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# Prediction method for ignition delay time of liquid spray combustion in constant volume chamber

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# Abstract

A prediction method, known as the Coupled Time Scale (CTS) method, is proposed in the current work to estimate the ignition delay time (IDT) of liquid spray combustion by only performing an inert spray simulation and a zero-dimensional (0-D) homogeneous reactor (HR) simulation. The method is built upon the assumption that if the majority of the vapor regions in a spray has composition close to the most reactive mixture fraction, which can be obtained by performing 0-D HR calculations, then these regions will have a high probability to undergo high-temperature ignition and ultimately leading to autoignition in spray. The proposed method is applied to estimate hightemperature IDT of *n*-dodecane sprays. Two nozzle diameters  $(D_{noz})$  of  $90\mu m$ and  $186\mu$ m are considered, which correspond to Spray A and Spray D in the Engine Combustion Network [1], respectively. Both  $D_{noz}$  are tested at three ambient temperatures  $(T_{\rm am})$  of  $800\,{\rm K},\,900\,{\rm K}$  and  $1000\,{\rm K}.$  The fidelity of the proposed CTS method is verified by comparing the predicted IDT against CFD simulated IDT and measured IDT. Comparison of the estimated IDT from the CTS method to measured IDT yields a maximum relative difference of 24%. Meanwhile, a maximum relative difference of 33% is obtained between the IDT computed from the CTS method and the computed IDT from the large eddy

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simulations of the associated reacting sprays across the different  $T_{\rm am}$ ,  $D_{\rm noz}$  and chemical mechanisms considered in this study. *Keywords:* Ignition delay time, Homogeneous reactor, Probability density

function, Large eddy simulations, n-dodecane spray

#### 1 1. Introduction

Ignition delay time (IDT) plays a vital role in a diesel engine as it significantly influences the engine combustion and emission characteristics. Hence, an accurate prediction of the IDT in numerical studies is of the utmost importance. Apart from the mixing process, the type of chemical mechanisms used in numerical studies have significant influence on the prediction of IDT. A detailed chemical 6 mechanism consisting of hundreds of species is expected to provide a better accuracy across a wide range of conditions, but the use of such a large mechanism is computational demanding. This leads to the popularity of reduced mechanisms which retain only the essential chemical species and reactions for specific conditions 10 to achieve a balance between accuracy and computational cost. Nevertheless, 11 any chemical mechanisms must first be validated in zero-dimensional (0-D) 12 homogeneous stagnant adiabatic mixtures, such as shock tubes [2] and rapid 13 compression machines [3], before they are used for applications in three-dimensional 14 (3-D) computational fluid dynamics (CFD). Using the correlation between temperature 15 and mixture fraction predicted from CFD simulations [4, 5], the most reactive 16 mixture fraction  $(Z_{\rm mr})$  and IDT (IDT<sub>mr</sub>) [6] can be calculated from 0-D homogeneous 17 reactor (HR) simulations of a diesel spray flame. The parameter  $Z_{\rm mr}$ , defined as 18 the mixture fraction which has the shortest IDT, is known to play a significant 19 role in the autoignition process [7]. Autoignition in pure gaseous cases have 20 shown to occur where the mixture composition is close to  $Z_{\rm mr}$  and having 21 low scalar dissipation [7]. Numerous studies in spray autoignition [8, 9, 10] 22 showed similar observation in the ignition process. There are, however, also 23 numerical studies [11, 12, 13] which disagreed with this observation and showed 24 the ignition to occur in mixtures richer than  $Z_{\rm mr}$ . On the other hand, the 25

corresponding IDT<sub>mr</sub>, which is also computed from 0-D HR simulations, is 26 unable to represent the IDT of spray combustion as turbulence effects of fluid 27 flow and the liquid spray characteristics (e.g. breakup and evaporation) are not 28 considered [6] in 0-D HR simulations. This finding is supported by Dahms et 29 al. [14] who carried out one-dimensional flamelet calculations at the standard 30 Spray A condition from Engine Combustion Network (ECN) [1]. It is thus 31 apparent that performing a full reacting spray simulation, which accounts for 32 the turbulent flow field, is essential to obtain the IDT of the spray combustion. 33 However, this process may be costly depending on the size of the chemical 34 mechanism, grid resolutions, and combustion models used. 35

