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Origins of the Instability of Non-precious HER Catalysts at Open Circuit Potential

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Abstract: Non-precious hydrogen evolution reaction (HER) catalysts commonly suffer from severe dissolution under open circuit potential (OCP). In this work, using calculated Pourbaix diagrams, we quantitatively analyze the stability of a set of well-known active HER catalysts (MoS₂, MoP, CoP, Pt in acid, and Ni₃Mo in base) under working conditions. We determine that the large thermodynamic driving force towards decomposition created by the electrode/electrolyte interface potential is responsible for the substantial dissolution of non-precious HER catalysts at OCP. Our analysis further shows the stability of HER catalysts in acidic solution is ordered as Pt ~ MoS₂ > MoP > CoP, which is confirmed by the measured dissolution rates using an inductively

coupled plasma mass spectrometer. Based on gained insights, we suggest strategies to circumvent the catalyst dissolution in aqueous solution.

Electrochemical water splitting utilizing renewable energy sources enables sustainable hydrogen production. The development of active and stable non-precious electrocatalysts for hydrogen evolution reaction (HER) would make the deployment of water electrolyzers more attractive. Over the past decades a large volume of research from both experiment and computation has been devoted to the design and search for active non-precious HER catalysts that can achieve reaction rates comparable to Pt.¹⁻¹³ However, studies pertaining to catalyst stability under operating conditions lag far behind.^{14,15} Accurately characterizing the stability of an HER catalyst in an experiment is challenging. Similarly, there are few standardized methods in computation to estimate stability efficiently and accurately. More importantly, non-precious HER catalysts commonly suffer from severe corrosion at open circuit potential (OCP),¹⁶⁻¹⁸ which is a well-known problem for Ni-based HER catalysts in alkaline media,¹⁹⁻²¹ but has been largely overlooked in the development of non-precious HER catalysts in acid solutions. Using an inductively coupled plasma mass spectrometer (ICP-MS), Ledendecker et al.¹⁸ recently investigated the stability of binary metallic compounds (WC, MoS₂, Ni₅P₄ and Co₂P) and their corresponding metals under HER conditions in acid and found that the dissolution rate of these catalysts at OCP is much higher than during electrocatalysis. Nevertheless, the fundamental reason why non-precious HER catalysts experience severe dissolution at OCP remains elusive.

By mapping the chemical potential of species as a function of electrode potential and ambient pH, the Pourbaix diagram serves as a valuable tool in evaluating the stability of an electrocatalyst in aqueous environment. Experimental Pourbaix diagrams sometimes have limited

predictive capability for a material's stability due to inadequate thermodynamic data. The emergence of large computational materials databases (*e.g.*, the Materials Project²²) created from density functional theory (DFT) calculations provides a convenient and comprehensive way of assessing materials' stabilities in a high-throughput fashion.²³ Central to the applicability of these computational methods is that they are properly benchmarked against experiment. It is for instance found that Pourbaix diagrams calculated using the popular Perdew-Burke-Ernzerhof (PBE) functional²⁴ can be quite inaccurate in predicting aqueous stability in certain cases.²⁵ Leveraging the high accuracy of the strongly constrained and appropriately normed (SCAN) functional²⁶, we recently developed a simple method to accurately calculate the Pourbaix diagram of a given oxide.²⁵ In this work, we use this as a basis for analyzing the stability of four well-known active non-precious HER catalysts (MoS₂, MoP and CoP in acid, and Ni₃Mo in base) under working conditions and determine origins of the instability at OCP. The predicted stability of these catalysts is further verified by the measured dissolution rate using ICP-MS. In light of obtained insights, we finally discuss strategies to circumvent the dissolution of HER catalysts.

