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# The Role of Big Data in Industrial (Bio)Chemical Process Operations

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12 Keywords: Big Data applications, Chemical engineering, Closed-loop systems, Control  
13 engineering, Production management, Statistical analysis  
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## 22 Abstract

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26 With the emergence of Industry 4.0 and Big Data initiatives there is a renewed interest in  
27 leveraging the vast amounts of data collected in (bio)chemical processes to improve their  
28 operations. The objective of this manuscript is to provide a perspective of the current status of Big  
29 Data-based process control methodologies and the most effective path to further embed these  
30 methodologies in the control of (bio)chemical processes. Therefore, this manuscript provides an  
31 overview of operational requirements, the availability and the nature of data, and the role of the  
32 control structure hierarchy in (bio)chemical processes and how they constrain this endeavor. The  
33 current state of the seemingly competing methodologies of Statistical Process Monitoring and  
34 (Engineering) Process Control is examined together with hybrid methodologies that are attempting  
35 to combine tools and techniques that belong to either camp. The technical and economic  
36 considerations of a deeper integration between the two approaches is then explored and a path  
37 forward is proposed.  
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## 1. Introduction

Recent breakthroughs in Big Data-based algorithms and analytics have enabled the solution of complex and multi-faceted real-time problems at an extraordinary level of performance. A recent “poster child” for this transformation is Google DeepMind, which is able to defeat an expert player in the two-player abstract strategy game Go <sup>1</sup>. Similar examples can also be found in video games where Big Data-based algorithms are now capable of excelling at complex multi-level games <sup>2</sup>. A clear comparison can be drawn between the level of reasoning and the nature of these video games and some of the operational requirements of (bio)chemical plants. For example, the objective in plant operation is to react to the current “state” of the plant with the aim of delivering safe operations (similar to surviving in a video game) and improving the overall economics (similar to reaching the next level). However, there are some key difficulties that differentiate a video game from (bio)chemical operations.

First of all, even in a popular video game such as Angry Birds, the large number of possible actions and the need to plan beyond the current move has caused the Big Data-driven Artificial Intelligence (AI) to fail in matching a good human performance <sup>3</sup>. This is despite the fact that over 60 expert teams used multiple combinations of Big Data-based concepts such as advanced simulation, reasoning, planning, heuristic search and various Machine Learning (ML) approaches (including deep learning).

Secondly, most of these algorithms are inherently “data hungry”, which is not a problem in a video game environment. The game engine can be used to generate millions of scenarios, which is infeasible in a (bio)chemical plant. Although, “digital models” of (bio)chemical plants could be

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3 deployed to generate large amounts of process data <sup>4</sup> for the implementation of “data hungry”  
4 algorithms.  
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8 Thirdly, unlike in a video game, the Big Data-based algorithms must not trip production facilities  
9 during operation, which means that they must ensure near 100% safety, while delivering optimal  
10 overall performance. This duality is one of the grand challenges in the deployment of AI <sup>3</sup>  
11 applications.  
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17 Even though such methods and algorithms cannot simply be reapplied to (bio)chemical  
18 operations, there is promise in Big Data-based concepts, ranging from clustering methods to  
19 regression methods and data processing techniques to the different ML methods. The recent rapid  
20 advances in the field of Big Data has created momentum in the chemical and biochemical  
21 industries towards implementation of these algorithms in various capacities with the primary  
22 motivation of using Big Data to get better insight from available plant data that can improve the  
23 overall economic bottom line.  
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34 However, it should be noted that a similar momentum in the past decades failed to materialize  
35 into tangible solutions due to a lack of organizational readiness to support and maintain these  
36 implementations <sup>5</sup>. Many corporations, even today, do not realize the significance the huge  
37 increase in digitalization and the interconnectivity of things may bring about. This has strong  
38 implications on future strategic pathways, which may be observed in the automotive industry that  
39 is struggling with the change from a production-centric industry to a business differentiated by  
40 software offerings. Since the (bio)chemical industry is not an end-consumer-facing industry,  
41 cyber-physical developments are not easy to spot and their significance may not be properly  
42 accounted for in managerial decisions. Therefore, it is important that one should neither get carried  
43 away by the exciting new developments outlined above nor be apprehensive of them.  
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Besides the algorithmic “auto-piloting” of a (bio)chemical plant, there are many other operational objectives that are of relevance to ensure smooth operations. These include:

- Planning and logistics in general that are required to ensure sufficient raw material, utilities and personnel are available to carry out process operations; the requirement to handle non-routine process upsets (for example, non-routine upsets of plant utilities that require a change in operational objectives <sup>6</sup>) and plant scheduling requirements that take into account the contractual obligations that must be fulfilled.
- Ensuring both asset utilization and equipment efficiencies are kept at high levels; as a part of this endeavor, the implementation of a robust equipment maintenance schedule that facilitates optimal equipment uptime and asset utilization and, to this end, the use of data-driven predictive maintenance concepts that allow for “just-in-time” scheduling.
- Safety and environmental factors that include minimizing waste, reducing plant trips, avoiding uncertain states and reducing storage of hazardous substances.

It should be noted that the above objectives (with the exception of predictive maintenance) currently rely on mathematical planning systems, personnel insights and ingenuity, handcrafted analyses or a combination thereof. The advances of Big Data-based methodologies can also supplement or replace some of these tasks, freeing people from repetitive jobs, with specifically trained operators/engineers only acting as application support.

Another aspect that must be addressed when discussing Big Data in process operations is the flow of data and the data infrastructure that must be established, in particular, to allow for “real-time” data gathering required to implement some of these Big Data-based concepts in an operational environment. Although the Industry 4.0 initiative <sup>7</sup> and, in particular, the Internet of Things (IoT) part, has been leading the facilitation of the “4 Vs” (volume, variety, velocity and

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3 veracity) of plant data <sup>8,9</sup>, it can be seen that the process industries are lagging behind the  
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5 automotive industry, for example, where these concepts have resulted in step changes in  
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7 operations. This lag in the process industries is partially due to the lacking *value*, a 5th “V”, of the  
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9 data available. To this end, it is important to note that data flow from process plants needs to go  
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11 beyond the traditional and well established 4/20 mA analog process signals toward digital readings  
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13 and supporting infrastructure that can provide tangible improvements. Besides, new sensors that  
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15 are capable of capturing information-rich data are required. Whereas the recent advances in Big  
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17 Data-based algorithms together with the seemingly vast amount of “4 V” compatible data promise  
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19 a seismic shift in the way process control and operations are handled in a (bio)chemical plant, a  
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21 closer look at the current state of process control shows that these changes and their capabilities  
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23 have yet to trickle down to the operational level.  
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29 Yet it is important to realize that this is not only a matter of technology. The different approaches  
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31 put forward by statisticians and engineers, the former mainly in process monitoring and the latter  
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33 in closed-loop process control, need to be synergistically combined to make Big Data work in a  
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35 (bio)chemical plant. This, however, needs to start with a joint understanding of terminology. For  
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37 instance, Box et al. <sup>10</sup> use *Engineering Process Control* (EPC) as a catch-all term that involves  
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39 combinations of manipulated and controlled variables. *Statistical Process Control* (SPC) refers to  
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41 the detection of faults, not explicitly covering the diagnosis of the cause. To distinguish between  
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43 these, we will be using the term (Statistical) Process Monitoring (SPM) to encompass both  
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45 detection and diagnosis of faults while the term Process Control (PC) will indicate the presence of  
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47 various forms of closed-loop control structures as part of the operational assets.  
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52 Consequently, the objective of this manuscript is to provide a balanced perspective of Big Data  
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54 capabilities and the requirements imposed by the plant operations. To this end, a systematic  
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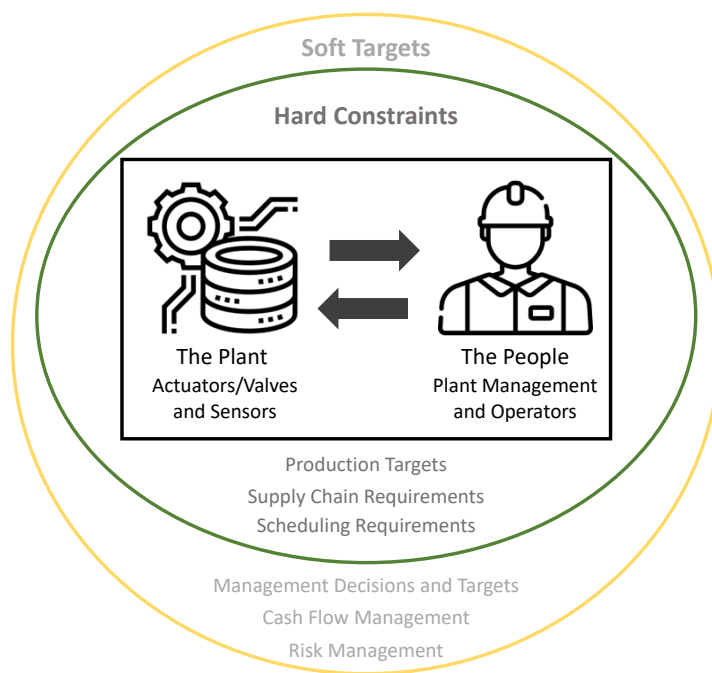


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3 analysis will be performed to understand the plant requirements and how the developments in  
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5 Big Data-based monitoring and control can fulfil them. Lastly, the focus of the manuscript will  
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7 shift to understanding the barriers that must be overcome to implement these evolving  
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9 developments.