Setting against this background, the present work first examines the mixture 36 fraction of the ignition mixture, then proposes a method to estimate IDT of 37 spray combustion by only computing the inert spray and by performing 0-D 38 HR calculations, without the need to perform a full reacting spray simulation. 39 The method assumes that if the majority of the spray regions has composition 40 close to  $Z_{\rm mr}$ , then the regions will have a high probability to undergo high-41 temperature ignition. The method requires the probability density function 42 (PDF) of the mixture fraction (Z) computed from 3-D simulations of inert 43 sprays, as well as the  $Z_{\rm mr}$  and  $\rm IDT_{\rm mr}$  obtained from 0-D HR simulations. 44 Since the proposed approach is based on the mixing time scale from inert spray 45 simulations and chemical time scale from 0-D HR simulations, it is henceforth 46 known as the Coupled Time Scale (CTS) method. 47

The paper is structured as follows. The next section describes the experimental 48 data used for model validation as well as the numerical setup. This is followed 49 by the results from inert spray simulations, 0-D HR simulations, and reacting 50 spray simulations in Sections 3.1, 3.2, and 3.3, respectively. The proposed CTS 51 method is subsequently described in Section 3.4. Verification of the estimated 52 IDT against measured and CFD simulated IDT is also shown in this section. 53 Next, a sensitivity study of the proposed CTS method using different mechanisms 54 is carried out and shown in Section 3.5. Conclusions from this work are outlined 55 in the final section. 56

# <sup>57</sup> 2. Case descriptions & CFD model formulation

The simulated spray combustion cases conducted in the present study correspond 58 to the Spray A [1] and Spray D conditions [1, 15] of the ECN. Details of the 59 ambient gas composition, thermodynamic conditions, and injector parameters 60 are shown in Table 1. The nominal nozzle diameter  $(D_{noz})$  for Spray A and 61 Spray D are 90  $\mu$ m and 186  $\mu$ m, respectively. Both Spray A and Spray D involve 62 injecting liquid *n*-dodecane  $(C_{12}H_{26})$  through their respective nozzle with an 63 injection pressure of 150 MPa into a constant volume combustion vessel. Three 64 ambient temperatures  $(T_{\rm am})$  of 800 K, 900 K and 1000 K are tested in the present 65 study. In the inert spray case, the molar fraction of  $O_2$  is set to 0 %, whereas in 66 the reacting spray case, it is set to 15%. An Eulerian-Lagrangian approach is 67 used within the LES framework for the spray modeling in OpenFOAM-v1712. 68 Both temporal and spatial terms are discretized using second-order schemes. 69 The sub-grid scale (SGS) is modeled using the Dynamic k-equation [16]. The 70 injected liquid phase of  $C_{12}H_{26}$  is modeled as discrete parcels whose motion is 71 described using the Lagrangian particle tracking approach. Spray breakup is 72 modeled by the Reitz-Diwakar spray model [17], where the stripping breakup 73 constant,  $C_s$  is set to 10. The skeletal  $C_{12}H_{26}$  mechanism developed by Yao et 74 al. [18] (54 species and 269 reactions) is used in this work. Detailed description 75 of the mechanism can be found therein [18]. The mechanism has shown good 76 performance in spray combustion context [19, 20]. The partially stirred reactor 77 (PaSR) [21] combustion model coupled with Chemistry Coordinate Mapping 78 (CCM) [22] is used here to account for the turbulence-chemistry interactions. 79 The mixing constant,  $C_{\text{mix}}$  in the PaSR model is set to 0.3. Details about 80 the CCM approach is available in [22, 23]. The computational domain is a 81 constant volume cubic chamber with side lengths of 108 mm, which corresponds 82 to the volume of the experimental combustion vessel [1]. The ambient mixture 83 composition, pressure, and temperature are initiated as uniform field based 84 on the values shown in Table 1, while the velocity field is set to zero. All 85 boundaries are set as no-slip wall with Neumann boundary condition for the 86