MoS₂ is a well-known, reasonably active non-precious HER catalyst.^{1,2} It has been reported to be stable under acidic HER conditions, but dissolves at OCP in experiment.^{17,18} Fig. 1A presents the SCAN-calculated Mo-S Pourbaix diagram. Unless stated otherwise, a default aqueous ion concentration of 10⁻⁶ M was used in the Pourbaix diagram generation. The color bar in the diagram shows the scale of aqueous stability of MoS₂. In DFT calculations, the aqueous stability of a material is quantitatively estimated by the calculated Pourbaix decomposition free energy (ΔG_{pbx}),²⁷ which is defined by the chemical potential difference between the material of interest (*e.g.*, MoS₂) and the stable chemical species, including any reaction-balancing electrons, protons, or water molecules at the corresponding electrode potential and pH on the diagram. The reaction

that defines ΔG_{pbx} may be written as $[Reactants] + a\text{H}_2\text{O} \rightarrow [Products] + m\text{H}^+ + ne^-$, where a , m , and n are determined by balancing the oxygen, hydrogen, and charge with the ambient water, proton, and electron species, whose chemical potential is determined by the pH and potential. By definition, a material with $\Delta G_{\text{pbx}} = 0$ is the most stable and will appear on the Pourbaix diagram. The larger ΔG_{pbx} , the more unstable of a material in aqueous solution. As shown in Fig. 1A, MoS_2 is predicted to be stable in acid around zero potential (0 vs. RHE). Fig. 1B shows the calculated ΔG_{pbx} as a function of potential from -0.6 V to 0.5 V at pH = 1. It can be clearly seen that MoS_2 is very stable at typical HER operating potentials (e.g., -0.4 ~ 0 V). At very negative potentials (< -0.46 V), MoS_2 tends to decompose to $\text{H}_2\text{S}(\text{s})$ and $\text{Mo}(\text{s})$ with a calculated ΔG_{pbx} of 0.2 eV/atom at -0.6 V. In the literature, it is suggested that a material with $\Delta G_{\text{pbx}} < 0.5$ eV/atom could be stabilized by self-passivation.²⁷ Specifically, the decomposition of MoS_2 into more stable solid phases, such as $\text{H}_2\text{S}(\text{s})$ and $\text{Mo}(\text{s})$ at very negative potentials, requires phase transitions which are generally slow at room temperature. MoS_2 is therefore considered to be stable at very negative potentials as well. At high positive potentials ($V > 0.35$ V), the calculated ΔG_{pbx} steeply increases with increasing potential and arrives at 0.75 eV/atom at 0.5 V, accompanied by the decomposition of MoS_2 to HSO_4^- and $\text{MoO}_2(\text{s})$. This thermodynamic trend explains why MoS_2 dissolves significantly at OCP, as experiments show that a positive potential (ca. 0.5 V in 0.1 M HClO_4) is created when bringing MoS_2 in contact with the electrolyte.^{17,18} More specifically, the large thermodynamic decomposition driving force induced by the interfacial (electrode/electrolyte) potential is responsible for the instability of MoS_2 at OCP. We note that the stability of MoS_2 under HER conditions predicted by the Materials Project PBE-calculated (abbr. MP-PBE) diagram is inconsistent with experiment. (Fig. S1)

