFD model was able to predict the spatial and temporal evolution of gaseous SO\(_x\) and H\(_2\)SO\(_4\) in the combustion chamber in the range between 0 to 90 CAD ATDC. To better compare the effect of changing operating conditions, the averaged concentrations were calculated as a function of the CAD ATDC. An example is shown in Figure 2.3, where the effect of varying the sulfur content in the fuel was simulated.

Figure 2.3. Temporal evolution of the (a) averaged SO\(_2\) concentration, (b) averaged H\(_2\)SO\(_4\) concentration, (c) averaged SO\(_3\) concentration, and (d) SO\(_2\) to SO\(_3\) conversion for fuel sulfur contents of 0.5 wt.%, 1.0 wt.%, and 2.0 wt.%. The start of injection is at 1.2 CAD ATDC and end of injection is at 23 CAD ATDC for the specific simulations. Also, no water was initially present in the gas phase and the simulations were based on high load conditions.\(^5\)

Figure 2.3 also shows the difference between the full sulfur-hydrocarbon (S-HC) model and the skeletal model. As expected, the averaged concentrations of SO\(_x\) and H\(_2\)SO\(_4\) increase when the sulfur content in the fuel is increased. The SO\(_2\) to SO\(_3\) conversion degree decreases, when more sulfur is present in the fuel. The reason is that more radicals are present relative to the sulfur amount when decreasing the sulfur content in the fuel. Figure 2.3(a) reveals that the formation of SO\(_2\) happens rapidly and is complete at 25 CAD ATDC for the skeletal S-HC model and around 35 CAD ATDC for the full S-HC model. Formation of SO\(_3\) begins shortly after the SO\(_2\) formation, and later (around 20 CAD ATDC), H\(_2\)SO\(_4\) begins to form in the gas phase.
2.2 Sulfur chemistry in the gas phase

This is due to the gradually decreasing temperature in the combustion chamber due to cylinder expansion, gradually favoring formation of SO$_3$ and H$_2$SO$_4$. Therefore, it is expected that formation of gaseous H$_2$SO$_4$ will continue after reaching 90 CAD ATDC and eventually terminate when the exhaust valves open. Pang et al. further observe that H$_2$SO$_4$ is formed very close to the cylinder liner wall where the temperature is low relative to the bulk gas temperature and H$_2$SO$_4$ is mainly formed when the local temperature is less than 600 K. The distance from the wall, where H$_2$SO$_4$ begins to form, increases at increasing CAD ATDC due to the cylinder expansion (lower bulk gas temperature). This behavior is depicted in Figure 2.4, where the local H$_2$SO$_4$ concentration against the distance from the cylinder wall for different CAD ATDC is presented. The local computational cells are grouped, based on the local gas temperature.

![Figure 2.4](attachment:image.png)

**Figure 2.4.** Local H$_2$SO$_4$ concentration against the distance from the cylinder liner wall at (a) 15, (b) 30, (c) 45, and (d) 60 CAD ATDC. The computational cells are grouped, based on the local gas temperature. The cylinder liner wall is fixed at 323 K for the simulations.

Generally, Figure 2.4 shows that the H$_2$SO$_4$ concentration is highest near the cylinder wall where the temperature is low. At 15 CAD ATDC, Figure 2.4(a), H$_2$SO$_4$ is mainly found within 0.1 mm from the cylinder liner wall. During cylinder expansion, the distance, wherein H$_2$SO$_4$ is formed, increases. Further, Pang et al. calculated dew point temperatures, indicating that H$_2$SO$_4$ condensation may already start at around 6 CAD ATDC, i.e., in the very top of the cylinder liner. The study by Pang et al. proves that H$_2$SO$_4$ is present very close to the cylinder liner wall during the expansion stroke and dew point calculations supported that H$_2$SO$_4$ may condense already in the very top of the cylinder. In practice, this is also the region, where the most corrosive wear is found.\(^{14}\)
2 Background

2.3 Models describing condensation of H$_2$SO$_4$ onto the lube oil film

Gaseous H$_2$SO$_4$ may condense on the cylinder liner wall if the local temperature is lower than the H$_2$SO$_4$ dew point temperature. The dew point temperature of H$_2$SO$_4$ can be determined from a simple empirical formula that is a function of the partial pressure of gaseous water and H$_2$SO$_4$. The formula predicts a high dependence on the H$_2$SO$_4$ concentration in the gas phase. Taking into account specific engine conditions, Hengeveld et al. predicted H$_2$SO$_4$ dew point temperatures as high as 553 K when combusting 3.5 wt.% sulfur fuel and having a pressure of 180 bar in the cylinder. For typical practical engine operating conditions and burning sulfur-rich fuels, the temperature of the cylinder liner is typically below the theoretically determined H$_2$SO$_4$ dew point temperatures, thereby promoting the likelihood of H$_2$SO$_4$ condensation throughout the whole vertical direction of the cylinder liner. The concentration of the condensing H$_2$SO$_4$ (diluted in water) depends on how far the cylinder liner temperature is from the dew point temperature of pure water. If below, highly diluted H$_2$SO$_4$ may condense. However, such correlations are based on fully equilibrated systems, which may be far from accurate in an engine application where conditions are extremely dynamic. Therefore, to predict realistic condensation rates of H$_2$SO$_4$ onto cylinder liners, it is important to include the effect of e.g. mixing, residence time, local SO$_3$/H$_2$O/H$_2$SO$_4$ concentrations, and local temperature.

The first study quantifying condensation of H$_2$SO$_4$ in a large two-stroke marine diesel engine application was performed by Cordtz et al. This work expanded on their earlier developed 0D multizone model, by the implementation of a condensation model. The condensation model was based on prediction of dew point temperatures by a two-phase vapor-liquid equilibrium (VLE) model combined with a coupled mass and heat transfer model assuming a homogenous gas phase in the cylinder. The model applies a calibrated mixing factor to adapt the effect of mixing between the fresh air and combustion products on the condensation. Further, the model involves a realistic cylinder liner temperature profile under low load operation. Simulations quantify total H$_2$SO$_4$ condensation profiles along the vertical direction of the cylinder liner at EVO (Exhaust Valve Opening). The simulations revealed that a few milligrams of H$_2$SO$_4$ are condensing during one expansion stroke until reaching EVO, e.g., 2 mg H$_2$SO$_4$ condenses at 4 wt.% sulfur in the fuel. The model predicts that condensation of H$_2$SO$_4$ increases for increasing sulfur content in the fuel and for increasing mixing between the combustion products and intake air. Most of the H$_2$SO$_4$ and water condense in the upper segment of the cylinder liner. While simulated water condensation revealed high dependence on cylinder liner temperature and humidity of the intake air, the effect was negligible on the H$_2$SO$_4$ condensation. This means that highly diluted aqueous H$_2$SO$_4$ may condense in the upper part of the cylinder liner for a liner temperature profile in the lower range and for humidified intake air.

The lack of information regarding the spatial distribution of the condensation of H$_2$SO$_4$ and water and taking into account a realistic flow pattern with a heterogeneous gas phase, substantiated the work of Karvounis et al. Their work originated and expanded the 3D CFD work performed by Pang et al. (described shortly in the section above) by including the condensation process. Their condensation model was validated against experimental data concerning condensation of H$_2$SO$_4$ and water in a laminar pipe. Their CFD model offers assessment of the spatial and temporal evolution of H$_2$SO$_4$ and water condensation at the cylinder liners during the expansion stroke. An example of such an evolution is illustrated in Figure 2.5, where the spatial mass fractions of liquid H$_2$SO$_4$ and water in the unwrapped cylinder liner are shown at different CAD ATDC for a high load baseline case. Figure 2.5 reveals that both H$_2$SO$_4$ and water condense primarily around TDC.
and that condensation of H₂SO₄ starts early in the combustion cycle, already around 15 CAD ATDC (Figure 2.5(b)), which is in agreement with the study by Cordtz et al. In addition, the figure illustrates that the distribution of condensed H₂SO₄ and water varies quite a lot along the vertical direction of the cylinder liner wall, but also along the horizontal direction due to the complex behavior prevailing inside the combustion chamber.

**Figure 2.5.** Mass fractions of liquid H₂SO₄ (left column) and water (right column) in the unwrapped cylinder liner lube oil film at (a) 10, (b) 15, (c) 20, (d) 25, (e) 30, (f) 35, (g) 40, (h) 45, (i) 50, and (j) 90 CAD ATDC. The simulations are carried out at specific baseline conditions: liner temperature = 323 K, sulfur in fuel = 2 wt.%, initial water content in gas phase = 0.5 wt.%, initial pressure = 152 bar, initial gas temperature = 924 K, engine speed = 123 rpm, and injected fuel mass = 44.6 g.
Karvounis et al. also performed a parametric study, to investigate the effect of different operating conditions on the total condensed mass of H$_2$SO$_4$ and water at 90 CAD ATDC. This analysis yielded that increasing the sulfur content in the fuel, increased the total condensed mass of H$_2$SO$_4$, whereas the total condensed mass of water was unaffected. Increasing the humidity of the scavenge air, significantly increased condensation of water, whereas the effect on H$_2$SO$_4$ was not as pronounced. Increasing the cylinder liner temperature from 323 K to 523 K, resulted in a slight decrease in total condensed H$_2$SO$_4$, however, almost no water was condensing at 523 K. This is due to the wall temperature is far above the dew point temperature of water and just below the dew point temperature of H$_2$SO$_4$. The above observations are in general agreement with the work by Cordtz et al.\textsuperscript{12} Increasing the lube oil film thickness decreased both the H$_2$SO$_4$ and water condensation with a higher dependence on condensation of water. For a low load case, the total condensed amount of H$_2$SO$_4$ and water decreased (29\% and 15\%, respectively, compared to the high load case). However, for the low load case, the injected fuel amount was reduced by around 50\% which also halves the total amount of sulfur species present in the gas phase. The percentage of initial sulfur from the fuel ending up as condensed H$_2$SO$_4$ is therefore increased when decreasing the load. This is due to a lower piston velocity at low load which gives more time for condensation to happen. Lastly, the effect of initial pressure revealed a counter-intuitive behavior, where condensation of H$_2$SO$_4$ and water decreased at increasing pressure. However, this was attributed to the change in resulting flame size and flow in the cylinder.

The above section highlighted that condensation of H$_2$SO$_4$ and H$_2$O onto the lube oil film in an engine application is a complex phenomenon which depends on the dimensions and operating conditions of the specific engine such as cylinder liner temperature, cylinder pressure, local H$_2$O/SO$_3$/H$_2$SO$_4$ concentrations, and the time available under favorable condensation conditions. To hamper contact between H$_2$SO$_4$ and the cylinder liner material, the liner wall is lubricated with cylinder lube oil.

### 2.4 Lube oil formulation

The specific lube oil formulation should be able to uphold sufficient performance even though it is present in a very hostile environment, as outlined above. The main purposes of the formation of a lube oil film at the cylinder liner are the following:\textsuperscript{2,19}

- Prevention of metal-metal contact between the cylinder liner and piston rings by spreading uniformly over the cylinder liner surface and forming a stable lube oil film.
- Prevent combustion gas from escaping to maintain the predefined internal pressure by providing a gas seal between the piston rings and cylinder liner.
- Neutralize the condensing H$_2$SO$_4$ to limit corrosion.
- Clean the cylinder liner and piston rings by the accumulation of combustion and neutralization products.

Fully formulated lube oils are therefore a complex formulation containing a lot of different components. The cylinder lube oils are based on a base oil where a specific additive package has been incorporated. For slow speed engines, paraffinic base oil is used because it has a good oxidation resistance, good thermal stability, low volatility, good demulsibility (prone to water contamination), and a high viscosity index (low change in viscosity with temperature).\textsuperscript{20} The choice of the correct additive package is crucial to achieving a high performing lube oil which sufficiently fulfills the above-mentioned purposes. The additive package consists
of various components, each of them having specific properties and functions. The main types with the corresponding function are outlined below with a detailed focus on the detergents.\textsuperscript{21,22}

### 2.4.1 Detergents

The function of the detergents is two-fold: (1) to suspend unwanted products which would otherwise deposit in the engine (called neutral detergents or soaps) and (2) supply the oil with alkalinity (called alkaline or overbased detergents) which can neutralize the condensing acids, mainly $H_2SO_4$, to prevent corrosion. The overbased detergents are simply neutral detergent complexes which surround and suspend alkaline particles in the oil, leading to large excess of alkalinity or base of the complex (thereof the term “overbased”).\textsuperscript{21,23} The structure of overbased detergents in lube oils are in the form of reverse micelles,\textsuperscript{24-27} illustrated in Figure 2.6. Here, the neutral detergents consist of a hydrophilic head which is attached to a hydrophobic hydrocarbon tail (e.g. an alkyl). Typical components of the head group are sulfonates, phenates, and carboxylates with typically calcium as the counterion.\textsuperscript{21,24,28} Based on molecular dynamics simulations of an overbased $CaCO_3$/calcium sulfonate reverse micelle, Tobias and Klein found that it is roughly spherical with an average diameter of the $CaCO_3$ core of 2.3 nm and a surfactant thickness of 0.9 nm, giving a total diameter of 4.1 nm.\textsuperscript{24} Hudson et al.\textsuperscript{29} reported core diameters of 1-10 nm and surfactant thicknesses of 1-5 nm, which gives total diameters of 3-20 nm. The detergents incorporating $CaCO_3$ are the most widely used\textsuperscript{21} and the concentration of $CaCO_3$ in lube oil is also known as the base number, BN. The BN is defined as “the quantity of acid, expressed in terms of the equivalent number of milligrams of KOH required to neutralize all alkaline constituents in a one gram sample”.\textsuperscript{30}

![Figure 2.6. Representation of an overbased detergent reverse micelle.](image)

### 2.4.2 Dispersants

Ashless dispersants have the same effect and structure as neutral detergents. They are used to clean the engine by solubilizing products, e.g. soot from the combustion, which would otherwise precipitate and possibly act as abrasive particles or disrupt the coherent lube oil film. A common component used for marine applications are of the type polyisobutylene-succinimide.\textsuperscript{21}
2.4.3 Antioxidants
The antioxidants prevent oxidation, i.e. degradation, of the oil. This could otherwise result in the formation of acids (thereby corrosion or unnecessary consumption of BN), increased viscosity of the lube oil (increased friction between sliding parts, thus increased wear), or formation of insoluble products (such as abrasive particles, leading to increased wear). Commonly, phenols, amines, dithiophosphate, and dithiocarbamates can be included in the lube oil formulations.

2.4.4 Corrosion inhibitors
The way of combating corrosion has already been outlined, however, (additional) additives are added to prevent rusting of the cast iron cylinder liners. These include neutral alkyl sulfonates, fosfates, amines, and alkyl succinic acids/esters. They have the function of forming a hydrophobic film on the liner surface to prevent water-metal contact, which eventually could lead to rusting.

2.4.5 Anti-wear and extreme pressure additives
These are used to form a film on the highly loaded metal surface to prevent metal-metal contact, thereby limiting wear. Also, if the normal hydrodynamic lube oil film breaks down under high pressure and temperature. Commonly used additives for this purpose are: zinc dithiophosphates, dithiocarbamates (also used as antioxidants), sulfurized fatty acids, disulfides, and sulfurized alkenes.

2.4.6 Pour-point depressants
Pour point is defined as the lowest temperature at which a lube oil will flow under specified conditions, i.e., defines the lowest temperature at which the lube oil is suitable. The paraffinic base oil contains waxes, which at low temperature start to crystallize and agglomerate, which impede the oil flow. The additives help to lower the pour point by modifying the wax crystal structure in the paraffinic base oil, preventing the waxes to precipitate out of solution at low temperature. The additives are commonly polyalkylmethacrylates, alkyl naphthalenes, and alkylated wax.

2.4.7 Anti-foam additives
The formation of foam in the lube oil film is undesirable because it among others hampers the lubrication and promotes oxidation of the lube oil. Common additives are silicone based oil insoluble additives which function by lowering of the surface tension of the foam bubbles to accelerate their collapse.

2.4.8 Viscosity index improvers
To ensure optimal lubrication, the establishment of a so-called hydrodynamic lube oil film (from the Strieber curve) between the piston rings and cylinder liner is essential. A hydrodynamic lube oil film is characterized by complete separation between the two sliding surfaces resulting in low friction and minimal wear. The viscosity of the lube oil is an important parameter to achieve and maintain the hydrodynamic film. This is a complicated matter because the viscosity of oil significantly changes with temperature. During engine start-up, the temperature is low and the viscosity is thereby high – and vice versa when the engine has been running for some time. Viscosity index improvers are therefore added to reduce the viscosity.
at low temperatures and increase the viscosity at high temperatures. Typical viscosity index improvers are polymethacrylates, olefin copolymers, styrene-diene copolymers, and styrene-ester copolymers.\textsuperscript{34} A typical viscosity grade of a cylinder lube oil is SAE50, having typical kinematic viscosities of $2.18 \times 10^{-4}$ m$^2$ s$^{-1}$ at 40 $^\circ$C and $1.9 \times 10^{-5}$ m$^2$ s$^{-1}$ at 100 $^\circ$C.\textsuperscript{21}

2.5 The lube oil film environment

The present section shortly describes the environment of the lube oil film on the cylinder liner surface, specifically the temperature of the cylinder liner surface, the surrounding pressure, the lube oil thickness, the lube oil consumption, and the residence time of the lube oil in the engine. The lube oil used for a two-stroke marine diesel engine is not recycled and is supplied once into the piston ring pack every third to eighth revolution when the piston approaches TDC.\textsuperscript{35} The lube oil is then moved up and down by the movement of the piston and becomes depleted by drainage in the lower part of the cylinder (the used oil is called drain oil).\textsuperscript{36} The piston rings help to spread the lube oil throughout the vertical direction of the cylinder liner. Figure 2.7 shows a close-up of the cylinder liner-piston ring package environment. The lube oil is contained in the orifice between the cylinder liner surface and the end of the piston rings. The figure also illustrates the secondary (horizontal) movement of the piston, besides the primary (vertical) movement.

\textbf{Figure 2.7.} A close-up illustration of the cylinder liner surface-piston rings environment.\textsuperscript{37}
2.5.1 Cylinder liner surface temperature and surrounding pressure

The cylinder pressure depends on the location of the piston during the combustion cycle. As stated earlier, the pressure has increased in recent years because of new engine designs and tunings to reduce the fuel consumption. This has reduced the maximum operating pressure gap between low and high load significantly.\textsuperscript{17} It is reported that the maximum operating pressure can be as high as 200 bar, which occurs just after the fuel injection.\textsuperscript{2,17,35} This means that the cylinder pressure is very high during the combustion phase when the piston is near TDC. Due to the rapid pressure evolution, the piston approaches BDC rapidly and the cylinder pressure decreases equivalently. After exhausting of the combustion gas, just prior to the piston approaching TDC again, the pressure is at its lowest which can be in the range of 10 bar.\textsuperscript{11} With respect to the temperature, this is very dependent on the specific design of the engine and operating conditions.\textsuperscript{17} The temperature is highest near TDC and lowest near BDC. The cylinder liner temperature is indeed highly dependent on the load. At high load, the cylinder wall temperature can be as high as 280 °C near TDC and 180 °C near BDC. At low load, the temperature at TDC can be in the range 150 °C and around 100 °C at BDC.\textsuperscript{3,12,17,38}

2.5.2 Lube oil film thickness

The lube oil film thickness is mainly dependent on the viscosity, piston speed, geometry, and contact load between cylinder liner and piston ring.\textsuperscript{32} Practically, the lube oil film thickness varies along the vertical direction of the cylinder liner, lowest near TDC,\textsuperscript{39} having a minimum thickness in this upper part between 2-5 µm. At higher piston speeds, the thickness increases to around 10-12 µm.\textsuperscript{40} Christiansen et al.\textsuperscript{39} performed simulations showing that the oil film thickness can be as high as 45 µm. Recently, Ayranci and Akalin\textsuperscript{41} used a reciprocating bench test rig to investigate the lube oil film thickness by use of laser-induced fluorescence (LIF) method. They found that high sliding speed and viscosity increases the lubrication whereas an increased load had the opposite effect, leading to metal-metal contact. Lube oil film thicknesses up to 20 µm were measured.\textsuperscript{41}

2.5.3 Lube oil dosage

The lube oil is fed through so-called quills (bores) to uniformly distribute the lube oil film around the liner circumference.\textsuperscript{3} The feed rate of the lube oil to the engine is primarily determined from the sulfur content in the fuel and a factor, called ACC factor with unit g/(kWh-wt.%S). Running on a 100 BN lube oil, the optimal ACC factor should be between 0.2 and 0.4 g/(kWh-wt.%S) and not take a value under 0.6 g/kWh. g/(kWh-wt.%S) (valid for newer engines).\textsuperscript{42} The feed rate in grams per hour can then be calculated by multiplying the ACC factor with the sulfur content in the fuel and the produced energy of the engine (in kW). It is recommended that the lube oil feed rate is initially based on a high value of the ACC factor and is then gradually reduced until reaching an optimal lube oil feed rate with respect to minimal lube oil consumption and wear.\textsuperscript{42} The ACC factor (and thereby the feed rate of the lube oil) can be reduced by increasing the BN of the lube oil equivalently.\textsuperscript{3,38}

The optimal lube oil flow rate to the cylinder liner is highly dependent on the specific engine, ambient conditions, operating pattern, lube oil type, injection system, etc.\textsuperscript{3,43} Therefore, it is recommended to perform a so-called cylinder lube feed rate sweep test, to determine the optimal ACC factor, in which the engine is operated for 24 hours on a specific lube oil feed rate followed by analysis of the drain oil. The lube oil feed
rate is hereafter decreased and a new test analysis of the drain oil is performed after 24 hours of operating at
the specific feed rate. The complete test period can be 4 to 6 days and the engine operation must be kept as
constant as possible. The drain oil samples are analyzed for the total content of iron (both corrosive and
abrasive iron) and BN. The optimal feed rate can then be determined by securing that drain oil samples are in
the safe area (denoted 1) of Figure 2.8 when operating on high sulfur fuels. It is recommended that the BN
(corrected for system oil dilution) is between 25 and 50, whereas the total iron content should be no higher
than 200 mg kg⁻¹. If a too low value of BN is observed (2), cold corrosion may be an issue and more BN has
to be supplied either by increasing the feed rate or increasing the BN of the oil. On the other hand, having a
too large BN value (4), liner polishing may develop (explained in section 2.7.1). The lube oil feed rate can
then be reduced or a lower BN oil can be used. Finally, if too much iron is measured in the drain oil sample
(3), it may be due to “cat fines” (worn-down catalyst particles from the fuel oil, see section 2.7.1). Inspection
of the fuel system is then required.

The BN of the drain oil sample can be analyzed on-board by a pressure cell, otherwise, it can be analyzed in
a laboratory by titration or infrared spectroscopy. Different analysis techniques are also available for
measuring iron, both abrasive/adhesive wear (magnetic iron) and wear due to corrosion (non-magnetic).
Besides this, visual inspections of e.g. the cylinder liner and piston rings should be carried out together with
measuring physically the wear of the cylinder liner, piston rings, and piston ring grooves.

Figure 2.8. Interpretation of the drain oil sample analysis: (1) safe area, keep current operating conditions, (2) cold
corrosion, increase lube oil feed rate or switch to a higher BN lube oil, (3) cat fines, inspect fuel centrifuge operation
and cleanliness of the fuel, and (4) liner polishing, reduce the lube oil feed rate or switch to a lower BN lube oil.

2.5.4 Lube oil loss

When balancing the dosage amount of lube oil with the condensing H₂SO₄, it is important to establish
whether there are other mechanisms which can lead to consumption of the lube oil. If this is the case, it has
to be included in the balancing to ensure that sufficient alkaline additives (described in section 2.4.1) are
present at the cylinder liner surface to neutralize the condensing $\text{H}_2\text{SO}_4$. Herbst and Priebsch\textsuperscript{37} stated that lube oil loss from the cylinder liner surface mainly happens by four mechanisms:

- Evaporation from the cylinder liner surface (depends on the temperature, pressure, and velocity of the combustion gas).
- Throw-off of accumulated oil above the top ring (uppermost ring of the piston ring package, depends on piston speed).
- Oil blow through the top ring end into the combustion chamber due to a reverse gas flow, which happens if the pressure in the second piston land exceeds the combustion gas pressure leading to a reversed flow carrying oil droplets.
- Oil scraping of the piston top land edge. During engine operation, the gap between the piston top land and cylinder liner gets rather low (decreases even further by deposit buildup and the secondary movement), possibly leading to direct contact, thus scraping off the lube oil film.

When the lube oil leaves the cylinder liner surface by one of the above mechanisms, it may reach the combustion chamber and thereby being combusted due to the higher temperature there.\textsuperscript{35,36}

2.5.5 Lube oil residence time

The residence time of the lube oil in the engine determines for how long the lube oil should be functional with respect to minimizing wear of the cylinder liners and is an important parameter to consider when studying the neutralization and wear process in an engine. An average lube oil residence time can be derived from the lube oil film thickness, the feed rate, the stroke length, the cylinder liner diameter, and the load, see Figure 2.9.\textsuperscript{14}

![Figure 2.9](image_url)

**Figure 2.9.** Calculated average residence times for a lube oil with an average lube oil thickness of 5 $\mu$m present at a cylinder liner with a diameter of 96 cm and having a stroke of 250 cm. The effect of engine load and lube oil feed rate are also shown in the figure.\textsuperscript{14}
The average lube oil residence time is based on a uniform lube oil film thickness of 5 µm for a 250 cm stroke and 96 cm in diameter engine and is calculated as a function of the engine load and lube oil feed rate. This figure also explains part of the issue with respect to slow steaming (sailing at low load) and the resulting increase in corrosive wear: when e.g. the engine load is reduced from 90 to 30% at a feed rate of 0.8 g/kWh, then the residence time is increased from about 30 to 90 seconds, i.e., a factor of three. This means that the lube oil should be durable for much longer times. In addition, the effect of slow steaming is colder cylinder liner surfaces thus more H2SO4 is possibly condensing on the lube oil film.14,46,47 However, when the load is decreased, the consumption of fuel is also decreased, thus having fewer sulfur species present in the system.

The actual residence time of the lube oil on the cylinder liners is difficult to exactly determine due to the reasons outlined in section 2.5.4, but also due to the highly dynamic environment of the cylinder system augmented by the moving piston. Nevertheless, Doyen et al.48 used a tracer technology to determine the residence time of the lube oil in the research engine of Wärtsilä. A specific amount of tracer was injected at once and the accumulation in the drain was then monitored. They found that a part of the lube oil goes directly to the drain because it is scraped off the cylinder wall rapidly thus not being used for lubrication. Further, the major part of the tracer left the engine within half an hour, but 8-10% stayed in the engine significantly longer. This was attributed to lube oil accumulation in the piston grooves and/or the physical/chemical interactions occurring between the liner wall and lube oil.48

2.6 Neutralization of H2SO4 in cylinder lube oil

When H2SO4 condenses onto the lube oil film, it is crucial that it is neutralized before interacting with the cylinder liner wall, which eventually may result in corrosion of the wall material. For this purpose, the lube oils are formulated with alkaline additives (described in section 2.4.1) to handle the job. However, the amount of alkaline additives in the lube oil formulation (BN) is not necessarily equal to the performance of neutralizing the condensing H2SO4. The BN of a specific lube oil formulation only represents the potential of neutralizing the condensed H2SO4. Comparison of the neutralization rate for different commercial lube oil formulations with the same BN value has been reported in the literature. For instance, Wu et al. reported a factor of more than 2.5 (70 BN lube oils at room temperature) and Roman49 reported a factor of up to 4 (70 BN lube oil at 353 K) between the fastest and slowest neutralization rate for different lube oil formulations having the same BN value.50 Therefore, an increased understanding of how H2SO4 is neutralized by alkaline additives in the lube oil film may pinpoint how to optimize the lube oil formulation optimally to boost the neutralization rate.24 Different investigations with this in mind have therefore been undertaken. Table 2.1 compactly presents a summary of the different research groups which experimentally has investigated the neutralization reaction with the aim of understanding the underlying neutralization mechanism.
Table 2.1. Historical overview of experimental investigations concerning the neutralization mechanism between acid droplets and alkaline additives in lube oil formulations.

<table>
<thead>
<tr>
<th>Research group</th>
<th>Hosonuma and Tamura\textsuperscript{51,52}</th>
<th>Roman\textsuperscript{49}</th>
<th>Hone\textsuperscript{28,53–56}</th>
<th>Papadopoulos\textsuperscript{24,50,57–66}</th>
</tr>
</thead>
<tbody>
<tr>
<td><strong>Temperature (°C)</strong></td>
<td>25-80</td>
<td>80-120</td>
<td>10-30</td>
<td>23-170</td>
</tr>
<tr>
<td><strong>Acid concentration (mol/L)</strong></td>
<td>2.5-12.5 (H\textsubscript{2}SO\textsubscript{4})</td>
<td>Concentrated (H\textsubscript{2}SO\textsubscript{4})</td>
<td>0.1 (HCl and H\textsubscript{2}SO\textsubscript{4})</td>
<td>H\textsubscript{2}SO\textsubscript{4}: 4.7-18 HNO\textsubscript{3}: 4.4-15.6 CH\textsubscript{3}COOH: 4.4-17.4 (Acid diameters: 70-200 µm)</td>
</tr>
<tr>
<td><strong>Molar ratio of base and acid (mol/mol)</strong></td>
<td>1-2</td>
<td>~0.5</td>
<td>~10</td>
<td>&gt;&gt;1 (order of magnitude: 100)</td>
</tr>
<tr>
<td><strong>Oil type and base number (BN)</strong></td>
<td>Diesel engine oil: 90 BN</td>
<td>Fully formulated experimental and commercial lube oils: 30-100 BN</td>
<td>Non-diluted base oil: 300 BN</td>
<td>Model oil: 30-75 BN Commercial cylinder oil: 70 BN Passenger car oil: 13 BN</td>
</tr>
<tr>
<td><strong>Product location</strong></td>
<td>Inside H\textsubscript{2}SO\textsubscript{4} droplets</td>
<td>Solubilized in bulk or precipitates</td>
<td>In acid droplets</td>
<td>At oil/acid interface at oil side, inside acid droplets, inside reverse micelles, and no products observed</td>
</tr>
<tr>
<td><strong>Experimental setup</strong></td>
<td>Stirred batch reactor</td>
<td>Rotating batch reactor to study reaction in a thin oil film</td>
<td>Stopped-flow technique (study microemulsions, acidic droplets ~2 nm in diameter)</td>
<td>Capillary video-microscopy</td>
</tr>
<tr>
<td><strong>Analysis method</strong></td>
<td>Evolved CO\textsubscript{2}</td>
<td>Evolved CO\textsubscript{2}</td>
<td>Spectroscopy by monitoring the pH change</td>
<td>Visually</td>
</tr>
<tr>
<td><strong>Mechanism of importance</strong></td>
<td>Adsorption of CaCO\textsubscript{3} micelles</td>
<td>“Probability of contact”</td>
<td>Base transfer from micelles into acid droplets (not diffusion-controlled)</td>
<td>Adsorption of micelles onto acid droplets</td>
</tr>
<tr>
<td><strong>Factors affecting the reaction rate</strong></td>
<td>H\textsubscript{2}SO\textsubscript{4} droplet size, CaCO\textsubscript{3} micelle size, ashless additives (indirectly)</td>
<td>H\textsubscript{2}SO\textsubscript{4} droplets size, CaCO\textsubscript{3} micelle size, BN, temperature</td>
<td>Temperature, base concentration, the concentration of water droplets, type of solvent (hydrocarbon chain length)</td>
<td>Oil formulation (e.g. concentration of nonionic surfactants and type), temperature, acid droplet size, the likelihood of strong-stick collisions</td>
</tr>
</tbody>
</table>

In the following, the most interesting results from the research groups will be outlined with a focus on describing the different proposed reaction mechanisms and which factors that affect the reaction rate of the neutralization reaction.
2.6 Neutralization of \( \text{H}_2\text{SO}_4 \) in cylinder lube oil

One of the earliest attempts to describe how \( \text{H}_2\text{SO}_4 \) and alkaline additives (also known as overbased detergents) in an oil media react, was proposed by Hosonuma and Tamura in 1984.\(^{51,52}\) In a stirred batch reactor, they investigated the reaction between \( \text{H}_2\text{SO}_4 \) and overbased detergents in a diesel engine lube oil by monitoring the formed \( \text{CO}_2 \) from the reaction and by obtaining micrographs of the reacted lube oils. From the investigations, the neutralization model shown in Figure 2.10 was proposed. The neutralization model highlights that the alkaline additives are present as \( \text{CaCO}_3 \) reverse micelles and that the \( \text{H}_2\text{SO}_4 \) is emulsified into the lube oil and is stabilized by exchangeable surfactants molecules (so-called calcium sulfonate). Further, the \( \text{CaCO}_3 \) reverse micelles adsorb onto the \( \text{H}_2\text{SO}_4 \) droplet interface where the reaction takes place and the reaction product, calcium sulfate (\( \text{CaSO}_4 \)), is located inside the \( \text{H}_2\text{SO}_4 \) droplet. Hosonuma and Tamura found that the reaction rate was increased with a decrease in \( \text{H}_2\text{SO}_4 \) droplet size and an increase in \( \text{CaCO}_3 \) particle size.

![Figure 2.10. Proposed neutralization model for the reaction between emulsified \( \text{H}_2\text{SO}_4 \) and \( \text{CaCO}_3 \) reverse micelles, proposed by Hosonuma and Tamura.\(^{52}\)](image)

Roman\(^{49}\) investigated the neutralization reaction in lube oil by use of a specially designed rotating vessel, wherein excess \( \text{H}_2\text{SO}_4 \) (compared to the molar \( \text{CaCO}_3 \) in the lube oil) was injected to react with the \( \text{CaCO}_3 \) overbased detergent additives in a thin lube oil film of about 100 \( \mu \text{m} \). The pressure evolution from the produced \( \text{CO}_2 \) gas was monitored. This study showed that the neutralization reaction occurs in three stages by observing three different stages of the measured pressure profiles. The first stage is solubilization of \( \text{H}_2\text{SO}_4 \) in the lube oil film, where \( \text{H}_2\text{SO}_4 \) droplets are formed and stabilized by the excess detergent and dispersant molecules. This process was observed by a decrease in pressure and took up to six seconds, depending on the lube oil formulation and temperature. The solubilization time can double between one additive package and another. The second stage is illustrated in Figure 2.11 and deals with the fast reaction between solubilized \( \text{H}_2\text{SO}_4 \) droplets and \( \text{CaCO}_3 \) reverse micelles, observed by a rapid increase in pressure. The neutralization speed depends on the lube oil formulation, temperature, and BN value. As stated above, the magnitude of this stage can vary up to a factor of 4 for lube oils with equal BN but different formulation. Thirdly, when the relative concentration of \( \text{H}_2\text{SO}_4 \) droplets and \( \text{CaCO}_3 \) particles fall below a critical value, the pressure profile reached a plateau, thus the neutralization reaction was significantly reduced or quenched, even if \( \text{H}_2\text{SO}_4 \) droplets were still present. It was explained by reaching a critical number of \( \text{H}_2\text{SO}_4 \) droplets, thus decreasing the reaction rate significantly. This was also observed by Hone et al.,\(^{28}\) who stated that the first 70% of the base particles in the oil is neutralized more rapidly than the last 30% for conditions where all base are neutralized. Roman\(^{49}\) further proposed that the formed \( \text{CaSO}_4 \) from the reaction was solubilized into the bulk by the excess surfactants present in the lube oil, see Figure 2.11. For the temperature range investigated, 80-120 °C, Roman observed that a higher temperature resulted in lowering of the difference
between the neutralization rates of the different lube oil formulations. This behavior was also confirmed by Wu et al.\textsuperscript{57} in the temperature range 25-55 °C. Roman further postulated that the neutralization reaction depends on the “probability of contact”, which is lower at higher dilutions.\textsuperscript{49} Whether this is translated to a diffusion- or adsorption-controlled (or something else) reaction is questionable.

Hone et al.\textsuperscript{28,53–56} used a stopped-flow method to investigate the reaction between nanometer-sized overbased additives and similar-sized acid droplets in model oils by monitoring the pH change, spectrascopically, accompanying the neutralization reaction. They suggested that the reaction between an emulsified acid droplet and an overbased detergent particle proceeds through the mechanism shown in Figure 2.12.
Upon a successful “sticky” collision, the base is transferred from the overbased detergent particle into the aqueous acid core of the droplet where neutralization of the solubilized acid happens. The work by Hone et al. is rather different from the work conducted within the field (see Table 2.1), more specifically with respect to the low acid concentration used (0.1 M) and the small size of the acid droplets (nanometer-sized). Nevertheless, they found that the reaction rate increased for increased overbased additive (i.e., CaCO₃) concentration, increased temperature (investigated in the range 10-30 °C), increased concentration of droplets (for a constant overall acid concentration), and increased hydrocarbon chain length of the solvent. Investigating the temperature dependency of the neutralization reaction, Hone et al. measured an activation energy of 54±2 kJ mol⁻¹ and concluded that the reaction is not diffusion-controlled because these would have activation energies ~20 kJ mol⁻¹.

The reaction between acid droplets and alkaline additives has over the years been extensively investigated using a capillary video-microscopy technique by the research group of Papadopoulos. This technique allows a visual assessment of the shrinking of an acid droplet in an oil phase containing alkaline additives due to the neutralization reaction, specifically to measure the shrinking rate of the injected acid droplet. In their earlier work, the neutralization mechanism shown in Figure 2.13 was proposed. The interface of the much larger acid droplet (S) is shown as a plane in Figure 2.13. The first step (step I) of the mechanism is adsorption (a successful “sticky” collision) of a reverse micelle (M₁) on the acid-oil interface followed by transfer of acid and water into the core of M₁ where the neutralization reaction occurs (step II). The reverse micelle then desorbs (step III) and are now denoted M₂ which contains the reaction products. Another M₁ can then adsorb onto the acid-oil interface to repeat the neutralization mechanism. That the acid is transferred from the acid droplet to the reverse micelle contradicts the proposed base-transfer channel mechanism by Hone et al., where the base was transferred into the acid droplet. In addition, Wu et al. suggested that adsorption of the reverse micelle onto the acid droplet interface was the controlling step in the neutralization mechanism. It was further found that the shrinking rate (proportional to the reaction rate) increased for an increased BN of the lube oil. The reaction rate of acid neutralization was also found to depend on the specific formulation of the commercial lube oil, around a factor of 2.5 was found between the best and worst performing lube oil (with respect to shrinking rate). This is in agreement with the factor of 4 found by Roman.

Figure 2.13. Neutralization mechanism between an acid droplet and an overbased detergent reverse micelle (M₁) proposed by Wu et al.
Later, Fu et al.\textsuperscript{60} observed four different reaction phenomena for the reaction between a H\textsubscript{2}SO\textsubscript{4} droplet and CaCO\textsubscript{3}-containing reverse micelles in different lube oil formulations (both commercial and model oils) in the temperature range 23-170 °C. The four different observations are summarized as: (1) CaSO\textsubscript{4} crystals and CO\textsubscript{2} gas were observed on the oil side of the oil/acid interface of the acid droplets (observed in the temperature range 25-170 °C), (2) crystals and gas bubbles were observed inside the acid droplet (110-170 °C), (3) no crystals, but gas bubbles were observed on the oil side of the acid/oil interface (23-27 °C), and (4) no reaction products were observed, but shrinking of the acid droplet was observed (23-170 °C). The first mentioned observed phenomenon is in agreement with the visual observations of Wu et al.,\textsuperscript{24,50} whereas the second phenomenon agrees with the proposed neutralization mechanism of Hosonuma and Tamura\textsuperscript{52} and Hone et al.\textsuperscript{28} Phenomenon 3 or 4 may explain the proposed mechanism of Roman,\textsuperscript{49} because he suggested that CaSO\textsubscript{4} crystals may solubilize into the bulk oil by the excess surfactants and detergents present in the lube oil formulation. Further, phenomenon 2 and 3 was observed in model oils whereas phenomenon 4 was observed in a commercial lube oil. This may augment that CaSO\textsubscript{4} formation at the oil/acid interface is not a hindrance for the neutralization mechanism in a commercial lube oil formulation, because these contain excess detergents and surfactants to solubilize the formed crystals. The four different observed phenomena were further divided into two types of reactions based on whether crystal formation was visually observed: strong/weak-stick collisions. The mechanism is illustrated in Figure 2.14 and is an extension of the proposed mechanism by Wu et al.\textsuperscript{24,50} The crystal-observed reactions was proposed to consist of a high frequency of strong-stick collisions and the crystal solubilized reaction phenomena were explained to mainly consist of weak-stick collisions. For a strong-stick collision, the rigid structure of the reverse micelle is destroyed and the CaCO\textsubscript{3} is directly exposed to the acid. For a weak-stick collision, the rigid structure of the reverse micelle is maintained, thus neutralization proceeds through the transfer of acid from the acid droplet into the reverse micelle. Fu et al.\textsuperscript{60} also found that crystal-observed reactions were faster than crystal-solubilized reactions (factor of ~2). Thus, the strategy of increasing the neutralization rate is to formulate the lube oils with as many surfactants as possible that enhance strong-stick collisions.\textsuperscript{60}

In another study, Fu et al.\textsuperscript{59} investigated the effect of temperature on the shrinking rate of a H\textsubscript{2}SO\textsubscript{4} droplet in commercial lube oil formulations with a base number (BN) of 70. They were able to track the shrinking of the H\textsubscript{2}SO\textsubscript{4} droplet over time and thereby calculate a shrinking rate. Constructing an Arrhenius plot of the measured temperature dependent shrinking rates, it is possible to calculate an activation energy of 52.8 KJ mol\textsuperscript{-1}, in great accordance with the value of 54±2 KJ mol\textsuperscript{-1} by Hone et al.\textsuperscript{28} Fu et al.\textsuperscript{61} also found that Ostwald ripening (growth of larger droplets at the expense of the smaller ones) could be an issue with respect to prolonging the existence of H\textsubscript{2}SO\textsubscript{4} droplets in a lube oil film by diminishing the interfacial area of the droplets gradually.