## 14 2. Process Operations and Plant Data

### 17 2.1 Operation of (Bio)Chemical Plants

19 Prior to moving forward with the exploration of Big Data-based process monitoring and control,  
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21 it is important to understand “the big picture” of a (bio)chemical plant in terms of its operational  
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23 doctrine.



49 *Figure 1. Operational requirements in a (bio)chemical plant.*

53 As illustrated in Figure 1, the “system” consists of both the plant (the physical infrastructure)  
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55 and the people, who operate the plant, support operations and assume managerial duties. The plant  
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3 not only includes the unit operations and piping, but also the physical devices that facilitate process  
4 data gathering and control. This comprises control valves, sensors (including analysers) as well as  
5 the digital infrastructure such as the DCS (distributed control system) and software that enables  
6 the interaction with the physical plant and the people who operate the plant. Conceptually, this  
7 system may be further extended to account for procedural requirements imposed by the  
8 organization, affecting the execution of operational tasks and beyond. This set-up may be  
9 understood in terms of the P3 framework<sup>11,12</sup>, which accounts for the interactions between  
10 different system element types as well as among elements of the same type. Together, the “system”  
11 works towards ensuring that all hard constraints are met. These constraints are, in general,  
12 contractual obligations such as promised production targets for both external customers as well as  
13 supply-chain requirements, or regulatory constraints such as safety related maintenance work.  
14 Then, the focus shifts to incorporating soft targets, which, in short, look at improving the overall  
15 economics of the plant based on top-level managerial decisions, cash flow optimization as well as  
16 risk management. Both process monitoring and process control work towards satisfying hard  
17 constraints and soft targets.  
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## 40 2.2 The Process Control Hierarchy and its Purpose

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42 The purpose of process monitoring and control is to ensure that both hard constraints and soft  
43 targets are met during daily operations. At the design phase of a plant, it is important to ensure that  
44 the variables that are required to calculate or infer these targets and constraints are actually  
45 included in the design. This is equally valid in the context of Big Data, as having the appropriate  
46 sensor allocation plan so that the data can truly be used to monitor the process and, ultimately,  
47 meet these constraints. To this end, the information needs to be interpreted and decisions need to  
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be made such that proper corrective actions are taken. SPM often requires operators to complete this loop where they have to interpret the result, decide what the remedial action is and implement it on the plant (either through physical action or through the automated controls).

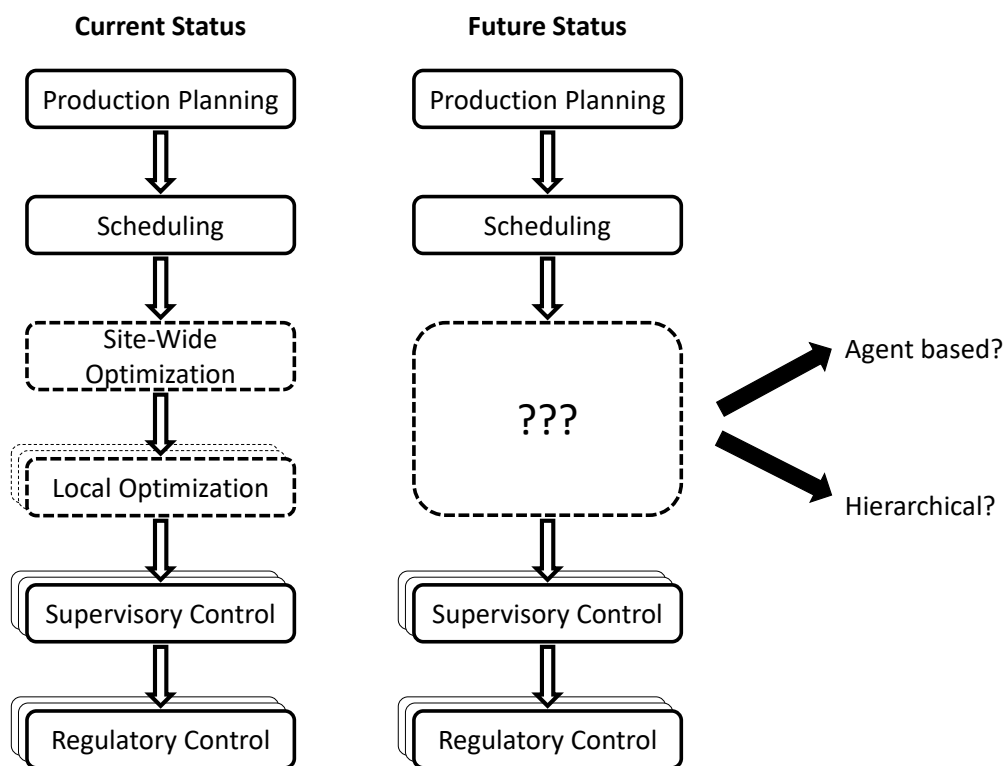


Figure 2. Process control hierarchy.

These targets and constraints are currently managed through a hierarchical approach as illustrated in Figure 2<sup>13</sup>. Both are introduced at the long-term planning, the scheduling and the site-wide optimization levels and passed down to the plant through the layered control structure. However, in practice, the site-wide and local online optimization levels are not available in many industrial operations, which means that these constraints are either pushed up to the planning level or executed at the supervisory control layer. This disconnect also means that the information flow may need to be facilitated by a plant operator or an engineer.

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3 Each layer (starting from the top) is progressively focusing on a subset, or a specific aspect, of  
4 the overall objective of managing targets / constraints and providing process targets (set-points) to  
5 the layer below. Thus, centralized planning decisions taken on time scales of months and years get  
6 distributed across the hierarchy down to “local” control loops that execute in the order of seconds  
7 or less. To this end, the lower levels of the hierarchy are increasingly focused on a smaller area  
8 (space) of the plant, but operate at a much higher frequency.  
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12 However, this hierarchical control structure might change with the current Industry 4.0  
13 developments, which aim at greater agility in instrumentation and its ability to deliver flexibility  
14 in operations with a potentially fully distributed agent-based control structure <sup>14</sup>. These agent-  
15 based control systems can be visualized as a collection of “local” controls (having a scope similar  
16 to advanced regulatory controls), which perform their “local” control function, but are also  
17 interconnected with all other local controls through direct communications. As a result, an agent-  
18 based control system can be visualized as a mesh/network of controls acting collaboratively,  
19 similar to what the internet is to a computer network. Together, these local controls can  
20 communicate directly with each other and share relevant process information and co-ordinate their  
21 actions, which nullifies the need for a hierarchical control structure, as is common today.  
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40 In this context, the key to self-organization is the ability to automatically identify relevant  
41 connections amongst field devices. For instance, the concepts of controllability and observability  
42 could be put to use in finding relevant relationships between variables. Quantitative information  
43 from input / output data could be coupled to structural information, e.g., obtained from P&ID's, to  
44 limit the range of (most) control actions to plant sectors, related fluid streams and equipment. This  
45 scope limitation will most certainly increase the robustness of the identification process, but also  
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3 provide a different type of hierarchy, not in terms of decision-making, but in terms of logical  
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5 composition of plant elements.  
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8 Without an actual implementation, it is difficult to assess benefits and drawbacks at scale.  
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10 Nonetheless, the ability to continuously adapt to varying process conditions and operational  
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12 requirements (as information flow to and from “local” controllers can be dynamically adjusted so  
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14 that different sets of information can be prioritized) appears to be a highly beneficial objective.  
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16 However, such a system does not exhibit natural means to prioritize control actions. All control  
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18 actions from safety requirements, process regulation and optimization are all handled with equal  
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20 levels of priority. Further, the relative complexity, especially for an outside engineer, requires  
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22 specific system assessment techniques and different infrastructure requirements.  
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27 Even though the overall process control hierarchy might not be “ripped and replaced”, data-  
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29 driven concepts will significantly influence the execution and hierarchical nature of site-wide  
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31 optimization, local optimization and, to some extent, the supervisory control layer. This is due to  
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33 the fact that these layers currently rely on fundamental process understanding that utilizes first-  
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35 principles-based models <sup>15</sup>, which have difficulty in accurately capturing secondary and tertiary  
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37 phenomena, such as the generation of impurities as well as long-term effects in (bio)chemical  
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39 processes (e.g., fouling and catalyst activity).  
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### 44 2.3 Process Monitoring vs. Process Control

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47 In the context of this manuscript, it is important to clearly demarcate the boundary between  
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49 statistical process monitoring (SPM) and process control (PC). While both schemes share the same  
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51 goal of lowering the variation in the process and ensuring that soft target and hard process  
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constraints are met (Figure 3), the way in which these two schemes achieve this outcome is different.