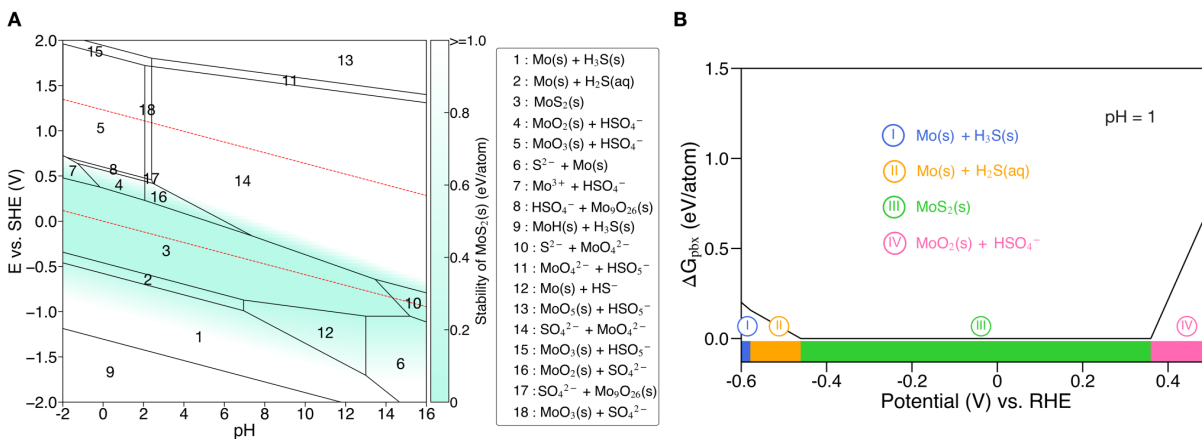


Fig. 1. Stability of MoS₂. (A) SCAN-calculated Mo-S Pourbaix diagram generated with aqueous ion concentrations 10⁻⁶ M at 25°C. The Lake blue color gauges the stability of MoS₂ at relevant potential and pH. The water stability window is shown in red dashed line. (B) Calculated Pourbaix decomposition free energy (ΔG_{pbx}) of MoS₂ from the potential -0.6–0.5 V vs. RHE at pH = 1. The projection of ΔG_{pbx} onto the potential axis highlights the stable species at the corresponding regions. Roman numerals are only to index the relevant decomposition products.

Prior reports^{23,25} have shown computational Pourbaix diagrams are primarily dictated by calculated formation enthalpies of a given chemistry. Herein, we calculated the formation enthalpies of 83 binary sulfides to examine the generality of this improved performance of the SCAN Pourbaix diagram in stability predictions. Fig. 2A shows calculated formation enthalpies (ΔH_{calc}) of 83 binary sulfides using the SCAN, PBE and MP-PBE functionals. The MP-PBE refers to the PBE ΔH_{calc} with a sulfur correction of 0.66 eV/S²⁸ applied to all sulfides in the MP. The mean absolute error (MAE) of ΔH_{calc} for SCAN, PBE and MP-PBE functionals are 0.082, 0.184 and 0.205 eV/atom, respectively. The root-mean-square error (RMSE) of ΔH_{calc} for SCAN, PBE and MPPBE functionals are 0.108, 0.226 and 0.245 eV/atom, respectively. Both the MAE and RMSE of the SCAN functional are less than half of those PBE and MP-PBE results, suggesting that the SCAN Pourbaix diagram may have higher accuracy than the MP-PBE for sulfides. Interestingly, we note that the sulfur correction used by the MP to calibrate the error in calculated formation energy for sulfides still results in a significant systematic error. Fig. 2B presents the error distribution in ΔH_{calc} of SCAN, PBE and MP-PBE functionals for 83 binary sulfides.

Compared to experimental values, the SCAN functional yields the smallest deviations, while the PBE and MP-PBE functionals largely overestimate and underestimate the results, respectively.