Duan et al.\textsuperscript{66} used Fourier Transform Infrared Spectroscopy (FTIR) and Nuclear Magnetic Resonance (NMR) spectroscopy to investigate the reaction between acetic acid and fully formulated passenger-car lube oil (base number of 13.1). Preparation time prior to obtaining the recorded spectra was around 30 seconds for FTIR and 2 min for NMR and included stirring of the batch emulsion. They concluded that the acetic acid was almost neutralized completely and the reaction was instantaneous for the conditions investigated. Besides using FTIR and NMR spectroscopy, video-microscopy was also used. Based on the experiments, they proposed a neutralization mechanism of overbased additives and acetic acid, describing that the reaction takes place at the oil/acid interface as well as in the bulk lube oil by diffusion of acetic acid in the lube oil. This is different from the reaction between overbased additives and H\textsubscript{2}SO\textsubscript{4}, which takes place exclusively at the oil/acid interface due to H\textsubscript{2}SO\textsubscript{4} being insoluble in base oil.\textsuperscript{56}
Figure 2.14. Illustration of the proposed strong/weak-stick collision mechanism by Fu et al.\textsuperscript{60} (a) strong-stick collision, where the base is directly exposed to acid. Here the rigid structure of the reverse micelle is destroyed at the interface, thus resulting in a fast reaction, which may have a chance to nucleate and grow crystals. (b) weak-stick collision, where the rigid structure of the reverse micelle is maintained before it desorbs back into the bulk lube oil. The reaction is dependent on the transfer of acid into the base core of the reverse micelle, thus resulting in a slow reaction and possible inability of nucleating and grow crystals.\textsuperscript{60}

The above described proposed neutralization mechanisms between acid droplets and alkaline reverse micelles have dissimilarities, however, there is a joint consensus that a successful collision between the droplet and reverse micelle is a precursor for the reaction to occur. Wu et al.\textsuperscript{24,50} even report that this may be the limiting step for a successful reaction. Even though the reaction has been investigated at rather different reaction conditions, it seems that the reaction rate is highly dependent on especially the specific lube oil formulation.\textsuperscript{60} However, it was found that the higher the temperature, the lower the difference between lube oils of various formulations.\textsuperscript{49,57,59} This may suggest that the neutralization efficiency of the commercial lube oils is optimized at realistic cylinder liner temperatures (>100 °C\textsuperscript{12}). It has also been indicated that the
reaction between H$_2$SO$_4$ and alkaline additives is diffusion-controlled, having a reaction rate constant equal to $8.4 \times 10^{17} \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}$.\textsuperscript{9,10,67}

2.7 Wear mechanisms

When condensing H$_2$SO$_4$ is not neutralized in the lube oil emulsion immediately (or not fast enough), there is a risk that it reaches and corrodes the internal parts of the cylinder environment, most exposed are the cylinder liner surface and the piston rings. Augmented by the fast movement of the piston, the corroded material may be scraped off. If the material loss rate gets too high (MAN Energy Solutions recommends a maximum wear rate of 0.1 mm/1000 h\textsuperscript{68}), then the cylinder liner and piston rings have to be replaced too often which is costly and time-consuming. Further, if an uncontrollable material loss rate is occurring for an extended period of time, it may eventually result in failure of the engine to operate (by the loss of operating pressure and prevention of formation of a lube oil film), which would be catastrophic. This combination of corrosion and wear (either abrasive or adhesive) is known as corrosive wear (or cold corrosion). These wear types are outlined below:\textsuperscript{3,69}

2.7.1 Abrasive wear

Abrasive wear is occurring when a harder material is rubbing against a softer material, which then leads to a loss of material.\textsuperscript{3,35} Two types of abrasive wear are sketched in Figure 2.15:\textsuperscript{3,35} two-body abrasive wear and three-body abrasive wear.

![Illustration of the two types of abrasive wear: upper, two-body abrasive wear and lower, three-body abrasive wear.\textsuperscript{35}](image.png)

The two-body abrasive wear is when asperities of the harder material rub against/collide the softer material, leading to a material loss. The three-body abrasive wear includes a hard particle embedded between the cylinder liner and piston ring, which then leads to a loss of material.\textsuperscript{70} The hard abrasive particles can originate from various sources, e.g. from the fuel oil (as small, worn down catalysts particles\textsuperscript{71}), the lube oil (calcium deposits), or from scraped off piston material.\textsuperscript{35,72} The latter means that abrasive wear can also be an effect of adhesive wear by the formation of abrasive particle. Abrasive wear may also lead to bore polishing (mirror-like appearance of the cylinder liner surface), e.g. by abrating of the cylinder liner surface.
by calcium deposits (if e.g. over-lubrication occurs). The cylinder liner surface can then not support a lube oil film, which may lead to adhesive wear and consequently scuffing (described next).

2.7.2 Adhesive wear

Adhesive wear is when direct contact is established between the cylinder liner and piston ring because of lack of a lube oil film, leading to local (micro-)welding between the two surfaces. The results of local welding are a loss of material and formation of abrasive particles. The mechanism is sketched in Figure 2.16. The situation of not having a coherent lube oil film may be a result of insufficient lube oil dosage or inadequate cylinder liner surface roughness which then cannot support a lube oil film (the latter may be a result of abrasive wear). When adhesive wear is pronounced on a larger (macroscopic-)scale in the engine, it is commonly known as scuffing.

![Figure 2.16. Illustration of adhesive wear.](image)

2.7.3 Corrosive wear

As stated, corrosive wear (or cold corrosion) is defined as loss of material when there is a combined effect of corrosion and wear (abrasive or adhesive). The cylinder liners are made out of cast iron, which mainly consist of iron. When aqueous H₂SO₄ is present at the cylinder liner surface, iron is dissolved eventually forming iron oxide and iron sulfate mainly, which normally act as a passive layer on top of the cylinder liner surface. However, the formation of a growing layer is continuously scraped off by the moving piston ring; see Figure 2.17(a).

![Figure 2.17. (a) Illustration of the protective oxide layer removal by the piston rings, which exposes the cylinder liner material for continuous corrosion. (b) arbitrary bar chart showing the combined effect of wear and corrosion on the rate of material loss compared to the individual contributions.](image)
Beneath the passive layer is then fresh iron which corrodes rapidly for continuous acid exposure. This means that the protective layer is continuously worn away by the piston rings, contributing to significant wear. The combined effect of wear and corrosion is therefore much higher than the sum of the individual contributions; see Figure 2.17(b).

The electrochemical corrosion of iron by $\text{H}_2\text{SO}_4$ is a rather complex reaction mechanism. The first step is the dissolution of the iron by the dissociated protons from the aqueous acid:

\[
\text{Fe}(s) \rightarrow \text{Fe}^{2+} + 2\text{e}^{-} \quad (2.5)
\]

\[
2\text{H}^+_{(aq)} + 2\text{e}^{-} \rightarrow \text{H}_2(g) \quad (2.6)
\]

The further progress of the reaction mechanism and possible products depends on the local conditions. For instance, Fe$^{2+}$ can combine with the salt of $\text{H}_2\text{SO}_4$, $\text{SO}_4^{2-}$, to form FeSO$_4$. However, if oxygen is present in the water, it is possible that the Fe$^{2+}$ reacts further to Fe$^{3+}$ and thereby Fe$_2$O$_3$, Fe$_3$O$_4$ (known as rust), etc. The resulting corrosion product can be a mixture of these precipitates. In $\text{H}_2\text{SO}_4$-water solutions under static conditions, using a rotating disc electrode, Yahagi found that the corrosion rate of cast iron peaked at around 20 wt.% $\text{H}_2\text{SO}_4$ and was non-existing at very high $\text{H}_2\text{SO}_4$ concentrations (>85 wt.%) at 23°C. At low concentrations, an increase in $\text{H}_2\text{SO}_4$ concentration leads to an increase in corrosion rate. This is valid until a certain point (around 20 wt.% for the study by Yahagi), where the corrosion rate is significantly reduced for an increase in $\text{H}_2\text{SO}_4$ concentration. The reason is that the concentration of water decreases at increasing concentration of $\text{H}_2\text{SO}_4$ in the solution, thus decreasing the concentration of resulting protons, which are used to dissolve the iron. In addition, it is reported that formation of a passive film is pronounced at higher $\text{H}_2\text{SO}_4$ concentrations, which suppresses the dissolution of cast iron by limiting the diffusion of reactive species to and from the iron surface. Rylands and Jenkinson reported that it is the silicon compounds, present in the cast iron, which are mainly responsible for the formation of a protective film on the cast iron surface (iron oxide will also be protective, however). At increased $\text{H}_2\text{SO}_4$ concentration, the silicon-based film would grow more stable and more protective which increases the resistance of cast iron to $\text{H}_2\text{SO}_4$ attack. Stott and Breakell report that it is a hydrated FeSO$_4$ film that forms at the cast iron surface for more concentrated $\text{H}_2\text{SO}_4$ solutions during static corrosion tests (60 vol.% $\text{H}_2\text{SO}_4$ in water).

The reciprocating pin-on-disc laboratory apparatus of Stott and co-workers included the sliding of a pin (made of cast iron piston ring material), with different loads applied, against a disc (different cylinder liner cast irons) submerged in a stirred, temperature-controlled base oil/$\text{H}_2\text{SO}_4$ solution. The effects of varying different operating conditions were examined, including temperature, the load on the pin, acid concentration, surface treatment, and materials. They found that the wear rate increased for an increased temperature of the oil/acid emulsion and attributed this to mainly three things: (1) the viscosity decreases at increased temperature, which increases the metal-to-metal contact during sliding, (2) the dissolution rate of the iron increases with increasing temperature, and (3) the solubility of the protective corrosion products film increases at increased temperature. Varying the roughness of the discs revealed that low wear was found for very smooth and very rough surfaces while the intermediate surface finish showed high wear. This was explained by very rough surfaces develop a protective film easily and very smooth surfaces develop an oil film easily. When increasing the applied load on the pin, it was found that the total wear increased significantly, in agreement with the study by Yahagi. However, the absolute value was higher for a more
diluted H$_2$SO$_4$ in the oil emulsion (10 vol.% acid in oil with acid concentrations of 10 and 40 vol.% in water). This was attributed to the formation of an adherent, wear-protective corrosion product film at the more concentrated acid, which prevented metal to metal contact. Increasing the volume percentage of acid solution in oil (up to 40 vol.% acid in oil with the concentration of the acid in water of 10 vol.%) increased the total wear significantly. The reason was that increased acid content in the oil emulsion disrupted the oil film, enhancing the metal-metal contact and also the formation rate of the electrochemical products which then were removed rapidly away from the disc surface by the sliding pin. When the acid in oil volume was 20 vol.%, the wear rates increased with increasing acid in water concentration. For 40 vol.% of acid in oil, the wear rates were very high and were reasonable independent of the acid in water concentration. This was explained by disruption of the oil film, leading to long periods of metal-met... 

Amblard presented results from corrosion experiments performed by submerging an iron plate into a stirred and heated lube oil volume followed by continuous H$_2$SO$_4$ addition by a syringe. The amount of total H$_2$SO$_4$ added over 1.5 hours corresponded to 90% conversion of the base number of the commercial lube oil. By measuring the weight loss of the iron plate, it was found that maximum corrosion (highest weight loss) occurred when using a 50% H$_2$SO$_4$ solution at 60 $^\circ$C (investigated in the range 0-95% H$_2$SO$_4$, it is not stated whether this is weight or volume percent, however). Amblard attributed this to water having a shielding effect which reduces the contact between H$_2$SO$_4$ and the alkaline additives at low H$_2$SO$_4$ concentrations. At higher H$_2$SO$_4$ concentrations, the reaction between H$_2$SO$_4$ and the alkaline additives was so fast that the interaction between H$_2$SO$_4$ and iron was minimized. The effect of temperature was investigated in the interval 40-100 $^\circ$C, yielding that the highest wear occurred at 70 $^\circ$C. Above this temperature, water began to evaporate thereby limiting the effect of H$_2$SO$_4$. The dosage rate of H$_2$SO$_4$ had no effect on the total mean weight loss, but the foam formation was increased. This could be an issue in practice because severe foam formation could disrupt the coherent lube oil film on the cylinder liner promoting corrosion. The effect of using nitric acid and carboxylic acid instead of H$_2$SO$_4$ showed that these are minor contributors to corrosion compared to H$_2$SO$_4$.

2.8 The role of SO$_2$ in a diesel engine

So far, the above sections (and the relevant literature in general) have mainly been focused on how H$_2$SO$_4$ condenses onto the cylinder liner wall, how it reacts with the alkaline additives present in the lube oil film, and how H$_2$SO$_4$ reacts with the cast iron liner wall and affects corrosive wear. However, Figure 2.3 showed that SO$_2$ is in vast excess in the combustion chamber compared to SO$_3$ and H$_2$SO$_4$, around a factor of 20. Actually, it has been reported that SO$_2$ can be in molar excess compared to SO$_3$/H$_2$SO$_4$ by a factor in the range 10-40. For the SO$_2$ to reach the bulk lube oil film, it has to be absorbed by the lube oil itself or by the condensing water droplets. Even though sulfur-induced corrosive wear has mainly been attributed to
some research studies advocate that SO\textsubscript{2} can also contribute to CaCO\textsubscript{3} consumption and corrosive wear. These will be outlined below.

Nagaki and Korematsu\textsuperscript{87–89} investigated the effect of EGR (Exhaust Gas Recirculation, i.e., recirculation a part of the exhaust gas into the combustion chamber, mainly done to reduce the combustion temperature and thereby reducing the formation of NO\textsubscript{x}\textsuperscript{3,90}) on the wear rate of the piston rings and cylinder liner. By recirculating a part of the gas, the SO\textsubscript{2} concentration in the combustion chamber is increased (nowadays, an internal scrubber is normally fitted together with EGR\textsuperscript{3}). It was done by model simulations, but also experiments where both an actual exhaust gas was recirculated and by adding SO\textsubscript{2} to the intake air. Experiments, carried out in a single-cylinder four-stroke diesel engine, revealed that increasing the EGR rate and the SO\textsubscript{2} addition to the intake air increased the wear of the piston rings and cylinder liner. Nagaki and Korematsu advocated that the main cause of increased wear was related to the absorption of SO\textsubscript{2} in the lube oil. It proceeded through the following three steps: (1) SO\textsubscript{2} is absorbed by the lube oil film, (2) SO\textsubscript{2} forms H\textsubscript{2}SO\textsubscript{4} and sulfates (e.g. CaSO\textsubscript{4}) in the lube oil film, (3) these cause wear on the piston rings and cylinder liner. The increase in SO\textsubscript{4}\textsuperscript{2-} concentration was also measured after 50 hours of operation (the lube oil is recirculated to the engine), showing no additional increase by adding SO\textsubscript{2} to the intake air, but more wear was measured.\textsuperscript{89} This means that the alkaline additives were not consumed in an observable degree when adding SO\textsubscript{2} to the intake air, possibly contradicting the hypothesis that SO\textsubscript{2} reacts to H\textsubscript{2}SO\textsubscript{4} or directly with the CaCO\textsubscript{3} to form CaSO\textsubscript{4}.

Naegeli and Marbach\textsuperscript{73} also investigated the effect of SO\textsubscript{2} on wear in laboratory engine setups. They found that less than 1\% of the SO\textsubscript{2} was converted to H\textsubscript{2}SO\textsubscript{4}, and concluded that H\textsubscript{2}SO\textsubscript{4} is unimportant with respect to the measured wear. They performed engine experiments, where sulfur was added in the fuel or as SO\textsubscript{2} in the intake air. It was concluded that the resulting corrosive wear was due to the formation of sulfurous acid (H\textsubscript{2}SO\textsubscript{3}) in the lube oil film which reacts with the cylinder liner wall (possibly also with the alkaline additives). Further, the effect of placing iron in aqueous solutions of SO\textsubscript{2} was investigated, yielding that the resulting corrosion product appeared to be a mixture of FeS, FeO, and Fe\textsubscript{2}O\textsubscript{3}. The following overall reaction was therefore suggested to happen:\textsuperscript{73}

\[
\text{SO}_2(aq) + 2\text{H}_2\text{O}(aq) + 3\text{Fe}(s) \rightarrow \text{FeS}(s) + 2\text{Fe(OH)}_2(s)
\]  
(2.7)

Based on their study, they concluded that SO\textsubscript{2} is the principal cause of fuel sulfur-induced wear and deposit formation in diesel engines, which complements the conclusions of Nagaki and Korematsu and may explain why an increase in SO\textsubscript{4}\textsuperscript{2-} concentration was not observed in their study.

From other research fields, it is found that SO\textsubscript{2} do react with CaCO\textsubscript{3} and iron. For instance, CaCO\textsubscript{3} is used to capture gaseous SO\textsubscript{2} in wet flue gas desulfurization (FGD) plants. The SO\textsubscript{2} is scrubbed from the flue gas by reacting with CaCO\textsubscript{3} in an aqueous slurry by the following reactions:\textsuperscript{91,92}

\[
\text{SO}_2 + \text{H}_2\text{O} \rightarrow \text{H}^+ + \text{HSO}_3^-
\]  
(2.8)

\[
\text{HSO}_3^- \rightarrow \text{H}^+ + \text{SO}_3^{2-}
\]  
(2.9)

\[
2\text{HSO}_3^- + \text{O}_2 \rightarrow 2\text{H}^+ + 2\text{SO}_4^{2-}
\]  
(2.10)

\[
\text{Ca}^{2+} + \text{SO}_4^{2-} + 2\text{H}_2\text{O} \rightarrow \text{CaSO}_4 \cdot 2\text{H}_2\text{O}(s)
\]  
(2.11)
If the system is not saturated in O$_2$, the formation of CaSO$_3$ may happen:

$$\text{Ca}^{2+} + \text{SO}_3^{2-} + 1/2 \text{H}_2\text{O} \rightarrow \text{CaSO}_3 \cdot 1/2 \text{H}_2\text{O} \text{(s)}$$

(2.12)

If dissolved iron is present from Eq. (2.5), FeSO$_3$/FeSO$_4$ may be possible corrosion products from Eqs. (2.8)-(2.12). Also, the reaction between humid SO$_2$ and CaCO$_3$ particles has been investigated (23-80 °C), finding that CaSO$_3$ and CaSO$_4$ were formed. This shows that it is possible for CaCO$_3$ (in aqueous systems) to react with SO$_2$, forming CaSO$_3$ and/or CaSO$_4$. Absorption data of SO$_2$ in lube oil and water even confirms that it is possible for SO$_2$ to be present in the lube oil film emulsion (lube oil + water).

With respect to the reaction between iron and aqueous SO$_2$, different studies, besides the study by Naegeli and Marbach, have been carried out. These find that aqueous SO$_2$ do react with iron to form corrosion products, such as FeSO$_3$, FeSO$_4$, and FeS, by different proposed reaction mechanisms. It is also found that FeSO$_4$ can react with water and oxygen to produce FeOOH and H$_2$SO$_4$. Thereby, H$_2$SO$_4$ is formed and can either react with the iron or the alkaline additives. Also, Fishman et al. found that saturating a 35% H$_2$SO$_4$ solution with SO$_2$ increased the corrosion rate significantly (a factor of “several tens”) compared to the case with no SO$_2$ in the H$_2$SO$_4$ solution.

To sum up this section, it was outlined that increased wear in laboratory diesel engines was observed when increasing the concentration of SO$_2$ in the combustion chamber. However, no increase of SO$_4^{2-}$ was found, which may be due to the formation of corrosive H$_2$SO$_3$ (aqueous SO$_2$), which may also react with CaCO$_3$ to form CaSO$_3$. From other research fields, it is found that SO$_2$ and CaCO$_3$ do react and the same is valid for aqueous SO$_2$ and iron.

### 2.9 Practical cases on how to mitigate cold corrosion

Significant attention has been given to the solution of the cold corrosion issue. This has mainly been done by implementing various countermeasures such as decreasing the scavenge air temperature (to minimize the amount of water vapor entering the cylinder). A very important step toward increasing the control of cold corrosion, has been the introduction of 100 BN lube oil (and 140 BN). In the following, a practical case will be presented which shows the effect on the iron and BN content in the drain oil by changing the BN of the lube oil and the feed rate. Other practical cases can be also be found in the reference.

Figure 2.18 shows the results of a sweep test performed on-board where half the engine was lubricated with 70 BN lube oil and the other half with 100 BN lube oil. The sulfur content in the fuel was 3% and the engine load was between 38-52% (but mostly at 39%). The figure shows both the measured iron concentration (mg/kg) and the BN in the drain oil samples at varying ACC factor. The figure reveals that for the 70 BN lube oil, an ACC factor larger than 0.31 g/(kWh·wt.%S) is needed to achieve an iron content lower than 200 mg/kg and a BN value larger than 20. For the 100 BN lube oil, an ACC factor of 0.20 g/(kWh·wt.%S) easily handles the limits. Thus the lube oil consumption can be reduced by approximately 35% and still achieve better protection. It is also shown that there is around 30 BN in difference between the two different lube oils for the same ACC factor (e.g. at 0.25 g/(kWh·wt.%S)), but the iron content is significantly decreased. This may mean that most of the corrosion is happening at a local spot on the cylinder liner where all the BN has been depleted with the 70 BN lube oil. Using the 100 BN lube oil then gives more protection in this exposed area, which decreases the corrosive wear significantly.
Corrosive wear can also be reduced significantly by increasing the temperature of the cylinder liner surfaces, thereby decreasing the H$_2$SO$_4$ condensation rate. The corrosive wear can also be decreased by optimizing the spatial lubrication. For instance, Jensen reported that the maximum wear was decreased when injecting the lube oil 1/8 from TDC instead of 1/3 from TDC, but the average wear rate was more or less unaffected. Because the durability of the cylinder liner is determined from the maximum wear (0.1 mm/1000 h), the reduction in maximum wear rate increases the lifetime of the cylinder liners. Because most wear is observed near TDC, the results of Jensen may mean that it is due to starvation of BN at TDC and a way to decrease the wear is to supply more lube oil (BN) in the upper part of the cylinder liner. How to reduce wear is a very complex situation and a lot of different measures can be taken. This section only illustrated a handful of different approaches.

2.10 Concluding remarks

To better understand the very complex and dynamic environment prevailing inside a large two-stroke marine diesel engine, the different sub-processes occurring, concerning the sulfur-induced corrosive wear, needs to be studied separately. This literature review has focused on experimental and theoretical studies on the different sub-processes from the formation of sulfur oxides in the gas phase to the governing wear reactions on the cast iron with the focus on the components SO$_2$ and H$_2$SO$_4$.

The formation of the sulfur oxides (SO$_x$) in the gas phase and subsequent formation and condensation of H$_2$SO$_4$ during the combustion stroke has been quantified through 3D CFD modeling by which it is possible to quantify the effect of changed operating conditions on the condensation of H$_2$SO$_4$ on the cylinder liner surface. The condensation of H$_2$SO$_4$ is mainly dependent on the pressure in the cylinder, the cylinder liner surface temperature, the sulfur content in the fuel, and the amount of water present. The formation and
condensation of H₂SO₄ may happen immediately upon each other due to the small distance from the wall where H₂SO₄ is formed. The alkaline additives in the lube oil (mainly CaCO₃ reverse micelles) have the job of neutralizing the condensing H₂SO₄. The lube oil is a complex formulation of many components, each of which has a very specific task in the hostile environment on the cylinder liner surface. The reaction between H₂SO₄ and CaCO₃ has been investigated separately and various reaction mechanisms have been proposed in the literature. It is suggested that the reaction may be adsorption-/diffusion-controlled; however, quantification of the reaction is lacking which hinders quantification of the conversion degree at specific conditions. The reaction between H₂SO₄ and cast iron has been investigated in various laboratory setups, both with and without base oil. Generally, a higher H₂SO₄ concentration leads to increased corrosion and water has to be present in order to dissociate the H₂SO₄ sufficiently. However, when the H₂SO₄ concentration is high, a protective layer may be formed rapidly which hampers the further corrosion process. Nevertheless, the sliding motion of a piston ring may gradually remove the formed protective layer and facilitate further corrosion. Even though it was found that a high concentration of H₂SO₄ forms a wear-resistant protective corrosion product layer, the load in a real engine may be large enough to scrape off the layer. This would lead to a substantial wear rate of the cylinder liner and piston rings. Also, when a large fraction of H₂SO₄/water is condensing, it would increase the metal-metal contact between the piston ring and cylinder liner surface thus increase the wear rate. The role of SO₂ on consumption of CaCO₃ reverse micelles is presently also not clear. However, the SO₂ is greatly present close to the lube oil film and it is known from other research fields that SO₂ indeed do react with CaCO₃. From practice, it is found that the most severe corrosion is happening near TDC, this is in general agreement with the CFD simulations which showed that most of the water and H₂SO₄ are condensing in this upper region. This may lead to a molar excess of H₂SO₄ compared to CaCO₃ reverse micelles and H₂SO₄ can thereby react with the cast iron liner. With the high load of water also condensing near TDC, this further augments the corrosive wear. To combat corrosive wear practically, many parameters (such as operating conditions, engine design, and lube oil formulation) can be adjusted. However, investigating the effect of each parameter in practice on the corrosive wear is ineffective (time-consuming and expensive). To support the optimization process, development of modeling tools of the sub-processes leading to corrosive wear is required. This includes quantifying the chemical/physical interactions taking place in the lube oil film on the cylinder liner, more specifically investigating the sulfur-related reactions with the alkaline additives in fully formulated lube oil. The subsequent chapters of the thesis will focus on this matter.

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2 Background


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3 | Reaction of sulfuric acid in lube oil:
Implications for large two-stroke diesel engines

Preceding work of this chapter can be found in Appendix A (lube oil analyses to determine and quantify the alkaline core of the overbased detergent) and Appendix B (investigation of the well-mixed lube oil film assumption by use of computational fluid dynamics simulations).

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Abstract

Slow-steaming operation and an increased pressure in the combustion chamber have contributed to increased sulfuric acid (H₂SO₄) condensation on the cylinder liners in large two-stroke marine diesel engines, thus causing increased corrosion wear. To cope with this, lube oils are formulated with overbased detergent additives present as CaCO₃ reverse micelles to neutralize the condensing H₂SO₄. In this present work, a mixed flow reactor (MFR) setup aims to investigate the neutralization reaction by varying Ca/S molar ratio, stirrer speed, H₂SO₄ inlet concentration, and residence time. Lube oil samples from the outlet of the MFR were analyzed by use of Fourier Transform Infrared Spectroscopy (FTIR) and a titration method. The MFR results indicate that the CaCO₃-H₂SO₄ reaction is very fast in a real engine, if the cylinder liner is well-wetted, the oil-film is well-mixed, and contains excess of CaCO₃ compared to the condensed H₂SO₄. The observed corrosion wear in large two-stroke marine diesel engines could consequently be attributed to local molar excess of H₂SO₄ compared to CaCO₃ reverse micelles on the cylinder liners.

Keywords: Corrosion, Lubrication, Neutralization, Mechanism
3 Reaction of sulfuric acid in lube oil: Implications for large two-stroke diesel engines

3.1 Introduction

Slow-steaming became popular during the recession in the last part of the 2000s. This meant that the large two-stroke marine diesel engines were now operated at a lower engine load in order to save fuel. To ensure optimal specific fuel oil consumption the engines were further optimized in this new part load range. This resulted in increased cylinder pressures and colder cylinder liners at part load among others. The lower liner surface temperature, in combination with an increased operating pressure, has led to increased water and acid condensation in the cylinder lube oil film on the cast iron liner surfaces. This causes accelerated corrosion and wear of the liners and piston rings, so-called cold corrosion. It is generally thought that the cold corrosion phenomenon originates mostly from corrosion by condensed sulfuric acid (H$_2$SO$_4$), due to the sulfur-rich fuel used in marine diesel engines. The heavy fuel oil sulfur oxidizes to SO$_2$ from which only a few percents oxidize further to SO$_3$. The SO$_3$ may react with water vapor to form gaseous H$_2$SO$_4$ that can condense, either as concentrated acid or as acid diluted in water, if the temperature locally is below the H$_2$SO$_4$ dew point.

However, alternative explanations involving corrosion wear from SO$_2$ are also found. Neageli and Marbach found that absorption of SO$_2$ in lube oil, followed by reaction with water, could lead to the formation of sulfurous acid (H$_2$SO$_3$), thus increasing corrosion wear. Nagaki and Korematsu advocate that H$_2$SO$_4$ can form in the cylinder lube oil from SO$_2$, causing corrosion wear, by: (1) absorption of SO$_2$ by lube oil, (2) formation of H$_2$SO$_4$ in the lube oil film, and (3) wear on the piston rings and cylinder liner caused by H$_2$SO$_4$.

3.1.1 Mechanisms of neutralization

Commercial lube oils are typically formulated with overbased detergent additives present as reverse micelles to neutralize H$_2$SO$_4$ in the lube oil film. The core of the reverse micelles consists primarily of calcium carbonate (CaCO$_3$), which has a diameter of between 4 and 14 nm. Together with the stabilizing surfactant monolayer, the overall diameter of the micelle is between 8 and 18 nm. Reaction products from the neutralization mechanism between H$_2$SO$_4$ and CaCO$_3$ are CaSO$_4$, CO$_2$, and water according to the following reaction:

$$\text{H}_2\text{SO}_4 (l) + \text{CaCO}_3 (s) \rightarrow \text{CaSO}_4 (s) + \text{CO}_2 (g) + \text{H}_2\text{O} (l) \quad (3.1)$$

Hosonuma and Tamura proposed the first neutralization mechanism between H$_2$SO$_4$ droplets and CaCO$_3$ by measuring the CO$_2$ gas produced from the reaction. Their neutralization model showed that the CaCO$_3$ particles and H$_2$SO$_4$ droplets are stabilized by surfactant molecules. The reverse micelles adsorb onto the oil/acid interface and react with H$_2$SO$_4$. CaSO$_4$ is formed inside the H$_2$SO$_4$ droplets. They found that the reactivity increased with decreasing size of the H$_2$SO$_4$ emulsion, larger base particle size, and the addition of ash-less dispersants. By use of a stopped-flow method, Hone et al. proposed a base-transfer channel neutralization mechanism, where base transfer from the CaCO$_3$ reverse micelles into nanometer-sized, dispersed water/acid droplet in a model oil occurred, upon an effective collision, followed by acid neutralization in the acid droplet. They report that the neutralization reaction becomes faster at higher temperatures (studied in the temperature range 10-30°C) and increasing concentration of overbased CaCO$_3$ particles. The neutralization mechanism between H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles has also been investigated extensively by a capillary video-microscopy technique, investigating the shrinkage of acid...
3.1 Introduction

drops in different lube oils. Wu et al.\textsuperscript{17} proposed an interfacial neutralization mechanism, Figure 3.1, between a nanometer-sized reverse micelle (RM) and a micrometer-sized acid drop.

![Diagram of neutralization mechanism between an acid droplet and CaCO$_3$ reverse micelle](image)

**Figure 3.1.** Neutralization mechanism between an acid droplet and CaCO$_3$ reverse micelle (adopted from Ref. 17).

Following diffusional approach by Brownian motion (step 1) of the micelle and a “sticky” collision, the second step is adsorption (step 2 in Figure 3.1) of an overbased reverse micelle (RM1) onto the acid/oil interface. A channel forms allowing the water and acid to enter into the micelle. The acid then reacts immediately with the CaCO$_3$ in the reverse micelle (step 3). After reaction, RM1 solubilizes the reaction products, becomes RM2, and desorbs back into the bulk oil (step 4). Another overbased reverse micelle can then adsorb onto the oil/acid interface, repeating the procedure. Wu et al. propose that the adsorption step (step 2 in Figure 3.1) is rate-limiting in the proposed interfacial neutralization mechanism, since the shrinking rate of the acid droplet increases as the concentration of CaCO$_3$ reverse micelles (BN) in the lube oil increases. However, their mechanism of the neutralization reaction was based on the fate of nitric acid droplets and not H$_2$SO$_4$ droplets in lube oil, since insoluble CaSO$_4$ was formed for the H$_2$SO$_4$-CaCO$_3$ reaction.\textsuperscript{16,17} When H$_2$SO$_4$ was used instead of nitric acid, formation of needle-like CaSO$_4$ crystals was observed, which deposited at the H$_2$SO$_4$ droplet surface, eventually breaking down the droplet. This may slightly contradict with the proposed neutralization mechanism in Figure 3.1, i.e. the formed CaSO$_4$ deposits on the acid/oil interface on the oil side instead of being solubilized in the reverse micelles followed by desorption back into the bulk oil. Wu et al. suggest that the deposition of CaSO$_4$ crystals may inhibit further reaction between CaCO$_3$ reverse micelles and H$_2$SO$_4$ droplets.

Hosonuma and Tamura\textsuperscript{14} found that the reaction products are formed inside the acid droplets, which agrees with the findings of Hone et al.\textsuperscript{15} by their proposed base-transfer channel neutralization mechanism. Contrary, Wu et al.\textsuperscript{17} advocate that it is the acid which is transferred to the overbased reverse micelles. However, there is a joint consensus that an effective collision between an overbased reverse micelle and an acid droplet is essential for the neutralization reaction to occur. Wu et al.\textsuperscript{17} conclude in their study that the neutralization rate is independent of initial acid droplet size, whereas Hosonuma and Tamura\textsuperscript{14} found a higher reactivity when decreasing the H$_2$SO$_4$ droplet size. Fu et al.\textsuperscript{19} combine the two findings by suggesting that the neutralization rate is independent of droplet size until reaching a certain change point, where the acid droplet has shrunk to a certain size. After this point, the shrinking rate of acid droplets increases. This effect
was not observed by Wu et al. since they probably did not reach the change point in their study. Also by use of capillary video-microscopy, Fu et al. observed visually four different reaction behaviors between different cylinder lube oil formulations and H2SO4 droplets at temperatures in the range 25-170°C: (1) CaSO4 crystals and CO2 gas bubbles were observed on the oil/acid interface on the oil side, (2) crystals and bubbles observed inside the acid droplet, (3) no crystals, but bubbles were found at the oil/acid interface on the oil side, and (4) no reaction products were observed. The first observation agrees with the results found by Wu et al., whereas the second observation may justify the neutralization mechanisms proposed by Hosonuma and Tamura and Hone et al., which indicated that reaction products were found in the acid droplets.

To explain the different reaction behaviors, Fu et al. introduced a strong-stick/weak-stick collision mechanism. A strong-stick collision is a result of direct exposure of the CaCO3 core of the reverse micelles to the acid, thus destroying the rigid structure of the reverse micelles at the oil/acid interface. A weak-stick collision is where the rigid structure of the reverse micelles is maintained before desorbing back into the bulk oil and is dependent on the acid transfer into the core of the reverse micelle. A faster neutralization rate for a strong-stick collision is expected since the CaCO3 is directly exposed to the acid. They further suggested that CaSO4 crystal-growing reactions (reaction behavior 1 and 2) are a consequence of a higher frequency of strong-stick collisions occurring. This was supported by the fact that a higher shrinking rate of an acid droplet was found, when crystals were observed (~23 seconds to break down an acid droplet of 177 μm at 110-140°C). The different observations of reaction products formation locations (reaction behavior 1 and 2) may be attributed to the use of different lube oil formulations, temperatures, and overbased detergents. The study by Fu et al. therefore indicates that increasing the neutralization reaction rate is a question of formulating cylinder oils which enhance the occurrence of strong-stick collisions.

The temperature dependence in the range 25-170°C on the neutralization reaction was also investigated by Fu et al. The neutralization rate increased around 1000 times at 170°C, when comparing to the rate at 25°C, which is a very notable effect. This effect was explained by a decrease of the time period that a base particle stays on the oil-acid interface of an acid droplet and increase of the frequency of effective collisions, thereby increasing the adsorption rate, thus increasing the neutralization reaction rate.

In the capillary video-microscopy technique investigations, great excess of CaCO3 reverse micelles is found compared to H2SO4 on a molar basis. This may not be representative for a large two-stroke marine diesel engine, where the molar ratio of H2SO4 and CaCO3 is closer to stoichiometry. Therefore, this study investigates if limitations are found for the oil-acid neutralization reaction at different molar ratios between H2SO4 droplets and CaCO3 reverse micelles. In a large two-stroke marine diesel engine, roughly two different lube oil-H2SO4 interactions take place. (1) When the piston is at the top dead center (TDC) and moves downwards. Here, H2SO4 may condensate as a film on top of the lube oil film present at the cylinder liner. Since no mixing is occurring, transport of CaCO3 micelles to the H2SO4 happen by diffusion. (2) When the piston moves towards TDC. Here, one important role of the piston rings is to spread and remove excess lube oil from the cylinder liner and combined with the high velocity of the piston, effective mixing of the condensed H2SO4 and lube oil, at the top of the piston, may be expected.

### 3.1.2 Aims of present work

The second H2SO4-lube oil interaction is investigated in this study, assuming that the high velocity of the piston contributes to a well-mixed lube oil-H2SO4 flow at the top of the piston. A mixed flow reactor (MFR) setup is therefore used to simulate the H2SO4-lube oil interaction at well-mixed conditions. The scope of this
paper is to investigate the neutralization reaction between H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles contained in a cylinder lube oil. This is done in a MFR setup by varying different operating conditions. The product samples are analyzed using Fourier Transform Infrared Spectroscopy (FTIR) and a potentiometric titration method to estimate the degree of conversion of H$_2$SO$_4$ droplets and CaCO$_3$ in the cylinder lube oil. The experimental results from the MFR setup can be used in the discussion of the problems found in a large two-stroke marine diesel engine.

3.2 Experimental section

3.2.1 Materials

The commercial lube oil used is obtained from Infineum with a base number (BN) value of 100 ± 2, which corresponds to (8.9 ± 0.18) wt.% CaCO$_3$. The BN is defined as the quantity of acid, expressed in terms of the equivalent number of milligrams of KOH, required to neutralize all alkaline constituents in one gram of sample.$^{24}$ The sulfuric acid is obtained from Sigma-Aldrich with a concentration of 95-98 wt.%. For calculations and experiments, an average concentration of 96.5 wt.% is used for the acid. For the potentiometric titration method, chlorobenzene, glacial acetic acid, and 0.1 M perchloric acid in glacial acetic acid are likewise received from Sigma-Aldrich.

3.2.2 Mixed flow reactor

To investigate the reaction between H$_2$SO$_4$ and the CaCO$_3$ contained in the lube oil, a mixed flow reactor (MFR) setup is used. The setup consists of three peristaltic pumps, which can provide flow rates between 7 µL/min and 380 mL/min depending on the type of tubing, a glass reactor (250 mL), and a motor-driven stirrer (stirrer speed up to 1200 rpm) as shown in Figure 3.2.

![Figure 3.2. Schematic representation of the experimental setup.](image)

The two inlet pumps supply the reactor with H$_2$SO$_4$/H$_2$O-solution as droplets and fresh 100 BN lube oil, respectively, whereas the third pump is an outlet pump controlling the level inside the reactor. A MFR is assumed to achieve perfect mixing, where the outlet composition is identical to the composition inside the reactor. The degree of conversion can then be studied inside the MFR by sampling and analysis of the outlet stream. The first step of the experimental procedure is feeding of H$_2$SO$_4$ solution as droplets and lube oil to the MFR, where the CaCO$_3$ in the lube oil reacts with H$_2$SO$_4$. A product sample is collected after five
residence times to make sure that steady state is reached. Immediately after sampling, the sample is analyzed by an FTIR to estimate the conversion of the CaCO₃ in the lube oil (denoted ‘fast analysis’). Practically this takes a couple of minutes and includes sampling, preparation of the sample, and measuring time. After additional stirring of the product sample to ensure complete reaction of H₂SO₄ droplets with CaCO₃, another IR spectrum is obtained (denoted ‘complete conversion analysis’). By comparing these two results, it is possible to conclude whether all the added H₂SO₄ droplets have reacted with the CaCO₃ in the lube oil within the specified residence time in the MFR.

A range of different operating conditions are investigated, varying stirrer speed, H₂SO₄ concentration, residence time, and inlet CaCO₃/H₂SO₄ molar ratio. Typical operating conditions are: max stirrer speed (1200 rpm), concentrated H₂SO₄ droplets in the inlet stream, and a residence time in the reactor of about 3 minutes. However, the effect of a stirrer speed down to around 120 rpm, a residence time down to around 1 minute, and a H₂SO₄ concentration of 38.3 wt.% are also investigated. Lastly, CaCO₃/H₂SO₄ molar ratios in the inlet streams between 1 and 10 are investigated. A low ratio implies that more H₂SO₄ is fed to the MFR compared to the CaCO₃ in the lube oil (on a molar basis), resulting in a higher consumption of CaCO₃ at complete conversion of acid. When the ratio is 1, 100% conversion of the CaCO₃ in the lube oil is achieved at complete acid conversion.

### 3.2.3 Analysis methods

Fourier Transform Infrared Spectroscopy (FTIR) is used to analyze the product samples immediately after sampling. It is then possible to calculate how much of the inlet H₂SO₄ and CaCO₃ that have reacted within the residence time in the reactor. The measurements were done on a Thermo Scientific Nicolet iS50 FTIR-ATR (Attenuated Total Reflectance) spectrometer. The infrared spectra are recorded using a resolution of 4 cm⁻¹ and 32 scans in the wavenumber range of 400-4000 cm⁻¹. The IR spectrum is unique for each chemical compound, making the approach applicable for identifying CaCO₃ and CaSO₄. To measure a concentration of CaCO₃ in the product lube oil sample a calibration curve is constructed, combining the peak height/area (output from an IR spectrum) to the concentration. A Mettler Toledo T50 potentiometric titrator is used for this purpose following the standard test method for measuring base number in lube oil, ASTM D-2896. This analysis technique measures the concentration of CaCO₃ in a lube oil sample and the value is then converted to the unit of BN. The repeatability of the method showed a 2σ (σ = sample standard deviation) of less than ± 3 % from the mean, by measuring on fully formulated unused lube oil samples with base numbers in the range 6 to 100. This repeatability is consistent with that reported for the standard test method. The calibration curve is constructed by mixing lube oil with H₂SO₄ in different ratios, i.e. from 10% to 90% conversion of the CaCO₃ in the lube oil. After stirring of the samples till complete conversion of the added H₂SO₄, they are analyzed in the titrator and then analyzed by FTIR. The resulting IR spectra are analyzed in OriginPro 2015, extracting peak height and peak area by defining the baseline as a straight line connecting the end points of the respective peak. The calibration curve is constructed based on the CaCO₃ peak, due to a better linear fit compared to using the CaSO₄ peak. The resulting calibration curve is shown in Figure 3.3 for the peak height of the CaCO₃ peak. Duplicate analyses are performed on each sample for the titrator method, i.e. the y-axis of Figure 3.3 is an average. The FTIR analyses are based on single measurements. To estimate the accuracy of the calibration curve, lube oil-H₂SO₄ samples are analyzed both by the titrator and the FTIR. The measured BN from the titrator is then compared to the BN calculated by the calibration curve (Figure 3.3). This analysis shows a difference of 2 BN (2σ, σ = sample standard deviation) between the two methods, i.e. roughly within the uncertainty of the titrator method. A similar result is found using the CaCO₃ peak area calibration curve. This means that the FTIR, by use of the calibration curve, can measure the concentration
of CaCO₃ (BN) in an unknown sample within ± 2 BN. The repeatability of the FTIR method lies within ± 1 % (2σ), which is within the uncertainty of the calibration curve method. The experiments are carried out at ambient temperature and pressure, however, due to the heat of reaction between CaCO₃ and H₂SO₄ droplets, the temperature in the MFR increased till steady state. The difference in temperature did not influence the resulting IR spectra noticeably.