Table 1: Injector specifications and operating conditions [1, 15].				
	Spray A	Spray D		
Nozzle diameter, $D_{\rm noz}~[\mu{\rm m}]$	90	186		
Injected fuel mass flow rate $[{\rm g/s}]$	The mass flow rate $[g/s]$ 2.295 11.71			
Injection pressure [MPa]	150			
Ambient density, $\rho_{\rm am}  [\rm kg/m^3]$	22.8			
Ambient temperature, $T_{\rm am}$ [K]	800, 900, 1000			
Ambient gas composition [mol %]	Inert	Reacting		
$O_2$	0.00	15.00		
$N_2$	89.71	75.15		
$CO_2$	6.52	6.22		
$H_2O$	3.77	3.62		

ambient mixture composition, pressure, and temperature. The injector is placed
at the center of one of the chamber walls. A uniform mesh spacing of 0.125 mm
is used for the spray combustion region (80 mm axially and 15 mm radially from
the nozzle location) with coarser mesh outside the region.

#### 91 3. Results & Discussion

#### 92 3.1. Inert spray

The validation of the computational setup is carried out by comparing 93 the liquid penetration length (LPL) and vapor penetration length (VPL) with 94 experimental data [1, 15, 24]. LPL is defined as the maximum axial location 95 from the injector to the location where  $95\,\%$  of the total liquid mass is found. 96 VPL is determined using the farthest downstream location of 0.1% fuel mass 97 fraction. It is shown in Figure 1 that the simulated LPL and VPL for Spray A 98 and Spray D agree well with measurement data. The LPLs are shown to decrease 99 with increasing  $T_{\rm am}$  for both Spray A and Spray D, with the trend being more 100 apparent in the Spray D cases [24]. On the other hand, the VPLs for Spray A 101



Figure 1: Temporal evolution of liquid penetration lengths (LPL) and vapor penetration lengths (VPL) for Spray A and Spray D at varying  $T_{\rm am}$ . Symbols represent measurement data.

and Spray D are shown to be insensitive to temperature variation. This also
 agrees with the experimental findings [24].

From the inert spray simulations, one can extract the temperature (T) in the flow field as a function of the local mixture fraction (Z) for Spray A and Spray D at various  $T_{\rm am}$ . The upper boundary of the T-Z diagram follows a quadratic relation,

$$T(T_{am}, Z) = T_{am} + b(T_{am}) Z + c(T_{am}) Z^2, \qquad 800 \,\mathrm{K} \ge T_{am} \ge 1000 \,\mathrm{K}$$
 (1)

where  $b(T_{\rm am}) = -4T_{\rm am} + 2700$ , and  $c(T_{\rm am}) = 6T_{\rm am} - 4700$  for Spray A;  $b(T_{\rm am}) = 6T_{\rm am} - 4700$ 108  $-2T_{\rm am} + 1100$ , and  $c(T_{\rm am}) = T_{\rm am} - 300$  for Spray D. This fitting function is 109 known as the spray mixing line, which shows the maximum T that can be 110 achieved at different Z for the inert spray case. The T-Z diagram and the 111 corresponding spray mixing line for Spray A at  $T_{\rm am} = 900 \,\mathrm{K}$  is provided in 112 Figure 2 for illustration purpose. The most reactive state,  $Z_{\rm mr}$  and  $\rm IDT_{\rm mr}$  is 113 obtained by performing 0-D HR simulations along the spray mixing line, which 114 is shown in the next section. 115



Figure 2: Scatter plots of temperature (T) and mixture fraction (Z) for Spray A at  $T_{am}$  of 900 K. Spray mixing line is represented by the red dashed-line.