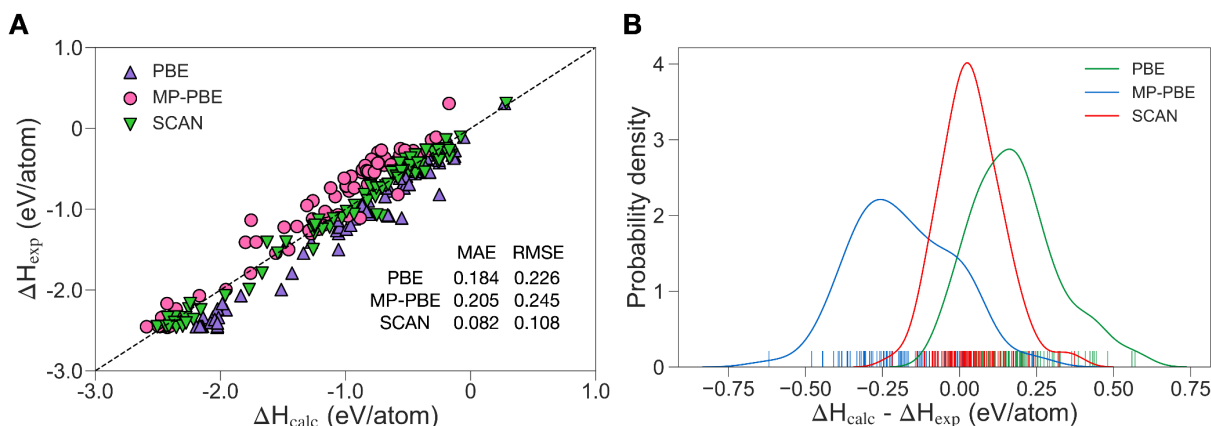


Fig. 2. Formation enthalpies (ΔH) of sulfides. (A) Experimental ΔH_{exp} as a function of calculated ΔH_{calc} for 83 binary sulfides. MP-PBE refers to ΔH_{calc} with a sulfur correction of 0.66 eV/S²⁸ adopted by the Materials Project. MAE: mean absolute error; RMSE: root mean squared error (b) Probability density distribution of energy difference between ΔH_{calc} and ΔH_{exp} for 83 binary sulfides. MP-PBE/PBE and experimental data were obtained from the Materials Project^{22,29,30} and Ref^{31,32}, respectively. Raw data are provided in Table S1.

Phosphides are another class of materials that are widely studied in search of active non-precious HER catalysts.^{33,34} Here we selected MoP^{7,9} and CoP^{8,10}, two active non-precious HER catalysts as representative to investigate their stability behaviors under HER working conditions. Fig. 3A-D show the calculated ΔG_{pbx} of MoP and CoP from potentials -0.6 to 0.5 V at pH = 1. Given that 3d transition metals are in general unstable in acidic solution,³⁵ we also calculated ΔG_{pbx} for these two catalysts at higher aqueous ions concentration (10^{-3} M) for comparison. The calculated Pourbaix diagrams of the Mo-P and Co-P chemistries are provided in Figure S2-3. At 10^{-6} M, MoP exhibits a stable range over -0.4 ~ -0.2 V, while CoP is predicted to be unstable or metastable. At 10^{-3} M, the stable range of MoP is significantly expanded with a ΔG_{pbx} of 0.66 eV/atom at 0 V. CoP now appears in a narrow stable range at ~ -0.3V with a ΔG_{pbx} of 0.97 eV/atom at 0 V. At very negative potentials (< -0.5 V), the calculated ΔG_{pbx} slightly increases with the formation of Mo(s) + PH₃(aq) for MoP and CoH(s) + PH₃(aq) for CoP. The solid phases in these

decomposition products may prevent the corrosion of the catalyst because of self-passivation or a high barrier for solid-solid phase transitions.²⁷ While the large $\Delta G_{\text{pbx}} (>1.0 \text{ eV/atom})$ beyond 0 V suggests that these catalysts would be corroded. The experimentally measured OCPs in acid for MoP and CoP are 0.38 V and 0.11 V vs. RHE, respectively. (See Fig. 4A) Similar to MoS₂, the severe dissolution of MoP and CoP at OCPs can be therefore attributed to the large thermodynamic driving force to decompose.

Platinum is one of the best HER catalysts in terms of activity and stability in acid.^{18,36-38} As a benchmark reference, we evaluated the stability behavior of Pt at pH = 1 and potential -0.6 ~ 1.0 V, as shown in Fig. 3E. The calculated Pt Pourbaix diagram is presented in Fig. S4. Clearly, Pt is predicted to be very stable under HER conditions in acidic solution, which is consistent with the experimental observation that the dissolution of Pt in 0.1 M HClO₄ can hardly be detected by ICP-MS.¹⁸ With our previous discussions, we conclude the stability of HER catalysts under hydrogen evolution is in ordered as Pt ~ MoS₂ > MoP > CoP.