Figure 3.3. Calibration curve connecting the BN determined by the titrator with the peak height of the CaCO₃ peak measured by FTIR. The circles are measurements and the dotted line is a linear fit curve.

3.3 Results and discussions

A series of experiments was conducted in the MFR setup, varying the CaCO₃/H₂SO₄ (Ca/S) molar ratio in the inlet stream, residence time (τ), stirrer speed (N), and H₂SO₄ droplet concentration in the inlet stream, followed by analysis with the FTIR spectrometer. The experimental settings for each experiment are presented in Table 3.1.

Here, experiments 3-4 and 6-9 investigate the effect of residence time, 3 and 9-12 the effect of stirrer speed, 1-5 and 9 the effect of Ca/S molar ratio, and 4 and 13 the effect of concentration of inlet H₂SO₄. Figures 3.4, 3.5, 3.6, and 3.7 show results of the percentage conversion of CaCO₃ in the lube oil and H₂SO₄ as a function of the Ca/S molar ratio. The Ca/S molar ratio (x-axis of the figures) is calculated based on the inlet flow rates of H₂SO₄ and lube oil, respectively.
Table 3.1 Experimental settings for the lube oil-H$_2$SO$_4$ experiments in the MFR, varying CaCO$_3$/H$_2$SO$_4$ molar ratio (Ca/S), residence time (τ), stirrer speed (N), and H$_2$SO$_4$ concentration (C$_{H2SO4}$) in the inlet stream.

<table>
<thead>
<tr>
<th>Exp. #</th>
<th>Ca/S (mol/mol)</th>
<th>τ (min)</th>
<th>N (rpm)</th>
<th>C$_{H2SO4}$ (wt.%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>9.18</td>
<td>3.3</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>2</td>
<td>3.86</td>
<td>3.1</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>3</td>
<td>2.12</td>
<td>3.1</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>4</td>
<td>1.26</td>
<td>3.5</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>5</td>
<td>1.11</td>
<td>3.0</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>6</td>
<td>1.93</td>
<td>0.8</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>7</td>
<td>1.38</td>
<td>1.9</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>8</td>
<td>1.40</td>
<td>0.9</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>9</td>
<td>2.08</td>
<td>2.5</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>10</td>
<td>1.94</td>
<td>2.5</td>
<td>600</td>
<td>96.5</td>
</tr>
<tr>
<td>11</td>
<td>1.94</td>
<td>2.5</td>
<td>120</td>
<td>96.5</td>
</tr>
<tr>
<td>12</td>
<td>1.94</td>
<td>2.5</td>
<td>360</td>
<td>96.5</td>
</tr>
<tr>
<td>13</td>
<td>1.30</td>
<td>2.9</td>
<td>1200</td>
<td>38.3</td>
</tr>
</tbody>
</table>

Two measurements are made for each inlet flow, and an average is used to calculate Ca/S. The uncertainty of this procedure is not shown in the figures. The conversion of CaCO$_3$ in the lube oil is calculated as:

$$X_{CaCO_3} = \left(1 - \frac{BN_{outlet}}{BN_{inlet}}\right) \cdot 100\%,$$

(3.2)

where the BN of the outlet sample is measured and calculated by FTIR and use of Figure 3.3. The conversion of H$_2$SO$_4$ is calculated as:

$$X_{H2SO4} = \left(\frac{(BN_{inlet} - BN_{outlet})v_{oil}\rho_{oil}}{2MKOH} \right) \cdot 100\%,$$

(3.3)

where the numerator is the molar flow of reacted H$_2$SO$_4$ in the MFR and the denominator is the inlet molar flow of H$_2$SO$_4$. The reacted molar flow of H$_2$SO$_4$ is calculated as the difference between the molar inlet CaCO$_3$ and outlet CaCO$_3$. The following parameters are used: volumetric flow rate ($v_i$), density ($\rho_i$), the molar weight ($M_i$), and the weight fraction of H$_2$SO$_4$ in the H$_2$SO$_4$ inlet flow ($w_{H2SO4}$). The number ‘2’ comes from the stoichiometry between the CaCO$_3$/KOH-H$_2$SO$_4$ reactions since the unit of BN is mg KOH per g sample.

The dotted line in the figures presents the conversion of CaCO$_3$ in lube oil, when the reaction between CaCO$_3$ and H$_2$SO$_4$ droplets is instantaneous and complete, i.e. all added H$_2$SO$_4$ has reacted since Ca/S > 1. For a Ca/S molar ratio of 4, the molar ratio between CaCO$_3$ and H$_2$SO$_4$ is 4. When all H$_2$SO$_4$ has reacted with CaCO$_3$, 25% conversion of the CaCO$_3$ in the lube oil is expected, as the dotted curve predicts. The
3.3 Results and discussions

measured conversion of CaCO₃ in the MFR (denoted ‘Fast Analysis’ in figures) at specific conditions is then compared to this curve. If equal, within the uncertainties, it means that complete conversion between H₂SO₄ droplets and CaCO₃ has been reached in the MFR setup. The measured conversions of CaCO₃ in the lube oil in the MFR are presented by the squared symbols in Figures 3.4, 3.6, and 3.7. The circled symbols present the measured conversion of CaCO₃ in the lube oil sample at complete conversion (after additional reaction time with stirring of the samples). Ideally, the complete conversion measurements and the dotted curve should be equal to each other. When there is a difference between the complete conversion points (circles) and fast analysis point (squares), e.g. when Ca/S approaches 1, complete conversion of H₂SO₄ droplets was not achieved in the MFR. The numbers in the figures identify each experiment according to Table 3.1. The effects of varying the described parameters are discussed in the following sub-sections.

3.3.1 Experimental Uncertainty

The experimental uncertainty can be estimated by comparing experiments 3 and 9 (called experiment 3/9). Table 3.1 reveals minor differences in residence time and Ca/S molar ratio between the two experiments due to variations in the oil flow from day to day dependent of wear of tubing, among others. Average CaCO₃ conversions and 2σ (σ = sample standard deviation) for the fast and complete conversion analysis sample are calculated to be 46.51% ± 4.29% and 47.62% ± 3.40% with a Ca/S molar ratio of 2.10 ± 0.06. Average H₂SO₄ conversions and standard deviations for the fast and complete conversion analysis sample are found to be 97.74% ± 5.99% and 100.08% ± 4.06%, respectively. It is worth noting that the conversion of H₂SO₄ exceeds 100%, which is not possible. The reason is that a minor deviation on the Ca/S determination has a significant impact on the conversion calculation especially at lower Ca/S molar ratios. The two times sample standard deviations for experiment 3/9 are shown in Figures 3.4, 3.5, 3.6, and 3.7 as error bars.

3.3.2 Ca/S molar ratio

The effect of varying the Ca/S molar ratio in the range 9.18-1.11 is shown in Figures 3.4 and 3.5. Figure 3.5 shows the conversion of H₂SO₄ droplets as a function of Ca/S molar ratio. Data points for experiment 1 are not shown in Figure 3.5. The figures show that the conversions for the fast and complete analysis sample for experiments 1, 2, and 3/9 are equal to each other within the uncertainties. This means that all the H₂SO₄ droplets react with the CaCO₃ in the lube oil within the available residence time in the MFR. Contrary to this, for experiments 4 and 5 only 85.6% and 82.6%, respectively, of the available H₂SO₄ reacts with the CaCO₃. This indicates that the H₂SO₄-CaCO₃ total reaction rate slows down, when reaching a critically low Ca/S molar ratio value and becomes more pronounced when the Ca/S value is decreased further. The explanation for such an observation could be that the neutralization reaction is controlled by the rate of micelle adsorption (or desorption) onto the acid droplets. According to the Gibbs adsorption equation, a decrease in surfactant (in this work a CaCO₃ micelle) concentration results in a decrease in adsorption. At decreasing Ca/S molar ratio, the concentration of CaCO₃ micelles decreases significantly compared to the H₂SO₄ droplets. The reduction in conversion of H₂SO₄ droplets at lower Ca/S ratios can therefore be explained by a decrease in adsorption rate of the CaCO₃ micelles on the H₂SO₄ droplet, thereby reducing the total reaction rate of CaCO₃ micelles. Wu et al. also suggested that for an acid droplet (μm-sized) the adsorption of CaCO₃ micelles on the H₂SO₄ droplet interface is the controlling step in the neutralization reaction mechanism. The present study addresses further that the effect of reducing adsorption becomes noticeable at a Ca/S ratio lower than around 2 for the conditions studied.
The observation that the H$_2$SO$_4$-consumption is diminished when the excess of CaCO$_3$ is reduced (corresponds to a lower Ca/S molar ratio) could also indicate that the reaction is mixing limited. Even though maximum stirrer speed is applied, it may be impossible to achieve perfect mixing. Therefore, when most of the H$_2$SO$_4$ droplets are converted, insufficient contact between H$_2$SO$_4$ droplets and CaCO$_3$ micelles may arise, having some local depletion regions with an excess of H$_2$SO$_4$ droplets in the lube oil compared to CaCO$_3$, resulting in incomplete reaction of the added H$_2$SO$_4$. Both explanations describe that the limiting factor is a reduced contact between CaCO$_3$ micelles and H$_2$SO$_4$ droplets at lower Ca/S ratio. The results suggest that by having a Ca/S molar ratio larger than around 2, complete conversion of H$_2$SO$_4$ droplets is obtained in the MFR.

Figure 3.4. Effect of varying Ca/S molar ratio on the CaCO$_3$ conversion in the lube oil.

Figure 3.5. Effect of varying the Ca/S molar ratio on the H$_2$SO$_4$ conversion.
3.3 Results and discussions

3.3.3 Residence time

The effect of residence time was investigated at two different Ca/S molar ratios. Experiments 3/9 and 6 investigate the effect of residence time at Ca/S equal to around 2. Figure 3.6 shows that the data points for these experiments lie on the dotted curve. Complete conversion of the H₂SO₄ droplets was therefore obtained within the range of residence times (0.8 - 2.8 min). When the Ca/S molar ratio was decreased to 1.3 - 1.4 (experiments 4, 7, and 8), conversion of the H₂SO₄ droplets in the MFR was limited to 85.6 - 91.2%. By decreasing the residence time from 1.9 min to 0.9 min (experiment 7 and 8, respectively), only a very minor difference in the degree of conversion is found. Even though the residence time in experiment 4 is higher (3.5 min) than in experiment 7 (1.9 min) and 8 (0.9 min), a larger difference between the fast and complete conversion analysis data points is found. This is attributed to the lower Ca/S molar ratio in experiment 4 compared to experiment 7 and 8. Based on these results, we conclude that within the investigated range the residence time does not influence the CaCO₃-H₂SO₄ reaction. This illustrates that the reaction is very fast at well-mixed conditions. However, the CaCO₃-H₂SO₄ reaction becomes limited in the MFR at a Ca/S molar ratio somewhere between 1.4 and 1.9, as also shown in Figures 3.4 and 3.5.

![Figure 3.6. Effect of varying the residence time (τ) on the CaCO₃ conversion in the lube oil.](image)

3.3.4 Stirrer speed

The results of varying the stirrer speed and inlet H₂SO₄ concentration are presented in Figure 3.7. Stirrer speeds ranging from 120 rpm to 1200 rpm at a residence time of 2.5 min are investigated. Reducing the stirrer speed by a factor of three (settings 1200 rpm, 600 rpm, and 360 rpm) has only a minor impact on the conversion, both for the fast analysis and complete analysis measurement. However, when reducing the stirrer speed down to 120 rpm (a factor of 10), the conversion of CaCO₃ in the lube oil decreases roughly from 50% to 40%, with similar conversions observed for the fast and complete analysis, respectively. This is attributed to insufficient mixing between H₂SO₄ droplets and lube oil, augmented by sedimentation of the heavier H₂SO₄. Still, most of the added H₂SO₄ droplets do react with the CaCO₃ (around 80%). This implies again that the reaction between H₂SO₄ droplets and CaCO₃ reverse micelles is very fast. An experiment without mixing was also carried out. Lube oil and H₂SO₄ were dosed in a beaker without applying any
stirring, but with an excess of H$_2$SO$_4$ compared to CaCO$_3$, on a molar basis. FTIR spectra were obtained approximately one week after, showing that no reaction had occurred in the bulk lube oil. Lube oil samples were collected at different locations in the beaker. This implies that some degree of stirring is needed in order to create the contact between H$_2$SO$_4$ and the CaCO$_3$ micelles to initiate the neutralization reaction. The Brownian motion of the micelles alone is apparently not sufficient to react with H$_2$SO$_4$ in a measurable degree over the lube oil-acid boundary. Wu et al.\textsuperscript{16,17} found that a H$_2$SO$_4$ droplet reacts immediately after injection into the lube oil. However, they injected single, µm-sized acid droplets, whereas, in the present experiments, where much larger amounts of acid are introduced, H$_2$SO$_4$ sediment and reaction can only take place over the lube oil-acid boundary. The Ca/S ratio in the lube oil-acid boundary may be significantly smaller than the Ca/S ratio for a small droplet in lube oil. Therefore, the adsorption is significantly lower in the lube oil-acid interface, thus no reaction is observed in the bulk lube oil.

![Figure 3.7](image)

**Figure 3.7.** Effect of varying the inlet concentration of H$_2$SO$_4$ and stirrer speed (N) on the CaCO$_3$ conversion in the lube oil.

### 3.3.5 H$_2$SO$_4$ inlet concentration

In a large two-stroke marine diesel engine, almost pure H$_2$SO$_4$ condenses just below the top dead center position (TDC), whereas the concentration is lower in the lower part of the cylinder liner,\textsuperscript{27} due to the higher temperature at TDC.\textsuperscript{20} Therefore, experiments were carried out with two different H$_2$SO$_4$ concentrations: 96.5 wt.% and 38.3 wt.% at a Ca/S molar ratio of around 1.3. The results are presented in Figure 3.7. The results show that the complete conversion samples are in accordance with the dotted curve. It is observed that less CaCO$_3$ has reacted in the MFR in experiment 13 (38.3 wt.% H$_2$SO$_4$) compared to experiment 4 (96.5 wt.% H$_2$SO$_4$). This indicates that a lower concentration of H$_2$SO$_4$ droplets yields a lower conversion of CaCO$_3$ in the lube oil. However, the use of a diluted H$_2$SO$_4$ also introduces more water to the lube oil, and a new calibration curve was constructed. The new calibration curve did only consist of two calibration points at 72% and 82% conversion of CaCO$_3$ respectively but is used to predict a conversion around 60% which is outside the calibration interval. The effect of this is investigated for the calibration curve in Figure 3.3, predicting a conversion in the range of 50%. This yields only a deviation of ± 0.5 BN, compared to using the full calibration curve. Therefore, the difference in CaCO$_3$ conversion of experiment 4 and 13 is probably not
due to less data point in the calibration curve constructed for the 38.3 wt.% H$_2$SO$_4$ experiment. The reason could be that the increase in water content decreases the contact between H$_2$SO$_4$ and CaCO$_3$ micelles in the MFR setup, further inhibiting the neutralization reaction. Taking the uncertainties into account and a slightly different Ca/S molar ratio, the difference between the two experiments is not significant.

### 3.3.6 Implications for large two-stroke diesel engines

When the CaCO$_3$-H$_2$SO$_4$ reaction approaches stoichiometry (Ca/S = 1), the H$_2$SO$_4$ conversion was reduced significantly and it was not possible to reach complete conversion in the MFR setup. This observation was independent of residence time within the range investigated. It was further noted, when starting to add H$_2$SO$_4$ droplets into the lube oil, an initiation time of approximately 10 seconds should elapse, before reaction was observed (sudden change in color, due to the heavy formation of CO$_2$ bubbles from the neutralization reaction). Even with a reduced stirrer speed, complete conversion of the H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles could be observed (experiment 11). It was also found that no reaction takes place when no stirring was applied. This implies that the reaction between H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles is instantaneous in the lube oil when contact has been established by some degree of stirring.

In a large two-stroke marine diesel engine, the role of the piston rings is to spread and remove excess lube oil from the cylinder liners. This fast movement will cause some degree of mixing/stirring of the lube oil at the top of the piston, justifying that the conditions, for the mixing of H$_2$SO$_4$ and lube oil films in a large two-stroke marine diesel engine, can be approximated in the MFR setup, but this has not yet been confirmed. It is unknown whether the conclusions also apply when only having film-film interaction in an engine. By varying the stirrer speed it was seen that even at lower stirrer speeds, the reaction between H$_2$SO$_4$ droplets and CaCO$_3$ micelles was fast. The stirring from cycle to cycle of the lube oil inside an engine does not necessarily need to be well-mixed in order to reach complete conversion of all the condensed H$_2$SO$_4$, but a certain degree is needed, however. We conclude based on this study that the neutralization of H$_2$SO$_4$ droplets by the CaCO$_3$ micelles in the lube oil is very fast. However, corrosion of the cylinder liners is still an issue, presumably because of other factors.

Local molar excess of condensed H$_2$SO$_4$ compared to CaCO$_3$ in the lube oil film could be one situation of concern. Here all the CaCO$_3$ would be consumed locally and H$_2$SO$_4$ can then interact with the cylinder liner directly. This may happen if a local cold spot is occurring, accelerating the condensation of H$_2$SO$_4$ on the cylinder liner. A large portion of water could also condense, breaking apart the lube oil film. The results showed that the H$_2$SO$_4$ conversion was reduced when Ca/S approached 1, therefore, even stoichiometric amounts of H$_2$SO$_4$ and CaCO$_3$ locally in the lube oil film could result in corrosion issues. According to the results, a Ca/S molar ratio larger than 2 is required to obtain complete conversion of the added H$_2$SO$_4$ droplets within the residence time range investigated. This can be achieved by increasing the feeding rate of the lube oil into the cylinder liner or increase BN in the lube oil. Incomplete mixing/stirring from stroke to stroke of the lube oil-H$_2$SO$_4$ by the piston may also result in acid-steel interaction since the experiments showed that this decreases the contact between H$_2$SO$_4$ droplets and CaCO$_3$ micelles. A significant part of the dosed lube oil into the cylinder liners can combust, losing CaCO$_3$ to the combustion air. In this study, it is assumed that only a negligible amount of lube oil is lost to the combustion air.

The most severe cylinder liner corrosion wear is seen near the TDC. An explanation could be that the upward motion of the piston collects the condensed acid above the top piston ring, and the acid cannot be neutralized quickly enough to prevent their corrosive action.

The lacking ability to neutralize the H$_2$SO$_4$ may be
explained by the findings outlined above, namely lack of proper mixing and excess of H₂SO₄ compared to CaCO₃ at local locations on the cylinder liners.

In practice, other issues than cold corrosion occur in the combustion chambers in large two-stroke diesel engines. These issues could be related to lacquering (film formed from the lube oil on cylinder liners and piston rings), scuffing (large metal-metal welding), etc. However, this was not covered in this work.

The MFR setup is scaled based on an approximate residence time in a large two-stroke marine diesel engine, which is calculated to be less than 4 minutes for a cylinder liner with a height of 3.45 m, diameter of 0.8 m, a lube oil thickness of 10 µm, and a lube oil flow rate of 23 ml/min. However, some of the lube oil stays in the engine for much shorter or longer time.²,28 The experiments were carried out at room temperature and atmospheric pressure, which are different from real conditions in a large two-stroke marine diesel engine. An increase in temperature dramatically increases the total reaction rate,²,15,19 and a faster reaction between H₂SO₄ droplets and CaCO₃ micelles is expected in a real application. This may decrease the effect of the observed limitation of the CaCO₃-H₂SO₄ reaction at lower Ca/S molar ratios. Only a minor difference is expected for the variation in pressure. The size of the H₂SO₄ droplets added to the MFR is in the millimeter-size range and the effect of varying droplet size is not investigated in the present study. The size of the acid droplets could have an effect on the neutralization reaction if H₂SO₄ is condensing on the lube oil film as a mist (aerosols). However, the most pronounced corrosion may be encountered, when larger H₂SO₄ droplets condense on the cylinder liner.¹⁴

3.4 Conclusions

The focus of this study has been to investigate the reaction between H₂SO₄ droplets and CaCO₃ micelles present in lube oil in a MFR at different conditions such as stirrer speed, H₂SO₄ concentration, residence time, and Ca/S molar ratio. The results show that the H₂SO₄-CaCO₃ reaction is not dependent on the investigated residence times. Furthermore, the H₂SO₄ conversion was reduced, when the Ca/S molar ratio approached unity, which may be explained by a significant reduction of the adsorption rate of CaCO₃ micelles on the H₂SO₄ droplets and insufficient macromixing, but this has not yet been confirmed. A certain degree of stirring is required in order to establish contact between H₂SO₄ droplets and CaCO₃ reverse micelles to initiate and maintain the reaction. The present study only investigated the CaCO₃ consumption from H₂SO₄ droplets, but CaCO₃ may also be consumed directly or indirectly by other species, e.g. SO₂.

The observations found here suggest that the neutralization reaction between H₂SO₄ droplets and CaCO₃ micelles in the lube oil is very fast and instantaneous in a real engine application if the cylinder liner is well-wetted, the oil-film is well-mixed, and contains an excess of CaCO₃ compared to the condensed H₂SO₄ (Ca/S > 2). Unfortunately, these ideal conditions may not be present in a large two-stroke marine diesel engine. This advocate that the workload of reducing the corrosion wear issue not necessarily should only lie in the optimization of the lube oil itself, but also the way lube oil is introduced into the engine and how it is spread out on the cylinder liner and perhaps other factors.
Acknowledgments

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Preceding work of this chapter can be found in Appendix A (lube oil analyses to determine and quantify the alkaline core of the overbased detergent) and Appendix B (investigation of the well-mixed lube oil film assumption by use of computational fluid dynamics simulations).

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Abstract

Lubrication oil for marine diesel engines contains additives in the form of CaCO₃-based reverse micelles, which can neutralize condensing H₂SO₄ and thereby limit uncontrolled corrosive wear of the piston rings and cylinder liner. In the present work, the neutralization mechanism was studied experimentally and through modeling. Using a mixed flow reactor (MFR), the rate of the acid-base reaction was measured as a function of relevant process parameters. In addition, the competition between CaCO₃ reverse micelles and NaOH droplets for a reaction with H₂SO₄ droplets in a lube oil emulsion was explored in a batch reactor. For the residence times investigated, the results show that CaCO₃ conversion is significantly reduced when reaching a critically low Ca/S ratio. Furthermore, a mathematical model for the neutralization of H₂SO₄ droplets by CaCO₃ reverse micelles in lube oil under well-mixed conditions was developed. Using the video-microscopy experiments of Fu et al. [Tribol. Lett. 2006, 22 (3), 221–225], it was possible to estimate kinetic parameters for the reaction. The model was used to predict conversion of H₂SO₄ in a lube oil film at the cylinder liner surface for conditions relevant for a full-scale application. Calculations indicated that H₂SO₄ may reach the liner surface regardless of how well-wetted the surface is.

4.1 Introduction

As a result of the economic crisis of 2008 and the abundance of ships in the shipping market, the slow-steaming operation principle for large two-stroke diesel engines emerged as a measure for increasing fuel efficiency. Use of slow-steaming, combined with new engine designs and tunings for further fuel savings, led to increased operating cylinder pressure and lower liner surface temperature. These changes in operating conditions result in increased water and acid condensation on the cylinder lubrication (lube) oil film on the cast iron liner surfaces, promoting a combination of corrosion and wear (cold corrosion) of the cylinder liners and piston rings and significantly reducing their lifetimes. The condensing acid is mainly aqueous sulfuric acid (H₂SO₄), originating from the oxidation of the sulfur-rich fuel oil burned in marine diesel engines. Commercial lube oils are typically formulated with calcium carbonate (CaCO₃) overbased detergent additives, present as nanometer-sized reverse micelles, which neutralize condensed H₂SO₄ in the lube oil film. To counteract the increased condensation rate of H₂SO₄, it is necessary to increase the amount of CaCO₃ being fed to the cylinder liners, which is preferably done by increasing the concentration of CaCO₃ in the lube oil rather than by increasing the oil feed rate. Under-lubrication may result in cold corrosion, which can occur within hours, whereas overlubrication is cost-intensive and may lead to bore-polish (creating a mirror-like cylinder liner surface), which prevents formation of a coherent lube oil film. Both may eventually result in scuffing (direct metal-to-metal contact). Actually, a certain degree of controlled corrosion is beneficial; if the cylinder liners are a little rough, they can better maintain a protective lube oil film. Therefore, to limit and control cold corrosion in engines, the lubrication strategy must be optimized. This is a challenge, especially when trying to set up general recommendations. The situation gets even more complicated when switching fuel during service to comply with the new, stricter sulfur regulations. An understanding of what affects and limits the reaction between the condensing H₂SO₄ and the neutralizing additives, CaCO₃ reverse micelles, in the lube oil can provide greater insight into how to optimize the lubrication strategy to limit cold corrosion.

The reaction between (sulfuric) acid droplets and CaCO₃ reverse micelles in lube oil has been investigated in laboratory experiments over a wide range of conditions. Data in batch mode were obtained using a video-
microscopy technique,\textsuperscript{20–29} a stopped-flow method,\textsuperscript{30–32} and by monitoring the CO\textsubscript{2} formed.\textsuperscript{33–36} The video-microscopy experiments employed placing single acid droplets (70-200 µm in diameter) in a batch of lube oil, followed by measuring the subsequent shrinkage of the acid droplets. These studies indicate that the controlling step of the neutralization reaction is adsorption of a reverse micelle onto the acid droplet. In the capillary video-microscopy technique investigations, CaCO\textsubscript{3} reverse micelles were present in great excess on a molar basis compared with H\textsubscript{2}SO\textsubscript{4},\textsuperscript{25} whereas an excess of concentrated H\textsubscript{2}SO\textsubscript{4} was used in the closed vessel experiments.\textsuperscript{35,37}

Within an engine, the reaction taking place in the lube oil occurs in a system with continuous feeding of fresh lube oil and condensation of H\textsubscript{2}SO\textsubscript{4}, followed by the removal of lube oil to the drain. Presumably, the lube oil film is effectively mixed by the motion of the piston rings. In order to provide a better approximation of the reaction conditions in the lube oil at the cylinder liners in a full-scale marine diesel engine, Lejre et al.\textsuperscript{38} used a mixed flow reactor (MFR) to study the reaction. They found that a certain intensity of stirring was required to initiate and maintain the reaction. Upon formation and stabilization of the H\textsubscript{2}SO\textsubscript{4} into micrometer-sized droplets by the excess emulsifier molecules, a fast reaction occurred, as indicated by a sudden color change of the oil due to the formation of CO\textsubscript{2}. The H\textsubscript{2}SO\textsubscript{4}-CaCO\textsubscript{3} reaction at steady-state was significantly reduced when a critically low Ca/S molar ratio was reached, in agreement with the observations of Roman.\textsuperscript{35} Lejre et al. suggested that macromixing or micelle adsorption or desorption could be the controlling step under their conditions.

Models for the neutralization reaction are scarce. Schramm et al.\textsuperscript{39} and Van Helden et al.\textsuperscript{40,41} modeled cylinder liner corrosion, assuming that the neutralization of H\textsubscript{2}SO\textsubscript{4} by CaCO\textsubscript{3} reverse micelles was acid diffusion-controlled. However, this assumption is contradicted by more recent investigations. Hone et al.\textsuperscript{31} determined an activation energy, $E_a$, for the reaction of 54±2 kJ mol$^{-1}$, concluding that the neutralization reaction is not diffusion-controlled, because diffusion-controlled reactions usually have activation energies of less than ca. 20 kJ mol$^{-1}$. The work of Hone et al. is supported by data from Fu et al.,\textsuperscript{24} who reported a 1000-fold increase in the neutralization rate when increasing the temperature from 25 to 170 °C, which corresponds to an activation energy of 52.8 kJ mol$^{-1}$.

The scope of the present work is to identify the rate-influencing steps (potentially a single rate-controlling one) in the neutralization reaction between H\textsubscript{2}SO\textsubscript{4} droplets and CaCO\textsubscript{3} reverse micelles and to set up a mathematical model for the reaction system in a mixed flow reactor. The first part investigates the mechanism of the reaction and identifies the possible rate-limiting steps. Batch reactor experiments are conducted, comparing the reaction rates of CaCO\textsubscript{3} reverse micelles and NaOH droplets with H\textsubscript{2}SO\textsubscript{4} in lube oil in order to assess the possibility of the reaction between CaCO\textsubscript{3} and H\textsubscript{2}SO\textsubscript{4} being diffusion-controlled. Next, a mathematical model for the reaction system in a mixed flow reactor is set up, and kinetic data for the reaction are extracted from the video-microscopy experiments performed by Fu et al.\textsuperscript{24} Simulations are validated against experimental data from the MFR experiments in our previous\textsuperscript{38} and present work. Finally, the H\textsubscript{2}SO\textsubscript{4}-CaCO\textsubscript{3} neutralization reaction is explored under conditions representative of a marine diesel engine.
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4.2 Experimental work

Experiments involving the reaction between H$_2$SO$_4$ droplets and CaCO$_3$-containing micelles in a lube oil were conducted in a reactor that could be operated in both batch and mixed-flow modes. The experimental procedure is described in detail in our previous work$^{38}$ and is therefore only touched upon briefly here.

4.2.1 Materials

The commercial lube oil used for the experiments was from Infineum and had a stated base number value (BN) of 100. The BN is defined as the quantity of acid, expressed in terms of the equivalent number of milligrams of KOH required to neutralize all alkaline constituents in a 1 g sample.$^{42}$ The H$_2$SO$_4$ was obtained from Sigma-Aldrich with a concentration of 95-98 wt.%. The NaOH solution used was 50 wt.% in water and also from Sigma-Aldrich.

4.2.2 Reactor

Operation in mixed flow reactor (MFR) mode is described elsewhere.$^{38}$ In short, H$_2$SO$_4$(aq) and lube oil were dosed separately to the reactor and mixed by a motor-driven stirrer. In MFR mode, the feeding was continuous, and the level of oil emulsion in the reactor was kept constant by an outlet pump. By taking measurements of the inlet flow rate and reactor volume, the residence time in the reactor could then be calculated.

The reactor was also operated in batch mode to study the competition between NaOH and CaCO$_3$ reacting in the lube oil. Specific amounts of lube oil and NaOH were mixed for 30 min at a maximum stirrer speed of 1200 rpm in order to ensure solubilization of the NaOH droplets into the lube oil. Maintaining 1200 rpm, concentrated H$_2$SO$_4$ was added dropwise by use of a syringe into the well-mixed lube oil emulsion, thus keeping a constant lube oil temperature of around 50 °C. A molar ratio between NaOH and CaCO$_3$ of 2 was chosen because NaOH and H$_2$SO$_4$ react 2:1, whereas CaCO$_3$ and H$_2$SO$_4$ react 1:1. CaCO$_3$-H$_2$SO$_4$ (Ca/S) molar ratios of 0.8 and 1.0 were also investigated. After the addition of H$_2$SO$_4$, mixing continued for 20 min to ensure complete conversion of H$_2$SO$_4$ by reaction with CaCO$_3$ reverse micelles and/or NaOH droplets.

4.2.3 Analysis method

The oil samples were analyzed by FTIR, and a calibration curve was used to convert the peak height of the CaCO$_3$ peak to the base number in the lube oil sample.$^{38}$ Selected infrared spectra (wavenumber range from 900 to 1700 cm$^{-1}$) are presented in Figure 4.1 for four different contents of BN in the lube oil after reaction with added H$_2$SO$_4$. The CaCO$_3$ concentrations were between 98.6 BN (in fresh lube oil) and 21.5 BN (around 80% conversion of the CaCO$_3$). When increasing the amount of H$_2$SO$_4$ added, more CaCO$_3$ is converted. This is shown as a decrease in the CaCO$_3$ band in Figure 4.1 and vice versa for the CaSO$_4$ band. For the MFR experiments, an outlet sample was sampled at steady state and analyzed immediately to estimate the conversion of CaCO$_3$ (this conversion is denoted as Fast Analysis). Afterward, the sample was stirred to ensure complete conversion of remaining H$_2$SO$_4$, if any. The sample was then analyzed again by FTIR and denoted Complete Conversion Analysis. Comparing the two conversions revealed if complete conversion of the added H$_2$SO$_4$ was achieved in the MFR within the specified residence time.
4.3 Neutralization mechanism and rate-limiting steps

The reaction between acid (H$_2$SO$_4$) droplets and alkaline (CaCO$_3$) reverse micelles (RM) is thought to proceed through the mechanism presented in Figure 4.2.$^{20,21}$
The first step (Step 1 in Figure 4.2) is a collision between the reverse micelle (RM1) and the acid droplet interface by Brownian motion. A successful collision leads to adsorption of the reverse micelle to the acid interface (Step 2 in Figure 4.2). Next, a channel forms and H₂SO₄ and CaCO₃ react by the transferring of the acid into the reverse micelles (Step 3 in Figure 4.2). After the reaction, the reaction products are located in the reverse micelle (now called RM2), which desorbs from the acid droplet and back into the bulk oil (Step 4 in Figure 4.2). However, different locations for the reaction products have been noted in the literature.²¹,²⁵,³¹,³⁴ Fu et al.²⁵ observed four different reaction behaviors in different lube oil formulations within a temperature range of 25-170°C and attributed these differences to different lube oil formulations, temperatures, and overbased detergents. The observed reaction behaviors were explained by a strong/weak-stick collision mechanism, in which the neutralization rate is enhanced by formulating lube oils with a high frequency of strong-stick collisions. On the basis of these studies and the work by Lejre et al.,³⁸ possible rate-limiting steps in the neutralization mechanism between H₂SO₄ and CaCO₃ reverse micelles in lube oil formulations include: micelle diffusion, micelle adsorption, surface reaction, micelle desorption, and macromixing. For micelle diffusion to be rate-limiting, the rate at which the micelles diffuse must be comparable to the overall rate of reaction. If the limiting step is adsorption of a micelle onto a H₂SO₄ droplet, the reaction is controlled by the occurrence of a successful “sticky” collision. This is in contrast to a diffusion-controlled reaction, where the reaction is taking place at every collision. If the CaCO₃ reverse micelles have a strong adhesion to the H₂SO₄ droplet surface, occupying the surface of the droplet and preventing unreacted CaCO₃ reverse micelles from adsorbing, desorption may become the rate-limiting step in the neutralization mechanism. If the surface reaction is the rate-controlling step, the reaction rate will be limited by the rate of the surface reaction between H₂SO₄ and CaCO₃. However, the reaction is an acid-base reaction occurring irreversibly. Because of the small size of the CaCO₃ particles in lube oil (8-18 nm in diameter²²) and the fact that the reaction rate increases with decreasing CaCO₃ particle size in acid,⁴³ it is presumed that the surface reaction between CaCO₃ and H₂SO₄ happens instantaneously, and the surface reaction is therefore not the rate-limiting step in the neutralization mechanism.²¹ Finally, the reaction can also be controlled by the rate at which H₂SO₄ droplets and CaCO₃ reverse micelles are mixed in the reactor. In the following, possible rate-limiting steps are investigated and evaluated from batch reactor and mixed flow reactor experiments.
4.3 Neutralization mechanism and rate-limiting steps

4.3.1 Batch reactor experiments – diffusion limitation

To evaluate whether or not the CaCO₃-H₂SO₄ reaction is diffusion-controlled, the relative rates of the H₂SO₄-CaCO₃ and H₂SO₄-NaOH reactions were investigated in batch reactor experiments:

\[
\text{H}_2\text{SO}_4 (aq) + \text{CaCO}_3 (s) \rightarrow \text{CaSO}_4 (s) + \text{CO}_2 (g) + \text{H}_2\text{O (l)} \quad (4.1)
\]

\[
\text{H}_2\text{SO}_4 (aq) + 2\text{NaOH (aq)} \rightarrow \text{Na}_2\text{SO}_4 (s) + 2\text{H}_2\text{O (l)} \quad (4.2)
\]

The reaction between H₂SO₄ and NaOH is diffusion-controlled,⁴⁴ as it can be considered instantaneous upon contact. If the reaction between CaCO₃ and H₂SO₄ is also diffusion-controlled, it would be expected that H₂SO₄ would react to a larger degree with CaCO₃ than with NaOH. A smaller particle size leads to a higher diffusion coefficient, thereby increasing the diffusion-controlled reaction rate on a molar basis,⁴⁴ and the NaOH droplets are much larger than the nanometer-sized micelles. In the experiments, the NaOH was solubilized into the lube oil by the excess dispersant and detergent molecules already present in the oil.³⁵ Common emulsions have a particle size distribution with a radius in the range of 1-10 µm,⁴⁵ which may be a representative size range for the emulsified NaOH droplets in the lube oil.

It is not expected that the controlling step for the NaOH-H₂SO₄ reaction would be changed when NaOH is solubilized into the lube oil emulsion. When the equal-sized H₂SO₄ and NaOH droplets (micrometer) collide, they are much larger than the nanometer-sized surfactants that may surround the droplets. It is therefore presumed that the surfactants do not constitute any hindrance for the NaOH-H₂SO₄ reaction. The reaction is further enhanced by the high stirring intensity used.

The batch reactor experiments were performed with a fixed molar ratio between NaOH and CaCO₃ of 2, corresponding to the stoichiometry of the reactions with H₂SO₄. Care was taken to provide equal mixing conditions for the NaOH and CaCO₃ to react with the added H₂SO₄ in the well-mixed reactor. Upon mixing of the lube oil and NaOH solution, concentrated H₂SO₄ was added dropwise. Two different Ca/S molar ratios were then investigated. At a Ca/S = 1, the neutralization ability of H₂SO₄ is 100%, meaning that the added H₂SO₄ has the ability to either convert all the CaCO₃, all the NaOH, or a mixture thereof. If all of the H₂SO₄ reacts first with the CaCO₃, 100% conversion of the CaCO₃ and 0% conversion of the NaOH would be found at complete conversion of the H₂SO₄. At Ca/S = 0.8, the H₂SO₄ is in excess compared with the CaCO₃ in the lube oil. Moreover, if all of the CaCO₃ is converted first, 25% conversion of the NaOH would be found at complete conversion of the H₂SO₄. The percentage conversions of CaCO₃ and NaOH with H₂SO₄ from the batch reactor experiments are shown in Figure 4.3.
Figure 4.3. Results from the NaOH-H\textsubscript{2}SO\textsubscript{4}-lube oil batch reactor experiments, showing the accumulative percentage conversions of NaOH and CaCO\textsubscript{3} at two different Ca/S values. Error bars represent 2 times the sample standard deviations based on two repetitions.

At Ca/S = 1, 91% conversion of the NaOH was found, whereas only 9% of the CaCO\textsubscript{3} was converted. At Ca/S = 0.8, 86% conversion of the NaOH and 39% conversion of the CaCO\textsubscript{3} were observed. For both Ca/S molar ratios, most of the H\textsubscript{2}SO\textsubscript{4} reacted with the NaOH, whereas only a minor fraction reacted with the CaCO\textsubscript{3} reverse micelles. From these results, it can be concluded that the H\textsubscript{2}SO\textsubscript{4}-CaCO\textsubscript{3} reaction is significantly slower than the H\textsubscript{2}SO\textsubscript{4}-NaOH reaction and is thus too slow to be diffusion-controlled.

Wu et al.\textsuperscript{22} found that increasing the concentration of nonionic surfactant in a model oil increased the particle size of the reverse micelles (though they were still in the nanometer range), consequently increasing the neutralization rate of the H\textsubscript{2}SO\textsubscript{4} droplet. They attributed this to the enlarged reverse micelles having space to accommodate more water and H\textsubscript{2}SO\textsubscript{4} upon sticking to the oil-acid interface. However, they also suggested that the addition of nonionic surfactants may make the tails of the surfactants more flexible and thus the access of H\textsubscript{2}SO\textsubscript{4} to the CaCO\textsubscript{3}-core more feasible. This may facilitate the transport of H\textsubscript{2}SO\textsubscript{4} into the reverse micelles, thereby increasing the neutralization rate when adding nonionic surfactants. However, it is difficult to directly compare the experiments performed by Wu et al. with the experiments performed in the batch reactor, because larger NaOH droplets were used in the present work and the effect of the CaCO\textsubscript{3} reverse micelle size on the neutralization rate was not isolated.

In conclusion, the batch reactor experiments support the findings of Hone et al.,\textsuperscript{31} that the neutralization reaction between H\textsubscript{2}SO\textsubscript{4} droplets and CaCO\textsubscript{3} reverse micelles cannot be diffusion-controlled. The mixed flow reactor experiments described next, serve to investigate the possible remaining rate-limiting steps.

4.3.2 Mixed flow reactor experiments

The MFR experiments serve both to partly provide information on the rate-limiting steps in the neutralization and partly as data for modeling validation. The data obtained in our previous work\textsuperscript{38} were complemented in the present work with additional experiments in order to increase the number of repetitions as well as to obtain data at a Ca/S molar ratio approaching unity at varying stirrer speeds (to clarify the effect of
macromixing). The experimental conditions of the expanded work for each experimental number are supplied in Appendix C, which also contains data on the effects of residence time and inlet \(\text{H}_2\text{SO}_4\) concentration on the \(\text{CaCO}_3\) conversion.

### 4.3.2.1 Stirrer speed

The neutralization reaction could conceivably be limited by the rate of macromixing. Even when maximum stirrer speed is applied, perfect mixing might not be achieved in the MFR. Therefore, insufficient contact between \(\text{H}_2\text{SO}_4\) droplets and \(\text{CaCO}_3\) micelles may arise, resulting in local regions with an excess of \(\text{H}_2\text{SO}_4\) droplets in the lube oil compared with \(\text{CaCO}_3\), and consequently incomplete reaction of the added \(\text{H}_2\text{SO}_4\).