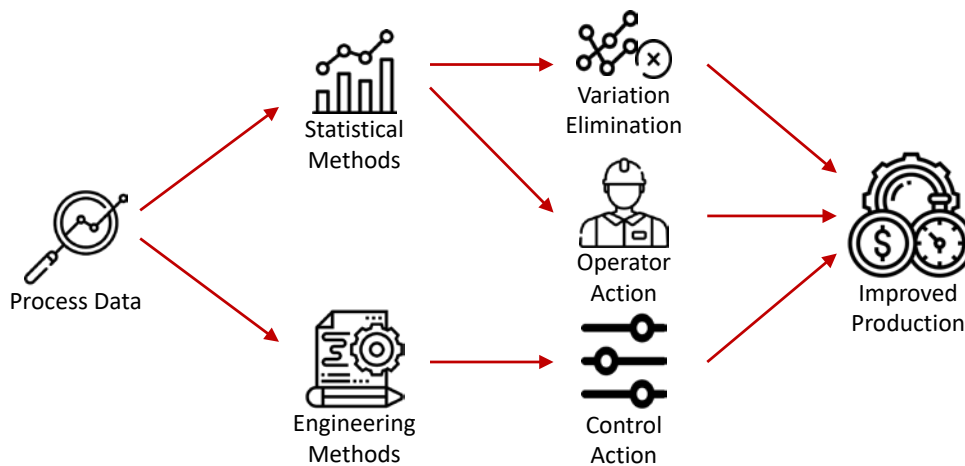


Figure 3. Routes from data to actions.

SPM refers to a broad term that encompasses Statistical Process Control (SPC) methodologies<sup>16</sup>, where the objective is to monitor the progress of the process in real-time and to detect unusual process behavior as it develops. “Unusual behavior” refers to a change in the expected or predicted amount of variation in the process. While this has been the primary concern in process monitoring, increasing emphasis has been placed on diagnosis in recent applications. In the past, the diagnosis was expected to be accomplished by the operators/engineers who possess process understanding and knowledge. This was perfectly reasonable, particularly when process performance was monitored through few process variables or quality metrics. In the evolving era of Big Data, however, processes are more commonly monitored through a multitude of variables. To compensate for issues stemming from multiple testing and potential strong correlation among these variables, summary statistics are often used. This leads to complications in identifying the root cause of an unusual behavior detected by the SPM scheme. Commonly used approaches based on chemometrics methods such as Principal Component Analysis (PCA) and Partial Least Squares

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3 (PLS) claim to achieve detection through summary statistics based on the principal components  
4 rather than the original variables and diagnosis through contributions of these variables to these  
5 statistics. However, the large contributions of certain variables to the monitored statistics may  
6 simply be a consequence and not the cause of the fault. Furthermore, it can be shown that while  
7 effective for simple faults, a diagnostic approach simply based on contributions may not be able  
8 to identify complex faults <sup>17,18</sup>.

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10 In that regard, there is a push towards incorporating data-driven methods for diagnosis on top of  
11 detection <sup>19</sup>, which, in principle, provides the operators with an idea of how to fix the anomaly.  
12 There have been attempts to also use ML algorithms towards achieving this goal <sup>19,20</sup>. This can in  
13 theory still be aligned with the original context of SPC where following an alarm, the culprit, a.k.a.  
14 assignable/specific cause generating the unusual behavior, is expected to be identified and  
15 eliminated, rather than the alarm tempting the practitioner to ‘tinker’ with the process to  
16 compensate for its effect.

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18 In comparison, (closed-loop) process control refers to a situation where data from sensors are  
19 used to calculate and then implement actions via the control valves and other actuators of a process  
20 in real-time. Thus, in real-time closed-loop control, the process is not only actively monitored, but  
21 corrective action is taken as the process progresses to ensure that targets / constraints are met. For  
22 example, Udugama et al. <sup>20</sup> investigated the reasons for off-specification product generation in a  
23 high-purity multi-component industrial methanol distillation column. The middle-boiling ethanol  
24 component that forms a bulge near the side-draw location was the culprit. A soft sensor, which  
25 combined three composition measurement signals (gathered from a multiplexed gas  
26 chromatograph) near the side-draw region, was then used to determine the ethanol bulge location  
27 and size. For normal operations, a PID controller performs the corrective control action by

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3 manipulating the reboiler duty based on the ethanol concentration at the side-draw. However, if  
4 the ethanol bulge was deemed out of the normal operation regime by the soft sensor, process  
5 variable conditioning was applied so that the PID controller would drive the energy balance to  
6 return the ethanol bulge to normal operation.  
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12 The different approaches of these two methodologies, process monitoring vs. closed-loop  
13 process control, often and unfortunately lead to an either-or situation for the practitioners. It  
14 certainly does not help that the two schemes belong to different camps, one led by statisticians and  
15 the other by engineers. Particularly, in many statistical process monitoring applications, the closed-  
16 loop nature of the process is simply ignored or overlooked. However, a few examples can be found  
17 that explicitly discuss this <sup>10,21-26</sup>.  
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26 In the more generic sense, closed-loop control can be seen as a symptom reliever and becomes  
27 effective if the control action is easy and cheap to take. For more persistent disturbances, however,  
28 control action may be too costly. Potentially, this can be more effectively resolved through  
29 monitoring methods. Yet most monitoring methods are developed under open-loop assumptions  
30 and can lead to erroneous conclusions if closed-loop control is present but ignored. Moreover, if a  
31 specific cause is detected and identified, its elimination may require costly actions as well. In that  
32 sense, hybrid approaches that incorporate both schemes can be expected to exploit the synergy that  
33 would be more efficient and effective in variation reduction and optimization.  
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#### 46 47 2.4 The Origin of Data in (Bio)Chemical Plants 48

49 Prior to defining Big Data for the purpose of process monitoring and control, it is important to  
50 understand the potential sources of relevant data available in (bio)chemical manufacturing. The  
51 data originate mainly from the following sources as illustrated in Figure 4.  
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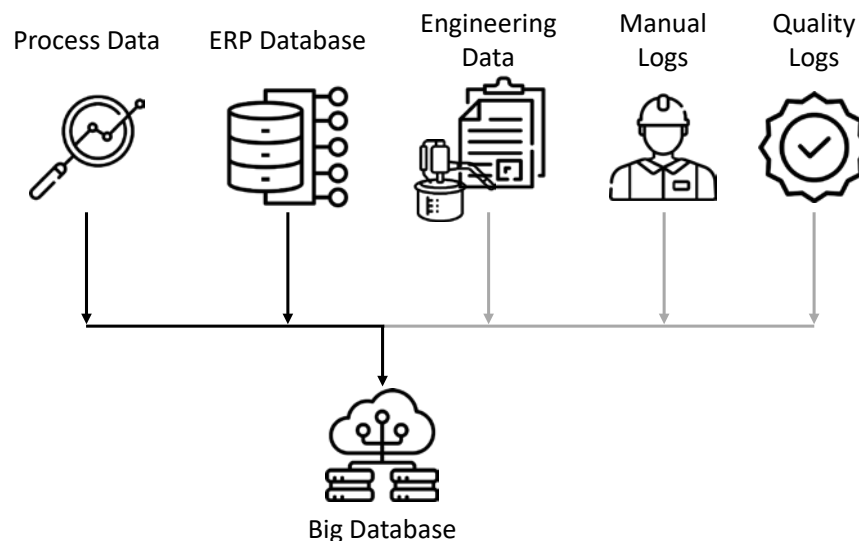


Figure 4. Data repositories in a (bio)chemical plant.

#### 2.4.1 Process Data

Process data comprises time-stamped information gathered from sensors installed in the plant. In general, the historical process data consist of all process variables that are available for plant operators as well as data related to actions taken by the operators over time. In addition, the historical process data may also contain calculated process values such as energy usage or the efficiency values of a key unit operation, start-up and shut-down data related to unit operations (generated at a PLC level). If available, variables that indicate the state of the process (e.g., normal operation, start-up / shut-down, plant trip), the status of control loops (e.g., automatic, manual or cascade) as well as other sensor data (e.g., valve positioner, vibrational measurements of rotating machinery) are tracked.