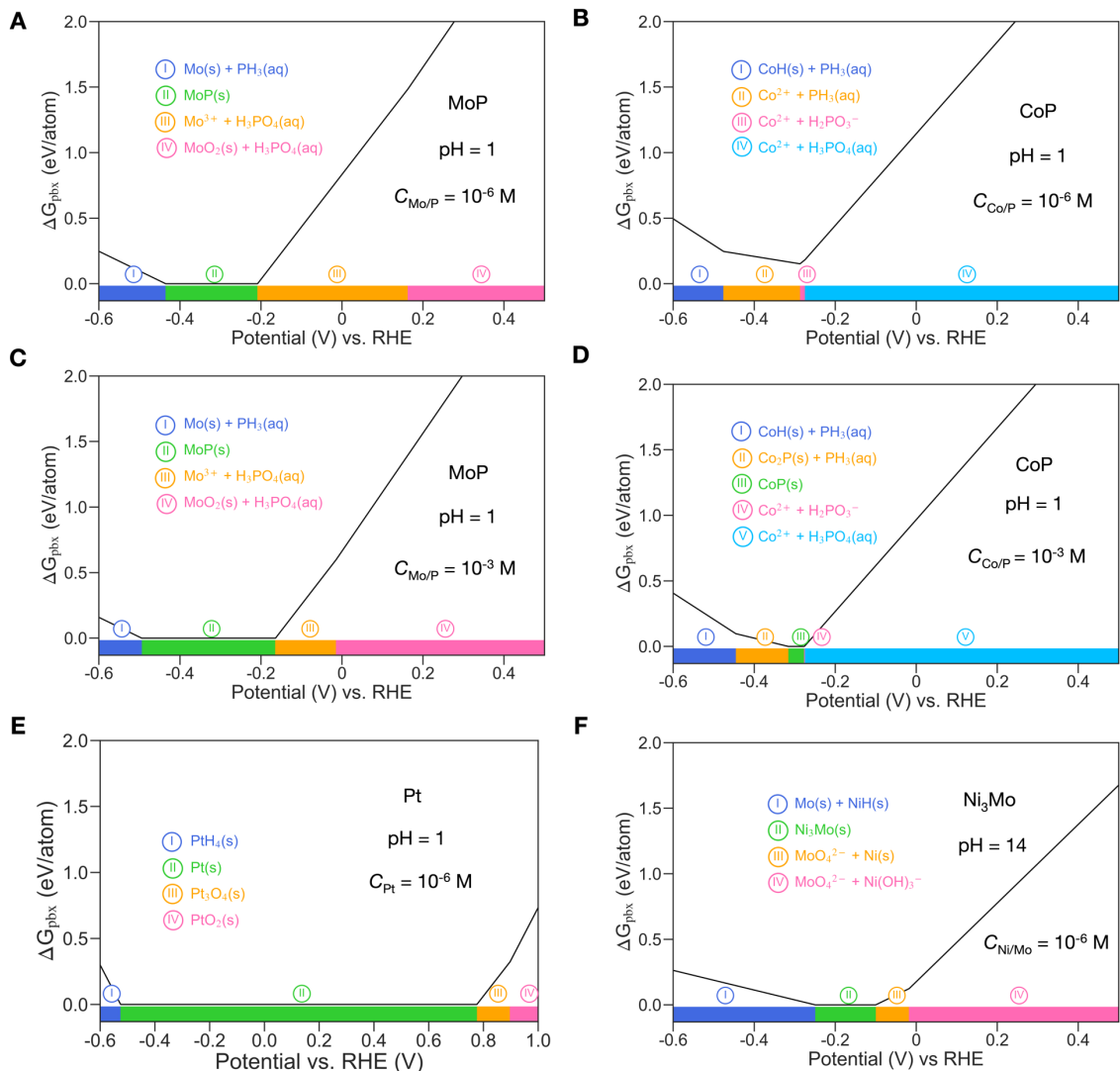


Fig. 3. Stability analysis of typical HER catalysts in both acidic and basic media. Calculated Pourbaix decomposition free energy (ΔG_{pbx}) of (A, C) MoP and (B, D) CoP and (E) Pt with different aqueous ion concentrations in acid (pH = 1). (F) Calculated ΔG_{pbx} of Ni_3Mo with aqueous ion concentrations of 10^{-6} M in alkaline (pH = 14). The projection of ΔG_{pbx} onto the potential axis highlights the stable species at the corresponding regions. Roman numerals are only to index the relevant decomposition products.

In analogy to our analysis of sulfides, we examine the accuracy of the SCAN functional in calculated formation enthalpies for 28 binary phosphides to estimate its performance in Pourbaix diagram calculations. We find that the SCAN functional slightly improves the accuracy of the PBE functional. (Fig. S5A) This small improvement for phosphides, compared to the considerable improvement for sulfides, may result from an inherent inaccuracy of the SCAN functional itself

or the large uncertainty (± 0.2 eV/atom) of experimental data. (Figure S5B, the uncertainties of ΔH_{exp} for the majority (90%) of sulfides are lower than 0.03 eV/atom.)

Ni-Mo alloys are the most active non-precious HER catalysts in alkaline conditions, whereas it has been found in experiment that Mo leaches out not only during electrocatalysis but also at OCP.