Figure 4.4 shows the effect of stirrer speed, \(N\) (1200, 600, and 360 rpm), on the \(\text{CaCO}_3\) conversion in the lube oil. The dotted line presents the theoretical conversion when the reaction between \(\text{CaCO}_3\) and \(\text{H}_2\text{SO}_4\) droplets is complete (i.e., complete conversion of the limiting reactant). The effect of reducing the stirrer speed by a factor of around 3 is negligible, both for the *Fast Analysis* and *Complete Conversion Analysis* conversions, as well as for both \(\text{Ca/S}\) molar ratios.

![Figure 4.4](image)

**Figure 4.4.** Effect of varying the stirrer speed \((N)\) on the \(\text{CaCO}_3\) conversion in the lube oil. Error bars represent 2 times the sample standard deviations. The experimental conditions were as follows: stirrer speed = 120-1200 rpm, inlet \(\text{H}_2\text{SO}_4\) concentration = 96.5 wt.%, residence time (for *Fast Analysis*) = 2.1-2.8 min (see Table C.1 in Appendix C for more information on each experimental number).

The stirrer speed affects the macromixing in the reactor, as well as the solubilization of \(\text{H}_2\text{SO}_4\) into the lube oil. If the \(\text{H}_2\text{SO}_4-\text{CaCO}_3\) reaction had been macromixing-controlled, an effect on the conversion of \(\text{CaCO}_3\) by decreasing the stirring intensity in the MFR would be expected. This was not the case, and it is concluded that the reaction is not controlled by macromixing when a certain degree of stirring is applied. Further, a reduced conversion of \(\text{CaCO}_3\) at reduced \(\text{Ca/S}\) values would not be expected for a macromixing-controlled reaction at the same stirring speed. When the stirrer speed is decreased, the solubilization of \(\text{H}_2\text{SO}_4\) into the lube oil may also be reduced, leading to an increased size of the \(\text{H}_2\text{SO}_4\) droplets in the lube oil emulsion. Assuming that the reaction is limited by adsorption, this decreases the adsorption rate because the total surface area of the \(\text{H}_2\text{SO}_4\) droplets also decreases. Reducing the stirrer speed by a factor of 10 (120 rpm), yields a conversion of only around 80% of the added \(\text{H}_2\text{SO}_4\) in the MFR (similar conversions were observed...
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for the fast and complete analysis). The incomplete conversion of H₂SO₄ at this low stirrer intensity is attributable to insufficient mixing between H₂SO₄ droplets and lube oil, because sedimentation of the heavier H₂SO₄ was observed. This implies that most of the H₂SO₄ droplets are readily solubilized into the lube oil emulsion upon a minor degree of stirring.

4.3.2.2 Ca/S molar ratio

The effects of varying the Ca/S molar ratio on the CaCO₃ and H₂SO₄ conversions are presented in Figure 4.5 and Figure 4.6.

**Figure 4.5.** Effect of varying the Ca/S molar ratio on CaCO₃ conversion in lube oil. Error bars represent 2 times the sample standard deviations. The experimental conditions were the following: stirrer speed = 1200 rpm, inlet H₂SO₄ concentration = 96.5 wt.%, residence time (for Fast Analysis) = 2.1-3.5 min (see Table C.1 in Appendix C for more information on each experimental number).

**Figure 4.6.** Effect of varying the Ca/S molar ratio on H₂SO₄ conversion. Error bars represent 2 times the sample standard deviations. The experimental conditions were the same as in Figure 4.5.
When the Ca/S ratio was larger than 2, complete conversion of H$_2$SO$_4$ was found in the MFR. The H$_2$SO$_4$ conversion was observed to decrease when reaching a critically low Ca/S ratio of between 1.26 and 2.10. This is attributable to the reaction being adsorption or desorption controlled. At decreasing Ca/S ratios, significantly fewer CaCO$_3$ reverse micelles encircle each H$_2$SO$_4$ droplet. The reduced conversion of H$_2$SO$_4$ at lower Ca/S ratios can therefore be explained by a decrease in the adsorption rate of the CaCO$_3$ micelles on the H$_2$SO$_4$ droplet, thus reducing the total reaction rate of CaCO$_3$ micelles. It is expected that a high bulk concentration of the adsorbate (in this work, CaCO$_3$ reverse micelles) leads to a high coverage of sites on a surface (H$_2$SO$_4$ droplet surface), thereby increasing the likelihood of the reaction mechanism being controlled by desorption. This situation corresponds to a high Ca/S, where no apparent limitation is found (Ca/S ratio > 2 in, e.g., Figure 4.5). When fewer micelles are surrounding each droplet (corresponding to a low Ca/S value), the driving force from bulk to the surface is also decreased, thereby approaching adsorption-control.

Wu et al. observed the formation of crystals (CaSO$_4$ from the neutralization reaction), which may deposit on the surface of the H$_2$SO$_4$ droplet, inhibiting further reaction (i.e., desorption-control). However, the occurrence of crystal formation depends on the lube oil formulation; the reaction products may be solubilized into the lube oil if the lube oil is formulated with the suitable dispersants. Assuming that a stable emulsion is formed when H$_2$SO$_4$ is introduced into the lube oil (droplet radii in the range of 1-10 µm), it is expected that inhibition by CaSO$_4$ crystal formation is not a concern. Wu et al. further suggested that the adsorption of CaCO$_3$ micelles on the acid droplet micrometer-sized interface is the controlling step in the neutralization reaction mechanism. The arguments and experimental results presented in this section support this conclusion.

### 4.4 Mathematical modeling

#### 4.4.1 Reaction rate expressions

The simulated degree of conversion of the H$_2$SO$_4$ droplets by the CaCO$_3$ reverse micelles is determined by the reaction rate expression. In Section 4.3, we concluded that reverse micelle adsorption onto the H$_2$SO$_4$ droplets is most likely the limiting step in the neutralization mechanism at well-mixed conditions, in line with the literature investigations. However, early modeling studies indicated that the neutralization reaction may be acid diffusion-controlled. In this study, a reaction rate expression that accounts for both micelle diffusion- and adsorption-resistance will be set up for comparison, and the rate-limiting step will be identified.

#### 4.4.1.1 Diffusion-controlled reaction rate expression

Under diffusion-control, a reaction occurs instantaneously upon collision. The CaCO$_3$ reverse micelles move by Brownian motion and because of their small size, a high collision rate with the H$_2$SO$_4$ droplets is expected. An expression for the reaction rate was derived following Laidler, assuming that the H$_2$SO$_4$ droplets are immobile compared with the much smaller CaCO$_3$ reverse micelles. This assumption is justified because the radius of the H$_2$SO$_4$ droplets is in the micrometer range, whereas the radius of the CaCO$_3$ reverse micelles is in the nanometer range. The diffusion-controlled reaction rate constant, $k_{diff}$, is given as:

$$k_{diff} = ...$$

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\[ k_{diff} = 4\pi D_L d_c N_A \]  

(4.3)

\( N_A \) is Avogadro’s constant, and \( d_c \), the critical distance from a droplet where a CaCO₃ reverse micelle immediately reacts under diffusion control, is assumed to be equal to the radius of the \( R = R_{SA}, C_L = 0 \). The diffusion coefficient of the CaCO₃ reverse micelles, \( D_L \), is given as:

\[ D_L = \frac{k_B T}{6\pi \eta R_L} \]  

(4.4)

Here, \( k_B \) is the Boltzmann constant, \( T \) is the temperature of the lube oil volume, \( R_L \) is the radius of the CaCO₃ reverse micelles, and \( \eta \) is the viscosity of the lube oil. The diffusion coefficient of the CaCO₃ reverse micelles increases with decreasing lube oil viscosity. The dependency on temperature is affected by that of the viscosity, which is typically a strong function of temperature.

The micelle diffusion-controlled reaction rate is first order with respect to each reactant (H₂SO₄ droplet and CaCO₃ micelle, respectively), and is given by:

\[ (-r_{A, diff}) = k_{diff} C_d C_L \]  

(4.5)

\( C_d \) is the concentration of sulfuric acid droplets and \( C_L \) is the molar concentration of the limestone, given as:

\[ C_d = \frac{N_{SA}}{N_A} \]  

(4.6)

\[ C_L = N_L n_{LM} = \frac{N_L V_L f_L \rho_L}{M_L} \]  

(4.7)

\( N_{SA} \) is the number of H₂SO₄ droplets per unit volume of lube oil, \( N_L \) is the number of micelles in the lube oil volume, \( n_{LM} \) is the moles of CaCO₃ in one micelle, \( V_L \) is the volume of one micelle, \( f_L \) is the volume fraction of CaCO₃ in a micelle, \( \rho_L \) is the density of CaCO₃, and \( M_L \) is the molar weight of CaCO₃. The diffusion-controlled reaction rate constant only contains physical parameters and can therefore be calculated directly from the expressions given in Eqs. (4.3) and (4.4).

### 4.4.1.2 Adsorption-controlled reaction rate expression

Different reaction behaviors are reported in literature for an H₂SO₄ droplet in oil (both model and commercial oils); however, when a droplet was placed in an optimized commercial lube oil, shrinkage over time of the droplet was observed. The droplet shrinkage experiments performed by Fu et al. are used in this work to derive a reaction rate constant, because a comparable lube oil formulation was used in this study. According to Fu et al., the reaction of a sulfuric acid droplet in a commercial marine cylinder oil, containing CaCO₃-based additives, is adsorption-controlled. Their droplet shrinkage experiments (reported as radius versus time graphs) at temperatures in the range 298-443 K are here used to extract the adsorption-
4.4 Mathematical modeling

controlled reaction rate constant by formulating molar rate balances of H₂SO₄ droplets and CaCO₃ reverse micelles. The molar H₂SO₄ consumption rate of one droplet is:

\[- \frac{dn_{SA}}{dt} = -\frac{d(V_{SA}C_{SA,d})}{dt} = 4\pi R_{SA}^2 C_{SA,d} \left( -\frac{dR_{SA}}{dt} \right) \]  

(4.8)

\(V_{SA}\) is the volume of one droplet and \(C_{SA,d}\) is the concentration of H₂SO₄ in the droplets. The molar adsorption rate of CaCO₃ reverse micelles to the surface of a H₂SO₄ droplet is expressed as:

\[- \frac{dn_{L}}{dt} = A_{SA} k_{ads} C_L (1 - \theta) \]  

(4.9)

Here, \(k_{ads}\) is the adsorption-controlled reaction rate constant \((\text{m s}^{-1})\), \(\theta\) is the fraction of the H₂SO₄ droplet surface that is covered by micelles, and \(A_{SA}\) is the surface area of the H₂SO₄ droplet. For an adsorption-controlled process, it is assumed that \(\theta = 0.24\). This means that immediately after a successful collision (adsorption) of a micelle onto the droplet surface, reaction occurs, followed by immediate desorption of the product back into the bulk. According to Eq. (4.9), the reaction rate depends on the concentration of CaCO₃ reverse micelles (or BN), which is in agreement with previous investigations. The molar consumption rate of H₂SO₄, Eq. (4.8), can be set equal to the molar adsorption rate of CaCO₃ reverse micelles onto the H₂SO₄ droplets, Eq. (4.9). Solving for \(k_{ads}\) gives:

\[k_{ads} = \left( -\frac{dR_{SA}}{dt} \right) \frac{C_{SA,d}}{C_L} \]  

(4.10)

The overall adsorption-controlled reaction rate is derived by multiplying Eq. (4.9) with \(N_{SA}\) and introducing the molar concentration of H₂SO₄ in the lube oil, \(C_{SA} = N_{SA} V_{SA} C_{SA,d}\):

\[(-r_{A,ads}) = A_{SA} \frac{1}{V_{SA} C_{SA,d}} k_{ads} C_{SA} C_L \]  

(4.11)

4.4.1.3 Estimation of adsorption-controlled reaction rate constant

As said, values for the H₂SO₄ droplet shrinking rate, \((-dR_{SA}/dt)\), were determined from the videomicroscopy experiments by Fu et al. in the temperature range of 298-443 K for H₂SO₄ droplets in fully formulated lube oil. A strong dependence on temperature was found; by increasing the temperature from 298 to 443 K, the shrinking rate increased by a factor of more than 1000. A linear relation between ln\((-dR_{SA}/dt)\) and \(1/T\) was also found, and a modified Arrhenius type plot was constructed. The relation between shrinking rate and temperature can be established as:

\[- \frac{dR_{SA}}{dt} = 11.3 \frac{m}{s} \exp \left( -\frac{52.8 \text{ kJ mol}^{-1}}{RT} \right) \]  

(4.12)
Here, $R$ is the ideal gas constant. The derived activation energy, $E_a$, of 52.8 kJ mol$^{-1}$, is in excellent agreement with the value of 54±2 kJ mol$^{-1}$ found by Hone et al.$^{31}$ Duan et al.$^{54}$ reported activation energies in the range of 27.0-30.7 kJ mol$^{-1}$ for the neutralization of acetic acid droplets in passenger-car lube oil, but this reaction involved a different mechanism compared with that of a H$_2$SO$_4$ droplet in marine lube oil.

Fu et al. used a lube oil with a base number of 70 and 50 vol.% H$_2$SO$_4$ droplets, corresponding to a concentration of CaCO$_3$ of $C_L = 586.5$ mol m$^{-3}$ and an acid concentration of $C_{SA,d} = 9.4 \cdot 10^3$ mol m$^{-3}$. By substituting Eq. (4.12) into Eq. (4.10) and inserting the concentrations, the following expression for $k_{ads}$ can be calculated:

$$k_{ads} = 180.6 \frac{m}{s} \exp\left(-\frac{52.8 \frac{kJ}{mol}}{RT}\right)$$

Equation (4.11), with $k_{ads}$ from Eq. (4.13), provides a quantitative expression for the neutralization reaction under adsorption control.

4.4.1.4 The functional reaction rate expression

A functional reaction rate expression can now be derived to have the following layout:

$$(-r_A) = k'_i C_{SA} C_L$$

Where $k'_i$ is either the diffusion- or adsorption-controlled reaction rate constant. To have the derived expressions, given in Eqs. (4.5) and (4.11), as presented as Eq. (4.14), $k'_{ads}$ and $k'_{diff}$ are given as:

$$k'_{ads} = \frac{3k_{ads}}{R_{SA} C_{SA,d}}$$

$$k'_{diff} = \frac{k_{diff}}{V_{SA} C_{SA,d} N_A}$$

Note that the micelle-diffusion and micelle-adsorption rate equations (based on Eq. (4.14)) are thereby identical, and only the rate constants (Eqs. (4.15) and (4.16)) are different.

4.4.2 Reactor System

A schematic illustration of the H$_2$SO$_4$ droplets-lube oil system in the mixed flow reactor setup is shown in Figure 4.7. The reactor has inlet flows for lube oil and H$_2$SO$_4$ droplets. The outlet flow serves to maintain a specific oil volume, $V_{oilt}$. The lube oil volume is well-mixed, and the H$_2$SO$_4$ droplets are therefore mixed immediately into the oil, forming a stable water-in-oil emulsion. The well-mixed conditions in the MFR resemble those of an actual engine cylinder, where the high velocity of the piston conceivably leads to a well-mixed region in front of the piston. The H$_2$SO$_4$ droplets with a uniform droplet radius of $R_{SA}$ and a concentration of $C_{SA,d}$ are fed to the mixed flow reactor with a flow rate of $F_{SA}$. The lube oil dosage is continuous, with a flow rate of $v_{oilt,f}$, containing CaCO$_3$ reverse micelles in a concentration of $N_{L,f}$. The lube
oil outlet flow, $v_o$, contains unreacted CaCO$_3$ reverse micelles in the concentration, $N_L$, and the H$_2$SO$_4$ droplet concentration is $N_{SA}$ (if any).

Figure 4.7. Schematic illustration of the neutralization of H$_2$SO$_4$ droplets in a lube oil by CaCO$_3$ reverse micelles under mixed flow reactor conditions. Lube oil volume and inlet and outlet conditions are indicated in the figure.

4.4.3 Mathematical Model

The present model describes the neutralization of H$_2$SO$_4$ droplets in a stirred lube oil volume containing CaCO$_3$ reverse micelles. The assumptions underlying the model are the following:

- The lube oil volume is well-mixed (no radial or axial concentration or temperature gradients) and in steady state with continuous, uniform feeding of lube oil and H$_2$SO$_4$ droplets.
- The outlet flow of lube oil, $v_o$, is equal to the sum of the inlet flows of lube oil, $v_{oil,f}$, and the droplets, $v_{SA,f}$. The reduction in outlet lube oil flow due to CO$_2$ (g) formation is not taken into account.
- The H$_2$SO$_4$ droplets are readily solubilized into the lube oil by excess surfactants as a water-in-oil emulsion.
- The only reaction considered in the lube oil is CaCO$_3$ (s) + H$_2$SO$_4$ (aq) $\rightarrow$ CaSO$_4$ (s) + CO$_2$ (g) + H$_2$O (l) with a reaction rate of $-r_A$.
- The CaSO$_4$ formation does not limit the neutralization reaction.
The CaCO$_3$ micelles and H$_2$SO$_4$ droplets are spherical and uniform in size.

Shrinking over time of CaCO$_3$ micelles and H$_2$SO$_4$ droplets is not taken into account; only consumption of entire droplets and micelles is considered.

### 4.4.3.1 H$_2$SO$_4$ number balance over a mixed flow reactor

The number balance for H$_2$SO$_4$ droplets is given as:

$$ F_{SA} - \frac{(-r_A)V_{oil}M_{SA}}{\rho_{SA}(V_{SA} - V_{SA,o})} \frac{c_{SA,d}M_{SA}}{\rho_{SA}} \text{produced} = \frac{N_{SA}V_o}{\text{out}} $$  \hspace{1cm} (4.17)

Here, $F_{SA}$ is the inlet H$_2$SO$_4$ droplet number flow, $V_{oil}$ is the volume of lube oil in the reactor, $M_{SA}$ is the molar weight of H$_2$SO$_4$, $\rho_{SA}$ is the density of H$_2$SO$_4$, and $v_o$ is the volumetric outflow. The term $c_{SA,d}M_{SA}/\rho_{SA}$ is the volume fraction of H$_2$SO$_4$ in the droplets. The term $(V_{SA} - V_{SA,o})$ accounts for the volume change of a H$_2$SO$_4$ droplet. $V_{SA}$ is the initial volume of a H$_2$SO$_4$ droplet, and $V_{SA,o}$ is the volume of a reacted H$_2$SO$_4$ droplet in the outlet. The latter is equal to 0, corresponding to a situation where a reacted H$_2$SO$_4$ droplet is entirely consumed. The volumetric outflow rate of lube oil emulsion, $v_o$, is equal to the sum of the volumetric inlet flow rates of lube oil, $v_{oil,f}$, and H$_2$SO$_4$ droplets, $v_{SA,f}$:

$$ v_o = v_{oil,f} + v_{SA,f} = v_{oil,f} + F_{SA}V_{SA} $$  \hspace{1cm} (4.18)

### 4.4.3.2 Reverse micelle number balance over mixed flow reactor

A number balance for the reverse micelles in the lube oil volume reads:

$$ \frac{N_{L,f}V_{oil,f}}{\text{in}} - \frac{(-r_A)V_{oil}M_L}{\rho_L(V_{oil} - V_{L,o,f})} \frac{f_{oil,w}}{\rho_{oil}} \text{produced} = \frac{N_{L}V_{o}}{\text{out}} $$  \hspace{1cm} (4.19)

Again, the term $V_{oil,f}$ is equal to 0 because only consumption of entire CaCO$_3$ reverse micelles is considered. $N_{L,f}$ is the number of CaCO$_3$ reverse micelles per volume of lube oil in the inlet feed, given as:

$$ N_{L,f} = \frac{f_{oil,w}\rho_{oil}}{ \rho_{oil}V_{oil,f} } $$  \hspace{1cm} (4.20)

Here, $f_{oil,w}$ is the weight fraction of CaCO$_3$ in the fresh lube oil, and $\rho_{oil}$ is the density of the lube oil.

### 4.4.3.3 Ca/S molar ratio

It is of interest to investigate how the H$_2$SO$_4$ droplet flow into the lube oil volume affects the conversion of the H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles in the lube oil film. This is done by introducing the molar ratio of CaCO$_3$ to H$_2$SO$_4$ in the inlet feed, Ca/S, defined from the molar balance:
4.4 Mathematical modeling

\[
\frac{Ca}{S} = \frac{v_{oil,fp} \rho_{oil,fL,oil,w}}{M_L F_{SA} V_{SA} C_{SA,d}} \tag{4.21}
\]

Solving for \( F_{SA} \) gives:

\[
F_{SA} = \frac{v_{oil,fp} \rho_{oil,fL,oil,w}}{M_L V_{SA} C_{SA,d} Ca/S} \tag{4.22}
\]

By substituting Eq. (4.22) into Eq. (4.17), the parameter \( Ca/S \) is now the independent variable. When \( Ca/S \) is equal to 1, then \( H_2SO_4 \) and \( CaCO_3 \) are present in stoichiometric amounts.

4.4.3.4 Estimation of model parameters

The chemical and physical properties for the \( H_2SO_4 \) droplets and \( CaCO_3 \) reverse micelles are shown in Table 4.1, together with typical operating conditions.

Table 4.1. Chemical and physical parameters for the \( H_2SO_4 \) droplets, \( CaCO_3 \) reverse micelles, and lube oil.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Parameter Value</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>( R_L )</td>
<td>( 5 \cdot 10^{-9} ) m</td>
<td>12,20,21,49–52</td>
</tr>
<tr>
<td>( f_L )</td>
<td>( 0.3 ) m (^3) m (^{-3})</td>
<td>12,20,21,49–52</td>
</tr>
<tr>
<td>( f_{L,oil,w} )</td>
<td>( 0.088 ) kg kg (^{-1}) (98.55 BN)</td>
<td>Measured (^{42})</td>
</tr>
<tr>
<td>( \rho_{oil} )</td>
<td>( 940 ) kg m (^{-3})</td>
<td>Measured</td>
</tr>
<tr>
<td>( \rho_L )</td>
<td>( 2710 ) kg m (^{-3})</td>
<td>55</td>
</tr>
<tr>
<td>( \rho_{SA} )</td>
<td>( 1840 ) kg m (^{-3}) (pure)</td>
<td>56</td>
</tr>
<tr>
<td>( M_{SA} )</td>
<td>( 98.1 \cdot 10^{-3} ) kg mol (^{-1})</td>
<td>Calculated</td>
</tr>
<tr>
<td>( M_L )</td>
<td>( 100.1 \cdot 10^{-3} ) kg mol (^{-1})</td>
<td>Calculated</td>
</tr>
<tr>
<td>( C_{SA,d} )</td>
<td>( 18 \cdot 10^2 ) mol m (^{-3}) (96.5 wt.%)</td>
<td>Calculated</td>
</tr>
<tr>
<td>( \tau )</td>
<td>( 126 ) s</td>
<td>Measured</td>
</tr>
<tr>
<td>( V_{oil} )</td>
<td>( 1.2 \cdot 10^{-4} ) m (^3)</td>
<td>Measured</td>
</tr>
<tr>
<td>( T )</td>
<td>( 327 ) K</td>
<td>Measured</td>
</tr>
<tr>
<td>( \eta ) (327 K)</td>
<td>( 6.2 \cdot 10^{-2} ) kg m (^{1}) s (^{-1})</td>
<td>Calculated (^{47})</td>
</tr>
</tbody>
</table>

Tobias and Klein \(^ {30}\) reported that a typical reverse micelle is roughly spherical, with an average diameter of the \( CaCO_3 \) core of 2.3 nm and a surfactant layer thickness of 0.9 nm. This gives a total diameter of the reverse micelle of 4.1 nm. Hudson et al. \(^ {49}\) reported core diameters in the range 1-10 nm, and a surfactant layer thickness in the range 1-5 nm, yielding total diameters in the range 3-20 nm. Lewis \(^ {21}\) reported an overall diameter in the range 8-18 nm, with core diameters between 4 and 14 nm. On the basis of these results, which are generally in accordance with other reported studies \(^ {12,50–52}\), an average reverse micelle diameter of 10 nm is chosen, and a volume fraction of \( CaCO_3 \) in a reverse micelle, \( f_L \), is estimated to be 0.3. The radius of the \( H_2SO_4 \) droplets will be discussed in Section 4.5.

The average base number (BN) of the lube oil used in the MFR experiments \(^ {38}\) was 98.55, corresponding to a weight fraction of \( CaCO_3 \) in the lube oil of 0.088 kg kg \(^{-1}\). The density of \( CaCO_3 \) was taken from CRC. \(^ {55}\)
4 Mixed flow reactor experiments and modeling of sulfuric acid neutralization in lube oil for large two-stroke diesel engines

density of H₂SO₄ was from Perry⁵⁶ (96.5 wt.% H₂SO₄ solution corresponding to a density of approximately 1840 kg m⁻³), and the density of the lube oil was measured using a scale and measuring glass.

The lube oil temperature in the MFR experiments was around 327 K. The lube oil viscosity was drawn from Sautermeister and Priest,⁴⁷ who measured the dynamic viscosity for a base oil at different temperatures. For the reference conditions, an average lube oil residence time in the reactor is taken as 126 s on the basis of the volumetric feed rate of lube oil, \( v_{oil} \), and the average volume of lube oil, \( V_{oil} \), used in the MFR experiments. The two output variables, \( N_L \) and \( N_{SA} \), can be expressed as the conversion of CaCO₃, \( X_L \), and H₂SO₄, \( X_{SA} \), respectively:

\[
X_L = 1 - \frac{N_L v_o}{N_{l,f} v_{oil,f}} \quad (4.23)
\]

\[
X_{SA} = 1 - \frac{N_{SA} v_o}{F_{SA}} \quad (4.24)
\]

In summary, the model consists of two coupled algebraic equations, Eq. (4.17) and Eq. (4.19), which are solved for \( N_L \) and \( N_{SA} \) by use of Matlab, with the parameter Ca/S as the independent variable. The model parameters presented in this section have been used for the calculations that follow in the next section, unless otherwise stated.

4.5 Validation of mathematical model against MFR results

To validate the model and investigate the rate-controlling step of the neutralization reaction between H₂SO₄ droplets and CaCO₃ reverse micelles, model simulations are compared to experimental data from the MFR, by applying diffusion- and adsorption-controlled reaction rate expressions.

The only parameter not available and required for the analysis is the radius of the H₂SO₄ droplets, \( R_{SA} \). \( R_{SA} \) was fitted to match the experimental data of CaCO₃ conversion from the MFR experiments (Figure 4.5), by use of a “least squares” approach. For the conditions given in Table 4.1, a value of \( R_{SA} \) equal to 0.5 µm was calculated by using the adsorption-controlled reaction rate expression given in Eq. (4.11) and a value of 0.7 µm for the diffusion-controlled reaction rate expression from Eq. (4.5). Goodwin⁴⁵ states that most common emulsions have a particle radius in the range of 1-10 µm. Typical acid and water droplet radii from used engine lube oils are found to be in the range of 2.5-15 µm.⁴₈ This is for a stable emulsion after drainage of the lube oil. Sautermeister and Priest⁴⁷ measured H₂SO₄ droplet sizes in a stable base oil emulsion, measuring radii in the range of 0.25-1.6 µm depending on the H₂SO₄ droplet concentration. Consequently, it is expected that these droplet sizes were instantly formed in the MFR experiments, where large excesses of dispersant and detergent molecules are present in the used lube oil. On the basis of these values from the literature, it is concluded that the radii of 0.5 and 0.7 µm, respectively, fitted from the modeling, are both realistic values. Consequently, it is not possible from the MFR analysis to decide whether the limiting step of the reaction is adsorption or diffusion.

To investigate this in greater detail, the diffusion-controlled reaction rate expression was applied to describe the experimental H₂SO₄ droplet shrinkage data from Fu et al.,²⁴ who visually observed the shrinkage of H₂SO₄ droplets surrounding in a lube oil emulsion. At temperatures in the range 25-170 °C, they monitored...
4.5 Validation of mathematical model against MFR results

the radius-versus-time behavior. The diffusion-controlled reaction rate expression was used to calculate the molar diffusion of CaCO$_3$ reverse micelles from the bulk oil to the droplet surface. This value was then compared to the actual molar conversion rate of the H$_2$SO$_4$. If comparable, this could indicate diffusion control, whereas an excessive molar diffusion of CaCO$_3$ reverse micelle to the droplet, compared to the molar conversion rate of H$_2$SO$_4$, would indicate that diffusion is not the controlling step of the reaction. This scenario is investigated and described in Appendix D. Interestingly, the analysis shows that the molar diffusion of CaCO$_3$ reverse micelles is lower than the actual molar conversion rate of the H$_2$SO$_4$ droplet (a factor of 28.4 at 25 °C and factors of 134-165 at temperatures in the range 100-170 °C). This observation is unexpected, since a diffusion-limited value presumably is the upper limit for the reaction rate. The discrepancy may be due to one of the following two possible explanations: 1) that the calculated diffusion-controlled reaction rate constant (from Eq. (4.3)) underestimates the actual value for the present system (up to a factor 165, see Appendix D); or 2) that an alternative mechanism is occurring that enhances conversion of an H$_2$SO$_4$ droplet in a commercial lube oil.

The first explanation is investigated by implementing the factor of 165 into the diffusion-controlled reaction rate expression for the MFR modeling (with parameters from Table 4.1), and subsequently solving for $R_{SA}$ gives an average radius of the H$_2$SO$_4$ droplets of 9.6 µm, which is still within the range of typical, realistic values.$^{45,47,48}$ This means that, even though the calculated diffusion-controlled reaction rate constant is increased by a factor of 165, a realistic averaged droplet radius is still found. It is therefore difficult to rule out diffusion as the controlling step for the reaction, at least from a computational point of view. Nevertheless, the batch reactor experiments with NaOH, as described in Section 4.3.1, indicated that the droplet-micelle reaction is not diffusion-controlled. In addition, Fu et al.$^{24}$ and Hone et al.$^{31}$ determined activation energies in the range of 54±2 kJ mol$^{-1}$ (see Section 4.1). This magnitude of the temperature-dependency of the reaction rate constant is larger than the temperature-dependency calculated by Eq. (4.3) (if translated to an activation energy, it is equal to 35 kJ mol$^{-1}$ by using the temperature-dependent viscosity measured by Sautermeister and Priest$^{47}$). Based on these arguments, it seems that the reaction between H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles in lube oil is not controlled by diffusion.

With respect to the second explanation, it is possible that another reaction mechanism is occurring. Duan et al.$^{29}$ showed that an H$_2$SO$_4$ droplet is not soluble in oil without additives. However, in a commercial marine lube oil, surfactants are present in great excess, having the task of solubilizing various products into the lube oil that would otherwise precipitate and possibly have adverse consequences for the lubrication of the engine.$^{57}$ It is conceivable that these surfactants may also solubilize the H$_2$SO$_4$ droplet into the bulk lube oil (the empty reverse micelles pull out the H$_2$SO$_4$ to the bulk oil), wherein, presumably, the H$_2$SO$_4$ is immediately converted due to its resulting very small size in the bulk oil. When a micelle adsorbs onto the droplet, it may also be that H$_2$SO$_4$(aq) is transferred into the micelle in a degree that exceeds the molar amount of CaCO$_3$ in a micelle. This may also be the reason why the droplets vanished completely in the experiments by Fu et al.$^{24}$ The H$_2$SO$_4$ is then subsequently converted quickly in the bulk oil. Both of these mechanisms, if active, would contribute to an increased shrinkage rate.

To sum up, from a computational point of view, it is difficult to settle whether the reaction is diffusion- or adsorption-controlled (or if another mechanism is limiting). However, from determined activation energies from literature$^{24,31}$ and the batch reactor experiments with NaOH contained in this work, it is advocated that the reaction is not (entirely) controlled by diffusion. Whether the reaction is then adsorption-controlled or controlled by another mechanism (or a mixture) is difficult to determine. However, either way the reaction rate expression given in Eq. (4.11) provides a quantitative description of the reaction rate and its
temperature-dependency of the droplet-micelle reaction, with a fitted $R_{SA}$ of 0.5 µm, which is based on actual, experimentally determined H$_2$SO$_4$ droplet conversion data from Fu et al. Based on this, Eq. (4.11) is used to describe the apparent reaction rate expression for the droplet-micelle reaction in the remaining part of this work. The corresponding reaction rate constant is likewise denoted as an apparent reaction rate constant, $k_{app}$, in the remaining work.

Modeling predictions for $R_{SA} = 0.5$ µm are compared with the MFR data (Figure 4.5 and Figure 4.6) in Figure 4.8, along with simulations increasing $R_{SA}$ by factors of 5 and 10, respectively. Modeling predictions with $R_{SA} = 0.5$ µm are in good agreement with experimental data, whereas larger droplet sizes lead to an underprediction of the degree of reaction. The predicted conversion of CaCO$_3$ and H$_2$SO$_4$ decreases significantly with increasing droplet radius. At Ca/S = 1, the conversions of H$_2$SO$_4$ and CaCO$_3$ are equal to each other. Here, the conversion decreases by 24 and 37% when the radius increases to 2.5 and 5.0 µm, respectively, relative to the reference conversion (for $R_{SA} = 0.5$ µm). This indicates that larger H$_2$SO$_4$ droplets present in the lube oil film may increase the risk of corrosive wear significantly, because of the surface to volume ratio of the droplets decreasing when the radius increases (i.e., fewer but bigger droplets).

Figure 4.8. Model simulations showing conversion of (a) CaCO$_3$ reverse micelles and (b) H$_2$SO$_4$ droplets as functions of Ca/S by using the reaction rate constant given in Eq. (4.11) at three values of H$_2$SO$_4$ radius, $R_{SA}$. Circles represent MFR experimental data from Figure 4.5 and Figure 4.6. Model parameters are presented in Table 4.1.

4.5.1 Evaluation of model assumptions

The reaction rate constant expression used in the model simulations, Eq. (4.13), is based on the video-microscopy single droplet experiments performed by Fu et al., who reported a shrinking rate. The present model considers only consumption of entire droplets. A model describing the reaction of partly consumed H$_2$SO$_4$ droplets in the lube oil emulsion would have to take into account a size distribution. However, because the droplets are very small in size (~1 µm in radius), and the size distribution mimics a normal distribution with a low standard deviation, one would argue that it is fair to assume that whole droplets are immediately consumed upon reactive contact.

Another difference is the size of the droplets. Fu et al. used initial droplet sizes in the range of 43.6-76.5 µm, reporting that a constant shrinking rate was found up until a certain radius was reached. After this point, the shrinking rate increases. This ‘change point’ was found to occur at around 28 µm at 403 K. Because even
smaller $\text{H}_2\text{SO}_4$ droplets are found in the MFR experiments, the derived reaction rate constant in Eq. (4.13) may underestimate the actual adsorption reaction rate. Further, Wu et al.\textsuperscript{21} reported significantly different shrinking rates for different lube oil formulations having the same BN value. It is not known whether the lube oil used in the study by Fu et al. matches the lube oil used in the MFR experiments.

4.6 Application of the MFR model to conditions in a large two-stroke marine diesel engine

The mixed flow reactor model was developed to interpret the laboratory MFR experiments, while allowing for a validation of the reaction rate expression for the neutralization reaction, which can be used in more complex models. A full simulation of the neutralization reaction at the cylinder liner in a large two-stroke marine diesel engine would require a computational fluid dynamics approach. However, as discussed in the following, the mixed flow reactor model offers a useful approximation to conditions in the lube oil film and can be used to assess the importance of different process parameters. In a large two-stroke marine diesel engine, the lube oil-$\text{H}_2\text{SO}_4$ interactions depend on the piston movement (see Figure 4.9).

![Figure 4.9. Illustration of lube oil dosage, $\text{H}_2\text{SO}_4$ droplet condensation, and mixing in an engine: (a) piston approaching top dead center (TDC), when fresh lube oil is dosed onto the piston ring pack\textsuperscript{59} (the injection frequency of fresh lube oil is typically once every third to eighth engine revolution); (b) $\text{H}_2\text{SO}_4$ condensing onto the lube oil film when the piston moves toward the bottom dead center (BDC); (c) piston moving toward TDC again, contributing to a well-mixed lube oil film where the $\text{H}_2\text{SO}_4$ droplets are emulsified in the lube oil; and (d) horizontal close-up of a piston ring-lube oil film, where a moving front may develop where the lube oil and $\text{H}_2\text{SO}_4$ droplets are effectively mixed.](image-url)
Dosing of the lube oil into the piston ring pack occurs during the piston’s upward stroke (Figure 4.9(a)). When the piston is at the top dead center (TDC) and moves downward (expansion stroke, Figure 4.9(b)), H$_2$SO$_4$ condensates as droplets (either dilute or pure) onto the distributed lube oil film on the cylinder liner surface. It is believed that condensed H$_2$SO$_4$ forms a thin film on top of the layer of lube oil film. The condensation of H$_2$SO$_4$ occurs in the gas phase just before reaching the lube oil film, where the temperature is lower than in the bulk gas phase. Because no mixing is occurring, transport of CaCO$_3$ micelles to the H$_2$SO$_4$ happens by diffusion. However, when the piston moves toward TDC (compression stroke, Figure 4.9(c)), the piston rings act to spread and remove excess lube oil from the cylinder liner. The high velocity of the piston may lead to effective mixing of the condensed H$_2$SO$_4$ and lube oil at the moving front, in front of the piston ring, thereby emulsifying the H$_2$SO$_4$ droplets into the lube oil (Figure 4.9(d)). After the piston has passed a specific point, the local lube oil film may be left stagnant, allowing the H$_2$SO$_4$ to react with the cast iron liner until the next time the piston passes by, when it once again mixes the lube oil film emulsion. The cycle is repeated roughly every 0.5 s, which is the time for one stroke. However, fresh lube oil is not injected in every cycle but instead typically at every third to eighth engine revolution. The cast iron wall temperature would be in the range 373-533 K, and highest in the upper part of the cylinder, whereas the lube oil film is expected to attain the same temperature because of the high heat capacity and thermal conductivity of the cast iron.

From an idealized perspective, two lube oil-H$_2$SO$_4$ interaction scenarios may take place. The first scenario involves condensation of H$_2$SO$_4$ onto the lube oil film during the expansion stroke, followed by diffusion of the H$_2$SO$_4$ through the lube oil film to the cylinder liner (Figure 4.9(b)). In the second scenario, the H$_2$SO$_4$ droplets are fully mixed with the lube oil by the action of the piston (Figure 4.9(d)). In scenario 1, transport of H$_2$SO$_4$ through the lube oil film toward the cylinder liner takes place by droplet diffusion. The diffusion coefficient, $D_{SA}$, can be estimated by the Stokes-Einstein relation given in Eq. (4.4). Taking the lube oil dynamic viscosity from Sautermeister and Priest and assuming that the radius of the diffusing H$_2$SO$_4$ droplets is similar to that of the MFR experiments (0.5 µm), the diffusion coefficient is on the order of $10^{-12}$ m$^2$ s$^{-1}$ at 533 K, decreasing to about $10^{-14}$ m$^2$ s$^{-1}$ at 373 K. The mean Brownian displacement, $\bar{x}$, of a droplet after a specific time, $t$, can then be calculated by:

$$\bar{x} = \sqrt{2D_{SA}t}$$  \hspace{1cm} (4.25)

In the diffusion scenario, the H$_2$SO$_4$ droplet has 0.5 s to reach the cylinder liner before the piston returns and mixes the H$_2$SO$_4$ film with the lube oil film. Within 0.5 s, the H$_2$SO$_4$ droplet moves 1 µm at 533 K and 0.1 µm at 373 K, according to Eq. (4.25). The minimum lube oil film thickness, which is in the upper part of the cylinder, is between 2 and 5 µm in a full-scale application. Unless the diffusing H$_2$SO$_4$ droplets are significantly smaller than the assumed value of 0.5 µm, it appears that little H$_2$SO$_4$ penetrates through the lube oil film on the cylinder liners in a film-film situation (Figure 4.9(b)). This finding is further supported by the fact that the lube oil is hydrophobic and the H$_2$SO$_4$ droplets hydrophilic.

The second lube oil-H$_2$SO$_4$ interaction scenario involves mixing between the H$_2$SO$_4$ film and the lube oil film by the piston rings at the moving front in front of the piston ring (Figure 4.9(d)). Presumably, this corresponds to a situation where the H$_2$SO$_4$-lube oil film is well-mixed. In this scenario, H$_2$SO$_4$ will be present on the wall and able to interact with the cylinder liner material. Every cycle serves to mix and replenish the lube oil and H$_2$SO$_4$ locally. The residence time of a H$_2$SO$_4$ droplet on the cylinder liner is
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assumed to be low because of the well-mixed situation. Even though the average residence time of a lube oil film in a cylinder liner is estimated to be a couple of minutes, the neutralization of H$_2$SO$_4$ has to be significantly faster to avoid reaction with the cylinder liner material. In a two-stroke marine diesel engine, the piston passes by a specific point on the cylinder liner twice per revolution. If rated at 70 rpm, the time for each stroke is around 0.5 s. The contact time for H$_2$SO$_4$ and lube oil may vary, however, depending on the vertical position on the cylinder liner. In the upper part, the gas phase contact time with the lube oil is the longest, allowing more time for the H$_2$SO$_4$ to condense. The temperature is higher, counteracting condensation, but the pressure is also higher, thereby increasing the dew point temperature. Thus, 0.5 s is an important time scale for the lube oil to neutralize H$_2$SO$_4$ and prevent it from reacting with the liner material.

With these considerations, scenario 2 appears most relevant because of the extent of interaction of H$_2$SO$_4$ with the cylinder liner material. Presumably, upon mixing with the lube oil film, H$_2$SO$_4$ becomes readily emulsified because of the large excess of detergents and dispersants in the lube oil, forming a stable emulsion. Thereby, conditions locally at the liner resemble those described by the MFR model: a well-mixed lube oil volume with a constant initial Ca/S molar ratio.

An average lube oil flow rate to the cylinder liner can be estimated to be $3.9 \times 10^{-7}$ m$^3$ s$^{-1}$ on the basis of the assumption that a 30 MW engine with eight cylinders at 50% load consumes 0.7 g kWh$^{-1}$. For typical dimensions of the cylinder liner and a lube oil thickness of 10 µm, an average lube oil residence time of 220 s is estimated, which is a value in accordance with the residence time applied in the MFR experiments. However, despite the efficient mixing caused by the piston, the full lube oil volume in a cylinder cannot be approximated as a single mixed flow reactor. In the full-scale application, the lube oil film thickness varies vertically, as does the H$_2$SO$_4$ condensation rate, because varying amounts of H$_2$SO$_4$ may condense locally on the cylinder liners. Moreover, the mathematical model can provide estimates of the degree of conversion of the condensing H$_2$SO$_4$ at confined, local points in a large two-stroke marine diesel engine. This corresponds to the discretizing of the vertical direction of the lube oil film into smaller volumes, assuming that each volume has the behavior as a mixed flow reactor. The model can then be used to predict the conversion of H$_2$SO$_4$ at specific local initial conditions, such as Ca/S and temperature.