Historically, for the purpose of storage, these data were mostly compressed, as hard disk space was expensive. Data compression is still used today, but perhaps not to the same extent. Setting standards on data compression and how to deal with inherent irregularities between sampling rates (temperature sensor vs. online composition analyzer) is of importance in ensuring that the recorded

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3 data can be easily accessed for Big Data-based development purposes as opposed to the significant  
4 efforts that are needed in data pre-processing currently. Similarly, having a uniform data time-  
5 stamping protocol between the other sources of data (in particular, quality and Enterprise Resource  
6 Planning (ERP) data) is crucial in ensuring smooth data reconciliation efforts. SPM and PC  
7 activities (including model building <sup>27</sup>) rely on the data that is continuously generated. Hence, it is  
8 important to recognize that the data must comprise unambiguous information about the structure  
9 of the process and any changes to it. For instance, a seemingly insignificant change (control on /  
10 off) may induce nonlinearities and changes the input / output structure.  
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#### 24 2.4.2 Enterprise Resource Planning (ERP) Database

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26 They contain time-stamped information related to what has actually been processed in a plant as  
27 well as information related to equipment usage and breakdowns, resembling a digital logbook. In  
28 particular, day-to-day, week-to-week, month-to-month operations that have a direct effect on the  
29 economic success of a company are documented here. This includes information such as data on  
30 raw materials and other inputs used in production, as well as information related to what has been  
31 processed, in particular, plant recipes and plant capacities. In addition, the ERP system carries  
32 information related to the supply-chain and its constraints. In the context of process control, ERP  
33 data are critical for tracking and tracing equipment breakdowns or changes to raw materials or  
34 production specifications, which inherently affect plant operations. Process historical data and  
35 ERP data can be jointly used to identify stable and relevant process operating periods.  
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### 2.4.3 Engineering Data

During plant design, a wealth of data is created. Steady-state process simulation work generally starts with the development of property data packages and their validation against experimental data and plants that serve as reference. From that foundation, the process layout (flowsheet) is developed, accompanied with material and energy balances. This essentially is the starting point of the plant's life cycle.

These data are subsequently used to engineer the plant in greater detail, spanning diverse domains from equipment design to piping, electrical and instrumentation to civil engineering. As every domain prefers specialized software, there is generally not one (e.g., simulation, calculation or 3D) model with a single database, but several. A case in point is the equipment design, which uses calculation tools with different scenarios (e.g., normal operation or water runs), so that property data packages tailored for process design are often not used. Instead, the rather limited property data needed for such design tasks is often individually specified by the engineers, whenever required. Every domain requires specialized data that is mostly of limited value to other domains. This is due to some extent that the veracity of data remains uncertain. Furthermore, even within the suite of tools of a single software provider, it is not always conveniently possible to exchange and reuse data. The large engineering contractors and in-house engineering divisions appear to have better aligned tools and databases, but even they rely to some extent on abundant labor to make up for the limitations that arise during data interchange. Although joint database systems (e.g., Smartplant Reference Data), data interchange protocols (ISO 15926) and ontologies<sup>28</sup> exist that permit and facilitate rapid data transfer in principle, many companies lack work process consistency (a.k.a. enforced work standards and interface ownership) to leverage such technologies. Besides, the data that is available often gets "lost" during commissioning, because

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3 of the direct and indirect cost of data handling and integration from the contractor. Since such data  
4 sets are not required to operate a plant and incur upfront costs without tangible benefits in sight, it  
5 remains a strategic decision to adopt a Big Data mindset<sup>9,29</sup>.  
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10 Consequently, P&ID data, equipment datasheets, HAZOP studies, operator handbooks and  
11 similar documents are the sole memory of the engineering process. As such, they contain the plant  
12 layout together with all available sensors and control structures. The equipment specifications  
13 encompass physical dimensions of the equipment including practical constraints, such as operating  
14 pressure and temperature, metallurgy and pipe wall thicknesses. This information can be used to  
15 cluster relevant process historical data to given unit operations and to define operating envelopes.  
16  
17 Such data are usually stored in separate repositories, either digital or analogue, and the relevant  
18 data are mostly unavailable for automatic analysis. In the context of process control, a modified  
19 form of the P&ID diagrams is used as the Human Machine Interface (HMI) in many DCS  
20 applications.  
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#### 35 2.4.4 Manual Logs

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37 Considering that many (bio)chemical plants were commissioned in an era prior to Big Data,  
38 there are many data sets that are still recorded manually and are often not available digitally,  
39 though, a shift towards digital logs can be observed. This information can include maintenance  
40 logs, observations, raw material additions or changes to actuators that are carried out by the  
41 operators.  
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#### 2.4.5 Quality Logs

Quality logs are a type of manual logs that are generally attributed to the laboratory analysis of samples. However, these logs may also be attributed to in-line and at-line quality measurements that are performed by plant operators on specialized equipment and are not necessarily carried out at a laboratory. These data are generated by scheduled off-line sampling and analysis recorded by operators as well as quality assurance personnel.

#### 2.4.6 Alternative Sources

In addition to the five areas of data repositories that represent the current state of data utilization, there is the possibility of also exploiting other sources of data. For example, validated dynamic process simulations of key unit operations in plants connected to the operation (also referred to as digital twins) are increasingly being developed in the industry. These simulations, unlike the “physical” process, can easily be used to explore the boundaries of the process envelope without placing the actual process at risk and generate large quantities of process data to augment plant data sets.

Similarly, emerging technologies such as free-floating sensors, tracer experiments and, for that matter, Computational Fluid Dynamics (CFD) models can be used to gather spatio-temporal data that is often missing from the traditional data repositories. Other data sources such as videos and other peripheral sensors may also be beneficial in tracking actions (in particular by operators) when such actions are not recorded.

### 3. Big Data in the Context of (Bio)Chemical Plants

In (bio)chemical plants the aforementioned data have been recorded for decades, but not automatically compiled into a joint database that can be efficiently analyzed and exploited. Consequently, significant efforts by process control engineers have been required to pre-process and pre-structure the different data sources. Hence, analyzing these data sets has been a challenge in (bio)chemical manufacturing even before the Big Data revolution.

Prior to moving forward with a detailed look at the use of data in SPM and PC applications in (bio)chemical processes, it is necessary to address the value proposition and nature of “big data”.

The value proposition of Big Data is somewhat intertwined with the advancement of data-driven process monitoring methodologies. Noticeable groundwork has, in fact, been carried out using data-driven methods to extract meaningful correlations out of Big Data, and it is the foundation of SPC activities<sup>30</sup>, illustrating that Big Data is capable of associating process variables with factors such as quality and the status of unit operations. For example, SPC techniques were employed to predict the harvest time in a fermenter<sup>30</sup>, which for all practical purposes is impossible to accomplish without the existence of Big Data sets. This is also the case even in hybrid approaches that rely on mechanistic models, since Big Data sets are required for both parameter and state estimation both in model development as well as real-time calibrations<sup>31</sup>. Data-driven models have been used to predict future behavior of critical quality parameters in seemingly chaotic systems<sup>32</sup>, where historical and current behaviors of the process are linked to the expected future behavior. In short, the value of “big data” in (bio)chemical operations is its ability to support the operation of complex mechanistic and data-driven tools which can transform this data into critical actionable information for plant operators (engineers) and process control systems. However, it

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3 should be noted that the process control engineers as well as field engineers find these tools  
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5 somewhat complicated to use as these are not off-the-shelf application solutions.  
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8 To understand the nature of big data and thus its inherent value, the “4 Vs” concept<sup>8</sup> can be  
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10 interpreted as follows for (bio)chemical operations:

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12 • Volume: What makes Big Data “big” is the volume of data that is available. This  
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14 is reflected in the number of variables that are recorded at a given frequency over a long-  
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16 enough time span, thus providing a large number of data points. Acquisition of current  
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18 data may be complemented with “static” and “quasi-static” data from other data  
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20 repositories, e.g., design data or internal transfer prices. By their nature, static or quasi-  
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22 static data usually represent many more variables, but fewer data points. It should be  
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24 mentioned that not all large data sets are necessarily “big”. In particular, if a phenomenon  
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26 of interest occurs quite rarely, a Big Data set should contain enough occurrences as to  
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28 provide sufficient insight. A similar point can be made about the breadth of data, or rather  
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30 the lack of it.  
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34 • Velocity: In the context of (bio)chemical operations, one may find two extremes of data  
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36 in terms of the speed with which such data are generated, whereas a faster update rate  
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38 often seems beneficial. Process data originating from process sensors generally have a  
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40 high velocity of data generation. It can be argued that the optimum velocity of data  
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42 generation is a function of the smallest meaningful time constant of the process. As such,  
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44 for process data it might even be beneficial to sacrifice some of the velocity for improved  
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46 accuracy. At the other end of the spectrum, quality logs and manual logs are often  
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48 recorded at a fairly low velocity due to time consuming tests that need to be performed  
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50 and the fact that operators are busy with managing the plant. In these cases, automating  
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3 sampling and testing efforts can significantly improve the speed at which such data  
4 become available. Process analytical technologies (PAT) tackle this need through the  
5 development of soft sensors and inferential sensors that provide operators with  
6 actionable information<sup>33–35</sup>.  
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12 • Variety: As detailed before, there is a large variety of process data available in a  
13 (bio)chemical plant, with different structural properties in separate repositories. For  
14 example, process data is stored with corresponding time stamps and other meta-  
15 information, while ERP data often contain start and end times or datasets sorted  
16 according to a batch number. Alternatively, ERP data may provide time spans for which  
17 settings, recipes, etc. are valid, whereas they do not necessarily indicate whether such  
18 settings are used or to which extent. Generally, ERP data come in many different flavors  
19 and colors, often dependent on organizational hierarchies (business units, geography,  
20 etc.). They often require extensive pre-processing and validation in addition to the  
21 creation of custom-extractors to assemble the data sets for further use, e.g., for BASF's  
22 Verbund-Simulation<sup>36</sup>. Similarly, the quality and manual logs are usually sorted with  
23 batch numbers, while P&ID diagrams contain “static” structural and to some extent  
24 spatial information of the process. As a consequence, the variety of data and the  
25 disjointed and uncoordinated nature of the data structures require significant pre-  
26 processing. By contrast, the difference in velocity within a single type of data (in  
27 particular in process data) necessitates careful reconciliation and pre-processing to align  
28 the data sets.  
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51 • Veracity: Data sets inherently differ in accuracy, precision and the level of trust that can  
52 be placed in them, which is covered by the term veracity. Data volume and data veracity  
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3 can complement each other to some degree, but it remains a challenge to infer insights  
4 and decisions from data of poor quality. Maintenance of sensors in industrial-scale  
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6 and decisions from data of poor quality. Maintenance of sensors in industrial-scale  
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8 chemical facilities is generally dependent on their relevance for operation and even more  
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10 so if the operating license depends on proper servicing and calibration. Safety  
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12 Instrumented Systems (SIS) that ensure a high Safety Integrity Level (SIL) are well  
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14 documented, regularly checked and calibrated. By contrast, conventional installations  
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16 often do not draw much attention, so that their reliability deteriorates over time. Hence,  
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18 readings from conventional sensors are often low quality and permit a qualitative view  
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20 into the process, but their quantitative value is limited. However, validated mechanistic  
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22 models could be used to track the quality of sensors through data reconciliation and to  
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24 infer true values. Similarly, the veracity of manually recorded data, e.g., in ERP systems,  
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26 depends on the organization's culture. Only if the value of correct data is fully ingrained  
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28 in the management and operational layers of an organization, such data can be harvested  
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30 and insights be generated that are indeed generalizable.  
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38 The "4 Vs" discussed above provide a framework for the assessment of the value of data.  
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40 Whenever the data available is sufficient to generate insight into the process, it is clearly of value.  
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42 To be of value, it must be available for analysis in sufficient volume and velocity, covering a  
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44 sufficiently broad variety of relevant factors and be trustworthy (veracity). Then, the data is  
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46 deemed rich in "information". Information richness is of great interest in particular for  
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48 fermentation-based processes, where the typical pressure, flow and temperature sensor data do not  
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50 contain sufficient "information" to predict states of interest such as product formation rates and  
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52 inhibition phenomena. In this instance, prior to unleashing Big Data tools, the focus needs to be  
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3 shifted to data gathering and augmentation that is, in aggregate, information rich, for example, by  
4 making use of image-based data sources<sup>37</sup>. Another example is the use of a non-linear infrared  
5 spectrometer to gather vital state information for a second-generation bioethanol process<sup>31</sup>.  
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#### 11 4. State-of-the-art in Process Monitoring and Process Control

12 As discussed before, Big Data relates to many data of differing characteristics, whose value  
13 arises from its exploitability. Big Data and associated methods are of great value if they provide  
14 actionable information either to operator teams or to automatic controls. In particular, results from  
15 Big Data analytics should provide guidance and insight to make better decisions. Accordingly,  
16 information must be presented in a comprehensible and coherent manner to well-trained operations  
17 staff and domain experts alike to elicit informed decisions.  
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28 To provide an answer to the question whether Big Data-based process monitoring and control  
29 currently exists, the recent developments in these fields and relevant Big Data-based  
30 methodologies employed in other domains are analyzed.  
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##### 38 4.1 Process Monitoring

39 The current state-of-the-art in process monitoring falls into three main classes: model-based,  
40 knowledge-based and data-driven methods<sup>38</sup>.  
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45 The term *model* is used broadly and applies equally to first-principles models derived from  
46 physico-chemical insights into the system as well as qualitative or quantitative relations between  
47 sets of variables. A model-based method in this context often relies on first-principles models. If  
48 such a model is able to represent the true plant state, any deviation between the model and the  
49 plant can be interpreted as an indicator of the health of the process, for which the “digital twin”  
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3 concept has gained increased attention <sup>31</sup>. However, the development and validation of high  
4 fidelity models can be expensive and difficult due to the complexity of current industrial processes  
5 and the size of the operating envelope.  
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10 The knowledge-based methods take advantage of expert domain knowledge, which may be  
11 represented as graphs and trees or as connected objects that represent structural information or  
12 functions <sup>38</sup>. Although the results tend to be more intuitive, gathering all the required knowledge  
13 is a lengthy and costly process.  
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19 Both approaches are of importance in the domain of process monitoring and employ process  
20 data for the purpose of validation and parameter estimation. However, these methods do not  
21 generally utilize large amounts of data and instead focus on specific information (i.e., selected  
22 process measurements). For that reason, neither model-based nor knowledge-based methods will  
23 receive any attention here. Nonetheless, they might prove invaluable in the hybridization of data-  
24 driven methods to compensate for the lack of *a priori*-structure.  
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#### 36 4.1.1 SPC and PCA

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38 Data-driven process monitoring methods have become quite popular, especially when dealing  
39 with complex industrial processes where models and expert knowledge are hard to obtain <sup>39</sup>.  
40 Moreover, the increasing availability of sensors and data gathering systems have subsequently  
41 motivated the development and evolution of data-driven industrial process monitoring methods.  
42 In fact, these methods enabled process control engineers to concatenate large data sets into  
43 comprehensible features to make predictions about crucial process variables. Statistical Process  
44 Control (SPC) involves schemes for continuous monitoring of a production process so as to  
45 identify situations exhibiting more than the expected amount of variation <sup>40</sup>. To this end, SPC  
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3 control charts have been effective over the years to maintain statistical control over critical  
4 manufacturing outputs and other complex systems where the variation originates from a broad  
5 range of sources. Taking into consideration that many industrial processes require simultaneous  
6 monitoring and control of several variables, multivariate extensions of the above-mentioned SPC  
7 methods have also been developed <sup>41</sup>.

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14 However, another important issue when dealing with multiple variables at once is the potentially  
15 high degree of correlation among them. Standard approaches to multivariate SPC as in the case of  
16 Hotelling's  $T^2$  chart are highly impaired under such conditions and an accepted practice to tackle  
17 this issue is to first transform the physical variable space to a space of uncorrelated latent variables,  
18 followed by the development of a low-order model, which captures most of the variance of the  
19 original dataset.

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PCA is the most popular latent structure method for process monitoring due to its ability to  
successfully handle high-dimensional, noisy and highly correlated data <sup>42</sup>. PCA (and PLS) models  
are built on historical datasets, which are assumed to come from a period of "in control" (normal)  
operation; then, the future observation/sample is checked to see if it follows the model <sup>41</sup>. PCA-  
based multivariate monitoring methods have been widely applied for fault detection in chemical  
processes to improve quality and productivity. These methods have the benefit that they can handle  
both process and product quality variables and, even though they have been used primarily in the  
area of chemometrics, they are appealing in any multivariate process setting.

However, in industry a great number of processes exhibit nonlinear behavior, and thus, the use  
of PCA or PLS in cases where the data has nonlinear characteristics leads to poor monitoring  
performance. If nonlinear systems are investigated by applying PCA or PLS, nonlinear effects can  
become partly visible in the higher latent variables. This may hinder the identification of the

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3 optimal number of significant latent variables. To tackle this, several approaches have been  
4 developed along the years, such as the nonlinear PCA method based on auto-associative neural  
5 networks <sup>43</sup> and principal curves modelled with neural networks <sup>44</sup>, which aim at performing a  
6 nonlinear data reduction analogous to PCA. Further, the general function approximation  
7 capabilities of neural networks have been exploited to expand PLS regression to nonlinear  
8 problems <sup>45-47</sup>.