#### 116 3.2. Autoignition of homogeneous mixture

The 0-D HR simulations are carried out using the ANSYS CHEMKIN-PRO 117 software. The predicted IDT profiles for Spray A and Spray D from the 0-D 118 HR simulation using the Yao mechanism are shown in Figure 3. The IDT here 119 is defined as the time when the mixture temperature increases to 400 K above 120 the initial temperature  $(T_{t=0})$ . From the figure, one can extract  $Z_{mr}$  which is 121 characterized as the Z with the shortest IDT, also known as  $IDT_{mr}$ , for different 122  $T_{\rm am}$ . It is depicted in Figure 3 that  $Z_{\rm mr}$  increases with increasing  $T_{\rm am}$  for both 123 Spray A and Spray D. 124

The extracted IDT<sub>mr</sub> for Spray A and Spray D are shown together with 125 the measured IDT from reacting spray experiments in Figure 4. It is apparent 126 from the figure that IDT<sub>mr</sub> are significantly lower than the measured reacting 127 spray IDT. Furthermore, the difference in IDT<sub>mr</sub> between Spray A and Spray D 128 does not vary with  $T_{\rm am}$ . This observation is inconsistent with the experimental 129 findings [15, 25] which shows increasing difference in the IDT between Spray A 130 and Spray D as  $T_{\rm am}$  decreases. This result also indicates that  $IDT_{\rm mr}$  itself is 131 unable to represent the IDT of the reacting spray. 132



Figure 3: Ignition delay time (IDT) of homogeneous mixtures as a function of mixture fraction (Z) for Spray A and Spray D at different  $T_{\rm am}$ . Solid black line represents stoichiometric mixture fraction,  $Z_{\rm st} = 0.045$ .

#### 133 3.3. Reacting spray

In this section, 3-D LES of reacting spray cases are performed using the 134 same setup used in Section 3.1. The reacting spray cases are validated by 135 comparing the simulated IDTs for Spray A and Spray D at different  $T_{\rm am}$  against 136 measurement data, which is depicted in Figure 4. The computed IDT from 137 3-D LES (henceforth known as  $IDT_{HT,CFD}$ ) have the same definition as the 138 measurement data, which is the time from start of injection to the time when 139 the maximum rate of maximum temperature rise in the domain occurs [13]. This 140 definition is in accordance with the ECN recommendation [1]. The predicted 141  $IDT_{HT,CFD}$  across different  $T_{am}$  and  $D_{noz}$  has a maximum relative difference of 142 14% compared to measurements. 143

Further analysis of the ignition process in mixture fraction space for Spray A and Spray D at different  $T_{\rm am}$  is conducted by examining the transition from lowto high-temperature ignition events, as shown in Figure 5. The low-temperature ignition first initiates in the fuel-lean region ( $Z < Z_{\rm st}$ ) (not shown here), where  $Z_{\rm st}$  is the stoichiometric mixture fraction with a value of 0.045. It is followed by an apparent temperature rise within the fuel-rich region ( $Z > Z_{\rm st}$ ), as shown in Figure 5a. Thereafter, the temperature rise "propagates" back towards a



Figure 4: Comparison of most reactive IDT (IDT<sub>mr</sub>), IDT from CTS method (IDT<sub>HT,CTS</sub>), IDT from CFD simulations (IDT<sub>HT,CFD</sub>), and measurements for Spray A and Spray D at various  $T_{\rm am}$ .

relatively less-rich mixture where the high-temperature ignition occurs, which is illustrated in Figure 5c. These observations agree with the findings from the LES performed by Pei et al. [13]. It is notable in Figure 5b that the transition from the low- to high-temperature ignition stage is shown to occur near  $Z_{\rm mr}$ . This implies that  $Z_{\rm mr}$  plays an important role in the ignition process.