4.6.1 Parametric study

In the following, a parametric study is presented with the aim of investigating the neutralization reaction at conditions representative for a large two-stroke marine diesel engine. This gives an indication of how the reaction would progress in a realistic application. For this purpose, reference case simulation parameters are defined as $T = 423$ K, $\tau = 0.5$ s, $f_{L,oil,lw} = 0.089$ kg kg$^{-1}$ (100 BN), and $C_{SA,t} = 18 \times 10^3$ mol m$^{-3}$. The remaining parameters used in the model simulations are based on the ones presented in Table 4.1. The effect of lube oil temperature is investigated in the range of 373 to 533 K, corresponding to the cylinder liner temperature range in a two-stroke marine diesel engine. Lube oils with different BN values are used in service, depending on the sulfur content in the burned fuel; therefore, the effects of using 70 and 140 BN are also investigated. Depending on the operating conditions, different concentrations of H$_2$SO$_4$ droplets can condense onto the lube oil film in a real engine application. The range from concentrated ($18 \times 10^3$ mol m$^{-3}$) to very dilute H$_2$SO$_4$ droplets ($1.8 \times 10^3$ mol m$^{-3}$) is therefore examined. Wu et al. found that the shrinking rate of acid droplets depends on the lube oil formulation (i.e., different lube oils may not have identical reaction rate constants). Therefore, the effect of varying the reaction rate constant is studied.
4.6.1.1 Lube oil formulation

Figure 4.10 shows the effects of the apparent reaction rate constant and H$_2$SO$_4$ droplet radius on the conversion, with the reference case value varying by a factor of 5. Increasing $k_{app}$ by a factor of 5 corresponds to decreasing $R_{SA}$ by a factor of 5.

Figure 4.10. Model simulations showing conversion of (a) CaCO$_3$ reverse micelles and (b) H$_2$SO$_4$ droplets as functions of Ca/S at three values of $k_{app}$ and $R_{SA}$. The model parameters are $T = 423$ K, $\tau = 0.5$ s, $f_{L,\text{oil},w} = 0.089$ kg kg$^{-1}$ (100 BN), and $C_{SA,d} = 18 \cdot 10^3$ mol m$^{-3}$, as well as those in Table 4.1.

A significant adverse effect is observed when decreasing the reaction rate constant (increasing $R_{SA}$). It shows that in order to enhance the performance of a specific lube oil with respect to neutralization, the oil should be formulated to increase the reaction rate constant. The simulations also suggest that the lube oil should be formulated with surfactants capable of emulsifying the H$_2$SO$_4$ sufficiently. If H$_2$SO$_4$ is poorly emulsified in the lube oil, resulting in enlarged droplets, significant amounts of H$_2$SO$_4$ may reach the cylinder liner material.

4.6.1.2 Base number

An important property of the lube oil is the base number (BN, i.e., CaCO$_3$ concentration). The effect of varying the BN in the lube oil is shown in Figure 4.11. The volumetric inlet flow rate, $v_{oil,f}$, is kept unchanged when the BN of the lube oil is altered. The weight fraction of CaCO$_3$ in the lube oil, $f_{L,\text{oil},w}$, is changed, affecting the number of micelles in the inlet lube oil (Eq. (4.20)), $N_{L,f}$, and also the H$_2$SO$_4$ droplet flow to the lube oil volume (Eq. (4.22)), $F_{SA}$. Figure 4.11 shows that the conversion of H$_2$SO$_4$ increases slightly with the BN of the lube oil at a constant Ca/S molar ratio. For a Ca/S equal to 1, the conversion increases by 5% when the lube oil BN increases from 100 to 140 BN, and it decreases by 6% when a 100 BN lube oil is switched to a 70 BN lube oil. This is due to the higher concentrations of CaCO$_3$ and H$_2$SO$_4$, resulting in an increase in the reaction rate. The results indicate that it could be beneficial to use a higher BN lube oil in combination with a decreased lube oil feed rate (maintained Ca/S value). However, there is a tradeoff because a reduced oil feed rate may lead to exposure of the liner surface and insufficient lubrication leading to scuffing, for example.
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Figure 4.11. Model simulations showing conversion of (a) CaCO₃ reverse micelles and (b) H₂SO₄ droplets as functions of Ca/S at three values of the base number of the lube oil. The model parameters are $R_S = 0.5 \, \mu m$, $T = 423 \, K$, $\tau = 0.5 \, s$, and $C_{SA,d} = 18 \cdot 10^3 \, mol \, m^{-3}$, as well as those in Table 4.1.

### 4.6.1.3 Concentration of H₂SO₄ droplets

The effect of varying the concentration of the H₂SO₄ droplets is investigated in Figure 4.12. At a Ca/S molar ratio equal to 1, the conversion of H₂SO₄ increases by 10 and 23%, respectively, when the H₂SO₄ droplet concentration is diluted by factors of 5 and 10 compared with the reference value. When the H₂SO₄ droplet concentration decreases, the H₂SO₄ droplet flow, $F_{SA}$, is increased to maintain a constant Ca/S molar ratio. The number of H₂SO₄ droplets emulsified into the lube oil film is thereby increased, but they are more dilute. This leads to an increase in the reaction rate according to Eq. (4.11), and consequently a higher conversion is found for decreasing H₂SO₄ droplet concentration. However, the effect is minor compared with that of changing $k_{app}$ and $R_S$ (Figure 4.10).

Figure 4.12. Model simulations showing conversion of (a) CaCO₃ reverse micelles and (b) H₂SO₄ droplets as functions of Ca/S at three values of H₂SO₄ droplet concentration. The model parameters are $R_S = 0.5 \, \mu m$, $T = 423 \, K$, $\tau = 0.5 \, s$, and $f_{L,oiw} = 0.089 \, kg \, kg^{-1}$ (100 BN), as well as those in Table 4.1.
The simulations in Figure 4.12 show an opposite effect from decreased \( \text{H}_2\text{SO}_4 \) concentration as compared with that in the MFR experiments, where a decrease in \( \text{H}_2\text{SO}_4 \) concentration from \( 18 \cdot 10^3 \) to \( 5 \cdot 10^3 \) mol m\(^{-3} \) led to a small reduction in conversion.\(^{38} \) However, significantly more water was introduced in the MFR experiments when decreasing the \( \text{H}_2\text{SO}_4 \) concentration and maintaining the Ca/S molar ratio. This may have reduced the solubilization of the \( \text{H}_2\text{SO}_4 \) droplets because of the limited amount of excess of dispersants and detergents in the lube oil, resulting in enlarged droplets. As shown in Figure 4.8, larger \( \text{H}_2\text{SO}_4 \) droplets result in a reduction in the conversion. The isolated effect of changing the \( \text{H}_2\text{SO}_4 \) droplet concentration may therefore be difficult to assess experimentally. Another explanation for the difference between the experimental and modeling results could lie in the assumption of the model that the used reaction rate constant does not depend on the \( \text{H}_2\text{SO}_4 \) droplet concentration. Duan et al.\(^{54} \) show that the shrinking rate \( (dR_{SA}/dt) \) of acetic acid droplets in fully formulated passenger-car lube oil decreases when the acetic acid droplet concentration is decreased. Also, Fu et al.\(^{26} \) report that the shrinking rate of a droplet of pure water is about 1 magnitude lower than that of a \( \text{H}_2\text{SO}_4 \) droplet. This suggests that the shrinking rate depends on the nature, chemical interactions, and concentration of the droplets. Local condensation of strongly diluted \( \text{H}_2\text{SO}_4 \) droplets will increase the water content of the lube oil emulsion. This could possibly lead to disruption of the lube oil film and direct \( \text{H}_2\text{SO}_4 \)-metal contact, causing accelerated corrosion of the cylinder liner material,\(^{62,63} \) especially at a low Ca/S molar ratio (Figure C.1 in Appendix C).

4.6.1.4 Residence time

The effect of reaction time is investigated in Figure 4.13. It is done by fixing the volume of the lube oil film and only changing the volumetric inlet lube oil flow rate, \( v_{\text{oil, in}} \). The conversion increases with residence time, as expected. At a Ca/S equal to 1, the conversion decreases by 35% when the residence time is decreased from 0.5 to 0.1 s, and increases 22% when the residence time is increased from 0.5 to 2.5 s. In the MFR experiments, no effect of residence time in the range from 48 to 210 s at Ca/S molar ratios around 1.4 and 2.0 was found.\(^{38} \) However, the model predicts an increase in the conversion of CaCO\(_3\) by 17% at Ca/S = 1.4 when the residence time is increased from 48 to 210 s in the MFR (Figure C.2 in Appendix C).

![Figure 4.13](image-url)
In Figure 4.14, the conversion of CaCO$_3$ (Figure 4.14(a)) and H$_2$SO$_4$ (Figure 4.14(b)) is shown as a function of residence time for three different Ca/S molar ratios. According to the predictions, the neutralization is initially very fast at engine conditions. This is in agreement with the findings of Roman, who performed stirred thin lube oil film batch reactor experiments with a Ca/S molar ratio of around 0.5, a 100 BN lube oil, and a temperature of 373 K. He concluded that the reaction is extremely rapid and takes place within only a few seconds before reaching a plateau with a significantly reduced reaction rate. Modeling simulations for the same conditions as those of Roman indicate a 50% conversion of CaCO$_3$ within 0.4 s, whereas 90% conversion is achieved for a residence time of 5 s. These values are roughly in agreement with the ones given by Roman.

![Figure 4.14. Model simulations showing conversion of (a) CaCO$_3$ reverse micelles and (b) H$_2$SO$_4$ droplets as functions of residence time at three values of Ca/S. The model parameters are $R_{SA} = 0.5$ $\mu$m, $T = 423$ K, $f_{L, oil,w} = 0.089$ kg kg$^{-1}$ (100 BN), and $C_{SA,d} = 18 \cdot 10^3$ mol m$^{-3}$, as well as those in Table 4.1.](image)

4.6.1.5 **Lube oil temperature**

The effect of the lube oil temperature in the range 373 to 533 K is investigated in Figure 4.15. The model predicts a significant effect of temperature on conversion. The H$_2$SO$_4$ is almost fully neutralized after 0.5 s when the temperature is higher than 473 K and Ca/S>1 (Figure 4.15(b)). For instance, 92.5% H$_2$SO$_4$ is neutralized after 0.5 s at 533 K at Ca/S = 1. When H$_2$SO$_4$ is in great excess (e.g. Ca/S = 0.1), the CaCO$_3$ is almost completely depleted locally at these temperatures.

At 373 K (i.e., the lower end of the liner temperature in a two-stroke marine diesel engine), a significant fraction of the H$_2$SO$_4$ is not neutralized, and the H$_2$SO$_4$ has the potential of interacting with the cylinder liner surface during the stagnant period until the next mixing stroke.
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Figure 4.15. Model simulations showing conversion of (a) CaCO$_3$ reverse micelles and (b) H$_2$SO$_4$ droplets as functions of Ca/S at varying temperatures between 373 and 533 K. The model parameters are $R_{SA} = 0.5$ µm, $\tau = 0.5$ s, $f_{\text{oil,w}} = 0.089$ kg kg$^{-1}$ (100 BN), and $C_{SA,d} = 18 \cdot 10^3$ mol m$^{-3}$, as well as those in Table 4.1. The vertical dotted line represents Ca/S = 1.

By use of Eq. (4.6), it is possible to calculate the average concentration of H$_2$SO$_4$ in the lube oil film emulsion after 0.5 s of reaction time after mixing by the passing piston rings and thereby also at the cylinder liner surface during the stagnant time period (see Figure 4.16). The H$_2$SO$_4$ concentration increases dramatically for Ca/S < 1, showing that it is important to avoid a local excess of H$_2$SO$_4$ compared with CaCO$_3$ on the cylinder liner surface, in order to minimize corrosion and wear of the cylinder liner and piston rings. The concentration of H$_2$SO$_4$ decreases with increasing lube oil temperature, as expected from Figure 4.15.

Figure 4.16. Model simulations showing the average concentration of H$_2$SO$_4$ in the lube oil film as a function of Ca/S at varying temperatures between 373 and 533 K. The model parameters are $R_{SA} = 0.5$ µm, $\tau = 0.5$ s, $f_{\text{oil,w}} = 0.089$ kg kg$^{-1}$ (100 BN), and $C_{SA,d} = 18 \cdot 10^3$ mol m$^{-3}$, as well as those in Table 4.1. The vertical dotted line represents Ca/S = 1.
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The results of Figure 4.15 and Figure 4.16 indicate that the H$_2$SO$_4$ is likely to reach the cylinder liner surface no matter how well lubricated the surface is. However, a certain degree of corrosion may be beneficial in order to maintain a rough cylinder liner surface for supporting a lube oil film.$^{11}$

4.6.2 Practical implications

The parametric study indicates that the neutralization of H$_2$SO$_4$ and the interaction of H$_2$SO$_4$ with the liner surface is a complex function of lube oil formulation; the flow pattern at the cylinder liner (mixing behavior); and the vertical, local position at the cylinder liner (which affects the lube oil temperature, the residence time, and the concentration of condensing H$_2$SO$_4$). The upper part of the cylinder liner is the segment where the most severe wear is found.$^{3,64}$ In this section, possible factors affecting the presence of H$_2$SO$_4$ at the liner surface in the upper region are discussed.

The cylinder liner temperature in the upper part is high.$^{1}$ Consequently, a decrease in H$_2$SO$_4$ condensation rate would be expected,$^{58}$ and the neutralization reaction would be fast (Figure 4.16), both ultimately contributing to a reduction in wear.$^{1,12}$ However, the pressure in the cylinder liner is highest when the piston is near top dead center (TDC) upon combustion (thus SO$_3$/H$_2$SO$_4$ partial pressures are highest near TDC), resulting in a high dew point temperature of H$_2$SO$_4$(aq) in this area.$^3$ Furthermore, the upper part of the cylinder is exposed to the combustion gas for the longest length of time.$^1$ Despite the higher temperature, most of the H$_2$SO$_4$ formed from oxidation of the fuel sulfur may thus condense on the upper part of the cylinder liner segment, as reported.$^7,58$ A high load of H$_2$SO$_4$ in the lube oil in this region could also be facilitated by the upward motion of the piston, collecting the condensed H$_2$SO$_4$ above the top piston ring.$^{26}$ The upper part of the cylinder is also the area where the piston speed is the lowest,$^1$ decreasing the degree of mixing of the lube oil film, and the lube oil film thickness is at its minimum.$^{60}$ A local excess of H$_2$SO$_4$ compared with CaCO$_3$ in the upper part of the cylinder liner would explain the corrosive wear that has been observed. In addition, more water is known to condense in the upper part of the cylinder,$^7$ increasing the risk of direct H$_2$SO$_4$-liner contact through disruption of the lube oil film.$^{62,63}$

One method to reduce the wear would be to increase the flow rate of lube oil and thereby the local Ca/S molar ratio in the upper segment. For a constant thickness of the lube oil film, the average residence time depends on the engine load and the feed rate of lube oil. When increasing the feed rate and the engine load, the average residence time decreases.$^{3,65}$ However, at the same time, more CaCO$_3$ is introduced, increasing the Ca/S molar ratio. The effect of increasing Ca/S is considerable when Ca/S<1.5, according to Figure 4.15. A lower engine load leads to a lower piston velocity, thus increasing the exposure time between lube oil and H$_2$SO$_4$. This gives more time for the neutralization reaction to occur, but it also gives more time for non-neutralized H$_2$SO$_4$ in the lube oil emulsion to react with the cylinder liner material at stagnant conditions. The Ca/S molar ratio can also be increased by using higher BN lube oil. According to the present work, increasing the BN of the lube oil at maintained Ca/S molar ratio, would lead to a slightly faster neutralization of H$_2$SO$_4$, thereby decreasing the contact between H$_2$SO$_4$ and the liner and consequently the corrosion. This is in accordance with experiences from service.$^1$

The above analysis shows that the prevention of cold corrosion is a complex challenge. H$_2$SO$_4$ will be present at the cylinder liner surface to some degree regardless of how well-lubricated the surface is. It is therefore more a matter of how much H$_2$SO$_4$ can be neutralized in the shortest period of time, in order to prevent undesired corrosion in large two-stroke marine diesel engines.
4.7 Conclusions

The reaction between H$_2$SO$_4$ droplets and CaCO$_3$ micelles in lube oil has been studied in a well-mixed flow reactor and a batch reactor at Ca/S molar ratios, relevant for a real engine application. The purpose was to isolate the rate-limiting steps of the neutralization mechanism, potentially a single one. For the residence times investigated, the results showed that the reactant conversion was significantly reduced when the Ca/S molar ratio approached unity. It was also found, that a certain degree of stirring is required to establish contact between H$_2$SO$_4$ droplets and CaCO$_3$ reverse micelles in order to initiate and maintain the reaction, probably to effectively emulsify H$_2$SO$_4$ into the lube oil.

A mathematical model for the neutralization of H$_2$SO$_4$ droplets by CaCO$_3$ reverse micelles in lube oil under mixed-flow conditions has been developed and verified by using mixed flow reactor experimental data obtained by the authors. It was difficult to identify conclusively the limiting step of the neutralization reaction, however, a quantitative description of the reaction rate and its temperature-dependency was determined. The mixed flow reactor model offers a useful approximation of conditions in the lube oil film on the cylinder liner and can be used to assess the importance of different process parameters. The neutralization reaction rate increases significantly with the lube oil temperature, whereas the lube oil base number and the H$_2$SO$_4$ droplet concentration have only a minor impact at a maintained Ca/S molar ratio. Modeling predictions indicate that H$_2$SO$_4$ will be present to some degree on the cylinder liner surface, independent of how well-wetted the liner is. The concentration of H$_2$SO$_4$ in the lube oil film is significantly increased for conditions with a local molar excess of H$_2$SO$_4$ compared with CaCO$_3$ micelles (Ca/S<1). To control the corrosion rate, it is important to ensure that sufficient lube oil is provided in critical regions, particularly at the upper part of the cylinder liner where the most pronounced wear is most often found.

Both the derived reaction kinetics, which can be used in computational fluid dynamics (CFD) models, and the mathematical model are expected to facilitate further studies to understand and control corrosion and wear in large two-stroke marine diesel engines. By connecting the knowledge of where H$_2$SO$_4$ is condensing with how it is neutralized (the present article), it may be possible to optimize the spatial lube oil dosage onto the cylinders to counteract severe corrosive wear.

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Nomenclature

- $A_i$ = Surface area of component $i$ (4π$R_i^2$) [m$^2$]
- $BN$ = Base number [(mg KOH) (g oil)$^{-1}$]
- $Ca/S$ = Molar ratio of CaCO$_3$ to H$_2$SO$_4$ in inlet feed [mol mol$^{-1}$]
- $C_i$ = Concentration of component $i$ [mol m$^{-3}$]

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$C_{SA,d} = $ Concentration of H$_2$SO$_4$ in droplets [mol m$^{-3}$]
$\text{d}_c = $ Critical distance where immediate reaction occurs [m]
$D_i = $ Diffusion coefficient of component $i$ [m$^2$ s$^{-1}$]
$E_a = $ Activation energy [J mol$^{-1}$]
$F_{SA} = $ H$_2$SO$_4$ droplet number flow [(number of droplets) s$^{-1}$]
$f_L = $ Volume fraction of CaCO$_3$ in reverse micelle [m$^3$ m$^{-3}$]
$f_{L,\text{oil},w} = $ Weight fraction of CaCO$_3$ in lube oil [kg kg$^{-1}$]
$i = $ Component $i$ [-]
$k_{ads} = $ Adsorption-controlled reaction rate constant [m s$^{-1}$]
$k'_{ads} = $ Adsorption-controlled reaction rate constant [m$^3$ mol$^{-1}$ s$^{-1}$]
$k_{app} = $ Apparent reaction rate constant [m s$^{-1}$]
$k_B = $ Boltzmann constant, $1.38 \times 10^{-23}$ [kg m$^2$ s$^{-2}$ K$^{-1}$]
$k_{diff}/k'_{diff} = $ Diffusion-controlled reaction rate constant [m$^3$ mol$^{-1}$ s$^{-1}$]
$k_{res} = $ Resulting reaction rate constant [m$^3$ mol$^{-1}$ s$^{-1}$]
$M_i = $ Molar weight of component $i$ [kg mol$^{-1}$]
$N = $ Stirrer speed [rpm]
$N_A = $ Avogadro’s constant, $6.022 \times 10^{23}$ [molecules mol$^{-1}$]
$n_i = $ Moles of component $i$ [mol]
$N_i = $ Number of component $i$ per volume [number m$^{-3}$]
$N_{i,f} = $ Number of component $i$ per volume in inlet feed [number m$^{-3}$]
$n_{L,M} = $ Moles of CaCO$_3$ per reverse micelle [mol]
$-r_{Ai} = $ Reaction rate [mol m$^{-3}$ s$^{-1}$]
$R = $ Ideal gas constant, $8.314$ [J mol$^{-1}$ K$^{-1}$]
$R_i = $ Radius of component $i$ [m]
$t = $ Time [s]
$T = $ Temperature in lube oil volume [K]
$V_i = $ Average volume of component $i$ ($4/3 \pi R_i^3$) [m$^3$]
$\nu_{L,f} = $ Volumetric feed rate of component $i$ [m$^3$ s$^{-1}$]
$\nu_o = $ Volumetric outflow of lube oil emulsion [m$^3$ s$^{-1}$]
$V_{oil} = $ Volume of lube oil in mixed flow reactor [m$^3$]
$\bar{x} = $ Mean Brownian displacement of a particle [m]
$X_i = $ Conversion of component $i$ [-]

Greek Letters
$\eta = $ Lube oil dynamic viscosity [kg m$^{-1}$ s$^{-1}$]
$\theta = $ Fraction of surface that is occupied [-]
$\rho_i = $ Density of component $i$ [kg m$^{-3}$]
$\tau = $ Residence time [s]

Subscripts
ads = Adsorption-controlled
app = Apparent
diff = Diffusion-controlled
d = Droplet
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f = Inlet feed  
L = Limestone, CaCO₃ or CaCO₃ reverse micelle  
o = Outlet  
Oil = Lube oil  
SA = Sulfuric acid, H₂SO₄ or H₂SO₄ droplet  
w = weight

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Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines

This chapter is a manuscript in preparation for submission. The supporting information for this chapter can be found in Appendix E.

Abstract

When sulfur-rich fuel is burned in diesel engines, SO$_2$ is formed, which may oxidize and react with water to form corrosive H$_2$SO$_4$. However, the gaseous SO$_2$ may also consume CaCO$_3$-containing reverse micelles present in lube oil. This study investigates the reaction in a batch reactor setup. The SO$_2$-CaCO$_3$ reaction exhibits a weak temperature dependence because the absorption of SO$_2$ in the lube oil emulsion decreases at increased temperature. Further, due to increased SO$_2$ absorbance, the reaction shows high dependence on the initial water concentration. The conversion of CaCO$_3$ is quantified and the resulting products are determined by Fourier Transform Infrared Spectroscopy (FTIR). Initially, CaSO$_3$ is formed, but CaSO$_4$ is also observed at extended residence times and increased temperature. A mathematical model is set up and kinetic parameters are determined by fitting the model to the experimental data. The batch reactor model is then used to predict CaCO$_3$ conversions in lube oil from SO$_2$ for worst-case conditions relevant for a full-scale engine application. Simulations show that consumption of CaCO$_3$ from SO$_2$ is insignificant in a two-stroke marine diesel engine application and that the H$_2$SO$_4$-CaCO$_3$ reaction is far more important than the SO$_2$-CaCO$_3$ reaction.
5 Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines

5.1 Introduction

Due to introduction of the so-called slow-steaming approach, where large vessels began to operate at a lower load (speed), and new engine designs and tunings, the maritime sector has experienced increased sulfuric acid (H$_2$SO$_4$) condensation, originating from the fuel sulfur, leading to abnormal corrosive wear of the cylinder liner and piston rings.$^{1-4}$ To control corrosion, lubrication (lube) oils are formulated with base additives, commonly present as nanometer-sized CaCO$_3$ micelles.$^{5-7}$ At present, in some specific control areas, it is allowed to operate with a high sulfur content in the fuel if using an exhaust cleaning technology capable of reducing the emissions to a level equivalent to that of burning low-sulfur fuel.$^{8,9}$ Depending on price and availability, it may therefore be cost-effective to burn high sulfur fuels in the future, and even burning fuels with a sulfur content higher than today’s limit of 3.5 wt.%. As the fuel burned switches and new engine designs are introduced, the lube oil dosing has to conform to maintain its satisfactory performance.

A defective dosing of lube oil has severe consequences, such as scuffing (direct metal to metal contact).$^{10,11}$ It is therefore crucial to have general guidelines on how lube oil should be dosed onto the cylinder liners in order to limit corrosion at a minimal cost. To achieve this, understanding of the formation of the relevant acids in the gas phase,$^{10,12-14}$ the transport to the lube oil film,$^{15-17}$ the neutralization mechanism by the base additives,$^{17-34}$ and the corrosion of the liner material$^{14,35-43}$ is pivotal. Information about how base additives (CaCO$_3$ micelles) are consumed is essential because this assists determination of the lube oil flow rate to the cylinder liners and its base additive concentration. In line with this, the neutralization mechanism between CaCO$_3$ micelles and H$_2$SO$_4$ droplets has been investigated and the corresponding reaction rate was determined.$^{19,21}$ Research has mainly been focused on H$_2$SO$_4$ which is thought to be the main cause for the observed corrosive wear and CaCO$_3$ consumption.$^{4,36}$ However, some studies claim that SO$_2$ can also contribute directly to corrosive wear and CaCO$_3$ consumption.$^{4,44-48}$ If this is the case, determination of reaction kinetics of the CaCO$_3$-SO$_2$ reaction, and the relative importance to the CaCO$_3$-H$_2$SO$_4$ reaction would allow for an assessment of what consumes the CaCO$_3$ reverse micelles. Nagaki and Korematsu$^{46,47}$ advocate that SO$_2$ absorbs into the lube oil film in an engine and forms H$_2$SO$_4$, which subsequently reacts with the cylinder liner and/or CaCO$_3$. Naegeli and Marbach$^{48}$ likewise found an increased wear rate for increasing SO$_2$ addition to the intake air through the formation of sulfurous acid (H$_2$SO$_3$). The formation of H$_2$SO$_3$ in lube oil may also contribute to consumption of CaCO$_3$. However, both research groups added the SO$_2$ to the intake air and one may speculate if this contributed to increased SO$_2$(g) formation upon the compression stroke and thereby increased the condensation rate of H$_2$SO$_4$. The isolated effect of SO$_2$ on consumption of CaCO$_3$ in lube oil is therefore not clear. Nevertheless, it is known from other research fields that SO$_2$ does indeed react with CaCO$_3$ e.g., in wet flue gas desulfurization (FGD) plants.$^{49,50}$ Here, SO$_2$ is removed (scrubbed) from flue gas by reacting with CaCO$_3$ in an aqueous slurry:$^{49}$

\[
\begin{align*}
\text{SO}_2 + \text{H}_2\text{O} & \rightarrow \text{H}^+ + \text{HSO}_3^- \\
\text{HSO}_3^- & \rightarrow \text{H}^+ + \text{SO}_3^{2-} \\
2\text{HSO}_3^- + \text{O}_2 & \rightarrow 2\text{H}^+ + 2\text{SO}_4^{2-} \\
\text{Ca}^{2+} + \text{SO}_4^{2-} + 2\text{H}_2\text{O} & \rightarrow \text{CaSO}_4\cdot2\text{H}_2\text{O(s)}
\end{align*}
\]

This means that SO$_2$ reacts with CaCO$_3$ to form CaSO$_4$, which is the same product when CaCO$_3$ is reacting with H$_2$SO$_4$. However, if the system is not saturated with O$_2$, the following may happen.$^{49}$
The above illustrates that, besides CaCO$_3$ and SO$_2$, water and O$_2$ have to be present in the reaction system. The reactions only happen when water is present because SO$_2$ is absorbed into the water according to Eq. (5.1). Furthermore, the reaction between gaseous SO$_2$, in a humid simulated flue gas, and CaCO$_3$ particles has been investigated in a sand bed reactor. Here, it was found that the oxygen content in the simulated flue gas (0-9%) had a minor effect on the initial reaction rate, whereas the relative humidity (0.24-0.92) and particle diameter (4-100 µm) had significant effects. Also, the temperature dependency of the reaction indicated a weak dependency (investigated in the range 40-80 °C). At 23 °C in another study, both in presence and absence of water, the reaction between gaseous SO$_2$ and CaCO$_3$ particles was investigated, finding that both CaSO$_3$ and CaSO$_4$ were formed and that the reaction was significantly enhanced when water was present. However, dissimilarities exist between the reaction conditions of the above-mentioned examples and the conditions prevailing in a lube oil film; the most crucial one being the presence of the lube oil phase itself. However, precursors for a successful reaction may be present in a lube oil film in an engine: plenty of condensing water, plenty of SO$_2$ and O$_2$ in the combustion chamber, reactive CaCO$_3$ reverse micelles, and that SO$_2$ absorbs in oil.

The scope of the present work is to investigate the reaction between gaseous SO$_2$ and CaCO$_3$ reverse micelles in lube oil in the presence of water and O$_2$, and more specifically to decide if SO$_2$ is able to consume any of the CaCO$_3$ in the lube oil. The components are pressurized in a batch reactor setup at specific conditions such as residence time, Ca/S molar ratio, pressure, temperature, and water content. Upon an experiment, the lube oil is analyzed and the conversion of CaCO$_3$ and the products are determined. Reaction kinetics is derived by setting up a model of the batch reactor setup, followed by fitting of the model to the experimental data. The mathematical model is then used to investigate the importance of the SO$_2$-CaCO$_3$ reaction at specific marine diesel engine conditions.

5.2 Experimental section

5.2.1 Materials

Lube oil from Infineum, with a base number (BN) value of 100±2, which corresponds to 8.9±0.18 wt.% CaCO$_3$, was used. The BN is defined as the quantity of acid, expressed in terms of the equivalent number of milligrams of KOH, required to neutralize all alkaline constituents in a 1 g sample. The two gas mixtures (technical air and 1 mol% SO$_2$ in air) were obtained from AGA A/S. For the Karl Fischer titration method, Hydranal Solvent-Oil, Hydranal Titrant 2, and Toluene were applied, all obtained from Sigma-Aldrich. The CaSO$_3$·0.5H$_2$O and CaSO$_4$·2H$_2$O powders were from Wako and Sigma-Aldrich, respectively, and the CaCO$_3$ powder was Faxe Bryozo limestone from Faxe, Denmark.

5.2.2 Batch reactor setup

The reaction was investigated in a stirred batch reactor (Parr 4575) at temperatures and pressures similar to a full-scale marine diesel engine application. The batch reactor setup is illustrated in Figure 5.1.
Lube oil and water were weighed prior to an experiment in a glass beaker (liner) to achieve specific water and CaCO₃ contents in the lube oil emulsion. Typical values were 9 g of lube oil and 0.5 g of demineralized water. The beaker was then placed inside the reactor. It was possible to achieve a maximum pressure of around 200 bar and a maximum temperature of around 350 °C in the reactor. The reactor was pressurized with technical air and/or with 1 mol% SO₂ in air. The lube oil was stirred during an experiment. The heating profile of the batch reactor is presented in Figure 5.2.

After the lube oil emulsion was placed inside the batch reactor, the latter was assembled, flushed three times with air, and a pressure leak test was carried out with air at 20 bar. The batch reactor was then gradually...
heated to a specific temperature and the heating was conducted under pressure (20 bar at room temperature) to keep as much of the added water in the liquid phase as possible. Two temperature sensors were used: one inside the reactor and another just below the bottom of the reactor. The temperature in the reactor was difficult to control because the reactor had thick steel walls and was heated by an outer heating jacket. Less than 10 °C in difference between these two measurement points was generally observed. The temperature used for data treatment was an average of these two measurement points. When a specific temperature was reached, a mixture of 1 mol% SO₂ in air was introduced to the batch reactor till a specific pressure. After a specific residence time (\(\tau\)), the gas phase was ventilated and the reactor was immediately flushed with N₂, while the reactor was cooled. During this flushing/cooling stage, the major part of the added water evaporated. The SO₂ was introduced after heating to a specific temperature in order to control the residence time and temperature. Using this procedure, all the water was kept inside the batch reactor during an experiment, limiting the evaporation of water from the lube oil.

5.2.3 Analysis methods

The lube oil samples were analyzed by a Thermo Scientific Nicolet iS50 ATR-FTIR (Attenuated Total Reflectance Fourier Transform Infrared Spectroscopy) spectrometer to obtain an infrared spectrum. The resulting base number (BN) was calculated by a calibration curve relating the height of the CaCO₃ band from an infrared spectrum to the base number. The latter was determined by titration following a standard test method, ASTM D-2896. Applying this method made it possible to determine the degree of conversion of CaCO₃ after reaction with SO₂. The water content in the fresh lube oil was measured by Karl Fischer titration using a 701 KF Titrino autotitrator from Metrohm. Toluene was used to assist the Hydranal-Solvent Oil in dissolving the lube oil sample sufficiently. The water content in the fresh 100 BN lube oil was determined to 1.1 wt.% with a sample standard deviation of 0.3 wt.%, based on four measurements. The water contents given in this work are overall initial water content values taking into account both the already present water in the lube oil (taken as the averaged value, 1.1 wt.%) and the added demineralized water.

5.2.3.1 Spectra of products from the reaction between SO₂ and CaCO₃

Upon an experiment, the lube oil was analyzed by FTIR-ATR to investigate the degree of reaction of CaCO₃, but also to determine the reaction products. The use of FTIR allowed distinction between CaCO₃, CaSO₃, and CaSO₄. This is illustrated in Figure E.1 in Appendix E, where infrared spectra of the pure powder components are shown.

5.2.3.2 Blank experiments

Blank experiments were conducted according to the experimental procedure described, but without SO₂ in the gas phase. The results revealed that all the added demineralized water evaporated during the cooling stage and that no effect of the experimental procedure on the resulting lube oil infrared spectra was found. Consequently, the observed change in CaCO₃ band, when SO₂ is present in the gas phase, is the isolated effect of reaction with SO₂. The calibration curves determined earlier are therefore useful in quantifying the CaCO₃ in a lube oil sample for the SO₂ experiments. The resulting infrared spectra together with an unused 100 BN lube oil spectrum are shown in Figure E.2 in Appendix E.
5.2.3.3 Spectrum of drain oil
To get an idea of which products to expect, an infrared spectrum of a drain oil sample was obtained (presented in Figure E.3 in Appendix E). From titration results, the base number was around 20. Only CaSO₄ and CaCO₃ are contained in the drain oil sample, because CaSO₃ has a band in the range 800-1000 cm⁻¹ that is absent in the spectrum. However, this is only one randomly analyzed lube oil sample from practice. Further, no information in the literature about the observation of CaSO₃ in an engine application has been found. This does therefore not necessarily mean that CaSO₃ is not formed in an engine followed by oxidation to CaSO₄.

5.3 Results and discussion

5.3.1 Batch reactor experiments
The batch reactor experiments seek to clarify if SO₂ and CaCO₃ reverse micelles react in a lube oil emulsion and if reaction is observed, which products that are formed. The reaction is investigated at conditions relevant for an engine application. Further, the effect of temperature, residence time, and initial water concentration on the product distribution and CaCO₃ conversion are also studied.

5.3.1.1 Product determination and effect of temperature
An experiment at room temperature was carried out with a Ca/S ratio of around unity and a total pressure in the batch reactor of 50 bar of 1 mol% SO₂ in air. The Ca/S molar ratio is defined as the initial molar ratio between CaCO₃ in the oil phase to SO₂ in the gas phase. 6.2 wt.% of water was initially present in the lube oil sample. The residence time was 60 minutes. Figure 5.3 compares the resulting infrared spectrum with an infrared spectrum of the fresh 100 BN lube oil and the pure CaSO₃ spectrum (from Figure E.1).

![Infrared spectra comparison](image)

**Figure 5.3.** Infrared spectra from room temperature experiment (red), unused 100 BN lube oil (blue), and pure CaSO₃ (green). Experimental conditions: Ca/S=1, P_total=50 bar, 6.2 wt.% water in lube oil, and \( \tau = 60 \) min. Note, that a shift in baseline due to water is found in the range 400-1000 cm⁻¹ and 1600-1700 cm⁻¹ for the room temperature experiment spectrum (red).
By using calibration curve data for the CaCO$_3$ band,$^{18}$ it was found that no CaCO$_3$ was left in the lube oil sample. The results in Figure 5.3 also show that no or very little CaSO$_4$ was formed, i.e., all CaCO$_3$ reacted to CaSO$_3$. Figure 5.4(a) shows spectra obtained as a function of temperature and in Figure 5.4(b), the resulting conversions of CaCO$_3$ together with the Ca/S molar ratios are shown. It is observed that the conversion increases slightly with temperature (with exception of the 27 °C experiment), while it decreases slightly with Ca/S molar ratio (see Figure 5.4(b)). When the temperature is increased, the absorption of SO$_2$ to the lube oil emulsion decreases. Therefore, it is expected that the reaction rate constant will have a more significant dependence on the temperature than depicted in Figure 5.4. The significantly higher conversion observed for the room temperature experiment (27 °C) may therefore be linked to a larger absorption of SO$_2$ into the lube oil emulsion. Another explanation could be that the SO$_2$ had an increased reaction time at lower temperatures, because the desorption time of SO$_2$ after an experiment may be increased at decreased temperature.

To investigate if the reaction between SO$_2$ and CaCO$_3$ is limited by equilibrium, an experiment with a residence time of 24 hours was carried out with the following conditions: $T=120$ °C, Ca/S=0.90, $P_{\text{total}}=90$ bar, and 6.8 wt.% water in the lube oil emulsion. The resulting infrared spectrum revealed that complete conversion of CaCO$_3$ was found, i.e., the conversions of CaCO$_3$ shown in Figure 5.4 are not limited by equilibrium in the system. According to the resulting spectrum (shown in Figure E.4 in Appendix E), an observable fraction of the CaCO$_3$ was converted to CaSO$_4$. No CaSO$_4$ was found for temperatures up to 153 °C for a residence time of 10 minutes, Figure 5.4(a), indicating that CaSO$_3$ is formed first followed by a change in the reaction mechanism. It was not possible to investigate the effect of temperature above 163 °C with the present experimental configuration because the oil would ignite.

![Figure 5.4](image-url)
5.3.1.2 Effect of residence time

The effect of residence time on the reaction of CaCO$_3$ with SO$_2$ was investigated at temperatures of 131 °C and 153 °C, depicted in Figure 5.5. Apparently, the reaction is fast initially and then slows down significantly with time. For the experiments carried out at 153 °C, more CaSO$_4$ was observed at increased residence time, but the amount of CaSO$_3$ was more or less constant. This supports that CaSO$_3$ is formed initially followed by either oxidation of CaSO$_3$ to CaSO$_4$ or formation of CaSO$_4$ directly from the SO$_2$-CaCO$_3$ reaction. The spectra can be found in Figure E.5 in Appendix E.

![Figure 5.5](image)

**Figure 5.5.** The effect of varying the residence time on the degree of conversion of CaCO$_3$ at two temperatures, 131 °C and 153 °C. Experimental conditions. P$_{\text{total}}$=90-105 bar, 6.6 wt.% water in the lube oil emulsion, and Ca/S around 1. The error bars represent lower and upper conversions determined from two experiments and the data points are the averaged conversions.

5.3.1.3 Effect of water concentration

The effect of initial water concentration (1.1-12%) in the lube oil emulsion on the CaCO$_3$ conversion at 131 °C is shown in Figure 5.6. The conversion of CaCO$_3$ increases linearly with the initial water content in the lube oil. The water content in the fresh lube oil was measured by Karl Fischer titration to around 1.1 wt.%, and the low water content experiment was carried out without addition of demineralized water. The water contents presented in Figure 5.6 are therefore overall water content values, both taking into account the already present water and the added demineralized water. The increased conversion at increased water content in the lube oil emulsion may be attributed partly to an increased SO$_2$ absorption in the lube oil emulsion because the solubility of SO$_2$ is higher in water than in lube oil. However, also the reaction rate may depend on the water concentration. An experiment at room temperature, without any added water to the lube oil, was also carried out with conditions similar to the room temperature experiment shown in Figure 5.3. Instead of reaching complete conversion of CaCO$_3$, a conversion of only 25.6% was observed. The initial molar ratio between water and CaCO$_3$ was calculated to 0.7, meaning that enough water was present assuming that CaSO$_3$·½H$_2$O is formed from the reaction. A reason for not observing this could be due to some of the water not being available to participate in the reaction; the Karl Fischer titration gives only the
5.3 Results and discussion

total amount of water in a sample, or that a different hydrated CaSO₃ product is formed. Nevertheless, the effect of water content on the conversion of CaCO₃ is significant and apparently, the reaction between SO₂ and CaCO₃ only proceeds when water is present.

![Graph showing the effect of varying the initial water content in the lube oil emulsion on the degree of conversion of CaCO₃.](image)

**Figure 5.6.** The effect of varying the initial water content in the lube oil emulsion on the degree of conversion of CaCO₃. Experimental conditions: \(P_{\text{total}}=90\text{bar}, T=131\,\text{°C}, \tau=10\,\text{min}, \) and Ca/S around 1. The error bars represent lower and upper conversions determined from two experiments and the data point is the averaged conversion.

5.3.1.4 Stability of CaSO₃

As shown previously, the main product formed between SO₂ and CaCO₃ was CaSO₃. However, at increased temperature (see Figure 5.4(a)) and residence time (see Figure E.4 and Figure E.5 in Appendix E) also CaSO₄ was formed. This may imply that CaSO₃ oxidizes to CaSO₄ at elevated pressure and temperature. However, heating a CaSO₃ containing lube oil sample in an oven at atmospheric pressure at 150 °C did not lead to the formation of CaSO₄, showing that CaSO₃ is stable over time. Pressurizing the lube oil sample, containing CaSO₃, to 80 bar at 150 °C for 1 hour indicated that a small fraction of the CaSO₃ had oxidized to CaSO₄; however, this observation was not conclusive because the loss of water from the sample resulted in a shift in baseline. The associated infrared spectra (Figure E.6 and Figure E.7) and a detailed description are found in Appendix E. The above indicates that CaSO₃ is stable when first formed. The formed CaSO₄ found at increased residence time and temperature is therefore attributed to that, at some point, when the concentration of CaSO₃ reaches a certain point, the CaCO₃ starts to be converted into CaSO₄ and the formation rate of CaSO₃ is significantly reduced (or even stopped).