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17 Several examples of the application of PCA to real chemical data from DuPont and other  
18 chemical companies have been discussed and published <sup>42</sup>. Likewise, there have been reported  
19 cases of the application of PLS models in SPC as in monitoring of a distillation unit and a fluidized  
20 bed reactor <sup>48</sup>. It is also important to mention Controller Performance Assessment (CPA) as a  
21 branch of these data-driven methodologies that focus on monitoring and diagnosis of the  
22 performance of process control loops, in particular at the regulatory level <sup>49</sup>.

#### 33 4.1.2 t-SNE, LargeVis and UMAP

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35 t-SNE <sup>50</sup>, LargeVis <sup>51</sup> and UMAP <sup>52</sup> belong to a group of manifold learning techniques that aim  
36 at data reduction. Similar to PCA, such techniques map vectors to a lower dimensional space while  
37 preserving the intrinsic structure of the data. These methods scale to large data sets with millions  
38 of data points, while capturing nonlinearities, in contrast to PCA. UMAP, which represents the  
39 current state of the art, has recently been applied to the visualization of industrial chemical process  
40 data by Dow Inc. <sup>53</sup>. In principle, UMAP and similar techniques may be applied to any monitoring  
41 task.  
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### 4.1.3 Neural Networks

One of the significant commercial applications of (artificial) neural networks (ANNs) is in image classification. Generally, layers of Convolutional Neural Networks (CNNs) are combined with pooling layers to extract features from 3-D data sets, i.e., images. Additional layers provide the ability to extract more complex features. In the context of process monitoring, these type of networks are employed in analyzing time-series of variables that can be “color-coded” either for direct identification of characteristic patterns or Fourier-transformed. An example is given by Wu and Zhao<sup>54</sup>, who use CNNs to identify faults in the Tennessee Eastman process. CNNs have also been proposed and employed in the classification of hyperspectral imaging<sup>55</sup>, which has potential applications in the bio(chemical industries), such as the “real-time” functional property identification<sup>56</sup>. It should be noted that these applications are generally employed to compare a given time window of operations (be it classical process data or data from novel sensors/methods) with overall process operations to identify if there is a departure from the normal operation and to which group this time window of data belongs. As such, these approaches belong to grouping and clustering methods, which are primarily used in process monitoring.

On the other hand, regression-based methodologies such as Recurrent Neural Networks (RNNs) attempt to act as a model identification mechanism, which can ultimately be used in closed-loop control. RNNs feed outputs back to the network and thereby realize a storage (memory) mechanism. This mechanism captures temporal dependencies between input and output data, conceptually similar to a system of discretized ordinary differential equations (ARX-type models). Because of the difficulties that arise from training deep networks (e.g., vanishing gradients), plain RNNs cannot cope with effects that span more than a few time steps, rendering them unsuitable to handle widely differing time constants. For process control and monitoring applications, they

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3 cannot account for the long time-scale associated with process dynamics that must be captured by  
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5 a dynamic model.  
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8 This has led to the development of new architectures such as the Long-Short Term Memory  
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10 (LSTM) <sup>57</sup> or the Gated Recurrent Unit (GRU) <sup>58</sup>, a simplified variant, that enable the training of  
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12 deep networks and thus capturing long-range trends in parallel to short-term effects. In the context  
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14 of (bio)chemical processing, training of such models on input-output data is an act of model  
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16 identification and the resulting model can, in principle, be used for every task that requires dynamic  
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18 models. As stated before, if such a model is able to replicate the true plant state, any deviation  
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20 between the model and the plant can be interpreted as an indicator of the health of the process.  
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24 The pre-processing of data prior to being used in an RNN type model identification is of practical  
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26 importance when dealing with industrial plant data. Auto-encoders learn structural information,  
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28 e.g., correlations among variables, by setting the targets to be the input values. Recreating the input  
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30 through a constrained network helps in the identification of features, similar to PCA <sup>59</sup>. This is  
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32 valuable in high dimensional process data to observe trends. Besides, an auto-encoder could be a  
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34 useful pre-processor to transform input data to latent variables, thus easing the training of the  
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36 network segment, e.g., an RNN-type network attached to the auto-encoder.  
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40 However, the training of ANNs does not just require a lot of data, but a lot of information-rich  
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42 data. This is in particular an issue in continuous production processes such as in chemical and fine  
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44 chemical operations where time-series are often stable and tightly regulated for most of the time,  
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46 as such processes do not provide much dynamic information. Similarly, semi-continuous processes  
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48 such as fermentations often follow similar trends during batch operations, which effectively limits  
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50 the information content of the data obtained. To this end, repurposing of pre-trained models, i.e.  
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52 transfer learning <sup>60,61</sup>, may soften this requirement and widen the range of successful applications.  
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#### 4.1.4 Soft Sensors

Soft sensors are advanced inferential on-line calculations, which combine different types of variables to predict the desired output. This output can then be employed for the purpose of control. Often these sensors are based on data-driven methodologies and are used as input process variables to feedback controllers. They generally rely on models, be they derived from data (e.g., PLS, ANNs or SVM), first principles or part of a Kalman-type filter. In general, such soft sensors are not exclusively a true process monitoring or control concept, but rather an enabling data-driven technology. Luttmann et al.<sup>62</sup> provide an overview of soft sensor techniques applied to bio-based production processes, mainly focusing on mechanistic models and purely data-driven approaches. In recent years, soft sensing techniques using hybrid models have been researched intensively as well<sup>63</sup>.

In some publications, spectroscopic measurements have also been labelled as ‘soft sensors’, which can be explained by the fact that spectra (e.g., near-infrared, Raman) are usually pre-processed followed by a chemometric modelling step, where the chemometric model (in most cases PLS, the industry standard) produces information similar to hardware sensors. It is the authors’ experience that attempts made to employ ANNs in general has not added further value yet to practical applications.

In general, despite the large number of publications on development of soft sensors for bio-based production processes, most developments have been and remain academic with relatively few well-documented applications industrially. This situation is only changing gradually, and is often driven by the fact that there is much easier access to process data in modern bio-based production plants.



## 4.2 Process Control

The domain of closed-loop process control, in contrast to process monitoring, exhibits very few purely data-driven methodologies and concepts that are currently applied in industrial settings. Even though there are examples of data-driven closed-loop control concepts in academia, most are hybrid approaches that augment the capabilities of classical mechanistic process control concepts. These examples are not necessarily Big Data-type applications, but rather methods that act on limited data to account for process nonlinearities.

### 4.2.1 Self-Optimizing Control (SOC)

An established and long-standing example of using data in closed-loop process control is in improving controller performance through self-optimizing or self-tuning controls. In general, self-optimizing control adjusts parameters of a controller (e.g., PID), to improve closed-loop performance. These controllers can adapt in real-time to deal with process nonlinearities and changes in operational requirements. One method of achieving this is to first identify the dynamics of the plant (online model identification) and subsequent decision making based on this model. This is then used to modify the controller parameters in accordance with closed-loop performance measures<sup>64–66</sup>. Alternatively, an ANN can carry out simultaneously both the model identification and the decision-making. For instance, Kumar et al.<sup>67</sup> completely replaced the PID structure with an ANN-based controller with three hidden nodes that acts similar to a PID controller, where a recursive least square training method is used to optimize the performance in real-time.

In general, the concept of a self-optimizing PID controller can be considered as a hybrid approach, where both mechanistic and data-driven concepts are merged to provide a feasible

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3 solution. However, with the relatively sparse use of data (often a single process variable and  
4 manipulated variable value) an argument can be made that SOC applications at a regulatory control  
5 level do not truly utilize Big Data.  
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#### 10 11 12 4.2.2 Model Predictive Control (MPC) 13

14 Model predictive control (MPC) is a control concept used primarily for constraint optimization  
15 of unit operations. In particular, most commercial implementations of MPC structures rely on step-  
16 testing data to derive the input and output relationships (model identification) required to set up an  
17 MPC, be it a linear or a nonlinear model<sup>15,68</sup>. Consequently, even the classic MPC implementations  
18 rely on data in the development of the models used. The use of ANNs for the purpose of model  
19 identification has been an area of both industrial and academic interest since the 90's with Pavilion  
20 Technologies leading the industrial implementation drive. In industry, these model identification  
21 tasks are generally performed offline during the set-up process of an MPC. This is mainly because  
22 the online ("real-time") model identification is seen as a technically complex activity, which  
23 requires a high degree of robustness and well-trained operational support that can be often missing.  
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37 One key technical issue that arises when implementing "real-time" model identification is the  
38 need to extract a model in closed-loop as opposed to the open-loop step tests that can be performed  
39 in an "offline" identification situation. For this reason, MPC concepts suitable for online closed-  
40 loop model re-identification have been explored, in particular for polymerization reactions<sup>69,70</sup>. A  
41 similar concept has also been applied to the control of an artificial pancreas<sup>71</sup>. These MPCs  
42 employ a combination of model accuracy monitoring together with closed-loop model re-  
43 identification to adapt "online" to inherently nonlinear process conditions. In general, these models  
44 employ some form of regression, such as recursive least squares techniques in the model  
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3 identification part, while concepts such as Kalman filters are used to identify the mismatch  
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5 between the model employed and the current state of the process together with performance criteria  
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7 to decide when model identification should be carried out. However, the structure of the process  
8  
9 model is constrained by the initial user specification, hence, these attempts are best categorized as  
10  
11 hybrid approaches.  
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14 In contrast, Akpan and Hassapis<sup>72</sup> have developed a completely ANN-based implementation  
15  
16 of adaptive MPC, representing an almost purely data-driven control attempt. In this instance, an  
17  
18 adaptive recursive least square (ARLS) method is employed for initial model identification, which  
19  
20 is then used to derive a controller design and tuning for control purposes. This process is repeated  
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22 at each point in time whenever new data are available<sup>73</sup>.  
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#### 28 4.2.3 Machine Learning-based Methodologies 29