^{21,39-41} Based on the calculated Ni-Mo Pourbaix diagram (Fig. S6), we plotted ΔG_{pbx} of Ni₃Mo from potentials -0.6 to 0.5 V at pH = 14, shown in Fig. 3F. In experiment, the measured overpotentials of Ni-Mo alloys are close to 0 V^{21,39-42}, and the measured OCP in 1 M NaOH is ~ 0.2 V⁴³. From Fig. 3F, we may observe that Ni₃Mo decomposes to MoO₄²⁻ + Ni(s) at potential of -0.1 ~ 0 V and MoO₄²⁻ + Ni(OH)₃⁻ at potential > 0 V. Similar results are obtained at a higher ion concentration (10⁻⁴ M). (Fig. S7) In particular, the calculated ΔG_{pbx} of Ni₃Mo significantly increases with the potential turning more positive. These results suggest that the leaching of Mo during electrocatalysis and at OCP is likely because of the intrinsic instability of the catalyst and the large thermodynamic decomposition driving force, respectively.

To validate our theoretical predictions, the electrochemical stability of MoS₂, MoP and CoP under HER and successive lower working potentials were investigated by chronoamperometry in H₂-saturated 0.5 M H₂SO₄. Before applying relevant hydrogen evolution potentials, the electrode was brought into the electrolyte under OCP, as shown in Fig. 4A. There is an OCP transition for each catalyst during the first 60s, which is likely from the catalyst dissolution. The measured OCPs for MoS₂, MoP and CoP are 0.23 V, 0.38 V and 0.11 V vs. RHE, respectively. After 1 min at OCP, the potential subsequently stepped down to relevant HER working potentials from 0 to -0.6 V vs. RHE (Fig. S9). The electrolyte was then collected after each potential for the further catalyst dissolution analysis by ICP-MS (Fig. S10). Fig. 4B displays the metal dissolution rate at different potentials. All three catalysts show a similar corrosion