5.3.1.5 Neutralization ability of CaSO₃

The neutralization ability of CaSO₃ was investigated by converting all initial CaCO₃ to CaSO₃ followed by addition of 96 wt.% H₂SO₄. A lube oil emulsion with 6.2 wt.% water was pressurized to 50 bar of 1 mol% SO₂ in air at room temperature. An FTIR spectrum recorded after one hour of residence time confirmed that all CaCO₃ had converted to CaSO₃. Then, 96 wt.% H₂SO₄ was added to the lube oil sample, making sure that...
Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines

CaSO$_3$ was in molar excess compared to H$_2$SO$_4$ at complete conversion of the H$_2$SO$_4$. The resulting infrared spectra revealed that the CaSO$_3$ was converted to CaSO$_4$. This reaction proceeds in the following way:

\[
\text{CaSO}_3 + \text{H}_2\text{SO}_4 \rightarrow \text{CaSO}_4 + \text{SO}_2 + \text{H}_2\text{O} \quad (5.6)
\]

The release of SO$_2$ from the sample after addition of H$_2$SO$_4$ was verified by a gas detector. The observation that CaSO$_3$ reacts with H$_2$SO$_4$ shows that the neutralization ability is retained when CaCO$_3$ reacts with SO$_2$ to form CaSO$_3$. Whether the CaSO$_3$-H$_2$SO$_4$ has a similar reaction rate as the CaCO$_3$-H$_2$SO$_4$ reaction is unknown. In addition, the existence of CaSO$_3$ in the lube oil prevented accurate determination of the BN by the titration method. The resulting spectra are depicted in Figure E.8 in Appendix E.

5.3.2 Mathematical modeling of lube oil batch reactor

A mathematical model for the reaction in the batch reactor setup is developed with the aim of extracting a kinetic expression for the CaCO$_3$-SO$_2$ reaction. The model is fitted to the experimental data to extract a reaction rate constant for the reaction. The rate expression is then used to investigate the relative importance of the CaCO$_3$-SO$_2$ and CaCO$_3$-H$_2$SO$_4$ reactions at engine conditions.

The assumptions underlying the batch reactor model are:

- The lube oil emulsion volume is well-mixed (no radial or axial concentration or temperature gradients).
- The only reaction considered in the lube oil is CaCO$_3$ (s) + SO$_2$ (aq) $\rightarrow$ CaSO$_3$ (s) + CO$_2$ (g) with a reaction rate of $(-r_A)$.
- SO$_2$ from the gas phase absorbs both in the lube oil and in the water. A combined expression for Henry’s constant, $H_s$, dependent on the water concentration in the lube oil emulsion, is used.
- Even though it is thought that SO$_2$ only reacts with CaCO$_3$ in the presence of water, SO$_2$ is also present in the lube oil itself. This SO$_2$ is assumed to be available for reaction, because water may be present in/near the CaCO$_3$ reverse micelles.
- The effect of the initial water concentration on the conversion of CaCO$_3$ is reflected in the combined Henry’s constant only.
- The effect of O$_2$ is not considered, because a large excess of O$_2$, on a molar basis compared to SO$_2$/CaCO$_3$, was present in the batch reactor experiments.
- Formation of CaSO$_3$ does not limit the CaCO$_3$-SO$_2$ reaction.
- The ideal gas law is used to calculate the concentration of SO$_2$ in the gas phase.
- Only the transfer of SO$_2$ from the gas phase to the liquid phase is considered, i.e., the release of SO$_2$ from the liquid phase to the gas phase is not taken into account.

5.3.2.1 Reaction rate expression

The reaction rate expression is based on the reaction between SO$_2$ and CaCO$_3$ forming CaSO$_3$ because it was found that CaSO$_3$ was the main product in the temperature range from room temperature to 163 °C for a residence time of 10 min. Therefore, the simple overall reaction rate expression is assumed to be given as:

\[
(-r_A) = k C^L_{SO_2} C^L_{CaCO_3} \quad (5.7)
\]
Here, $C_{SO_2}^L$ is the bulk concentration of SO$_2$ in the lube oil emulsion and $C_{CaCO_3}^L$ is the bulk concentration of CaCO$_3$ in the lube oil emulsion (proportional to the base number, BN). The concentrations are with respect to the lube oil emulsion, which consists of the lube oil and the added demineralized water. The bulk concentration of SO$_2$ in the lube oil emulsion is estimated from the absorption of gaseous SO$_2$ into the emulsion. The model takes into account the uptake of SO$_2$ from the gas phase to the lube oil emulsion followed by reaction between SO$_2$(aq) and CaCO$_3$(s). It includes mass balances for SO$_2$ in the gas phase and oil phase, respectively, and for CaCO$_3$ in the oil phase. An illustration of the system is shown in Figure 5.7. For now, the reaction order of the water concentration in the lube oil emulsion is assumed to be zero, even though a dependence on conversion from the water concentration was found (Figure 5.6). This dependence is assumed to be due to an increased SO$_2$ uptake from the gas phase and is reflected by the combined Henry’s constant depending on the initial water concentration.

![Figure 5.7. An illustration of the batch reactor setup: SO$_2$(g) has to be absorbed by the lube oil emulsion (oil and/or water) before it can react with the CaCO$_3$(s) in the lube oil.](image)

5.3.2.2 Mass balance of SO$_2$ in the gas phase
A mass balance for the SO$_2$ in the gas phase is set up:

$$\frac{dC_{SO_2}^G}{dt} = -N_{SO_2} \frac{V_t}{V_G}$$  \hspace{1cm} (5.8)

Here, $N_{SO_2}$ (mol m$^{-3}$ s$^{-1}$) is the absorption rate of SO$_2$ from the gas phase to the lube oil emulsion, which is assumed to be given as:49
Experimental investigation and mathematical modeling of the reaction between SO\(_2\)(g) and CaCO\(_3\)(s)-containing micelles in lube oil for large two-stroke marine diesel engines

\[
N_{SO_2} = K_G a \left( p_{SO_2}^G - p_{SO_2}^* \right) \tag{5.9}
\]

\(K_G\) (mol m\(^{-2}\) bar\(^{-1}\) s\(^{-1}\)) is the overall mass transfer coefficient of SO\(_2\) on gas basis, \(a\) (m\(^2\) m\(^{-3}\)) is the specific gas-liquid interfacial area, \(p_{SO_2}^G\) is the bulk partial pressure of SO\(_2\) in the gas phase, and \(p_{SO_2}^*\) is the partial pressure of gas-phase SO\(_2\) in equilibrium with the bulk lube oil concentration \(C_{SO_2}^L\). The equilibrium relationship is given by Henry’s law by introducing Henry’s constant of the lube oil emulsion, \(H_L\):

\[
p_{SO_2}^* = H_L C_{SO_2}^L \tag{5.10}
\]

The partial pressure of SO\(_2\) in the gas phase, \(p_{SO_2}^G\), is linked to the concentration of SO\(_2\) in the gas phase by the ideal gas law:

\[
p_{SO_2}^G = C_{SO_2}^G RT \tag{5.11}
\]

The overall gas-side mass transfer coefficient, \(K_G\), is given as:

\[
K_G = \frac{1}{\frac{1}{k_G} + \frac{H_L}{k_L}} \tag{5.12}
\]

Here, \(k_G\) (mol m\(^{-2}\) s\(^{-1}\) bar\(^{-1}\)) is the gas film mass transfer coefficient and \(k_L\) (m s\(^{-1}\)) is the liquid film mass transfer coefficient.

5.3.2.3 Mass balance of SO\(_2\) in the lube oil emulsion

In the lube oil emulsion, SO\(_2\) enters from the gas phase and is consumed by the CaCO\(_3\) reverse micelles. The mass balance of SO\(_2\) in the lube oil emulsion is formulated as:

\[
\frac{dC_{SO_2}^L}{dt} = N_{SO_2} - (-r_A) \tag{5.13}
\]

Here, Eq. (5.7) describes \((-r_A)\) and Eq. (5.9) describes \(N_{SO_2}\).

5.3.2.4 Mass balance of CaCO\(_3\) in the lube oil emulsion

The CaCO\(_3\) is consumed by reaction with SO\(_2\), which gives the following mass balance:

\[
\frac{dC_{CaCO_3}^L}{dt} = -(-r_A) \tag{5.14}
\]

Three differential equations are thereby derived describing the concentration change over time in the batch reactor of SO\(_2\) in the gas phase, Eq. (5.8), SO\(_2\) in the lube oil emulsion, Eq. (5.13), and CaCO\(_3\) in the lube oil emulsion, Eq. (5.14). The aim is to derive the reaction rate constant, \(k\), given in Eq. (5.7), by fitting the model to the experimental data.
5.3 Results and discussion

5.3.2.5 Initial conditions

Three initial conditions are needed: one for the CaCO₃ concentration in the lube oil, one for the SO₂ concentration in the gas phase, and one for the SO₂ concentration in the lube oil emulsion. The fresh lube oil was measured to have an average base number (BN) of 98.55 BN, which corresponds to a CaCO₃ concentration of 825.6 mol m⁻³. Because the fresh lube oil contains 1.1 wt.% water, the water-free lube oil has a CaCO₃ concentration of 834.8 mol m⁻³. The concentrations and reaction rates are based on the volume of the lube oil emulsion (lube oil + water), thus the water-free concentration of CaCO₃ is multiplied by the ratio of lube oil volume to lube oil emulsion. The initial concentration of SO₂ in the total gas phase is calculated by the ideal gas law using the partial pressure of SO₂ in the gas phase and the temperature. Lastly, it is assumed that the initial concentration of SO₂ in the lube oil emulsion is zero. The Ca/S molar ratio is defined as the initial molar ratio between CaCO₃ in the emulsion and SO₂ in the gas phase, calculated as:

$$\frac{Ca}{S} = \frac{C_{CaCO₃,L}}{C_{SO₂,G}}$$

(5.15)

If equal to e.g. 0.5, 50% conversion of the gaseous SO₂ is expected for complete conversion of the CaCO₃ reverse micelles in the lube oil emulsion.

5.3.2.6 Estimation of input parameters

The input parameters to the model include experimental conditions and estimation of $K_G$, $a$, $H_L$, and $k$. The experimental conditions are found in Table E.1 in Appendix E for the experiments from Figure 5.4. The volumes of the water and lube oil in the emulsion were calculated by scaling the weighted values with the densities (940 kg m⁻³ for lube oil and 1000 kg m⁻³ for demineralized water). The water content of the lube oil itself (1.1 wt.%) was also taken into account.

It is unknown whether the SO₂(g) is absorbed into the water droplets, which are emulsified in the lube oil, the lube oil itself, or a mixture thereof. For the present purpose, Henry’s constant for SO₂ in both water and lube oil were estimated. The temperature dependent Henry’s constant for SO₂ in water was estimated from NIST. Henry’s constant for SO₂ in a fully formulated lube oil is more challenging to assess. The experimental results showed that SO₂ reacts with the CaCO₃ in the lube oil; this makes the determination of only solubility in the lube oil difficult. Costa and Underhill, who studied uptake of SO₂ in different lube oil formulations at 25 °C, also observed that SO₂ reacted with the base content in the lube oil, resulting in an overestimation of the ‘solubility’. For the present study, Henry’s constant at 25 °C was calculated from the study of Costa and Underhill, based on a lube oil not containing base additives reacting with the SO₂. The resulting Henry’s constant indicates that SO₂ is more soluble in water than in lube oil. A combined Henry’s constant is derived based on the amount of water present initially in a lube oil sample in the following way, using a scaled resistance-like expression:

$$H_L = \frac{1}{H_{oil}} \left( \frac{V_{oil}}{V_L} \right) + \frac{1}{H_{water}} \left( \frac{V_{water}}{V_L} \right)$$

(5.16)
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Here, $H_{oil}$ and $H_{water}$ are Henry’s constants for lube oil and water, respectively, and $V_{oil}$, $V_{water}$, and $V_L$ are the volumes of lube oil, water, and lube oil emulsion ($V_L = V_{oil} + V_{water}$). A detailed assessment of the derivation of the Henry’s constants can be found in Appendix E.

The collected parameter $K_G\alpha$ is then estimated. The specific gas-liquid interfacial area, $\alpha$, represents the area between the gas phase and the liquid phase where the mass transfer takes place. It is assumed that the mass transfer happened at the gas-oil interface. The specific interfacial area for the gas-oil interface is calculated as:

$$\alpha = \frac{A_L}{V_L} = \frac{\pi R_{reactor}^2}{V_L}$$

(5.17)

Because the radius of the batch reactor is 3.15 cm, and a typical amount of the lube oil emulsion was 10.1 ml, $\alpha = 308.7$ m$^2$ m$^{-3}$. This is for a stagnant lube oil volume.

Further, an evaluation of the resistance of the mass transfer of SO$_2$ from the gas phase to the liquid phase was carried out, revealing that mass transfer is controlled by the liquid-side resistance, viz, $K_G = k_L/H_L$. The calculations can be found in Appendix E. A crude estimate of the liquid film mass transfer coefficient, $k_L$, is given as:

$$k_L = \frac{D_L}{\delta_L}$$

(5.18)

$D_L$ is the diffusion coefficient of SO$_2$ in the liquid phase and $\delta_L$ is the liquid film thickness. The calculation of $k_L$ is likewise found in Appendix E.

The only unknown in the model is thereby $k$, which is fitted to match the modeling results to the experimental data (conversion of CaCO$_3$ at specific $\tau$, Figure 5.4). However, implementing and solving the above described model revealed that only an insignificant degree of conversion of CaCO$_3$ can be achieved irrespectively of the magnitude of $k$, which is in disagreement with the experimental results. The reason for this discrepancy between simulation and experimental results is attributed to an underestimation of the overall film mass transport coefficient of SO$_2$, $K_G$, and specific gas-liquid interfacial area, $\alpha$, because the estimated $K_G$ and $\alpha$, based on Eqs. (5.17) and (5.18), are based on a stagnant lube oil film and pure surface diffusion. Therefore, $K_G\alpha$ for the present system was estimated by use of the work from Meille et al., who measured $k_L\alpha$ ($K_G\alpha = k_L\alpha/H_L$) values as a function of stirrer speeds for different batch reactor dimension, finding that stirring of a liquid in a batch reactor contributed to an increased value of $k_L\alpha$. Based on their work, a factor of 120 between $k_L\alpha$ for a stagnant case (based on Eqs. (5.17) and (5.18) and the experimental parameters from Meille et al.) and an agitated case (stirrer speed of 600 rpm which was the stirrer speed applied in this work) was found and was used in the subsequent modeling. The justifications and calculations are found in Appendix E.

5.3.2.7 Arrhenius plot

Based on the fitting of $k$, an Arrhenius expression, which takes the temperature dependence into account, was then constructed, by Eq. (5.19), and is shown in Figure 5.8 for the temperature range 107-163 °C.
ln(k) = ln(A) - \frac{E_a}{R} \frac{1}{T} \tag{5.19}

A satisfactory linear fit is observed between ln(k) and 1/T from which an activation energy ($E_a$) of 6.7 kJ mol$^{-1}$ and a pre-exponential factor ($A$) of $2.03 \times 10^{-3}$ m$^3$ mol$^{-1}$ s$^{-1}$ are determined by use of Eq. (5.19) and the linear fit of Figure 5.8. The determined $E_a$ reveals that the temperature dependence of the reaction rate constant is weak, in accordance with literature. Figure 5.8 also shows a rather high uncertainty on the determination of the fitted $k$.

A maximum simulated CaCO$_3$ conversion of 19.6% could be achieved for the room temperature experiment conditions (assuming infinite fast reaction, i.e., completely mass-transfer controlled), which is far from the experimentally determined conversion (56.3%). The reason for this may be due to a viscosity effect because the viscosity highly affects $K_G a$ and the viscosity of lube oil drastically changes with temperature,$^{50,61}$ thus it may be difficult to estimate an exact value of $K_G a$ at room temperature. Another explanation may be that another limitation/mechanism exists at room temperature than for the higher temperature experiments or that the SO$_2$ is better maintained in the lube oil emulsion during the desorption stage of the experimental procedure. This may lead to an extended reaction time of the SO$_2$ in the lube oil emulsion, leading to an increased conversion of CaCO$_3$. If increasing the calculated $K_G a$ at stagnant conditions by a factor of 600, it was now possible to simulate the experimentally determined conversion of CaCO$_3$ at room temperature, however, the resulting fitted $k$ is not in line with the ones determined at higher temperatures (see Figure E.9 in Appendix E). Lastly, the value of $K_G a$ may still be underestimated even though a factor of 120 between stagnant and stirred conditions was determined previously and used in the fitting procedure. Nevertheless, the room temperature case was excluded in the process of extracting a reaction rate constant, because this temperature is not relevant for an engine application. It was found that the SO$_2$ from the gas phase is readily
absorbed into the lube oil, illustrated by a steep increase in the concentration curve for the SO$_2$ in the lube oil emulsion. This can be seen in Figure E.10 in Appendix E which shows the concentration profiles of CaCO$_3$ in the lube oil emulsion, SO$_2$ in the oil film emulsion, and SO$_2$ in the gas phase for the 131 °C simulation.

5.3.2.8 Comparison between model and experimental data for varying residence time
The model was used to compare with the experimental data from Figure 5.5, as shown in Figure 5.9. The differences between modeling predictions and experimental data may be due to SO$_2$ not desorbing immediately after ventilation of the SO$_2$ gas phase and flushing with N$_2$, resulting in an extended reaction time. The effect of prolonged reaction time may be more pronounced for the shorter residence time experiment. Another explanation could be that the reaction reaches a plateau where no more CaSO$_3$ is formed, but instead, CaCO$_3$ is converted to CaSO$_4$, but at a much lower reaction rate, possibly because O$_2$ also has to participate in the reaction. The above was indicated from the experiments, see e.g. Figure E.5 in Appendix E, and may explain the mismatch between the model and simulation trends.

![Figure 5.9](image)

**Figure 5.9.** The effect of varying the residence time on the degree of conversion of CaCO$_3$ at two temperatures, 131 and 153 °C. The figure compares the model predictions with the experimental data from Figure 5.5.

5.3.2.9 Comparison between model and experimental data for varying initial water concentration
The effect of varying initial water concentration on the conversion of CaCO$_3$ was predicted by the model and compared with the experimental data from Figure 5.6. The result of this is shown in Figure 5.10. This figure shows that the model captures the experimentally determined conversions sufficiently within the uncertainty of the analysis technique. This means that the combined Henry’s constant expression, Eq. (5.16), describes the water dependence sufficiently. The effect of water concentration is minor relative to the change because increasing the initial water concentration by a factor of 11 increases the conversion of CaCO$_3$ by a factor of around 1.5.
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Figure 5.10. The effect of varying the initial water content in the lube oil emulsion on the degree of conversion of CaCO₃ at 131 °C. The figure compares the model predictions with the experimental data from Figure 5.6.

The lube oil emulsion was gradually heated under pressure prior to introducing the SO₂ in air gas mixture to keep as much of the water in the liquid phase. However, a fraction of the water may evaporate during an experiment and the exact concentration of water in the lube oil emulsion may not equal the initial water concentration in the emulsion. The vapor pressure of water at 131 °C was calculated to 2.7 bar, and comparing this value with the pressure prior to introducing the SO₂ gas mixture (around 30 bar at 131 °C), it is advocated that most of the water was present in the liquid phase during an experiment. This, together with the minor effect of changing the water concentration on the conversion of CaCO₃ (relative to the change) suggests that the initial water concentration can be used for estimation of the combined Henry’s constant from Eq. (5.16).

5.3.2.10 Discussion on model simulations

The above sections emphasize that accurate estimation of the correlated parameters $K_G\alpha$ and $k$ are required in order to predict the conversion of CaCO₃ by reaction with SO₂ precisely. Therefore, $K_G\alpha$ was estimated by use of data from the literature, and Figure 5.8 was constructed. Whether these two parameters are estimated correctly is unknown, however, the estimated values of $K_G\alpha$ and $k$ are one pair of parameters to the model which simulates the conversions of CaCO₃ in accordance with the experimentally determined conversions.

To verify if the determined parameters are true, one solution could be to measure the parameter $K_G\alpha$ independently as done in the work of Meille et al. The effects of $K_G\alpha$ and $k$ on the conversion of CaCO₃ are simulated in Figure 5.11 for the experimental conditions of the 131 °C experiment.
Three different regions are illustrated in Figure 5.11. At low $K_G a$ values, the reaction between SO$_2$ and CaCO$_3$ is mass transfer controlled, i.e., no effect of reaction rate is found. However, the mass transfer of SO$_2$ from the gas phase to the liquid phase is too low in order to achieve an observable degree of conversion of CaCO$_3$ (for the specific residence time available, i.e., 10 min), or at least a degree comparable to the experimental degree of conversion. At high $K_G a$ values, only a minor effect of increasing $K_G a$ even further is found, however, the effect of increasing $k$ is large relative to the increase. In-between, an intermediate region is found. At stagnant conditions, $K_G a$ was calculated to $1.62 \cdot 10^{-2}$ mol m$^{-3}$ s$^{-1}$ bar$^{-1}$, which explains the insignificant degree of reaction of CaCO$_3$ if comparing this value with Figure 5.11. Multiplying $K_G a$ by 120 gives $1.95$ mol m$^{-3}$ s$^{-1}$ bar$^{-1}$, which translates to being in the intermediate region of Figure 5.11 where both mass transfer and reaction control. Knowing the conversion of CaCO$_3$ (e.g. 42.2% at 131 °C) and $K_G a$, $k$ was calculated to $2.65 \cdot 10^{-4}$ m$^3$ mol$^{-1}$ s$^{-1}$, in accordance with Figure 5.11. In the intermediate region, a large change in $k$ only lead to a relative minor effect on the conversion of CaCO$_3$. Because analysis uncertainties may be in the order of ±2 BN, this has a large effect on the uncertainty of $k$ as shown in Figure 5.8. However, at increasing $K_G a$ the resistance to the conversion of CaCO$_3$ goes toward chemical reaction. This means that a small change in $k$ has a large impact on the conversion, which would decrease the corresponding uncertainty in an Arrhenius plot. Further, the temperature dependency on $k$ increases for increasing $K_G a$. If applying a factor of 600 instead of the estimated 120 used to construct Figure 5.8, the activation energy becomes 23.5 kJ mol$^{-1}$ and the uncertainty of the 131 °C data point in the Arrhenius plot was significantly decreased due to the stronger temperature effect (see Figure E.9 in Appendix E).

For the mathematical model, an overall reaction rate expression was set up only considering the overall reaction between SO$_2$ and CaCO$_3$. The mechanistic details of the reaction mechanism were thereby collected in the overall reaction rate constant, $k$. In reality, SO$_2$ may further react to HSO$_3^-$ or SO$_3^{2-}$ after entering the
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water in the lube oil emulsion. These reactions are not taken into account in the modeling and further studies are required to map the exact reaction mechanism between SO$_2$, water, lube oil, and CaCO$_3$ reverse micelles.

5.3.3 Application of the batch reactor model to conditions in a large two-stroke diesel engine

The batch reactor model developed in this work was used to interpret the experiments carried out at varying conditions in a batch reactor for determination of absorption and reaction rate expressions for the SO$_2$-CaCO$_3$ reaction. These expressions are intended to be used in e.g. computational fluid dynamics simulations to provide a full overview of the effect of SO$_2$ on the consumption of CaCO$_3$ and accumulation of SO$_2$ in the lube oil at the cylinder liner in a large two-stroke marine diesel engine. As will be discussed in the following, the batch reactor model derived in this work offers a useful approximation to local conditions prevailing in a marine diesel engine and can be used to assess the importance of the SO$_2$-CaCO$_3$ reaction as well.

The entire combustion chamber in an engine can be considered as one batch reactor, where the gas volume is much larger than the lube oil volume, as in the case of the batch reactor experiments. However, the size of the combustion chamber changes as a stroke progresses. Assuming stagnation at different piston positions, each volume can therefore be considered as a batch reactor with associated partial pressure of SO$_2$ in the gas phase and lube oil emulsion volume. Under this circumstance, the batch reactor model of this work can assist in determining the absorption of SO$_2$ and subsequent degree of reaction between SO$_2$ and CaCO$_3$.

Assuming that all fuel-S is instantaneously converted to SO$_2$ prior to the expansion stroke, the partial pressure of SO$_2$ will be highest at the very top of the cylinder (at top dead center, TDC). As the expansion stroke progresses, the partial pressure of SO$_2$ in the gas phase decreases as the combustion chamber volume increases, the combustion gas is exhausted, and later further diluted by the intake air. Ideally, this leads to desorption of SO$_2$ from the lube oil emulsion due to the changed SO$_2$ concentration gradient across the gas-liquid interface. Due to the fast passage of the piston, it may be fair to assume that the desorption rate of SO$_2$ is too slow to actually come into force. That desorption of SO$_2$ from the lube oil emulsion is not an instantaneous process, was also observed in the batch reactor experiments. However, this means that the absorption rate of SO$_2$ decreases as the expansion stroke progresses and may be stopped during the compression stroke where all the exhaust gas has been ventilated and replaced by fresh intake air. This means that at a local, discretized volume section of the cylinder liner, the partial pressure of SO$_2$ is constantly changing. To keep it simple, the partial pressure of SO$_2$ in the gas phase is assumed to be constant for each piston position, which also serves as a worst-case scenario. Further, the residence time has to be chosen. Because the gas phase is constantly renewed, the residence time for the simulations is chosen as the residence time for the lube oil in the engine. This is augmented by the fact that the lube oil is in contact with the SO$_2$ throughout this time either through the gas phase or in the oil. Assuming, in the following simulations, that the partial pressure of SO$_2$ is constant throughout the residence time may ultimately overestimate the degree of conversion of CaCO$_3$ from SO$_2$. Average lube oil residence times of up to 4 min in an engine have been calculated.$^{1,18,62}$

5.3.3.1 Engine simulation: SO$_2$-CaCO$_3$ reaction

The modeling of the SO$_2$-CaCO$_3$ reaction in discretized combustion chamber volumes by the batch reactor model underlies the following assumptions, besides the ones given previously:
- The cylinder liner is discretized into smaller volumes, where each subvolume assumes constant gaseous SO₂ concentration, lube oil temperature, and lube oil thickness throughout the specified residence time. The change in gaseous SO₂ concentration at a specific subvolume during the expansion stroke is thereby neglected.
- Desorption of SO₂ from the lube oil film is neglected.
- The lube oil temperature and thickness are constant throughout the vertical length.
- The dilution of gaseous SO₂ during the expansion stroke by exhaustion of the combustion gas and intake air is not taken into account. The gaseous SO₂ concentration profile varies along the vertical direction, but only by the volume expansion, i.e., when the gas volume doubles, the gaseous SO₂ concentration halves. This means that the gaseous SO₂ concentration is highest at top dead center, TDC, and lowest at bottom dead center, BDC.
- All the injected fuel-S is instantaneously converted to gaseous SO₂.
- Oxidation of SO₂ to SO₃ is not considered, i.e., no H₂SO₄ is present in the system.
- The gas and liquid volumes are well-mixed (no radial or axial concentration or temperature gradients).

An illustration of the discretized volumes with corresponding gaseous SO₂ concentrations are presented in Figure 5.12, where each subvolume assumes the behavior of a batch reactor.

![Figure 5.12](image)

**Figure 5.12.** An illustration of a cylinder showing the discretized subvolumes, where \( h \) is the height of a subvolume, \( D \) is the diameter of the cylinder, \( V_G \) is the gas volume of a subvolume, \( l \) is the subvolume number, \( C_{SO_2,l} \) is the gaseous concentration of SO₂ in subvolume \( l \), and \( f' \) is the last subvolume number.
During expansion, the pressure decreases (volume increases). This leads to a reduced concentration of SO₂ in the gas phase and thereby in the lube oil emulsion (the absorption rate is decreased). Therefore, it is expected that the degree of reaction between SO₂ and CaCO₃ is reduced as the expansion in the engine progresses.

Input parameters used for the engine simulations are found in Table 5.1.

**Table 5.1.** Input parameters used for the engine simulations. The engine dimensions are based on an 8S80ME-C9.5 engine from MAN Energy Solutions.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Parameter Value</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>Cylinder diameter, (D)</td>
<td>0.8 m</td>
<td></td>
</tr>
<tr>
<td>Cylinder height, (H)</td>
<td>3.45 m</td>
<td></td>
</tr>
<tr>
<td>Gas volume of a subvolume, (V_g)</td>
<td>0.08 m³</td>
<td></td>
</tr>
<tr>
<td>Vertical height of a subvolume, (h)</td>
<td>0.16 m</td>
<td></td>
</tr>
<tr>
<td>Number of cylinders</td>
<td>8</td>
<td></td>
</tr>
<tr>
<td>Specific fuel oil consumption</td>
<td>175 g kWh⁻¹</td>
<td>63, 64</td>
</tr>
<tr>
<td>Engine power</td>
<td>30 MW (at 100% load)</td>
<td>64</td>
</tr>
<tr>
<td>Sulfur content in fuel</td>
<td>4.5 wt.%</td>
<td>Assumed</td>
</tr>
<tr>
<td>Engine speed</td>
<td>60 rpm</td>
<td>Assumed</td>
</tr>
<tr>
<td>Temperature</td>
<td>100 °C</td>
<td>Assumed</td>
</tr>
<tr>
<td>Lube oil film thickness</td>
<td>1 μm</td>
<td>Assumed</td>
</tr>
<tr>
<td>Specific gas-liquid interface, (a)</td>
<td>(10^\circ \text{m}^2 \text{m}^{-3})</td>
<td>Eq. (5.17)</td>
</tr>
<tr>
<td>Water content in lube oil film</td>
<td>5 wt.%</td>
<td>Assumed</td>
</tr>
<tr>
<td>Residence time, (\tau)</td>
<td>10 min</td>
<td>Based on 1, 62, 65</td>
</tr>
</tbody>
</table>

The concentration of SO₂ in the gas phase in each subvolume was based on the first subvolume concentration, \(C_{SO_2,1}\). When the pressure is highest in the engine, it is assumed that all the fuel has just been burned and thereby all the fuel sulfur is present as SO₂. This was assumed to happen when the piston is at TDC. At TDC, the compression volume of the gas is around 80 liters (typical value of a two-stroke marine diesel engine), corresponding to \(h\) being equal to 16 cm. The dimensions of the cylinder liner were based on typical values from a two-stroke marine diesel engine, having a diameter, \(D\), of 0.8 meter. The concentration of SO₂ in the gas phase was based on a typical fuel flow (assuming that all fuel-sulfur is immediately converted to SO₃) and the gas volume. The fuel flow was found to be 175 g kWh⁻¹, when having 8 cylinders rated at 30 MW (at 100% load), 4.5 wt.% sulfur in the fuel (a high, worst-case value), and that new fuel was injected every second (corresponding to 60 rpm), 0.2559 mol SO₂ was present in the uppermost cylinder subvolume at complete combustion. Dividing by 80 liters, yields \(C_{SO_2,1} = 3.2 \text{ mol m}^{-3}\). The fuel flow rate was also calculated by MAN’s CEAS Engine Calculator for the specific engine (but with 73.1 rpm), confirming that an approximate fuel flow rate is 175 g kWh⁻¹. It was assumed that SO₂ is not exhausted during the expansion stroke, therefore: \(C_{SO_2,i} = C_{SO_2,1}/i\). This means that the SO₂ concentration rapidly decreases in the subsequent subvolumes as the expansion stroke progresses. This behavior was also modeled by Nagaki and Korematsu. It should be emphasized, even though the concentration of SO₂ decreases in the whole volume between the top of the cylinder and the piston during the expansion stroke, that the SO₂ concentration of the preceding
subvolume is unaffected of the present subvolume. In other words, it was assumed that $C_{SO_2}$ kept the value of 3.2 mol m$^{-3}$ throughout the whole simulation even though the SO$_2$ gas concentration decreases to 1.6 mol m$^{-3}$ when the piston has moved 16 cm further downwards and so forth for the remaining subvolumes. The temperature also varies along the stroke length, being highest near TDC and lowest near BDC and depends on the load. Preliminary simulations carried out under engine conditions revealed that conversion of CaCO$_3$ increased at decreasing temperature. The reason for this behavior is that the absorption of SO$_2$ from the gas phase to the lube oil film happens almost instantaneously and the SO$_2$ concentration in the lube oil film reaches therefore equilibrium instantaneously. This is attributable to the large amount of SO$_2$ in the gas phase compared to CaCO$_3$ in the lube oil film (on a molar basis) and that $\alpha$ is large. Further, the temperature dependence of $k$ is weak (Figure 5.8) which cannot completely counteract the stronger temperature dependency of the Henry’s constant: more SO$_2$ is absorbed at decreasing temperature (increasing $C_{SO_2}^H$), which increases the overall conversion because $k$ is more or less unaffected by the temperature. Therefore, a lower temperature of 100 °C was chosen for the simulations. The results of the simulations are found in Figure 5.13, where the conversions of CaCO$_3$ in each subvolume are presented.

![Figure 5.13](image)

**Figure 5.13.** The simulated conversion of CaCO$_3$ in each subvolume (Figure 5.12) for the conditions given in Table 5.1. The average CaCO$_3$ conversion (7.9%) is also provided in the figure by the horizontal line.

When sampling a lube oil off-shore, it is an averaged CaCO$_3$ conversion throughout the whole vertical direction of the cylinder liner that is sampled. The average CaCO$_3$ conversion throughout the vertical direction of the cylinder is therefore also given in Figure 5.13 (7.9%). A typical recommendation is to achieve between 50-75% conversion of CaCO$_3$ in practice, which means that SO$_2$ cannot solely be accounted guilty for the observed consumption of CaCO$_3$ in practice. Further, the inputs to the model presented in Table 5.1 are chosen in order to enhance the conversion of CaCO$_3$, e.g., the chosen temperature, load, sulfur content in the fuel, residence time, etc. That means, under a worst-case scenario, maximum 7.9% of the available CaCO$_3$ in lube oil can be neutralized by reaction with SO$_2$. 

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5.3 Results and discussion

5.3.3.2 Engine simulation: Competition between SO₂-CaCO₃ and H₂SO₄-CaCO₃ reactions

The previous section showed that around 40% of the CaCO₃ could potentially be consumed by SO₂ in the lube oil at worst-case conditions near TDC (Figure 5.13, for a residence time of 10 min). However, if H₂SO₄ is present in the lube oil emulsion, the effect of SO₂ on the consumption of CaCO₃ may be even smaller if the reactivity of the H₂SO₄-CaCO₃ reaction outmatches the SO₂-CaCO₃ reaction. The H₂SO₄-CaCO₃ reaction has been investigated by the authors previously, simulating that 38% of the CaCO₃ is consumed after a residence time of 0.5 s, for a temperature of 100 °C and for a Ca/S molar ratio equal to 1 (remaining parameters: radius of H₂SO₄ droplets: 0.5 µm, 100 BN lube oil, and concentration of H₂SO₄ droplets: 18·10³ mol m⁻³). Comparing this conversion degree to the one determined in this work reveals that the rate of the H₂SO₄-CaCO₃ reaction is superior compared to the SO₂-CaCO₃ reaction. This means, if both SO₂ and H₂SO₄ are present in the lube oil film, the CaCO₃ would rather react with H₂SO₄ than with SO₂. If H₂SO₄ is limited compared to CaCO₃, on a molar basis, then CaCO₃ would first consume the majority of the H₂SO₄, followed by reaction with SO₂. However, H₂SO₄ gradually condenses onto the cylinder liner (during each expansion stroke), which means that H₂SO₄ may be available for reaction with CaCO₃ continually. That the H₂SO₄-CaCO₃ reaction outmatches the SO₂-CaCO₃ reaction adds to the argument that the significance of SO₂, as consumption source of CaCO₃ reverse micelles, is negligible in a marine diesel engine application. This is further augmented by the possibility of formation of CaSO₃ as the product from the SO₂-CaCO₃ reaction, which also can react with H₂SO₄ forming CaSO₄.

It is also possible to directly compare the H₂SO₄-CaCO₃ and SO₂-CaCO₃ reaction in an engine application through the present batch reactor model. This can be implemented by extending the reaction mechanism as described in Appendix E. However, the competition between the two reactions highly depends on the initial concentration of H₂SO₄ in the lube oil emulsion. It was found (simulations are not shown here) that the H₂SO₄-CaCO₃ reaction is generally dominant over the SO₂-CaCO₃ reaction. The dominance increases for increasing temperature, decreasing SO₂ partial pressure, and increasing initial H₂SO₄ concentration. Near TDC, the temperature is highest and most H₂SO₄ is condensing, and toward the bottom of the cylinder liner, the partial pressure of SO₂ in the gas phase is rapidly declining. This yet again reinforces that H₂SO₄ is responsible for consuming the vast majority of the CaCO₃ in the lube oil in an engine application.

Nagaki and Korematsu even concluded that increased absorption of SO₂ in the lube oil film by EGR (Exhaust Gas Recirculation), increased the wear, however, the consumption of base additives remained unchanged. This contradicts their postulate that H₂SO₄ is formed from SO₂ in the lube oil film, unless H₂SO₄ readily reacts with the cylinder liner surface upon formation, preventing interaction with CaCO₃. Yet, this seems to be unlikely, taking into account the reactivity of the CaCO₃ reverse micelles and the magnitude of the reaction rate of the H₂SO₄-CaCO₃ reaction. Instead, this may again point in the direction of SO₂ not being responsible for consuming CaCO₃, but still, in combination with water, have a corrosive effect on the cylinder liner surface.

As shown by this study, SO₂ is absorbed into the lube oil film and interaction with the liner is thereby possible. If local conditions allow a large amount of water to condense, SO₂(aq) may have direct access to the liner material, possibly promoting corrosive wear.
5.4 Conclusions

The reaction between gaseous SO2 and CaCO3 reverse micelles in lube oil has been studied using a batch reactor setup, and a mathematical model was set up in order to extract kinetic parameters of the reaction. The model was then used to predict the significance of the SO2-CaCO3 reaction at worst-case conditions similar to the ones prevailing in a large two-stroke marine diesel engine.

The experimental work in a batch reactor revealed that SO2 and CaCO3 do react in lube oil, initially forming CaSO3, but at increased residence times and temperatures, CaSO4 was also formed. Further, water had a significant effect on the degree of conversion of CaCO3, which was attributed to an increased absorption rate of SO2 in the lube oil emulsion. The effect of temperature was minor because the absorption of SO2 decreases at increased temperature and the temperature dependence on the reaction rate constant was found to be weak. Modeling of the experimental data showed that the mass transfer coefficient, \( K_G \), and reaction rate constant, \( k \), are highly correlated and multiple solutions can be found when fitting the model to the experimental data. Therefore, \( K_G \) was estimated by use of experiments from literature, and a resulting Arrhenius plot was constructed from which kinetic parameters were determined.

The batch reactor model was then used to predict CaCO3 conversions by reaction with SO2 at worst-case conditions similar to the ones prevailing in a large diesel engine by discretizing the vertical direction of the cylinder liner. The simulations revealed that the CaCO3 conversion highly depended on the SO2 concentration in the gas phase and the highest conversion of CaCO3 was therefore at TDC. However, the SO2 concentration in the gas phase readily decreases as the expansion stroke progresses and the averaged worst-case CaCO3 conversion determined (7.9%) cannot explain the CaCO3 conversions found in practice. The present study also showed that, when H2SO4 is present in the lube oil film, it will be converting the major part of the CaCO3.

Therefore, it is concluded that the reaction SO2-CaCO3 is not playing any significance in a two-stroke marine diesel engine with respect to consumption of CaCO3 reverse micelles in the lube oil. If SO2(aq) can react with the cylinder liner material and contribute to corrosion is unknown, however. This study, together with earlier work on the H2SO4-CaCO3 reaction from the present authors, are expected to facilitate and support further studies on how to control corrosive wear in large two-stroke marine diesel engines at a minimal lube oil consumption.

Acknowledgments

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Nomenclature

\( a \) = Specific gas-liquid interfacial area [m² m⁻³]
\( A \) = Pre-exponential factor [m³ mol⁻¹ s⁻¹]
\( A_L \) = Stagnant area of lube oil emulsion [m³]
\( BN \) = Base number [(mg KOH) (g oil)⁻¹]
\( Ca/S = \) Initial molar ratio of CaCO₃ in lube oil to SO₂ in gas phase \([\text{mol mol}^{-1}]\)

\( C_i^j = \) Concentration of component \( i \) in component \( j \) \([\text{mol m}^{-3}]\)

\( D = \) Diameter of the cylinder \([\text{m}]\)

\( D_i = \) Diffusion coefficient of SO₂ in component \( i \) \([\text{m}^{2} \text{s}^{-1}]\)

\( E_a = \) Activation energy \([\text{J mol}^{-1}]\)

\( f = \) Last subvolume number \([-\text{-}]\)

\( h = \) Height of a subvolume \([\text{m}]\)

\( H = \) Height of cylinder liner \([\text{m}]\)

\( H_i = \) Henry’s constant of SO₂ in component \( i \) \([\text{bar m}^{3} \text{mol}^{-1}]\)

\( i = \) Component \( i \) \([-\text{-}]\)

\( j = \) Component \( j \) \([-\text{-}]\)

\( k = \) Reaction rate constant \([\text{m}^{3} \text{mol}^{-1} \text{s}^{-1}]\)

\( k_G = \) Gas film mass transfer coefficient \([\text{mol m}^{-2} \text{s}^{-1} \text{bar}^{-1}]\)

\( K_G = \) Overall gas-side mass transfer coefficient of SO₂ \([\text{mol m}^{-2} \text{bar}^{-1} \text{s}^{-1}]\)

\( k_L = \) Liquid film mass transfer coefficient \([\text{m} \text{s}^{-1}]\)

\( l = \) Subvolume number \([-\text{-}]\)

\( N_i = \) Absorption rate of component \( i \) from the gas phase to the lube oil emulsion \([\text{mol m}^{-3} \text{s}^{-1}]\)

\( p_i^j = \) Bulk partial pressure of component \( i \) in component \( j \) \([\text{bar}]\)

\( P = \) Pressure in batch reactor \([\text{bar}]\)

\( R = \) Ideal gas constant, 8.314 \([\text{J mol}^{-1} \text{K}^{-1}]\)

\( (-r_A) = \) Reaction rate \([\text{mol m}^{-3} \text{s}^{-1}]\)

\( R_{\text{reactor}} = \) Radius of batch reactor \([\text{m}]\)

\( t = \) Time \([\text{s}]\)

\( T = \) Temperature \([\text{°C or K}]\)

\( V_i = \) Volume of component \( i \) \([\text{m}^3]\)

**Greek Letters**

\( \delta_L = \) Liquid film thickness \([\text{m}]\)

\( \tau = \) Residence time \([\text{s}]\)

**Superscripts and subscripts**

G = Gas phase

L = Lube oil emulsion (lube oil + water)

oil = Lube oil

**References**


5 Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines


Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines.