30 Machine Learning-based algorithms can in general be classified into the three main areas of  
31  
32 supervised and unsupervised learning as well as Reinforcement Learning (RL). Supervised and  
33  
34 unsupervised learning algorithms attempt to find mappings of variables that can be employed to  
35  
36 explain the movement of variables of interest. Unsupervised learning thereby relies on matching  
37  
38 similarities in the data, whereas supervised learning relates input-output data. RL is different as it  
39  
40 aims to derive a control policy by interacting with the system. Random deviations from a policy  
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42 that is acting on the system improve the learned policy, which improves the policy over time. The  
43  
44 general versatility of ML-based methodologies allows these concepts to be applied to a multitude  
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46 of tasks in aiding or performing closed-loop process control.  
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51 A prime example of ML concepts applied in an actual closed-loop setting is the ANN-based  
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53 implementation of an adaptive MPC as discussed in the previous section<sup>72</sup>. In this instance, the  
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3 MPC is used to compute the controller response, but all other aspects of the controller rely on a  
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5 ML concept. Further, concepts such as predictive representation of states <sup>74,75</sup> may be combined  
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7 with a standard MPC in making a decision about whether or not to compensate for a given process  
8  
9 disturbance. The benefit of such a combined MPC strategy is that it reduces the frequency of  
10  
11 control moves a MPC will make, which can have ramifications for some unit operations where,  
12  
13 for example, temperature and pressure swings are undesirable.  
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17 Gautier et al. <sup>76</sup> implemented a model-free strategy based on genetic algorithms (GA) to control  
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19 fluid flow in aerodynamics. This controller performs equally or better than the “state-of-the-art”  
20  
21 mechanistic benchmark. The real value of this approach comes with the identification of a new  
22  
23 control policy. RL utilizes agents that learn a strategy to maximize rewards. They are particularly  
24  
25 well suited to play relatively complicated video games such as Super Mario <sup>77</sup>, whereas more recent  
26  
27 video games with less deterministic gaming engines, such as Angry Birds, have been rather  
28  
29 challenging <sup>78</sup>. These algorithms are somewhat similar to classic closed-loop process control  
30  
31 concepts as they are trained to meet targets and to maximize an objective. They represent another  
32  
33 promising area of research that has been exploited in a limited manner in closed-loop control <sup>79</sup>.  
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37 Mnih et al. <sup>80</sup> trained a deep Q-network to play Atari games with 38 days of game experience.  
38  
39 Considering that only discrete actions are possible and rapid responses from the game engine may  
40  
41 be observed, a direct application to a (bio)chemical plant appears feasible only if the network is  
42  
43 trained on a simulation. Besides, one has to keep in mind that many control actions are continuous  
44  
45 and long-range effects are difficult to pick up and thus to learn. As with the approach by Gautier  
46  
47 et al. <sup>76</sup>, the real value would arise from the identification of new operation policies.  
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51 Further, ML can augment the capabilities of other closed-loop process control concepts, and as  
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53 such establish a pillar in hybrid closed-loop applications. For instance, high-dimensional data such  
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3 as camera pictures (including hyperspectral imaging <sup>56</sup>) can be used to extract features of interest,  
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5 such as functional properties. These features can then be combined with traditional mechanistic  
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7 control concepts such as Fuzzy Logic <sup>81</sup> in control applications. As previously discussed, data pre-  
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9 processors such as auto-encoders extract the relevant features from input data. By omitting the  
10  
11 unneeded data fraction, they reduce noise in the data. This advanced noise filter would allow  
12  
13 controllers to be tuned more aggressively while maintaining robustness.  
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17 Similarly, online monitoring of sensor performance is another avenue in which ML concepts can  
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19 add value to mechanistic control <sup>82,83</sup>, especially when sensors lack the desired level of robustness.  
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21 Process classification and benchmarking with local models <sup>84</sup> can further be used to adjust  
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23 operational objectives, e.g., in the course of catalyst deactivation. This also applies to the controller  
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25 performance assessment (CPA) domain, which focuses on issues such as valve stiction,  
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27 deteriorating measurements and control performance <sup>49</sup>. Beyond the assessment on the individual  
28  
29 controller level, plant-wide clustering methods may help to identify external influences that cause  
30  
31 individual controller performance issues. It should be noted that the content in MPC, SOC and ML  
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33 subtopics in this section seem to be somewhat intertwined. From a “helicopter” perspective, both  
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35 SOC and MPC controllers were originally developed based on “classical” mechanistic process  
36  
37 control philosophies. However, these concepts have increasingly moved towards ML and  
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39 statistical methodologies, in particular when contemplating real-time implementations and  
40  
41 diagnosis, as such becoming hybrid in nature. In contrast, the practical ML methodologies have  
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43 also borrowed elements or concepts from mechanistic process control philosophies. Hence, one  
44  
45 key difference among MPC, SOC and ML is the proportion of mechanistic and data-driven  
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47 methodologies that are employed.  
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## 5. Future Directions

An analysis of the current state of process monitoring and control applications shows that a key step will be the development of methods that merge closed-loop process control with additional functionality. Such functionality may comprise methods for troubleshooting and diagnosing as well as (closed-loop) model identification and the triggering of model updates. This is going to be a natural extension of the established SPM and ML concepts. In this context, it might even be more appropriate to talk about Big Data-*assisted* methods instead of Big Data-*based* methods, to distinguish between added functionality vs. hitherto unseen approaches to closed-loop control.

By contrast, monitoring methods must become aware of implications that arise from the presence of feedback control loops, which are part of the system under investigation and may be turned on and off or modified to account for changing process characteristics. Clearly, monitoring of the system's integrity and performance is of value, but functions that provide quick diagnosing of the underlying issues yield significant additional benefits, especially in the face of retirement of experienced personnel and other organizational restructuring initiatives. Supplementing quantitative monitoring methods with structural information, i.e., engineering data such as P&IDs or knowledge-based methods<sup>38</sup>, may provide the needed reasoning capability.

There are three main drivers that are currently pushing the development of Big Data-based closed-loop control in the (bio)chemical industry. First is the economic value proposition for Big Data-based methods as opposed to the classical mechanistic process control concepts, while second is the availability of ever improving SPM and ML algorithms. The third and final driver comprises the improvements in the digital infrastructure including wireless sensing and cloud computing capabilities.

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3 Any process control concept that promises to reduce the expert time requirement has an inherent  
4 economic drive. Thus, the economic value of SPM and ML methods originates from minimum  
5 engineering and/or expert time for development. However, in practice, these methods can take  
6 similar development and deployment times and expert involvement as classical concepts. Second,  
7 the field of information technology, i.e., computer science and AI, continues to develop advanced  
8 algorithms for a multitude of purposes including facial recognition and natural language  
9 processing (NLP), with increasing capabilities and sophistication. From a process engineering and  
10 (bio)chemical industry perspective, these developments are improving the capabilities of what  
11 SPM and ML algorithms may be able to achieve with limited investment. This relatively ‘free’  
12 technology development is a natural driver to adopt Big Data-based process monitoring and  
13 control. From an implementation point of view, the effort for adopting suitable technologies must  
14 be reasonable, but more importantly, should become well defined over time so that risks and  
15 benefits may be properly assessed ahead of a project’s start. In addition, the assessment of risks  
16 and benefits should become easier over time as the investments in digital infrastructure facilitate  
17 “bolt-on” software implementations and access to additional data sources (data warehousing), for  
18 instance, at the ERP and top layer of the operational hierarchy.  
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### 43 5.1 Added Value in the Control Hierarchy

44 From a fundamental point of view, one can argue that data-driven methods, as opposed to  
45 mechanistic methods, have a greater value proposition when processes appear to be complex and  
46 domain knowledge is lacking.  
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51 At the *regulatory control* level, it is unlikely that Big Data-based SPM concepts will be able to  
52 add further value to the established PID controllers individually. In the authors’ experience, Big  
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3 Data and/or ML tools, including Performance Monitoring tools, may be able to identify  
4 inappropriate, undesirable and/or inadequate PID loop behavior, but, at least to-date, they are  
5 unable to provide causal insights for the same (i.e., interaction with other loops, nonlinear process  
6 behavior or just poor tuning). Thus, while PID control is, in principle, simple and, for many  
7 applications, straightforward to develop for experts and novices alike, domain knowledge (e.g.,  
8 process understanding) is still required to trouble-shoot and resolve unacceptable loop  
9 performance. However, SPM methods that benchmark the performance of control loops<sup>49</sup> have a  
10 distinct value proposition when considering the large number of industrial applications that must  
11 be kept in check by fewer domain-knowledgeable personnel. Furthermore, the value at the  
12 regulatory level arises most likely from the ability of data-driven methodologies to identify  
13 relevant operational issues that may be otherwise difficult to detect on-line, for example, long-  
14 term structural or operational changes at a plant-wide level that affect certain clusters of regulatory  
15 control loops.