behavior that the dissolution rate at OCP is one order of magnitude higher than that during hydrogen evolution, which is in line with previous study.¹⁸ Different dissolution rates of these catalysts ($\text{MoS}_2 < \text{MoP} < \text{CoP}$) clearly showcase their distinct stability behaviors in acidic solution, which qualitatively confirms our theoretical predictions. During HER (0 to -0.6 V vs. RHE), each catalyst exhibits a constant dissolution rate at different working potentials. The dissolution ratio of each electrode, (Fig. 4C) computed based on the dissolution rate and total loading of each catalyst, reveals that the main dissolution process occurs at OCPs, and the dissolution ratio of MoS_2 is three orders of magnitude higher than that of CoP and MoP. In addition, the stability number (S-number) has been reported to be a good metric to evaluate the stability of an electrocatalyst.⁴⁴ The S-number is defined as the ratio between the amount of generated product and dissolved active center. The average S-numbers of CoP, MoP, and MoS_2 were obtained according to the produced H_2 (calculated from Q_{total}) and the dissolved Co/Mo (extracted from ICP-MS) during HER (-0.2 to -0.5 V vs. RHE), as shown in Fig. 4D. MoS_2 shows the highest S-number, which is three orders and one order of magnitude higher than those of CoP and MoP, respectively. Note that S-numbers of these catalysts depend on working potentials (Fig. S11) because of the constant dissolution rates of these catalysts during hydrogen evolution. A high-performance HER catalyst is, therefore, expected to possess a higher S-number even at low overpotentials.