(61) Sautermeister, F. A.; Priest, M. Physical and Chemical Impact of Sulphuric Acid on Cylinder

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This chapter revisits the hypotheses presented in Chapter 1 in order to clarify whether each of the hypotheses was true or false.

**Hypothesis 1** The neutralization reaction between $H_2SO_4$ and the alkaline additives (present as micelles) in lube oil is limited by a single rate-limiting step; micelle diffusion, micelle adsorption, chemical reaction, micelle desorption, or macromixing.

The mathematical modeling in Chapter 4 could not distinguish between the potential limiting-steps outlined; however, the experimental batch reactor data together with data from literature indicate, that the neutralization reaction is presumably adsorption-controlled. In addition, a reaction rate expression with associated kinetic parameters was derived and determined.

Therefore, hypothesis 1 was found to be partly clarified. More investigations are needed to truly confirm that the rate of adsorption is the rate-controlling step.

**Hypothesis 2** The $H_2SO_4$ droplets get into the bulk of the lube oil film, eventually reaching the cylinder liner surface, by either:

- Diffusion, or
- Mixing by the piston rings

The MFR experiments revealed that decreasing the stirring rate to a very low intensity (120 rpm), led to sedimentation of the $H_2SO_4$ and thereby prevented emulsification of the $H_2SO_4$. Also, an experiment with no stirring was carried out (large excess of $H_2SO_4$ compared to CaCO$_3$ on a molar basis was present), yielding that $H_2SO_4$ sedimented. Subsequent analysis of the bulk lube oil revealed that no conversion of the CaCO$_3$ had happened. This indicates that a certain degree of stirring is needed in order to solubilize the $H_2SO_4$ into the lube oil. Further, the diffusion of the $H_2SO_4$ droplets depends very much on the size of the droplets.
Calculations of the mean Brownian displacement under engine conditions (Chapter 4) revealed that the diffusion of the H\textsubscript{2}SO\textsubscript{4} droplets is too slow to reach the cylinder liner upon condensation onto the lube oil film within the time frame available. Lastly, the lube oil is hydrophobic and H\textsubscript{2}SO\textsubscript{4} is hydrophilic, which advocates that H\textsubscript{2}SO\textsubscript{4} would just deposit on top of the lube oil film in an engine application. In conclusion, for the H\textsubscript{2}SO\textsubscript{4} to be emulsified (formation of tiny H\textsubscript{2}SO\textsubscript{4} droplets) and eventually reach the cylinder liner wall, the lube oil film has to be mixed, which happens by the piston rings.

Therefore, hypothesis 2 was found to be partly true.

**Hypothesis 3** *The specific engine conditions will have a significant impact on the conversion rate of the acidic sulfur components.*

From the H\textsubscript{2}SO\textsubscript{4} experiments and modeling, it was found that the resulting droplet size of the emulsified H\textsubscript{2}SO\textsubscript{4} is crucial for the conversion rate of H\textsubscript{2}SO\textsubscript{4}, i.e., the smaller the droplets, the faster the neutralization. The resulting droplet size may depend on the lube oil formulation, but may also be highly affected by the mixing of the piston rings (affected by for instance piston speed and design). The lube oil film temperature was also showed to exhibit a significant effect on the conversion rate. In addition, a low Ca/S molar ratio was found to significantly reduce the reactant conversions (depends for instance on the conditions in the gas phase and the lube oil dosage strategy). The available reaction time was also showed to impact the resulting conversion degree (affected by factors such as load and piston speed). An increased base number (BN) value at a maintained Ca/S molar ratio would also increase the conversion rate, but the effect is not that pronounced.

With respect to SO\textsubscript{2}, the simulations at engine conditions and the batch reactor experiments revealed that the lube oil temperature, the partial pressure of SO\textsubscript{2} in the gas phase, and the water concentration in the lube oil impact the conversion degree (which is affected by operating temperature in gas phase, pressure, sulfur content in fuel, engine speed, etc.).

Therefore, hypothesis 3 was found to be true.

**Hypothesis 4** *Different experimental setups can be used to individually investigate the sub-processes happening in a lube oil film.*

From the literature review (Chapter 2), it was found that H\textsubscript{2}SO\textsubscript{4} and SO\textsubscript{2} are the main contributors with respect to consumption of the alkaline additives and corrosive wear of the cylinder liners. To isolate the effect of each component, the reactions between H\textsubscript{2}SO\textsubscript{4}-CaCO\textsubscript{3} and SO\textsubscript{2}-CaCO\textsubscript{3} were studied individually in separate experimental setups. Modeling tools were used to extract kinetics and the relative importance of the two reactions was assessed. Furthermore, the MFR setup was used to investigate how H\textsubscript{2}SO\textsubscript{4} emulsifies and reacts in the lube oil film and a batch reactor setup was used to investigate how gaseous SO\textsubscript{2} reacts in the lube oil.

Therefore, hypothesis 4 was found to be true.
**Hypothesis 5** *The SO$_2$ reacts with the alkaline additives in the lube oil in an engine due to the high partial pressure of SO$_2$ prevailing in the combustion chamber.*

SO$_2$ is in molar excess in the engine compared to H$_2$SO$_4$, because only up to 10% of the SO$_2$ is converted to SO$_3$ (and eventually H$_2$SO$_4$). It was therefore thought that the large concentration gradient of SO$_2$, between the combustion gas and the lube oil film, would lead to rapid absorption and reaction with the alkaline additives. However, the SO$_2$ is rapidly diluted in the combustion chamber as the expansion stroke progresses and is eventually exhausted and ventilated. Simulations carried out at worst-case large engine conditions revealed that the consumption of CaCO$_3$ reverse micelles in the lube oil film from SO$_2$ is insignificant compared to the conversion from H$_2$SO$_4$. Nevertheless, if SO$_2$ consumes CaCO$_3$ in an engine, it will likely happen in the upper part of the cylinder liner, where the partial pressure of SO$_2$ in the combustion gas is highest.

Therefore, hypothesis 5 was found to be partly true, because SO$_2$ do react with CaCO$_3$, but the reaction is insignificant in a marine diesel engine application.

**Hypothesis 6** *Different analysis equipment can be used to accurately measure the BN and determine the reaction products in the lube oil.*

It was found that the titration approach is a reliable and accurate analysis method for determining the BN of lube oils. However, for the purpose of quantifying the BN rapidly upon sampling (for determining if unreacted H$_2$SO$_4$ was present in a lube oil sample), the titration method was not applicable. Also, when CaSO$_3$ was present in a lube oil sample (after reaction with SO$_2$), the titration method had difficulties in analyzing the lube oil samples. Different analysis methods were explored, such as gas analysis, ED-XRF, TGA, and FTIR (described in Appendix A). TGA proved to be applicable for determining the BN of fresh lube oils accurately. ED-XRF was useful in determining the BN from the calcium content, but also for determining the conversion by the sulfur uptake in the lube oil from SO$_2$ and H$_2$SO$_4$. However, FTIR was mainly used for analyzing the lube oil samples (after reaction with H$_2$SO$_4$ and SO$_2$), due to having various advantages compared to the other analysis techniques. Firstly, the analysis method is accurate and reliable, reflected by the low standard deviations on the resulting spectra. Secondly, it was possible to analyze the lube oil samples from the outlet of the MFR rapidly, making it possible to investigate whether complete conversion of the H$_2$SO$_4$ had been achieved within the MFR. Thirdly, with the use of FTIR, it was possible to investigate which reaction products that were formed from the reactions between H$_2$SO$_4$ and SO$_2$ with CaCO$_3$ reverse micelles.

Therefore, hypothesis 6 was found to be true.
Hypothesis 7  
*Modeling results can be used to estimate the acid concentration on the cylinder liner surface, which can be used in a model concerning the corrosive wear of the surface material.*

The mathematical model derived in Chapter 4 was used to estimate the average $\text{H}_2\text{SO}_4$ concentration in the lube oil film. Because the lube oil film was assumed to be well-mixed, the concentration of $\text{H}_2\text{SO}_4$ at the cylinder liner surface is equal to the bulk concentration of $\text{H}_2\text{SO}_4$ in the lube oil emulsion. If a corrosive wear model is derived, having the average $\text{H}_2\text{SO}_4$ concentration as an input parameter, it may be possible to predict the resulting wear rate. The mathematical model regarding $\text{SO}_2$ in Chapter 5, could also predict the $\text{SO}_2$ concentration in the lube oil film emulsion. However, a refined overall mass transfer coefficient or the validation of the model by performing laboratory scale engine experiments may be needed to improve the accuracy of the model predictions. The kinetic expressions derived in Chapters 4 and 5 may also be used in computational fluid dynamics (CFD) models to predict the temporal and spatial concentrations of $\text{H}_2\text{SO}_4$ and $\text{SO}_2$ at the cylinder liner surface.

Therefore, hypothesis 7 was found to be true.
7 | Conclusions and future work

This chapter consists of two parts. First, the results of the work presented in the preceding chapters are summarized. Then follow suggestions for further work.

7.1 Conclusions

In this thesis, the potential sulfur-related neutralization reactions, which may take place in a lubrication (lube) oil film present on a cylinder liner in large two-stroke marine diesel engines, were investigated. More specifically, the chemistry includes SO₂(g)/H₂SO₄(aq) reactions with CaCO₃(s) in reverse micelles, formulated into commercial lube oils with the purpose of protecting the cast iron cylinder liner wall and piston rings. The reactions were investigated separately using experiments and mathematical modeling.

A literature review of the two-stroke engine principle and the sulfur-related processes occurring during the combustion cycle were outlined. This included formation of SO₂ and H₂SO₄ in the combustion chamber, condensation of H₂SO₄ onto the cylinder liner surface, the reaction between H₂SO₄ and CaCO₃ reverse micelles in the lube oil, the reaction between H₂SO₄ and cast iron both with and without wear and base oil, and finally the reaction mechanism between SO₂ and CaCO₃/cast iron. Also, ways to control corrosion were described. The literature study revealed the complexity of the cold corrosion phenomenon and why it is important to develop predictive tools of the sub-processes to improve the ability to predict cold corrosion in the large two-stroke marine diesel engines, namely to accelerate and support the development process of new engine designs with improved engine efficiency.

The reaction between aqueous H₂SO₄ droplets and CaCO₃ reverse micelles in lube oil was investigated in a mixed flow reactor (MFR) setup. Lube oil samples were collected at steady state and were immediately analyzed by Fourier Transform Infrared Spectroscopy (FTIR) to determine the CaCO₃ conversion. For the residence times investigated in the MFR, it was found that the H₂SO₄-CaCO₃ reaction was significantly reduced when the Ca/S molar ratio approached unity. In addition, a certain degree of stirring was needed in order to maintain and initiate the reaction, probably due to the necessity of achieving a sufficient degree of emulsification of the H₂SO₄ into the lube oil emulsion. While the investigated range of residence times

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showed no effect on the CaCO$_3$ conversion, dilution of the inlet H$_2$SO$_4$ concentration resulted in a slight decrease in CaCO$_3$ conversion. A mathematical model of the MFR setup was developed and the only unknown parameter in the model was the average radius of the H$_2$SO$_4$ droplets. This parameter was fitted by matching simulations with experimental MFR data and values in the range 0.5-9.6 µm were estimated. From the mathematical modeling, an apparent reaction rate expression, including kinetic parameters, was presented. The mathematical modeling could not distinguish between the potential limiting-steps outlined; however, the experimental batch reactor data together with data from literature indicate, that the neutralization reaction is presumably adsorption-controlled. Because the MFR model offers a useful approximation to the conditions in the lube oil film on the cylinder liner wall, the model could be used to predict the influence of different process parameters on the H$_2$SO$_4$ conversion at conditions relevant for a full-scale application. It was found that the lube oil temperature significantly affects the H$_2$SO$_4$ conversion, while the base number (BN) of the lube oil and the H$_2$SO$_4$ droplet concentration have only a minor impact at a maintained Ca/S molar ratio. The H$_2$SO$_4$ concentration in a well-mixed lube oil film was also simulated and it was concluded that H$_2$SO$_4$ may be in contact with the cylinder liner wall regardless of how well-wetted the liner is. The H$_2$SO$_4$ concentration at the cylinder liner wall was pronounced when having a low Ca/S molar ratio (even worse when having a molar excess of H$_2$SO$_4$ compared to CaCO$_3$). This situation may correspond to the situation prevailing near TDC, where the most severe corrosive wear is found in practice. One way of reducing the wear here would thereby be to increase the amount of lube oil supplied in this upper region. To combat uncontrolled corrosive wear of the cylinder liner, it may therefore be a matter of optimizing the vertical distribution of the lube oil, having sufficient lube oil (i.e., CaCO$_3$) at the critical regions.

The reaction between gaseous SO$_2$ and CaCO$_3$ in lube oil was investigated in a stirred high-pressure high-temperature batch reactor setup. The reacted lube oil samples were analyzed by FTIR-ATR. It was observed that SO$_2$ does react with CaCO$_3$ reverse micelles in lube oil. The reaction products were found to be a mixture of CaSO$_3$ and CaSO$_4$, however, CaSO$_4$ was formed at increased residence times and temperatures. The initial concentration of water in the lube oil emulsion had a significant effect on the CaCO$_3$ conversion, while the effect of temperature was minor. These observations were explained by a change in SO$_2$ absorption in the lube oil emulsion because the absorption increases at increased water concentration and decreases at increasing temperatures. The formed CaSO$_3$ was found to react with H$_2$SO$_4$ in a similar way as the CaCO$_3$. This means that the conversion from CaCO$_3$ to CaSO$_3$ may not reduce the neutralization ability of the lube oil emulsion in terms of BN. In addition, a mathematical model was derived to describe the experimental batch reactor data in order to extract a kinetic expression for the SO$_2$-CaCO$_3$ neutralization reaction, The modeling showed a strong correlation between the mass transfer coefficient and the reaction rate constant. To cope with this, the mass transfer coefficient was estimated by the use of experimental results from the literature, and it was then possible to determine kinetic parameters for the reaction. The derived model was used to predict CaCO$_3$ conversions from SO$_2$ at conditions relevant for a full-scale marine diesel engine application. The modeling showed that CaCO$_3$ conversion is dependent on the SO$_2$ concentration in the gas phase, and the conversion of CaCO$_3$ was therefore most pronounced near TDC. Simulations carried out at worst-case conditions revealed that less than 8% of the total CaCO$_3$ in the lube oil would react with SO$_2$. The study also showed that the H$_2$SO$_4$-CaCO$_3$ reaction is much faster than the SO$_2$-CaCO$_3$ reaction at relevant full-scale conditions. This means that SO$_2$ is only expected to consume a negligible fraction of the CaCO$_3$ in the lube oil film in a marine diesel engine application. However, simulations revealed that SO$_2$ absorbs readily into the lube oil emulsion and aqueous SO$_2$ may therefore be present in the lube oil emulsion and at the cast iron cylinder liner wall in a significant amount. Even though SO$_2$ is not expected to consume any significant amount of BN, it may contribute to corrosive wear in a similar way as the H$_2$SO$_4$. 
Overall, the models developed in this thesis could be used as part of a larger diesel engine model that considers the entire cylinder. This could include gas phase modeling and H$_2$SO$_4$ condensation modeling, presented in Chapter 2, which can serve as boundary conditions for the lube oil emulsion modeling. The output from the lube oil emulsion modeling would be the H$_2$SO$_4$ concentration in the lube oil emulsion, which would serve as an input to a corrosive wear model for modeling of the corresponding wear rate. It may eventually be possible to calculate the wear rate from specific engine conditions and designs, with the aim of determining optimal lubrication strategies.

7.2 Future work

Suggestions for future work are divided into four main parts: H$_2$SO$_4$ experiments and modeling, SO$_2$ experiments and modeling, analysis methods, and overall outlook.

7.2.1 H$_2$SO$_4$ experiments and modeling

For the investigated residence times, it was observed that the H$_2$SO$_4$ neutralization reaction was significantly reduced at low Ca/S ratios, making an investigation of the limiting step possible. However, it would be interesting to investigate the reaction at even lower residence times (<48 seconds). This has been done in the literature, but without any success in quantifying the conversion of H$_2$SO$_4$ as a function of time and for different reaction systems. The FTIR proved to be a reliable and fast analysis method, which may be useful in achieving the above. The progress of the reaction could be investigated in a reciprocating pin-on-disc laboratory apparatus, which would take into account the actual mixing of the lube oil and realistic residence times.

Exploring the reaction of an H$_2$SO$_4$ droplet in commercial lube oil formulations is also recommended, in order to settle how H$_2$SO$_4$ is consumed in lube oil. This could include use of model oils and different commercial lube oils in order to map the influence of various formulations. It was suggested that the H$_2$SO$_4$ droplet may be solubilized by the excess surfactant, leading to an increased shrinking rate. It would be interesting to investigate this hypothesis in greater detail, eventually by use of the video-microscopy setup by Fu et al. It would be useful with an experimentally determined average H$_2$SO$_4$ droplet size in a fully formulated lube oil emulsion, if possible. This would also allow for the implementation of a size distribution of the H$_2$SO$_4$ droplets into the model. The literature values are based on typical emulsions, stable base oils, and stable drain oils. The H$_2$SO$_4$ droplet size may be significantly smaller than the found values due to the large amount of detergents and dispersants present in a fully formulated lube oil. In addition, the shrinkage of the H$_2$SO$_4$ droplets (instead of the assumption about a droplet is consumed at once) could also be implemented.

Mixed flow reactor experiments with different commercial or model lube oils could be carried out to assess the importance of different formulations on the kinetics, with the aim of improving the lube oil formulation. However, it was found in literature that the higher the lube oil temperature, the lower the difference between lube oils of various formulations. It would also be of interest to determine and quantify the effect of H$_2$SO$_4$ droplet concentration on the reaction rate constant.
Performing CFD simulations may be useful to verify the assumed well-mixed situation occurring in a full-scale marine diesel engine. Initial CFD simulations of a reciprocating piston ring sliding over a lube oil film were performed (a short description is given in Appendix B), but various issues arose due to the very dynamic and complex environment of the lube oil-piston ring environment. Refinement of the CFD model is highly needed.

Full-scale measurements would be interesting to perform to investigate the lube oil coverage on the cylinder liner and to investigate the hypothesis that corrosive wear is most pronounced near TDC due to an insufficient amount of lube oil containing the necessary amount of CaCO$_3$ reverse micelles. By use of FTIR immediately after sampling, it would allow for assessment of the reaction products, and thereby if CaSO$_3$ can be observed in practice. Investigation of different lube oil dosage strategies practically could provide new insight into how to improve the lube oil coverage in the critical locations where corrosive wear is pronounced without using more lube oil. It would also be useful to estimate the fraction of lube oil which is lost due to for example evaporation and combustion. This knowledge is important to optimize the lube oil feed rate by model simulations.

### 7.2.2 SO$_2$ experiments and modeling

As shown in Chapter 5, it is crucial to estimate the accurate value of the overall mass transfer coefficient $K_G$ in order to get an accurate estimate of the reaction rate constant. Therefore, carrying out experiments which measure $K_G$ would be useful. It would also be beneficial to measure the temperature dependency of Henry’s constant for SO$_2$ in lube oil. These measurement campaigns may be challenging, because measurements have to be done with a lube oil containing all the emulsifying agents, but not containing the CaCO$_3$ reverse micelles.

From literature, it is indicated that SO$_2$ has a corrosive effect on cast iron.$^9$–$^{11}$ If this is the case in an engine application, a model simulating the SO$_2$ concentration in the lube oil film at specific engine conditions is required for determination of the corresponding corrosion (and thereby wear rate). In the light of this, it is therefore crucial to verify the SO$_2$ absorption model derived in Chapter 5. The simulated absorption concentrations of SO$_2$ in the lube oil emulsion at engine conditions could be validated against laboratory scale engine experiments capable of measuring the SO$_2$ accumulation or CaCO$_3$ conversion in the lube oil.$^{12}$

Further investigations of the reaction mechanism between aqueous SO$_2$ and CaCO$_3$ reverse micelles could also be of interest. Interestingly, CaSO$_4$ was only observed in the lube oil samples at extended residence times and higher temperatures. This would clarify if CaSO$_4$ is formed by oxidation from CaSO$_3$ or directly from the reaction between CaCO$_3$-H$_2$O-SO$_2$-O$_2$. This would also be useful in improving the existing SO$_2$ model to better predict the effect of residence time on the CaCO$_3$ conversion.

### 7.2.3 Analysis methods

FTIR-ATR was mainly used to analyze the lube oil samples after reaction with H$_2$SO$_4$ and SO$_2$. Off-shore, the BN of a lube oil sample is mainly determined by a ‘BN shaker’. However, this analysis method is not that accurate, consumes solvents, breaks easily, is time-demanding, and needs a relatively large sample size. In this PhD, the FTIR-ATR analysis method proved to be reliable, accurate, easy to use, fast, and uses a little
sample size. However, a handheld FTIR-ATR apparatus for use on-board vessels is pricy and reliable calibration models are needed for accurate BN determination. The learnings from using the FTIR-ATR apparatus in this PhD can be used in further development of a handheld FTIR apparatus which can be used on-board the large vessels for lube oil analysis. This would include the development of reliable chemometric models.

7.2.4 Overall outlook

The work presented in this thesis is expected to be combined with the remaining work carried out within the SULCOR umbrella (described in Chapter 1) in order to map the influence of modified engine designs or operating conditions on the corrosive wear rate, thus providing knowledge about how to minimize lube oil and fuel consumptions without sacrificing component lifetime and reliability of the marine diesel engines. The kinetics of this work can, for instance, be used in more complex models such as 3D CFD models and coupled with gas phase\(^{13}\) and condensation\(^{14}\) models, the combined model can be used to predict the local \(\text{H}_2\text{SO}_4\) and \(\text{SO}_2\) concentrations prevailing at the liner surface. These concentration profiles at the cylinder liner surface can then be used as an input for a wear/corrosion model, which can predict the expected wear rate. Ultimately, it would be possible to estimate the wear rate of a cylinder liner at specific operating conditions and engine design and predict how different operating conditions and engine designs affect the wear rate. This would allow for optimization of the lube oil and fuel consumptions with respect to achieving low levels of cold corrosion. This would be a valuable predictive tool because engine experiments carried out in practice are often expensive, difficult, time-consuming, and non-representative.

References


(9) Xiang, Y.; Wang, Z.; Xu, C.; Zhou, C.; Li, Z.; Ni, W. Impact of \(\text{SO}_2\) Concentration on the Corrosion Rate of X70 Steel and Iron in Water-Saturated Supercritical \(\text{CO}_2\) Mixed with \(\text{SO}_2\). *J. Supercrit. Fluids*
7 Conclusions and future work


Appendix A | Lube oil analyses to determine and quantify the alkaline core of the overbased detergents

The present chapter describes shortly the different analyses carried out to determine and quantify the alkaline component(s) of the overbased detergent core that is formulated into the lube oil used for the work described in the subsequent chapters. The lube oil was supplied from Infineum and had a stated base number (BN) value of 100. The unit of BN is defined as the quantity of acid, expressed in terms of the equivalent number of milligrams of KOH required to neutralize all alkaline constituents in a one gram sample (mg KOH (g oil sample))\(^{-1}\).\(^1\) It is important to know the component(s) of the alkaline additive core to determine the H\(_2\)SO\(_4\) neutralization mechanism and which analysis methods that can be utilized for product analysis of the spent lube oils. Generally, it is reported that the core consists of either a metal carbonate or a mixture of metal carbonate and metal hydroxide. The metal cation can be Ca\(^{2+}\), Na\(^{2+}\), Mg\(^{2+}\), or a mixture thereof.\(^2\)\^-\(^5\) The reactions between the metal carbonate/hydroxide with H\(_2\)SO\(_4\) are shown in Eqs. (A.1) and (A.2), where M is the metal cation. The major difference between these two reactions is the formation of gaseous CO\(_2\) in Eq. (A.1).

\[
\begin{align*}
MCO_3(s) + H_2SO_4(aq) &\rightarrow MSO_4(s) + H_2O(l) + CO_2(g) \\
M(OH)_2(s) + H_2SO_4(aq) &\rightarrow MSO_4(s) + 2H_2O(l)
\end{align*}
\]

A.1 Titration

The standard test method of measuring BN is by titration using the method ASTM D2896.\(^1\) This method was applied in this PhD project to determine the BN in the lube oil samples using a Mettler Toledo T50 potentiometric titrator. The BN determined by this method and apparatus was regarded as the ‘actual’ BN value. Therefore, the performance and reproducibility were tested by measuring different cylinder lube oils having BN in the range 6-100. The 6 BN lube oil was a system oil, however. The results of this analysis are presented in Table A.1. The table shows the mean BN value measured by five repetitions and the two times the sample standard deviation which was found to be less than 1 BN. This means that the titration method is a precise and robust analysis method to determine the BN of a lube oil sample. However, the method does not give any information about which kind of alkaline components that are present in the lube oil.
### Table A.1. BN results from analyzing different lube oils with the ASTM D2896 method.

<table>
<thead>
<tr>
<th>#</th>
<th>6 BN</th>
<th>25 BN</th>
<th>40 BN</th>
<th>70 BN</th>
<th>100 BN</th>
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<td>6.35</td>
<td>24.58</td>
<td>40.9</td>
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</tr>
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<td>2</td>
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<td>40.62</td>
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<td>3</td>
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<td>72.84</td>
<td>98.24</td>
</tr>
<tr>
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<td>24.67</td>
<td>40.89</td>
<td>73.02</td>
<td>98.73</td>
</tr>
<tr>
<td>5</td>
<td>6.29</td>
<td>24.36</td>
<td>40.77</td>
<td>73.05</td>
<td>99.03</td>
</tr>
<tr>
<td>Mean, ( \bar{x} )</td>
<td>6.32</td>
<td>24.70</td>
<td>40.95</td>
<td>72.70</td>
<td>98.55</td>
</tr>
<tr>
<td>Standard deviation, ( s )</td>
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<td>0.29</td>
<td>0.36</td>
<td>0.44</td>
<td>0.41</td>
</tr>
<tr>
<td>( 2s / \bar{x} \times 100% )</td>
<td>2.02</td>
<td>2.35</td>
<td>1.76</td>
<td>1.20</td>
<td>0.83</td>
</tr>
</tbody>
</table>

### A.2 Gas analysis

On-board, the analysis of drain oils are often carried out by a small pressure cell for the sake of simplicity, which relates the \( \text{CO}_2 \) evolution from the reaction between an acid and \( \text{MCO}_3 \), equivalent to the reaction given in Eq. (A.1), to the BN.\(^3\) This method only has the opportunity of measuring the gas-generating reactions, thus it will not include the BN related to \( \text{M(OH)}_2 \) (Eq. (A.2)).

In relation to this, continuous analysis of the outlet gas from mixed flow reactor (MFR) experiments (the setup is described in detail in Chapter 3) by dosing \( \text{H}_2\text{SO}_4 \) and lube oil was carried out. The system was flushed continuously with nitrogen in order to only measure the \( \text{CO}_2 \) produced from the neutralization reaction, Eq. (A.1). It was found that \( \text{CO}_2 \) was produced, however, it was observed that the vast majority of the produced gaseous \( \text{CO}_2 \) was captured in the outlet lube oil stream and did thereby not go into the gas phase. Three experiences were made from these experiments: (1) gas analysis was not a suitable analysis method for detection of base number conversion in a continuous setup, (2) desorption of gaseous \( \text{CO}_2 \) from the lube oil is a slow process, and (3) \( \text{CO}_2 \) is formed from the reaction indicating that a part of the alkalinity is certainly from metal carbonate.

### A.3 Energy Dispersive X-Ray Fluorescence (ED-XRF)

To determine the metal cation of the core of the overbased detergent, Energy Dispersive X-Ray Fluorescence (ED-XRF) measurements were carried out following the standard method ASTM D7751.\(^6\) Measurements of the 100 BN lube oil from Table A.1 yielded that no sodium (Na) was present and only a negligible amount of magnesium (Mg), around 150 mg kg\(^{-1}\). On the contrary, calcium (Ca) was highly present, around 35000 mg kg\(^{-1}\) (3.5%). Converting the Ca amount in the lube oil to BN (mg KOH (g oil sample)\(^{-1}\)) gives 99.24 BN, where two times the sample standard deviation of two repetitions was 1.35 BN. Doing the same with the Mg content gives less than 1 BN. It was therefore concluded that the metal cation of the core of the reverse micelles is Ca\(^{2+}\). The ED-XRF measurements also revealed a sulfur content of around 1% in the 100 BN lube oil.
oil. Whether it is only CaCO$_3$ or a mixture of CaCO$_3$ and Ca(OH)$_2$ that are formulated into the lube oil was then investigated. Moreover, the ED-XRD method was also able to measure the conversion of CaCO$_3$, at complete reaction of the limiting reactant, by considering the sulfur uptake in the lube oil samples from reaction with SO$_2$ and H$_2$SO$_4$.

### A.4 Thermogravimetric Analysis (TGA)

The thermogravimetric analysis (TGA) method measures the weight of a sample over time as the temperature changes. This may be used to distinguish between CaCO$_3$ and Ca(OH)$_2$ with the proposed method of Kim and Olek. The products of thermal decomposition of Ca(OH)$_2$ are CaO and water and for CaCO$_3$, the products are CaO and CO$_2$. It is reported that Ca(OH)$_2$ decomposes in the temperature range 350-550 °C, whereas CaCO$_3$ decomposes in the temperature range 500-700 °C, possibly making it possible to distinguish between the two components in the lube oil. The measurements were carried out having a heating rate of 10 °C min$^{-1}$ and inert (nitrogen) atmosphere over the sample. By tracking the weight loss of a Faxe Bryozo limestone powder sample (96.9 wt.% CaCO$_3$ and 1.2 wt.% MgCO$_3$), it was found that the limestone sample started to decompose around 520 °C and the decomposition is complete around 850 °C.

A typical TGA curve of a 100 BN lube oil is presented in Figure A.1.

![TGA curve of 100 BN lube oil sample](image)

Figure A.1. TGA curve of a 100 BN lube oil sample carried out at a heating rate of 10 °C min$^{-1}$ and inert (nitrogen) atmosphere over the sample.

It is shown that the lube oil already starts to lose weight at a temperature of 150 °C. The largest fraction of the lube oil evaporates in the temperature range 300-475 °C. This may be attributed to evaporation of the lube oil itself. Just after 500 °C, the mass of the lube oil sample stagnates shortly and then decreases again at increasing temperature, until around 800 °C. The mass loss in this temperature range may be ascribed to the decomposition of CaCO$_3$. Measuring the mass loss in the temperature range 520-850 °C (the approximate decomposition temperature range for the limestone powder sample, as described above) and assumes that
Appendix A

this is solely due to evaporation of CO₂ from the CaCO₃, the resulting BN value is calculated to 99.45, which is in agreement with the actual value (98.55 BN from titrator results, see Table A.1).

This procedure was then repeated for the different lube oil samples shown in Table A.1. The resulting base numbers, determined by the TGA procedure, are graphically illustrated in Figure A.2 as a function of the BN determined from the titrator. The analysis was repeated three times for each lube oil (except for the lube oil with around 6 BN, which was only repeated twice) and the BN determined by the TGA is thereby an averaged value with corresponding two times the sample standard deviation, presented as error bars in Figure A.2. The error is larger for the TGA method than for the titrator method. The diagonal is also shown with a scattering of ±2BN. An acceptable agreement between the two analysis methods is found. Taking this into account together with the reported decomposition ranges of CaCO₃ (500-700 °C) and Ca(OH)₂ (350-550 °C), respectively, it is more than likely that the alkaline core of the overbased detergents consists solely of CaCO₃.

![Figure A.2.](image)

Figure A.2. The determined BN values from the titrator approach as a function of the BN determined from the TGA method. The error bars are two times the sample standard deviation. The grey area is the diagonal with a scattering of ±2BN.

A.5 Fourier Transform Infrared Spectroscopy (FTIR)

An analysis method capable of determining the conversion of CaCO₃ while the reaction with H₂SO₄ was in progress (at incomplete conversion of H₂SO₄) was needed for the study of the neutralization reaction (described in details in Chapters 3 and 4). The titration method was not capable of this, because the lube oil sample is first dissolved by a solvent, followed by stirring and titration with an acid, in the titration method. If unreacted H₂SO₄ was present in the lube oil prior to analysis with the titrator, it would have plenty of time and opportunity to further react with the CaCO₃. A possible analysis method measuring the immediate conversion degree of CaCO₃, regardless of the presence of H₂SO₄, was found to be Fourier Transform Infrared Spectroscopy (FTIR) with the accessory Attenuated Total Reflectance (ATR). How the FTIR-ATR could be used for this purpose is described in greater detail in Chapters 3 and 4.
Appendix A

The FTIR method was also able to distinguish between Ca(OH)$_2$ and CaCO$_3$, by obtaining an infrared spectrum of the pure components. The analyzed CaCO$_3$ is a Faxe Bryozo limestone (96.9 wt.% CaCO$_3$ and 1.2 wt.% MgCO$_3$), whereas the Ca(OH)$_2$ powder was obtained from Sigma-Aldrich (>95 wt.% Ca(OH)$_2$ and <3 wt.% CaCO$_3$). The resulting infrared spectra are depicted in Figure A.3 together with the spectrum of the 100 BN lube oil. The spectrum of the CaCO$_3$ powder has been scaled for the sake of comparison with the intensity of the two other spectra.

The locations of the bands of the powders are in agreement with reported literature locations. From the infrared spectra, it is observed that Ca(OH)$_2$ has a distinctive band around a wavenumber of 3640 cm$^{-1}$, whereas the CaCO$_3$ has several bands: at 710, 870, and 1390 cm$^{-1}$. The lube oil and CaCO$_3$ have three similar bands at the wavenumbers 710, 870, and 1400-1500 cm$^{-1}$. In addition, the lube oil spectrum has no observable band at 3640 cm$^{-1}$. Based on those observations, it is evident that no Ca(OH)$_2$ is present in the 100 BN lube oil (or at least a vanishingly small fraction, which is within the detection limit of the FTIR analysis method). It should also be noted that the very distinct band in the range 2750-3000 cm$^{-1}$ for the 100 BN lube oil spectrum is a Carbon-Hydrogen (C-H) peak.

![Infrared spectra](image)

**Figure A.3.** The infrared spectra of Ca(OH)$_2$, CaCO$_3$, and the 100 BN lube oil.

A.6 Concluding remarks

Different analysis methods were employed to determine the composition of the alkaline additive core formulated in the 100 BN lube oil used in the work of this thesis. By use of titration, gas analysis, ED-XRF, TGA, and FTIR it was concluded that the core consists of CaCO$_3$. From the different analyses, it became obvious that FTIR is a very robust, reliable, and fast analysis method. To convert from an infrared spectrum of a lube oil sample to BN, the characteristic CaCO$_3$ band at 1400-1500 cm$^{-1}$ may be useful. However, the band height/width has to be related to the BN by another technique, e.g. the titration approach, which is regarded as the most accurate analysis method for BN determination of lube oil samples. This is explored and described in greater detail in Chapters 3 and 4.
Appendix A

References


Appendix B | Short description of preliminary CFD simulations concerning the mixing of lube oil by a sliding piston ring

The mixing of the lube oil film between the cylinder liner surface and a piston ring was studied by use of CFD simulations. A report of the simulations was written by the author with the title “Mixing of Lubrication Oil at the Cylinder Liner in Marine Diesel Engines”. However, in the sake of simplicity, only a short summary of the main results from this preliminary study is provided here. The system investigated was a segment of a piston ring sliding over a cylinder liner with an initial thickness of the lube oil film of 60 µm (10 µm between piston ring tip and cylinder liner). The scope was to investigate the mixing of the lube oil accumulating in front of the moving piston ring. The system used for the simulations is shown in Figure B.1.

![Figure B.1. A sketch of a slice of a piston ring and lube oil film. The lube oil film is located on top of the cylinder liner.](image)

The simulations proved to be computationally expensive and a lot of different problems were encountered, mainly related to stability issues because of the very dynamic behavior of the piston ring-lube oil-cylinder liner system. However, it was possible to extract some indicative results when assuming no gravity. These results are shown in Figure B.2. As shown, the piston ring moves in the positive x-direction, scraping off the lube oil. Some lube oil is accumulated in front of the piston ring, making a curl. Due to the assumption of no gravity, nothing is forcing the curl downward, and the curl therefore increases in length with increasing time. One could argue that the implementation of gravity would have the effect of providing additional mixing between the curl and the lube oil film. The simulation snapshots given in Figure B.2 indicate that mixing will occur when the piston ring is moving, scraping off the lube oil film, thereby forming a curl, which eventually will mix with the stationary lube oil film phase. Taking into account the fast movement of the piston in practice, these simulations may translate to the lube oil curl in front of the moving piston ring being well-mixed. However, much more work needs to be done on this subject in order to increase the reliability of the simulations.
Figure B.2. The lube oil-piston ring simulations at different times (t) and moved piston ring lengths (L). The cross illustrates the initial position of the piston ring at t = 0 s. Main simulation parameters were: velocity of piston ring = 2.62 m s\(^{-1}\), initial lube oil film thickness = 60 µm, distance between piston ring tip and cylinder liner = 10 µm, no gravity taking into account, temperature = 25 °C, pressure = 1 atm, density of lube oil = 870 kg m\(^{-3}\), molar mass = 120 g mol\(^{-1}\), dynamic viscosity = 0.05 Pa s, time step = 10\(^{-5}\) s.
Appendix C | Supporting information for Chapter 4: Mixed flow reactor experiments and modeling of sulfuric acid neutralization in lube oil for large two-stroke diesel engines

C.1 Experiments: MFR conditions

The dotted line in the experimental figures in the main text presents the theoretical conversion of CaCO$_3$ in lube oil and added H$_2$SO$_4$, when the reaction between CaCO$_3$ and H$_2$SO$_4$ droplets is complete, i.e. all added H$_2$SO$_4$ has reacted since Ca/S $\geq$ 1. For a Ca/S molar ratio of 4, 25% conversion of the CaCO$_3$ in the lube oil is expected, as the dotted curve predicts. The dotted line for complete conversion of H$_2$SO$_4$ is therefore 100%. The measured conversions of CaCO$_3$ in the MFR (denoted Fast Analysis in figures) at specific conditions are then compared to this curve. If the values match within the uncertainties, complete conversion of H$_2$SO$_4$ has been reached in the MFR setup. The measured conversions of CaCO$_3$ in the lube oil in the MFR are represented by the squared symbols in the figures. The circled symbols represent the measured conversion of CaCO$_3$ in the lube oil sample at complete conversion (after additional reaction time with stirring of the samples, denoted Complete Conversion Analysis). Ideally, the complete conversion measurements and the dotted curve should be equal to each other. When there is a difference between the complete conversion points and fast analysis point, e.g. when Ca/S approaches 1, complete conversion of H$_2$SO$_4$ droplets was not achieved in the MFR. The numbers in the figures identify each experiment according to Table C.1.

The total residence time is longer than specified since the time between sampling and obtaining an infrared spectrum was a couple of minutes. The effect of post-sampling time on the conversion is expected to be little due to the minor effect of residence time on the conversion. Also, no stirring in the lube oil sample took place after sampling, which may contribute to quenching of the neutralization reaction.
Table C.1. Experimental conditions for the lube oil-H$_2$SO$_4$ experiments in the MFR, varying CaCO$_3$/H$_2$SO$_4$ molar ratio (Ca/S), residence time (τ), stirrer speed (N), and H$_2$SO$_4$ concentration (C$_{H_2SO_4}$) in inlet stream. Experimental uncertainty for the determination of the Ca/S molar ratio is given as two times sample standard deviation for experiments 1-3 and 5.

<table>
<thead>
<tr>
<th>Exp. #</th>
<th>Ca/S (mol mol$^{-1}$)</th>
<th>No. of exp.</th>
<th>τ (min)</th>
<th>N (rpm)</th>
<th>C$_{H_2SO_4}$ (wt.%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>9.19 ± 0.17</td>
<td>2</td>
<td>2.9</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>2</td>
<td>3.84 ± 0.07</td>
<td>2</td>
<td>2.8</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>3</td>
<td>2.10 ± 0.06</td>
<td>2</td>
<td>2.8</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>4</td>
<td>1.26</td>
<td>1</td>
<td>3.5</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>5</td>
<td>1.12 ± 0.04</td>
<td>5</td>
<td>2.2</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>6</td>
<td>1.05</td>
<td>1</td>
<td>2.1</td>
<td>1200</td>
<td>96.5</td>
</tr>
<tr>
<td>7</td>
<td>1.94</td>
<td>1</td>
<td>2.5</td>
<td>600</td>
<td>96.5</td>
</tr>
<tr>
<td>8</td>
<td>1.94</td>
<td>1</td>
<td>2.5</td>
<td>360</td>
<td>96.5</td>
</tr>
<tr>
<td>9</td>
<td>1.94</td>
<td>1</td>
<td>2.5</td>
<td>120</td>
<td>96.5</td>
</tr>
<tr>
<td>10</td>
<td>1.05</td>
<td>1</td>
<td>2.2</td>
<td>600</td>
<td>96.5</td>
</tr>
<tr>
<td>11</td>
<td>1.05</td>
<td>1</td>
<td>2.2</td>
<td>360</td>
<td>96.5</td>
</tr>
</tbody>
</table>

C.2 Residence time

Minor effect of the investigated residence times (0.8-3.5 min) on the conversions was found.$^1$ It was attributed to the reaction being very fast at well-mixed conditions until an unspecified point where the reaction is significantly reduced (or more or less stops). This behavior was also observed by others as described in Chapter 4.$^{2,3}$
C.3 Inlet sulfuric acid concentration

Decreasing the inlet H$_2$SO$_4$ concentration by a factor of 2.5, decreased the CaCO$_3$ conversion around 10\%.$^1$ This may be attributed to the introduction of large amount of water which alters the conditions in the MFR. For instance, when introducing dilute H$_2$SO$_4$ in the inlet, more droplets are needed in order to maintain a certain Ca/S molar ratio. When more water is present in the inlet and the amount of surfactants in the lube oil is limited, the dilute H$_2$SO$_4$ droplets may not be solubilized fully or fast enough. Thereby, some droplets may exist in bulk and are thereby enlarged, contributing to an increased neutralization time. In addition, fewer CaCO$_3$ reverse micelles encircle each H$_2$SO$_4$ droplet, also decreasing the adsorption rate. The trend of decreased reaction rate at decreased acid concentration is in accordance with the video-microscopy experiments performed by Duan et al.$^4$ with acetic acid droplets in a fully formulated passenger-car lube oil. A decrease in the acetic acid concentration led to a decrease in shrinking rate of the acetic acid droplet;$^4$ however, when decreasing the acid concentration, the Ca/S molar ratio increases and the isolated effect is thereby difficult to extract from the video-microscopy experiments.