#### <sup>156</sup> 3.4. Coupled Time Scale (CTS) method

Recently, Borghesi et al. [9] investigated the spontaneous ignition of n-157 heptane sprays at high-pressure using 3-D direct numerical simulations. The 158 study demonstrated that the higher the probability of finding regions with 159 composition closer to  $Z_{\rm mr}$ , the larger the number of ignition spots. This leads 160 to the proposed CTS method which builds upon similar hypothesis that, if the 161 majority of the vapor regions in a spray has composition close to the  $Z_{\rm mr}$ , 162 these regions will undergo high-temperature ignition and ultimately result in 163 the ignition of the whole spray. Two main assumptions are considered: i) 164 the mixture composition at  $Z_{\rm mr}$  undergoing high-temperature ignition has an 165  $\mathrm{IDT}$  equal to  $\mathrm{IDT}_{\mathrm{mr}},$  and ii) the whole spray is assumed to undergo high-166 temperature ignition when the majority of the vapor regions in the spray has 167 mixture composition equal to  $Z_{\rm mr}$ . It is also worth mentioning that scalar 168



Figure 5: Temporal evolution of the scatter plot of temperature (T) and mixture fraction (Z) for Spray A and Spray D at various  $T_{\rm am}$  conditions. Solid vertical black line represents the stoichiometric mixture fraction  $(Z_{\rm st})$ . Green and red solid vertical lines represent most reactive mixture fraction  $(Z_{\rm mr})$  for Spray A and Spray D, respectively. Columns (a), (b), and (c) represent the low-temperature ignition stage, transition stage, and high-temperature ignition stage, respectively.

dissipation rate is not considered in the proposed method. In order to examine the distribution of mixture composition in the spray, a probability density function (PDF) of Z is computed. It is expected that the spray distribution in the reacting spray case (before ignition) and in the inert spray case are similar to one another. Therefore, the PDF of Z is carried out only for the inert spray cases.

#### 175 3.4.1 Probability density function of Z for inert sprays

The PDF of Z is computed from the inert spray cases in Section 3.1 to examine the distribution of the mass originated from the fuel. The PDF of Z is defined as

$$p(Z) = \frac{\sum_{i=1}^{N_{\text{cell}}} \rho_i Z_i V_i \alpha_i}{\Delta Z \sum_{i=1}^{N_{\text{cell}}} \rho_i Z_i V_i}, \quad \alpha_i = \begin{cases} 1, & Z_i \in (Z - \Delta Z/2, \ Z + \Delta Z/2) \\ 0, & \text{otherwise} \end{cases}$$
(2)

where  $V_i$  is the volume of the *i*-th mesh cell,  $\rho_i$  is the density, and  $N_{\text{cell}}$  is the 179 total number of cells in the domain.  $\Delta Z$  is the interval of Z and is set to 0.005. 180 A moving average is then carried out on the p(Z) to filter out fluctuations. 181 Figure 6 illustrates the different time instances of p(Z) obtained from the inert 182 Spray A case at  $T_{\rm am} = 900 \,\text{K}$ . The Z value with the highest probability is 183 denoted as  $Z_{\text{peak}}$ , which is indicated by the symbols in Figure 6. It is noticeable 184 from the figure that the  $Z_{\text{peak}}$  at t = 0.1 ms and 0.2 ms are debatable as the PDF 185 of Z at these two time instances shows a plateau with two peaks. Nevertheless, 186 it does not change the fact that  $Z_{\text{peak}}$  is still decreasing over time as the PDF 187 of Z is shifting towards  $Z_{\rm st}$ . 188