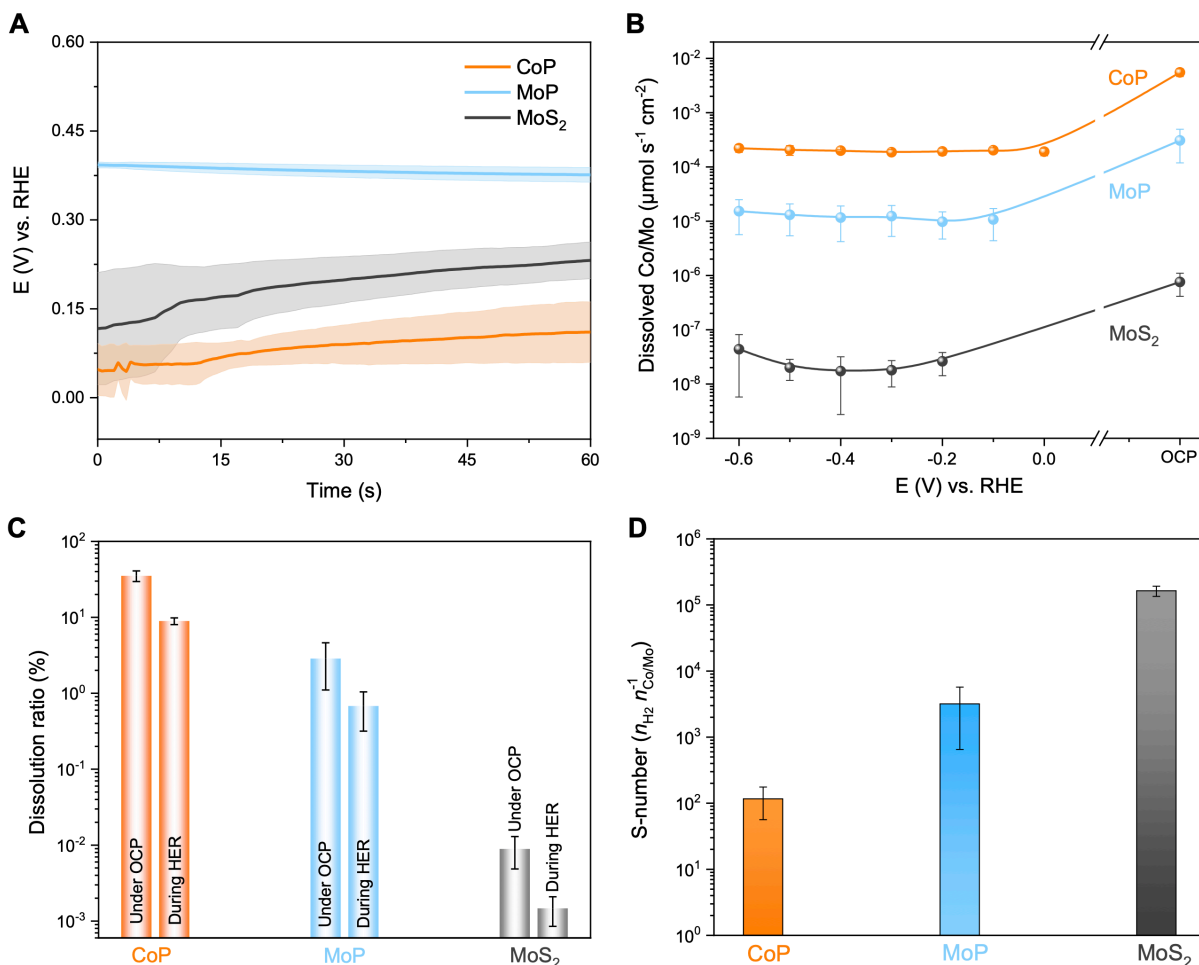


Fig. 4. Corrosion measurements of MoS₂, MoP, and CoP during HER process. (A) Open circuit potentials at CoP, MoP, and MoS₂ electrodes as a function of time in H₂-saturated 0.5 M H₂SO₄. (B) Dissolution rates of CoP, MoP, and MoS₂ at different potentials. (C) Dissolution ratios of CoP, MoP, and MoS₂ at OCP and HER working potentials (0 to -0.6 V vs. RHE). (D) The average S-numbers of CoP, MoP, and MoS₂ during HER (-0.1 to -0.5 vs. RHE). Average and standard deviations are based on three independent measurements.

We note that the measured OCP for MoS₂ in 0.5 M H₂SO₄ (0.23 V vs. RHE) is lower than that in 0.1 M HClO₄ (*ca.* 0.5 V)¹⁸. The SCAN Pourbaix diagram predicts MoS₂ to be stable up to 0.35 V (Fig. 1B), which is inconsistent with the experimental results in Fig. 4. While this difference is small (0.12 V) and does not change our conclusion of MoS₂'s robustness under acidic HER, the discrepancy suggests that there is still some error in either the accuracy of the oxidative corrosion threshold for MoS₂ predicted by SCAN or in the comparative interpretation of our results with experiment.

Based on the above stability analysis of HER catalysts, we propose possible strategies to circumvent the dissolution under working conditions. Since the corrosion of an active HER catalyst during reaction primarily results from the intrinsic instability of the material, the introduction of aqueous-stable species⁴⁵ or coating with aqueous-stable materials⁴⁶ might be conducive to enhancing the catalyst stability. At OCPs, most of, if not all non-precious HER catalysts experience higher dissolution because of the large thermodynamic decomposition driving force. One approach is to develop new active non-precious HER catalysts with a large stability window and minimal OCP. Another, and much easier, approach is to mitigate OCP by applying potential control and never let the catalyst go to OCP.⁴⁷

We also note the Pourbaix diagram construction is grounded on thermodynamics. Kinetics could also contribute to the stabilization and/or dissolution of an electrocatalyst in aqueous solution. Our results indicate the stability behavior of an electrocatalyst under working conditions could be assessed by simple thermodynamic Pourbaix analysis. Along with the widely used HER activity descriptor,⁴⁸ we anticipate that the protocol of stability analysis demonstrated in this work could contribute to the development of stable and active non-precious electrocatalysts for practical applications.

Supporting Information

Computational and experimental methods; MP-PBE Mo-S Pourbaix diagram; Mo-P, Co-P, Pt and Ni-Mo Pourbaix diagrams; Formation enthalpies of phosphides; X-ray powder diffraction; Stability measurement protocol; Calculated and experimental formation enthalpies for sulfides and phosphides; Calculated and experimental formation Gibbs free energy of solids and aqueous ions.

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