C.4 Mathematical modeling: Ratio between outlet and inlet flow rates at varying H$_2$SO$_4$ droplet concentration

**Figure C.1.** Model simulations showing ratio of outlet volumetric flow rate to inlet volumetric flow rate of lube oil for three different H$_2$SO$_4$ droplet concentrations. Model parameters are: $R_{SA} = 0.5$ $\mu$m, $T = 423$ K, $\tau = 0.5$ s, $f_{L,oil,w} = 0.089$ kg kg$^{-1}$ (100 BN), as well as those in Table 4.1 in Chapter 4.
C.5 Mathematical modeling: Residence time variation for MFR conditions

Figure C.2. Model simulations showing conversion of (a) CaCO₃ reverse micelles and (b) H₂SO₄ droplets as a function of Ca/S at three values of residence time. Model parameters are: $R_{SA} = 0.5 \, \mu m$ as well as those in Table 4.1 in Chapter 4 (MFR conditions).
References


(3) Roman, J.-P. New Method of Measurement in Thin Film of the Neutralization of Marine Lubricants for Low-Speed and Medium-Speed Diesel Engines. In CIMAC Congress 1998, Copenhagen; Copenhagen, 1998; pp 913–926.

Appendix D | Supporting information for Chapter 4: Modeling of the experimental data from the work by Fu et al.

The scope of this appendix is to model the experimental shrinkage data of Fu et al., concerning reaction of a H₂SO₄ droplet in lube oil by use of a diffusion-controlled reaction rate expression. The objective is to assess whether the reaction between an H₂SO₄ droplet and CaCO₃ reverse micelles is limited by diffusion.

As presented in Section 4.4.1, the work of Fu et al. was used to calculate kinetic parameters (activation energy and pre-exponential factor) resulting in an adsorption-controlled reaction rate constant (Eq. (4.13)), since Fu et al. concluded that the reaction between an H₂SO₄ droplet and CaCO₃ reverse micelles was adsorption-controlled. However, it was found that the model (containing the diffusion-controlled reaction rate expression) matches the experimental MFR data when \( R_{SA} = 0.7 \, \mu m \) (Section 4.5). This radius of the H₂SO₄ droplets is within the expected range, as also discussed in Section 4.5 (a radius of 0.5 \( \mu m \) was calculated when using the kinetic parameters from Fu et al., see e.g. Figure 4.8). Therefore, to investigate whether the reaction is diffusion- or adsorption-controlled, the diffusion of CaCO₃ reverse micelles from bulk lube oil to the H₂SO₄ droplet is compared to the actual conversion rate of the H₂SO₄ droplet – for the experimental data given by Fu et al.

First, the molar conversion of H₂SO₄ in the droplet is related to the change in radius \( (−dR_{SA}/dt) \), according to:

\[
\frac{−dn_{SA}}{dt} = −\frac{d(V_{SA}C_{SA,d})}{dt} = 4\pi R_{SA}(t)^2C_{SA,d}\left(\frac{−dR_{SA}}{dt}\right) \tag{D.1}
\]

Here, \( V_{SA} \) is the volume of the H₂SO₄ droplet (m³), \( C_{SA,d} \) is the concentration of the H₂SO₄ in the droplet (mol m⁻³), and \( R_{SA} \) is the radius of the H₂SO₄ droplet (m).

The flux of CaCO₃ reverse micelles to the droplet is evaluated from Fick’s first law of diffusion, assuming that when \( R = R_{SA}, C_{L} = 0 \). Also, it is assumed that the H₂SO₄ droplet is immobile and much larger in size compared to the CaCO₃ reverse micelles, thus \( D_{AB} = D_{L} \) and \( R_{AB} = R_{SA} \). The flux is then given as:

\[
\bar{j} = 4\pi R_{SA}(t)D_{L}(T)C_{L} \tag{D.2}
\]

\( C_{L} \) is the bulk concentration of CaCO₃ in the lube oil (mol m⁻³) and is assumed to be constant throughout the reaction, because CaCO₃ is in great molar excess compared to H₂SO₄ in the reaction system. \( D_{L} \) is the diffusion coefficient of the reverse micelles (m² s⁻¹), which is given as:

\[
D_{L} = \frac{k_{B}T}{6\pi\eta(T)R_{L}} \tag{D.3}
\]
It is expected that $\dot{j} \geq -\frac{dn_{SA}}{dt}$, because reaction of the H$_2$SO$_4$ droplet only can progress if CaCO$_3$ is present in sufficient concentrations. If equal, this may indicate that the reaction is limited by diffusion. If the diffusive flux is much larger, it may indicate that the reaction is not controlled by diffusion. To investigate this further, the flux is put equal to $(-dn_{SA}/dt)$ and a factor, $F$, is introduced:

$$\dot{j}F = -\frac{dn_{SA}}{dt} \quad (D.4)$$

This factor describes the ratio between the molar conversion of H$_2$SO$_4$ and the flux of CaCO$_3$ reverse micelles to the droplet. If $F$ is smaller than 1, the diffusive flux is larger than the molar consumption rate, and vice versa for a value of $F$ larger than 1.

It is desirable to fit the parameter $F$ by use of the experimental data given by Fu et al.,$^1$ thus the expression given in Eq. (D.4) is solved for $dR_{SA}/dt$:

$$\frac{dR_{SA}}{dt} = -F \frac{D_L(T)C_L}{R_{SA}(t)C_{SA,d}} \quad (D.5)$$

With the initial condition: $R_{SA} = R_{SA,0}$ at $t = 0$, where $R_{SA,0}$ is the initial radius of the non-reacted droplet (from the experiments performed by Fu et al.$^1$: 71.4 µm at 25 °C, 76.45 µm at 100 °C, 58.3 µm at 130 °C, and 43.55 µm at 170 °C). The remaining parameters are given as (from Fu et al.$^1$):

- $C_{SA,d} = 9400 \frac{mol}{m^3}$ (= 50 vol.% H$_2$SO$_4$ in droplet)
- $C_L = 586.5 \frac{mol}{m^3}$ (= 70 BN lube oil, assumed constant)
- $R_L = 5 \cdot 10^{-9} m$

The temperature-dependent viscosity is calculated from the work of Sautermeister and Priest,$^4$ who measured dynamic viscosities for a base oil at different temperatures. An exponential fit of $\eta$ versus $T$ was used to describe the temperature variation of the viscosity, giving the viscosities presented in Table D.1.

| Table D.1. Calculated viscosities at temperatures in the range 25-170 °C based on work of Sautermeister and Priest.$^4$ |
|-----------------|------|------|------|------|
| Temperature, $T$ [°C] | 25   | 100  | 130  | 170  |
| Viscosity, $\eta$ [kg/(m s)] | 0.195 | 0.014 | 0.0066 | 0.0028 |

The radius-time behavior is illustrated in Figure D.1 from solving Eq. (D.5) for $F = 1$, where the points are the experimental data from Fu et al.$^1$ and the curves are the modeling results.
As shown in Figure D.1, the model does not fit the experimental data; the predicted conversion is much lower than the observed value for $F = 1$. This means that the diffusion is much slower than the actual molar conversion rate of the H$_2$SO$_4$ droplet. How much slower is investigated next by fitting the model to the experimental data by fitting of the parameter $F$, see Figure D.2.

As shown in Figure D.2, the model simulations describe the data sufficiently when having the fitted values of $F$ at each temperature. These values are shown in Table D.2.

### Table D.2. The fitted parameter $F$ at each temperature.

<table>
<thead>
<tr>
<th>Temperature, $T$ [°C]</th>
<th>25</th>
<th>100</th>
<th>130</th>
<th>170</th>
</tr>
</thead>
<tbody>
<tr>
<td>$F$ [-]</td>
<td>28.4</td>
<td>165</td>
<td>143</td>
<td>134</td>
</tr>
</tbody>
</table>
This means that the diffusion is up to 165 times ‘too slow’ in order to describe the molar conversion of the H$_2$SO$_4$ droplet. This is counterintuitive, because the molar conversion rate of H$_2$SO$_4$ cannot be larger than the molar diffusive flow of CaCO$_3$ reverse micelles to the H$_2$SO$_4$ droplet, unless the H$_2$SO$_4$ droplet is consumed by another mechanism than the direct reaction between the droplet and reverse micelle.

A small analysis is carried out below to verify that the factor cannot be attributed to uncertainties in the parameter estimation.

**Radius of the reverse micelles**
The radius of the reverse micelles was chosen as 5 nm, however, radii between 1.5 and 10 nm are reported in literature.$^{5-10}$ When the radius of the reverse micelles gets lower, the diffusion increases, but only a factor of around 3 can be found here (1.5 nm versus the 5 nm used for the calculations given here).

**Concentration of limestone in the lube oil**
The parameter $C_L$ is used to describe the concentration of limestone in the lube oil. It is assumed that this value is constant. It is assumed that this assumption is valid, since the lube oil is in great excess compared to the H$_2$SO$_4$ droplet. If a lower $C_L$ is used, this would decrease the diffusion of reverse micelles to the droplet (and thus the concentration gradient).

**Viscosity of the lube oil**
The viscosity of the lube oil was taken from Sautermeister and Priest;$^4$ it is based on a base oil. A temperature-dependent viscosity of an SAE50 cylinder lube oil was acquired from MAN Energy Solutions. Using this viscosity expression leads to the same conclusion, namely that the diffusion is much slower than the actual molar conversion rate of the H$_2$SO$_4$ droplet. The change in the fitted $F$-values, by using the changed viscosity expression, is within a factor of less than three at all temperatures.

**Concentration of the H$_2$SO$_4$ droplet**
The concentration of the H$_2$SO$_4$ droplet, $C_{S4/d}$ is equal to 9400 kg m$^{-3}$, which corresponds to a 50 vol.% H$_2$SO$_4$ solution – as used in the experiments from Fu et al. It is assumed that this value does not change during the experiments.

**Temperature**
It was assumed that the temperature is constant throughout the experiment. However, due to the heat of reaction ($\Delta H^o = -92.9$ kJ mol$^{-1}$)$^{11}$ it may be that the temperature is increased locally around the droplet. If setting $F = 1$, and fitting the temperature in order to match the model to the experimental data, the temperatures in Table D.3 are found.

<table>
<thead>
<tr>
<th>Reported temperature, $T$ [°C]</th>
<th>25</th>
<th>100</th>
<th>130</th>
<th>170</th>
</tr>
</thead>
<tbody>
<tr>
<td>Fitted temperature, $T$ [°C] (for $F=1$)</td>
<td>118</td>
<td>390</td>
<td>464</td>
<td>580</td>
</tr>
</tbody>
</table>

As shown, an extreme increase in temperature is required in the modeling in order to describe the experimental data for $F = 1$. 

---

D-4
References


Appendix E | Supporting information for Chapter 5: Experimental investigation and mathematical modeling of the reaction between SO$_2$(g) and CaCO$_3$(s)-containing micelles in lube oil for large two-stroke marine diesel engines

Nomenclature

\( a \) = Specific gas-liquid interfacial area [m$^2$ m$^{-3}$]
\( BN \) = Base number [(mg KOH) (g oil)$^{-1}$]
\( C \) = Temperature dependency constant [K]
\( Ca/S \) = Initial molar ratio of CaCO$_3$ in lube oil to SO$_2$ in gas phase [mol mol$^{-1}$]
\( C_i^j \) = Concentration of component $i$ in component $j$ [mol m$^{-3}$]
\( D_i \) = Diffusion coefficient of SO$_2$ in component $i$ [m$^2$ s$^{-1}$]
\( E \) = Liquid enhancement factor [-]
\( H_i \) = Henry’s constant of SO$_2$ in component $i$ [bar m$^3$ mol$^{-1}$]
\( i \) = Component $i$ [-]
\( j \) = Component $j$ [-]
\( k_i \) = Reaction rate constant for reaction $i$ [m$^3$ mol$^{-1}$ s$^{-1}$]
\( k_B \) = Boltzmann constant, 1.38 · 10$^{-23}$ [kg m$^2$ s$^{-2}$ K$^{-1}$]
\( k_G \) = Gas film mass transfer coefficient [mol m$^2$ s$^{-1}$ bar$^{-1}$]
\( K_G \) = Overall gas-side mass transfer coefficient of SO$_2$ [mol m$^2$ bar$^{-1}$ s$^{-1}$]
\( k_L \) = Liquid film mass transfer coefficient [m s$^{-1}$]
\( M_i \) = Molecular weight of component $i$ [g mol$^{-1}$]
\( P \) = Pressure in batch reactor [bar]
\( R \) = Ideal gas constant, 8.314 [J mol$^{-1}$ K$^{-1}$]
\( R_A \) = Radius of the solute [m]
\( t \) = Time [s]
\( T \) = Temperature [°C or K]
\( V_i \) = Volume of component $i$ [m$^3$]

Greek Letters
\( \delta_i \) = Film thickness of component $i$ [m]
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\[ \eta = \text{Viscosity \ [kg \ m^{-1} \ s^{-1}]} \]
\[ \Sigma_v = \text{Summation of atomic diffusion volumes [-]} \]
\[ \tau = \text{Residence time [s]} \]

Superscripts and subscripts

\[ G = \text{Gas phase} \]
\[ L = \text{Lube oil emulsion (lube oil + water)} \]
\[ \text{oil} = \text{Lube oil} \]

E.1 Spectra of possible products from the reaction between SO\(_2\) and CaCO\(_3\)

![Infrared spectra of pure CaCO\(_3\) (black), CaSO\(_3\) (green), and CaSO\(_4\) (red).](image)

**Figure E.1.** Infrared spectra of pure CaCO\(_3\) (black), CaSO\(_3\) (green), and CaSO\(_4\) (red).

E.2 Blank experiment

Both a room temperature and a 150 °C blank experiment were carried out by pressurizing the batch reactor to 90 bar of air for 60 minutes followed by flushing with N\(_2\). The resulting infrared spectra are shown in Figure E.2 together with an infrared spectrum of a fresh 100 BN lube oil. A little effect is observed in Figure E.2 for the room temperature blank experiment for the CaCO\(_3\) band, where water contributes to a shift in baseline, especially in the range 400-1000 cm\(^{-1}\) and 1600-1700 cm\(^{-1}\). A negligible difference between unused lube oil and the 150 °C blank experiment is also found, meaning that only the majority of the added demineralized water in the lube oil sample had evaporated during the flushing/cooling stage of the experiment. Furthermore, this also proved that the experimental procedure does not affect the CaCO\(_3\) band and more importantly that the observed change in CaCO\(_3\) band, when SO\(_2\) is present in the gas phase, is then due to reaction with SO\(_2\) only.
Figure E.2. Blank experiments at room temperature (blue) and 150 °C (red) together with a spectrum of a fresh 100 BN lube oil (black dots).

E.3 Spectrum of drain oil

Figure E.3. Infrared spectrum of a drain oil from service, showing a CaCO$_3$ and a CaSO$_4$ band.
E.4 Effect of temperature

![Infrared spectrum of an unused 100 BN lube oil (blue) and a spectrum of a lube oil exposed for SO₂ (red) at the following conditions: $P_{\text{total}}=90$ bar, 6.8 wt.% initial water in lube oil, $\text{Ca}/\text{S}=0.90$, $\tau=24$ hours, and $T=120$ °C. The locations of $\text{CaCO}_3$, $\text{CaSO}_3$, and $\text{CaSO}_4$ are also indicated in the figure.](image1)

Figure E.4. Infrared spectrum of an unused 100 BN lube oil (blue) and a spectrum of a lube oil exposed for $\text{SO}_2$ (red) at the following conditions: $P_{\text{total}}=90$ bar, 6.8 wt.% initial water in lube oil, $\text{Ca}/\text{S}=0.90$, $\tau=24$ hours, and $T=120$ °C. The locations of $\text{CaCO}_3$, $\text{CaSO}_3$, and $\text{CaSO}_4$ are also indicated in the figure.

E.5 Effect of residence time

![Spectra of lube oil samples with two different residence times. Experimental conditions: $T=153$ °C, $P_{\text{total}}=90$ bar, 6.6 wt.% initial water in lube oil, and $\text{Ca}/\text{S}$ around 1.](image2)

Figure E.5. Spectra of lube oil samples with two different residence times. Experimental conditions: $T=153$ °C, $P_{\text{total}}=90$ bar, 6.6 wt.% initial water in lube oil, and $\text{Ca}/\text{S}$ around 1.
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E.6 Stability of CaSO₃

A lube oil sample containing 6.4 wt.% of water was pressurized with 1 mol% SO₂ in air environment (initial Ca/S around 1.2) at room temperature. After one hour of reaction time, the obtained infrared spectrum revealed that almost all CaCO₃ had been converted to CaSO₃ (not all CaCO₃ was converted because Ca/S > 1); see Figure E.6. An infrared spectrum of the lube oil sample obtained the day after showed that no further reaction/oxidation had occurred. This means that the formed CaSO₃ is stable over time at room temperature and atmospheric pressure and surroundings (air). The sample was then heated in an oven for 2 hours at 150 °C. Figure E.6 shows that no CaSO₄ was formed; however, the CaSO₃ top has a different shape. The reason for this and the possibly formed product is unknown at the moment. Upon heating, most of the water evaporated. The difference in spectra before and after heating in the oven at around 1600-1700 cm⁻¹ and 400-800 cm⁻¹ is due to the removal of water (Figure E.6). This means that heating of the sample in an oven cannot oxidize the formed CaSO₃. The effect of increased air pressure and elevated temperature was then investigated, depicted in Figure E.7. No effect of pressurizing the lube oil sample at 90 bar for 2 hours at room temperature was found. A shift in baseline is found between the two spectra, which is due to an increased amount of water that was added between the two measurements prior to the experiment. Then, the sample was added to the reactor once again, pressurized with 80 bar of air (at 150 °C), and then heated to approximately 150 °C. After 1 hour at 150 °C, the reactor was cooled and a spectrum was recorded yet again. Figure E.7 reveals that the CaSO₄ band around 1060-1260 cm⁻¹ had increased in intensity, indicating that some of the CaSO₃ had oxidized to CaSO₄, however, less water was present in the sample resulting in a shift in baseline, which hampers the conclusion. No matter what, the oxidation is minor taking into account the reaction time available.

Figure E.6. Spectra of lube oil samples investigating the stability of CaSO₃: Room temperature lube oil sample with a residence time of 1 h and SO₂ in the gas phase (red), the spectrum of the lube oil sample analyzed the day after (black dotted), and a spectrum of the lube oil after heating at 150 °C in an oven for 2 h (blue).
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Figure E.7. Spectra of lube oil samples investigating the stability of CaSO₃: Room temperature lube oil sample with a residence time of 1 h and excess of SO₂ in the gas phase (Ca/S < 1) (red), followed by exposing the lube oil sample to 90 bar of air for 2 h at room temperature (green), and then exposing the lube oil sample to heating at 150 °C for 1 h at 80 bar (@150 °C) in air in the batch reactor (blue).

E.7 Neutralization ability of CaSO₃

Figure E.8. Room temperature spectrum of a lube oil sample where all CaCO₃ has been converted to CaSO₃, before (red) and after (blue) adding a specific amount of H₂SO₄.
E.8 Experimental conditions for experiments at varying temperature

Table E.1. Experimental conditions for the experiments carried out at varying temperature. The conditions for the 131 °C experiment are average values based on two similar experiments.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>#1</th>
<th>#2</th>
<th>#3</th>
<th>#4</th>
<th>#5</th>
</tr>
</thead>
<tbody>
<tr>
<td>Temperature (°C)</td>
<td>27</td>
<td>107</td>
<td>131</td>
<td>153</td>
<td>163</td>
</tr>
<tr>
<td>$P_{\text{total}}$ (bar)</td>
<td>90</td>
<td>105</td>
<td>90</td>
<td>90</td>
<td>100</td>
</tr>
<tr>
<td>$C_{SO_2,0}$ (mol m$^{-3}$)</td>
<td>16.83</td>
<td>16.77</td>
<td>17.26</td>
<td>16.93</td>
<td>17.65</td>
</tr>
<tr>
<td>$\frac{V_{\text{oil}}}{V_L}$ (m$^{-3}$ m$^{-3}$)</td>
<td>0.9388</td>
<td>0.9387</td>
<td>0.9373</td>
<td>0.9384</td>
<td>0.9377</td>
</tr>
<tr>
<td>$\frac{V_{\text{water}}}{V_L}$ (m$^{-3}$ m$^{-3}$)</td>
<td>0.0612</td>
<td>0.0613</td>
<td>0.0627</td>
<td>0.0616</td>
<td>0.0623</td>
</tr>
<tr>
<td>$V_C$ (m$^3$)</td>
<td>4.8·10$^{-4}$</td>
<td>4.8·10$^{-4}$</td>
<td>4.8·10$^{-4}$</td>
<td>4.8·10$^{-4}$</td>
<td>4.8·10$^{-4}$</td>
</tr>
<tr>
<td>$\tau$ (min)</td>
<td>10</td>
<td>10</td>
<td>10</td>
<td>10</td>
<td>10</td>
</tr>
<tr>
<td>Ca/S (mol mol$^{-1}$)</td>
<td>0.98</td>
<td>0.98</td>
<td>0.96</td>
<td>0.97</td>
<td>0.93</td>
</tr>
</tbody>
</table>

E.9 Determination of Henry’s constant for the lube oil emulsion

Henry’s constant for SO$_2$ in water was estimated from NIST.$^1$ The temperature dependence was estimated from the van’t Hoff equation:

$$H(T) = H^\circ \exp \left[C \left( \frac{1}{T} - \frac{1}{T^\circ} \right) \right] \quad (E.1)$$

Here, $H^\circ$ is Henry’s constant at $T^\circ$ (1.4 mol kg$^{-1}$ bar$^{-1}$ at 25 °C) and $C$ is a temperature dependency constant equal to 2900 K.$^1$

Costa and Underhill$^2$ present the solubility of SO$_2$ in different lube oils obtained at 25 °C in terms of the Ostwald solubility coefficient (ml of dissolved gas at the partial pressure and temperature of the experiment dissolved in 1 ml of solvent). Observing that a specific mineral oil did not react with SO$_2$ (“Squibb Medical Mineral Oil”), the average Ostwald solubility coefficient was measured to 4.97 ml ml$^{-1}$. This is converted to a Henry’s constant by use of the ideal gas law and stated density of the oil (885 kg m$^{-3}$), giving 0.227 mol kg$^{-1}$ bar$^{-1}$. Also, the Henry’s constant for SO$_2$ in a commercial lubricant (20W-40) was estimated by Nagaki and Korematsu$^3$ to 1.46±0.35 MPa mol$_{\text{oil}}$ mol$_{\text{SO}_2}^{-1}$ (one standard deviation) at 19 °C. To convert it to mol kg$^{-1}$ bar$^{-1}$, the molecular weight of the lube oil is needed. Because most of the lube oil may consist of mineral oil, the given molecular weight from Costa and Underhill for Squibb Medical Mineral Oil is used (250 g mol$^{-1}$). This gives a Henry’s constant in the range 0.221-0.360 mol kg$^{-1}$ bar$^{-1}$, which is in accordance to the value determined by Costa and Underhill.$^2$ To extrapolate Henry’s constant to elevated temperatures, the enthalpy of solution is required. However, this value is unknown for oil, to the knowledge of the authors. Therefore, the temperature dependency constant, $C$, for water is used to extrapolate Henry’s constant. Doing this gives an estimated Henry’s constant for SO$_2$ in lube oil at 131 °C equal to 0.0177 mol kg$^{-1}$ bar$^{-1}$ if using Henry’s constant determined by Costa and Underhill.
The Henry’s constants given above have the unit of \( \text{mol kg}^{-1} \text{ bar}^{-1} \), however, the unit of Henry’s constant in the modeling is \( \text{bar m}^3 \text{ mol}^{-1} \). In order to convert between these, the inverse of the Henry’s constant is divided by the density of the water and lube oil, respectively. The density of lube oil is measured at room temperature to 940 kg m\(^{-3}\), however, at elevated temperature the density decreases. The densities at higher temperatures are based on estimates. At 131 °C, the density of lube oil and water are estimated to be 871 kg m\(^{-3}\) and 934 kg m\(^{-3}\), respectively. The resulting Henry’s constants with unit \( \text{bar m}^3 \text{ mol}^{-1} \) are presented in Table E.2.

**Table E.2.** Henry's constants for water and lube oil at two temperatures (25 °C and 131 °C). Unit: bar m\(^3\) mol\(^{-1}\).

<table>
<thead>
<tr>
<th></th>
<th>25 °C</th>
<th>131 °C</th>
</tr>
</thead>
<tbody>
<tr>
<td>Water</td>
<td>(7.14 \times 10^{-4})</td>
<td>(9.80 \times 10^{-3})</td>
</tr>
<tr>
<td>Lube oil</td>
<td>(4.69 \times 10^{-3})</td>
<td>(6.50 \times 10^{-2})</td>
</tr>
</tbody>
</table>

E.10 Evaluation of resistance of SO\(_2\) from the gas phase to the liquid phase

The overall resistance to the transfer of SO\(_2\) from the gas phase to the liquid phase is equal to the sum of the resistances within the individual phases, given as:

\[
\frac{1}{K_G} = \frac{1}{k_G} + \frac{H_L}{k_L} \quad \text{(E.2)}
\]

Where the film gas mass transfer coefficient, \(k_G\), is given as:

\[
k_G = \frac{D_G}{\delta_G RT} \quad \text{(E.3)}
\]

And the film liquid mass transfer coefficient, \(k_L\), is given as:

\[
k_L = \frac{D_L}{\delta_L} \quad \text{(E.4)}
\]

\(D_G\) and \(D_L\) are the diffusion coefficients of SO\(_2\) in the gas phase and liquid phase, respectively, and \(\delta_G\) and \(\delta_L\) are the thicknesses of the gas film and liquid film, respectively. \(D_G\) is calculated by:

\[
D_G = \frac{1.43 \times 10^{-7} T^{1.75}}{P M_{AB}^{1/2} \left[ \left( \sum v \right)_A^{1/3} + \left( \sum v \right)_B^{1/3} \right]^2} \quad \text{(E.5)}
\]

Here, \(T\) is the temperature in K, \(P\) is the pressure in bar, \(M_A\) is the molecular weight of SO\(_2\) (64.1 g mol\(^{-1}\)), \(M_B\) is the molecular weight of air (29.0 g mol\(^{-1}\)), \(M_{AB} = 2 \left[ (1/M_A) + (1/M_B) \right]^{-1}\) (equal to 39.9 g mol\(^{-1}\)), and \(\sum v\) is summation of atomic diffusion volumes for each component (41.8 for SO\(_2\) and 19.7 for air). \(D_L\) is calculated by:
Here, $k_B$ is Boltzmann’s constant, $\eta$ is the viscosity of the solvent, and $R_A$ is the radius of the solute. The latter is assumed to equal half the collision diameter of the solute in the gas phase. The effect of temperature on the collision diameter is small (for nitrogen, argon, oxygen, and air), the value at room temperature is therefore used. The viscosity is estimated from the data provided by Sautermeister and Priest, who measured dynamic viscosities for a base oil at different temperatures. A linear fit of $\ln(\eta)$ versus $1/T$ was used to describe the temperature variation of the viscosity. It is assumed that pressure has a negligible effect on the diffusion coefficient in a liquid.

The combined Henry’s constant for the lube oil emulsion, as described in Chapter 5 and in the previous section, is calculated as:

$$H_L = \frac{1}{\frac{1}{H_{\text{oil}}} \left( V_{\text{oil}} \right) + \frac{1}{H_{\text{water}}} \left( V_{\text{water}} \right)}$$  \hspace{1cm} (E.7)

To evaluate the controlling resistance of the transfer of SO$_2$ from the gas phase to the liquid phase, two different temperatures are considered at a total pressure of 90 bar, 25 and 131 °C, respectively. The parameters are presented in Table E.3 and Henry’s constants of lub oil and water at 25 and 131 °C are shown in Table E.2.

**Table E.3. Input parameters used in the evaluation of resistance of SO$_2$ from the gas phase to the liquid phase.**

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Value</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>$\delta_G$</td>
<td>1·10$^{-3}$ m</td>
<td>12</td>
</tr>
<tr>
<td>$\delta_L$</td>
<td>1·10$^{-4}$ m</td>
<td>12</td>
</tr>
<tr>
<td>$R$</td>
<td>8.314·10$^{-5}$ m$^2$ bar K$^{-1}$ mol$^{-1}$</td>
<td>-</td>
</tr>
<tr>
<td>$M_{SO_2}$</td>
<td>64.1 g mol$^{-1}$</td>
<td>Calculated</td>
</tr>
<tr>
<td>$M_{air}$</td>
<td>29.0 g mol$^{-1}$</td>
<td>Calculated</td>
</tr>
<tr>
<td>$M_{SO_2,air}$</td>
<td>39.9 g mol$^{-1}$</td>
<td>Calculated</td>
</tr>
<tr>
<td>$(\Sigma v)_{SO_2}$</td>
<td>41.8</td>
<td>8</td>
</tr>
<tr>
<td>$(\Sigma v)_{air}$</td>
<td>19.7</td>
<td>8</td>
</tr>
<tr>
<td>$p$</td>
<td>90 bar</td>
<td>Exp. value</td>
</tr>
<tr>
<td>$k_B$</td>
<td>1.38·10$^{-23}$ m$^2$ kg s$^{-2}$ K$^{-1}$</td>
<td>-</td>
</tr>
<tr>
<td>$R_A$</td>
<td>1.8·10$^{-10}$ m</td>
<td>13</td>
</tr>
<tr>
<td>$\left( \frac{V_{\text{oil}}}{V_L} \right)$</td>
<td>0.9373</td>
<td>Exp. Value</td>
</tr>
<tr>
<td>$\left( \frac{V_{\text{water}}}{V_L} \right)$</td>
<td>0.0627</td>
<td>Exp. Value</td>
</tr>
<tr>
<td>$T_1$</td>
<td>25 °C</td>
<td>-</td>
</tr>
<tr>
<td>$T_2$</td>
<td>131 °C</td>
<td>-</td>
</tr>
<tr>
<td>$\eta @ T_1$</td>
<td>0.197 kg m$^{-1}$ s$^{-1}$</td>
<td>11</td>
</tr>
<tr>
<td>$\eta @ T_2$</td>
<td>0.006 kg m$^{-1}$ s$^{-1}$</td>
<td>11</td>
</tr>
</tbody>
</table>
The result of inserting the parameters, presented in Table E.2 and Table E.3, into the above equations is presented in Table E.4.

Table E.4. The calculated coefficients and constants from the equations given above: diffusion coefficients, Henry’s constants, and mass transfer coefficients.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Temperature</th>
<th>Calculated Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>(D_G)</td>
<td>(T_1)</td>
<td>(1.41 \times 10^{-7}) m(^2) s(^{-1})</td>
</tr>
<tr>
<td>(D_G)</td>
<td>(T_2)</td>
<td>(2.40 \times 10^{-7}) m(^2) s(^{-1})</td>
</tr>
<tr>
<td>(D_L)</td>
<td>(T_1)</td>
<td>(6.17 \times 10^{-12}) m(^2) s(^{-1})</td>
</tr>
<tr>
<td>(D_L)</td>
<td>(T_2)</td>
<td>(2.55 \times 10^{-10}) m(^2) s(^{-1})</td>
</tr>
<tr>
<td>(H_L)</td>
<td>(T_1)</td>
<td>(3.48 \times 10^{-3}) bar m(^3) mol(^{-1})</td>
</tr>
<tr>
<td>(H_L)</td>
<td>(T_2)</td>
<td>(4.80 \times 10^{-2}) bar m(^3) mol(^{-1})</td>
</tr>
<tr>
<td>(k_G)</td>
<td>(T_1)</td>
<td>(5.70 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
<tr>
<td>(k_G)</td>
<td>(T_2)</td>
<td>(7.16 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
<tr>
<td>(k_L)</td>
<td>(T_1)</td>
<td>(6.17 \times 10^{-8}) m s(^{-1})</td>
</tr>
<tr>
<td>(k_L)</td>
<td>(T_2)</td>
<td>(2.55 \times 10^{-9}) m s(^{-1})</td>
</tr>
<tr>
<td>(k_L/\dot{H}_L)</td>
<td>(T_1)</td>
<td>(1.77 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
<tr>
<td>(k_L/\dot{H}_L)</td>
<td>(T_2)</td>
<td>(5.30 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
<tr>
<td>(K_G)</td>
<td>(T_1)</td>
<td>(1.77 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
<tr>
<td>(K_G)</td>
<td>(T_2)</td>
<td>(5.26 \times 10^{-5}) mol m(^{-2}) s(^{-1}) bar(^{-1})</td>
</tr>
</tbody>
</table>

The calculated values in Table E.4 reveal that \(K_G \approx k_L/\dot{H}_L\), viz, mass transfer is controlled by mass transfer on the liquid side. Calculating the resistances (inverse values) give that the mass transfer of SO\(_2\) is 99.7% in the liquid phase at 25 °C and 99.3% at 131 °C. For the modeling in Chapter 5, it is therefore valid to assume that \(K_G = k_L/\dot{H}_L\).

E.11 Difference between stagnant and stirred batch reactor on \(K_G\)a

The scope of this section is to calculate the difference between a stagnant liquid film where mass transfer happens by surface diffusion and a stirred liquid volume where diffusion happens by surface convection.\(^{14}\) The calculated product \(k_La\) based on Eqs. (5.17) and (5.18) in Chapter 5 is for a stagnant case. According to Meille et al., the stirring rate has a significant effect on \(k_La\) in a batch reactor setting.\(^{15}\) They report \(k_La\) values as a function of stirring rate for four different batch reactor dimensions. The first step is to calculate \(k_La\) based on Eqs. (5.17) and (5.18) in Chapter 5, followed by comparing this value with the experimentally determined value from Meille et al. First, \(k_L\) is calculated by the procedure presented in the above section based on the conditions prevailing for reactor configuration 3 in the work of Meille et al., where the liquid was methanol and the gas phase was hydrogen.\(^{15}\) The temperature applied was 35 °C. The viscosity of methanol at this temperature is equal to 0.000474 kg m\(^{-1}\) s\(^{-1}.\(^{16}\) \(R_A\) is found to 1.45 \times 10^{-10} m which is half the collision diameter in the gas phase for hydrogen.\(^{17}\) The specific gas-liquid interfacial area is calculated to 50.7 m\(^2\) m\(^{-3}\) and \(k_La\) is then calculated to 1.66 \times 10^{-3} m s\(^{-1}\). The stirring rate applied in the batch reactor of this work was 600 rpm. At this stirring rate, a \(k_La\) of 0.1 s\(^{-1}\) was measured in the work of Meille et al. (reactor 3 without baffles).\(^{15}\) A factor of 60 is therefore found between the calculated, stagnant case and the measured.
stirred case for the conditions of Meille et al.

However, a fundamental difference is found between the present work and the work by Meille et al., viz, the liquid to reactor volume ratio. In the work of Meille et al., liquid volumes in the range 35-50% were used, and the stirrer was submerged into the liquid leading to mass transfer happening through surface convection. In the present work, the liquid volume was around 2% and the stirrer was not submerged completely into the lube oil, as illustrated in Figure 5.1 in Chapter 5. Here, the liquid surface break up and the gas entrains the liquid, called surface entrainment. Because stirrer speed has a strong effect on $k_La$, an extra factor of 2 is assumed between mass transfer achieved by surface convection and surface entrainment. This is also the factor between using baffles or not in the reactor configuration in the work of Meille et al. It is thereby assumed that the effect of surface entrainment compared to surface convection corresponds to using baffles or not. Thereby, the calculated $k_La$ determined by Eqs. (5.17) and (5.18) in Chapter 5 has to be multiplied by a factor of 120 to account for the actual stirring prevailing during the experiment.

So far, the liquid film enhancement factor, $E$, has taken the value 1. This factor is multiplied on $k_La$ and describes the enhancement of absorption of SO$_2$ when the reaction occurs within the liquid film. By evaluating the Hatta modulus using the estimated $k_L$ for a stirred case (assuming $k_La$ is increased by a factor 120 compared to the stagnant case), it is found that $E \approx 1$ and reaction is therefore occurring in the bulk liquid and not in the liquid film.

E.12 Arrhenius plot for a factor of 600 of $K_{Ga}$ between a stagnant and a stirred batch reactor

![Arrhenius plot](image)

**Figure E.9.** Arrhenius plot of the determined reaction rate constants at temperatures in the range from 107 °C to 163 °C for using 600 times the calculated $K_{Ga}$ at stagnant conditions. The linear fit, corresponding equation, and $R^2$ value are also shown. The error bars represent lower and upper $\ln(k)$ determined from two similar experiments and the data point is the average value. From the trendline, the activation energy is determined to 23.5 kJ mol$^{-1}$ and the pre-exponential factor to $1.25 \times 10^7$ m$^3$ mol$^{-1}$ s$^{-1}$. The 27 °C data point is excluded from the linear fit.
E.13 Concentration profiles for 131 °C simulation using a factor of 120 of $K_G$ between a stagnant and a stirred batch reactor

Figure E.10. Simulation results for a temperature of 131 °C showing the concentration profiles of the SO$_2$ in the gas phase, SO$_2$ in the lube oil emulsion, and CaCO$_3$ in the lube oil emulsion by fitting the reaction rate constant to achieve 42.2% conversion of CaCO$_3$ after 10 min. The following parameters were used for the simulations: $T=131$ °C, $P_{\text{total}}=90$ bar, $C_{SO_2,0}=17.26$ mol m$^{-3}$, 6.6 wt.% water, and Ca/S = 0.96.

E.14 Competition between SO$_2$-CaCO$_3$ and H$_2$SO$_4$-CaCO$_3$ reactions

To extend the reaction mechanism for the batch reactor model to include the H$_2$SO$_4$-CaCO$_3$ reaction, the following change to the CaCO$_3$ balance was implemented:

$$\frac{dC_{CaCO_3}^L}{dt} = -k_1 C_{CaCO_3}^L C_{SO_2}^L - k_2 C_{CaCO_3}^L C_{H_2SO_4}^L$$  \hspace{1cm} (E.8)

The consumption of H$_2$SO$_4$ is formulated as:

$$\frac{dC_{H_2SO_4}^L}{dt} = -k_2 C_{CaCO_3}^L C_{H_2SO_4}^L$$  \hspace{1cm} (E.9)

This assumes that the following two reactions are competing:

$$\text{CaCO}_3 + \text{SO}_2 \xrightarrow{k_1} \text{CaSO}_3 + \text{CO}_2$$  \hspace{1cm} (E.10)

$$\text{CaCO}_3 + \text{H}_2\text{SO}_4 \xrightarrow{k_2} \text{CaSO}_4 + \text{CO}_2 + \text{H}_2\text{O}$$  \hspace{1cm} (E.11)
The temperature dependent reaction rate constant for the $\text{H}_2\text{SO}_4$–$\text{CaCO}_3$ reaction is taken from Lejre et al.,$^4$ by using that the concentration of the $\text{H}_2\text{SO}_4$ droplets is $18.1 \times 10^{-3}$ mol m$^{-3}$ and that the average radius of the $\text{H}_2\text{SO}_4$ droplets is 0.5 µm, which is a typical value in emulsions.$^{19}$ There is a fundamental difference between how $\text{SO}_2$ and $\text{H}_2\text{SO}_4$ reach the bulk lube oil film. For the modeling, it was found that equilibrium occurred instantaneously between the $\text{SO}_2$ in the gas phase and lube oil emulsion film. This kept the $\text{SO}_2$ concentration in the lube oil constant (due to abundant excess of $\text{SO}_2$, on a molar basis, in the gas phase compared to the $\text{CaCO}_3$ in the lube oil) throughout the investigated residence time of 10 min. Considering $\text{H}_2\text{SO}_4$, it is believed that $\text{H}_2\text{SO}_4$ condenses during each expansion stroke on top of the lube oil film and is then mixed into emulsion during the compression stroke where it has the possibility of reacting with $\text{CaCO}_3$. This means that $\text{H}_2\text{SO}_4$ is gradually entering the lube oil emulsion during the residence time of the lube oil film. This is important to consider because the relative importance between the $\text{SO}_2$–$\text{CaCO}_3$ and $\text{H}_2\text{SO}_4$–$\text{CaCO}_3$ reactions is described by the fraction between their associated reaction rate expressions:

$$k_2C_{\text{CaCO}_3}C_{\text{H}_2\text{SO}_4}/k_1C_{\text{CaCO}_3}C_{\text{SO}_2}.$$  

The relative significance of the competing reactions is then also determined by the initial concentrations present in the lube oil emulsion. When a large fraction of $\text{H}_2\text{SO}_4$ condenses, the fraction increases. Assuming that the initial concentration of $\text{H}_2\text{SO}_4$ is equal to the initial concentration of $\text{CaCO}_3$ divided by 600 (stoichiometric molar amount between $\text{H}_2\text{SO}_4$ and $\text{CaCO}_3$ over 10 minutes and all the $\text{H}_2\text{SO}_4$ is therefore introduced over 600 combustion cycles). For subvolume 1 conditions and having one second in residence time yielded that the conversion of $\text{CaCO}_3$ was in total 0.23% and the conversion of $\text{H}_2\text{SO}_4$ was 87.1%. This means that 63% of the $\text{CaCO}_3$ was converted from $\text{H}_2\text{SO}_4$, and the rest was from $\text{SO}_2$. However, when the initial concentration of $\text{H}_2\text{SO}_4$ gets larger, more $\text{CaCO}_3$ is consumed (percentage) by $\text{H}_2\text{SO}_4$ and the same is valid for increasing temperature and decreasing partial pressure of $\text{SO}_2$ in the gas phase.

References

(10) Glassman, I.; Harris, B. L. Collision Diameters of Some Gases as a Function of Temperature. J. Phys.