The  $Z_{\text{peak}}$  at each time instance are extracted and subsequently plotted in Figures 7a and 7b for Spray A and Spray D, respectively, at different  $T_{\text{am}}$ . It is shown in Figure 7 that in all three  $T_{\text{am}}$  cases the  $Z_{\text{peak}}$  are initially fuel rich (Z > 0.1) and slowly decreasing towards  $Z_{\text{st}}$  as time progresses. This is expected as more liquid fuel evaporates and mixes with the ambient air. It is also notable that the initial  $Z_{\text{peak}}$  in Spray A is relatively richer than in Spray D (cf. Figures 7a and 7b). However, the rate at which  $Z_{\text{peak}}$  approaches  $Z_{\text{st}}$  is



Figure 6: Probability density function (PDF) of mixture fraction (Z) at different time instances for Spray A at  $T_{\rm am} = 900$  K. Solid black line represents stoichiometric mixture fraction ( $Z_{\rm st}$ ). Symbols represent mixture fraction at peak PDF ( $Z_{\rm peak}$ ).

<sup>196</sup> much faster in Spray A than in Spray D. This implies that Spray A has a faster
<sup>197</sup> mixing time than in Spray D, which is similarly shown in [25, 26]. As the mixing
<sup>198</sup> time is slower in Spray D, the majority of the spray is more fuel-rich than in
<sup>199</sup> Spray A at the same time instances, as shown in Figure 7.

# 200 3.4.2 IDT from CTS method

The  $Z_{\rm mr}$  obtained from the 0-D HR simulation in Section 3.2 at various 201  $T_{\rm am}$  are represented by horizontal dashed-lines in Figure 7. The time instance 202 when  $Z_{\text{peak}}$  intersects with the horizontal  $Z_{\text{mr}}$  line is denoted as  $t_{\text{mr}}$ , which 203 is represented as symbols in Figure 7. The parameter  $t_{\rm mr}$  indicates the time 204 taken for the majority of the spray to achieve a mixture composition close 205 to  $Z_{\rm mr}$ . It can also be interpreted as the mixing time of the spray to attain 206 mixture composition which is favorable for high-temperature ignition. Following 207 the assumption (ii) highlighted in Section 3.4, once  $t_{\rm mr}$  is attained the spray 208 undergoes similar autoignition process as computed in the 0-D HR simulations 209 with an IDT of  $IDT_{mr}$ . Therefore, the high-temperature IDT of spray combustion 210 can be estimated by adding  $t_{\rm mr}$  to its corresponding  $\rm IDT_{\rm mr}$ . This estimated 211 high-temperature IDT from using the CTS method is henceforth known  $IDT_{HT,CTS}$ . 212 The  $IDT_{HT,CTS}$  for each case is shown in Figure 4 together with the measured 213



Figure 7: Temporal evolution of mixture fraction at peak PDF ( $Z_{\text{peak}}$ ) for (a) Spray A and (b) Spray D at different  $T_{\text{am}}$ . Horizontal dashed-lines represent most reactive mixture fraction ( $Z_{\text{mr}}$ ) at different  $T_{\text{am}}$ . Symbols (•) indicate  $t_{\text{mr}}$ .

IDT [1, 15] and CFD simulated IDT<sub>HT,CFD</sub>. Comparison of IDT<sub>HT,CTS</sub> with 214 the measurement data shows good agreement with the relative differences being 215 less than 24%. Furthermore, comparison of  $IDT_{HT,CTS}$  with  $IDT_{HT,CFD}$  also 216 shows good agreement for both Spray A and Spray D cases across all three  $T_{\rm am}$ . 217 The relative differences of  $IDT_{HT,CTS}$  to  $IDT_{HT,CFD}$  are less than 33 % across 218 different  $T_{\rm am}$  and  $D_{\rm noz}$ . Scalar dissipation rate is shown to play a significant 219 role at low  $T_{\rm am}$  [27]. Its omission from the proposed method is likely the reason 220 for the larger discrepancy observed at  $T_{\rm am}$  of 800 K (cf. Figure 4). 221

It is shown experimentally in [15, 25] that IDT for Spray D is relatively longer 222 than Spray A. In addition, the difference between measured IDTs for Spray A 223 and Spray D increases as  $T_{\rm am}$  decreases. It is previously shown in Section 3.2 224 that  $IDT_{mr}$  fails to capture these experimental trend. In contrast,  $IDT_{HT,CTS}$ 225 is depicted in Figure 4 to correspond well with the measurement trend observed 226 across different  $T_{\rm am}$  and  $D_{\rm noz}$ . There is, however, a discrepancy at  $T_{\rm am}$  of 1000 K 227 where IDT<sub>HT,CTS</sub> for Spray D is shorter than Spray A. This can be attributed 228 to the uncertainty of the CTS method as the relative difference of the measured 229 IDT between Spray A and Spray D at  $1000 \,\mathrm{K}$  is  $\sim 0.02 \,\mathrm{ms}$ . Nevertheless, it is 230 clear that between  $IDT_{mr}$  and  $IDT_{HT,CTS}$ , the latter has a better agreement 231 with the experimental trend. 232



Another important feature of the proposed CTS method is the ability to

	Exp [ms]	IDT <sub>mr</sub> [ms]	IDT <sub>HT,CFD</sub> [ms]	$IDT_{HT,CTS}$ [ms]
Spray A, 800 K	1.04	0.43	1.18	0.80
Spray A, 900 K $$	0.40	0.14	0.42	0.44
Spray A, 1000 K $$	0.27	0.08	0.28	0.27
Spray D, 800 K $$	1.30	0.41	1.28	1.41
Spray D, 900 K	0.51	0.12	0.47	0.58
Spray D, 1000 K $$	0.29	0.07	0.30	0.25

Table 2: Summary of IDTs for Spray A and Spray D at various  $T_{\rm am}$ .

234 quantify the spray mixing time needed to achieve favorable mixture composition

for high-temperature ignition through the parameter  $t_{\rm mr}$ . This can be demonstrated 235 by analyzing the IDTs for the Spray A and Spray D cases at  $T_{\rm am}$  of 800 K. It 236 is previously shown in Figure 3 that the most reactive states  $(Z_{\rm mr} \text{ and } IDT_{\rm mr})$ 23 at 800 K are similar for both Spray A and Spray D. However, a noticeable 238 difference in the  $IDT_{HT,CTS}$  for Spray A and Spray D at  $T_{am}$  of 800 K can be 239 seen in Figure 4. This result can be attributed to the relatively longer  $t_{\rm mr}$ 240 obtained for Spray D than Spray A at 800 K (cf. Figure 7). This implies that 241 more time is needed to achieve the optimum composition for ignition in Spray D 242 than in Spray A due to the former having slower mixing time, which is similarly 243 postulated in [24, 25]. Overall, the results have demonstrated the feasibility of 244 the proposed CTS method in estimating the IDT for reacting spray combustion 245 without the need to perform a full reacting spray combustion simulation, as 246 well as highlight the advantages of IDT<sub>HT,CTS</sub> over IDT<sub>mr</sub>. The IDTs calculated 247 using the three methods across different conditions are also tabulated in Table 2 248 to facilitate quantitative comparisons. 249

# 250 3.5. Sensitivity of chemical mechanism

In this section, the sensitivity of the proposed CTS method to the chemical mechanisms used is evaluated by testing three other reduced mechanisms: (1)

- $_{253}$  the 57-species mechanism by Cai et al. [28] (Cai), (2) the 130-species mechanism
- <sup>254</sup> by Ranzi et al. [29] (Polimi), and (3) the 257-species mechanism by Narayanaswamy

Mechanisms	$IDT_{HT,CTS}$ [ms]	$IDT_{HT,CFD}$ [ms]	Relative difference $\%$
Cai	0.350	0.333	5.1
Polimi	0.438	0.390 [31]	11.4
Stanford	0.570	$0.530 \ [31]$	8.6

Table 3: IDTs and relative differences for different chemical mechanisms.

et al. [30] (Stanford). Detailed description of each mechanisms can be referred to in their original publications. The same methodology as those carried out for the Yao mechanism in the previous sections is applied to the three aforementioned mechanisms. It is worth mentioning that the sensitivity study is only carried out for Spray A at  $T_{\rm am}$  of 900 K.

The IDTs profiles along the spray mixing line from all three chemical mechanisms 260 are computed from the 0-D HR simulations and shown in Figures 8. The  $Z_{\rm mr}$ 261 obtained from Figure 8 for each chemical mechanism is plotted in Figure 9. 262 Their corresponding  $t_{\rm mr}$  are then extracted from the intersection points between 263  $Z_{\text{peak}}$  and  $Z_{\text{mr}}$ . Table 3 shows the calculated IDT<sub>HT,CTS</sub> for each mechanism. 264 It is also shown that the relative difference between  $IDT_{HT,CTS}$  and  $IDT_{HT,CFD}$ 265 for Cai mechanism is only 5.1 %. It is important to note that the  $IDT_{HT CFD}$ 266 presented in Table 3 for Cai mechanism is obtained by performing a 3-D LES 267 reacting spray combustion simulation using the numerical setup presented in the 268 current work. On the other hand, the IDT<sub>HT,CFD</sub> for the Polimi and Stanford 269 mechanisms shown in Table 3 are obtained from the LES results performed 270 independently and separately by Wehrfritz et al. [31] under similar Spray A 271 conditions at  $T_{\rm am}$  of 900 K. Despite obtaining the  $\rm IDT_{HT,CFD}$  from a different 272 numerical setup [31] than the present work, the  $IDT_{HT,CTS}$  computed using the 273 proposed method are still comparable with it. The relative difference for the 274 Polimi and Stanford mechanisms are within 12%. This further demonstrates 275 the feasibility of the proposed prediction method in predicting IDT of reacting 276 spray combustion using different chemical mechanisms. 277



Figure 8: Ignition delay time (IDT) of homogeneous mixtures as a function of mixture fraction (Z) for Spray A at  $T_{\rm am} = 900$  K from different mechanisms.



Figure 9: Temporal evolution of mixture fraction at peak PDF ( $Z_{\text{peak}}$ ) for Spray A at  $T_{\text{am}} =$  900 K. Horizontal dashed-lines represent most reactive mixture fraction ( $Z_{\text{mr}}$ ) for different mechanisms. Symbols (•) indicate  $t_{\text{mr}}$ .

# 278 4. Conclusion

The Coupled Time Scale (CTS) method is proposed to estimate high-temperature 279 ignition delay time (IDT) of liquid spray combustion. The method is applied to 280 *n*-dodecane spray under the ECN Spray A and Spray D conditions at ambient 281 temperature  $(T_{\rm am})$  of 800 K, 900 K, and 1000 K, where their ignitions are shown 282 to initiate at mixtures close to the most reactive mixture fraction  $(Z_{\rm mr})$ . The 283 method requires the probability density functions of mixture fraction (Z) computed 284 from 3-D LES inert spray cases, as well as the  $Z_{\rm mr}$  and most reactive IDT 285 (IDT<sub>mr</sub>) obtained from the 0-D homogeneous reactor simulations. The fidelity of 286 the proposed CTS method is verified by comparing the predicted IDT (IDT<sub>HT,CTS</sub>) 287 against measured IDT and CFD simulated IDT. The relative difference of  $IDT_{HT,CTS}$ 288 to measured IDT are less than 24 %. Meanwhile, the relative differences between 289 the  $IDT_{HT,CTS}$  and the computed IDT from CFD calculation are within 33%290 across different  $T_{\rm am}$ ,  $D_{\rm noz}$  and chemical mechanisms. It is noteworthy that scalar 291 dissipation rate is not considered in this method, which is likely the cause for 292 the larger discrepancy observed at low  $T_{\rm am}$ . Nevertheless, the proposed method 293 is shown to be capable of estimating high-temperature IDT of reacting spray 294 combustion. 295

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