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33 At the *supervisory and local optimization level*, the established technology is Model Predictive  
34 Control. MPC has a long track record of handling complex process dynamics. For the more  
35 complex situations (i.e., nonlinearities and state multiplicities), “workarounds” have been created  
36 and extensions implemented to enable the MPC to tackle a wide range of challenges. Thus, the  
37 value proposition of introducing SPM and ML at the “middle layer” is significant, if it improves  
38 dealing with complex process behaviors. In addition, the local optimization layer deals with  
39 hard/soft constraints, which requires on-going development. Nonetheless, even if purely data-  
40 driven controls overcome these deficiencies, they must outperform the current MPC controller if  
41 they are to be adopted in an industrial setting or provide the benefit of user-friendliness, because a  
42 changeover from the current MPC framework requires support staff to be retrained and the new  
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3 set-up to be integrated into the control structure hierarchy. The value proposition of this change  
4 must outweigh the associated burden. A more practical and intermediate step is the hybridization  
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6 of process control concepts of either the prediction (i.e., the replacement of the optimizer with an  
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8 alternative technique) or the implementation part, that is the identification of unstructured process  
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10 models, which could provide lasting value.  
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15 In comparison, at the *site-wide optimization and scheduling level*, the value proposition of SPM  
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17 methods seems to be limited, as the decisions made at these levels are mostly well-defined and  
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19 discrete. The current optimization algorithms (typically based on Linear Programming) are well  
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21 suited for scheduling and optimization tasks, sometimes even considering the stochastic nature of  
22  
23 the process. The value proposition of data-driven methodologies at these top layers therefore relies  
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25 on their ability to pre-detect situations and scenarios that would have otherwise been deemed  
26  
27 impossible to detect, or to incorporate unstructured information (e.g., contractual information) into  
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29 the decision-making process. One relatively recent development is the reformulation of MPC as  
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31 Economic MPC (EMPC) to integrate the real-time optimization hierarchy<sup>85</sup>. It would be important  
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33 to monitor the progress of this technology as a viable alternative for higher-level decisions.  
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## 40 5.2 Added Value in the Development of the Control Structure

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42 If automated and on-line model identification becomes feasible at all levels of the process control  
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44 hierarchy, SPM and ML methods will minimize the requirement for data treatment and model  
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46 identification that is currently carried out manually by process control engineers. Thus, such  
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48 methodologies may reduce the time and cost required to develop and implement process control  
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50 solutions. Furthermore, the process control structures that are developed from the regulatory  
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52 control to optimization layers could benefit from concepts such as real-time model adaptation and  
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3 tuning, which, in principle, would allow for better performance over time while providing the  
4 ability to handle a wider operating envelope. However, this could also be carried out as a  
5 monitoring task, so that a process control engineer can modify the models and tuning parameters  
6 as necessary.  
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12 Performance monitoring and diagnosis of process control structures throughout the hierarchy is  
13 another area that may benefit from SPM and ML methods. These methods can be used to  
14 effectively identify and “flag” controller structures that are not performing optimally and  
15 additionally identify time periods during which the process or a key process variable is out of the  
16 normal operating range.  
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24 Based on these observations, it can be seen that the future direction of integrating SPM and ML  
25 into closed-loop process control should focus on the development of complementary hybrid  
26 solutions where monitoring and control can be combined synergistically. This combined approach  
27 will have benefits at all levels of the process control hierarchy, but, in particular, at the supervisory  
28 and local optimization layers, both in terms of performance and effort required for implementation  
29 and on-going maintenance.  
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## 40 6. Practical Considerations

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42 Apart from the technical hurdles that need to be overcome, other practical limitations may hinder  
43 widespread adoption and implementation (Figure 5). Therefore, this section sheds light on issues  
44 that must be resolved in order to implement Big Data-based closed-loop control concepts in  
45 practice.  
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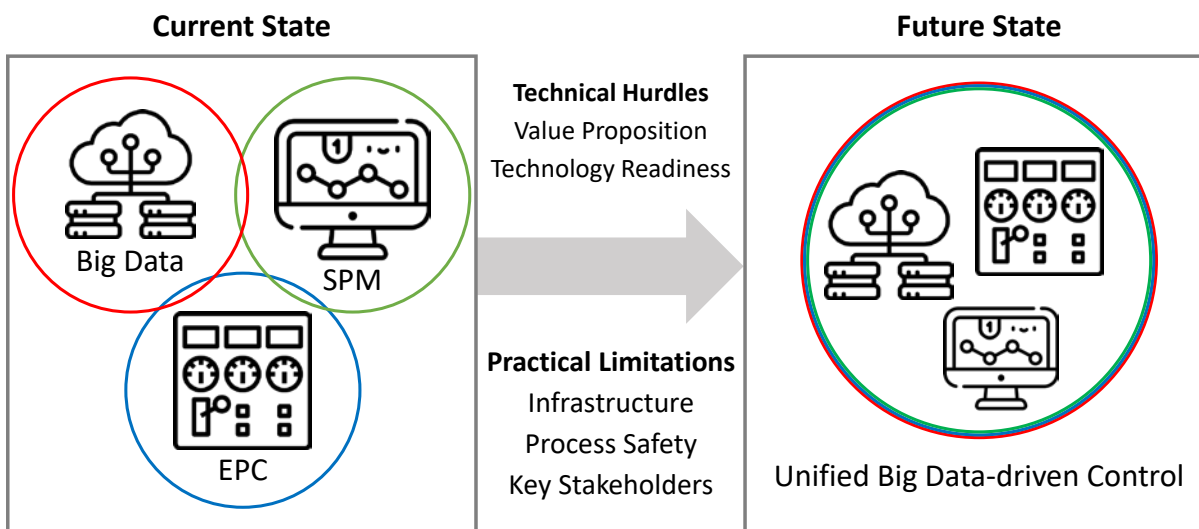


Figure 5. Practical limitations and hurdles in the implementation of data-driven closed-loop process control methods.

## 6.1 Operational Safety and Deterministic Behavior

A key “sticking point” that hinders the implementation of data-driven concepts is the aversion of process engineers to trust a concept they cannot inspect from the inside. This is because data-driven methods by nature represent grey-box or black-box models.

Both process control engineers and operators have very little understanding as to why a specific control action may be suggested by a data-driven methodology. In general, this is an issue when introducing any novel control concept. For example, the early MPC implementations were often abandoned as the operators neither understood nor agreed with the control moves made. The MPC’s mechanistic underpinnings were too complex for the field control engineer and the operator to easily understand.

One way to convince and educate both engineers and operators of the benefits and reliability of new data-driven control concepts is to develop platforms, i.e., digital twins, on which their capabilities are demonstrated without putting the actual process at risk<sup>86</sup>. There is also a need for

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3 new curricula and courses to educate and provide continuing education of students, engineers and  
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5 operators in Big Data tools and approaches.  
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## 10 6.2 Adding SPM Methods to Closed-loop Controlled Systems

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12 The day-to-day operations of many (bio)chemical plants have a significant number of closed-  
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14 loop controls at all levels of the control hierarchy. However, it has also been an industrial practice  
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16 for some local optimizing control loops to operate in pseudo-closed-loop where the operators make  
17  
18 changes based on information received from the process models. In order to capture the full benefit  
19  
20 of SPM in (bio)chemical process operations, there is a clear need to identify and develop SPM  
21  
22 methods that can operate within this framework. Both sparse PCA <sup>16</sup>, where the SPM method  
23  
24 operates on top of the regulatory and advanced regulatory control layer to provide valuable  
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26 information, and controller performance monitoring concepts <sup>49</sup> are designed to complement the  
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28 existing closed-loop controls. In both of these examples, the classic engineering based closed-loop  
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30 controllers are augmented with the capabilities of the statistical methods. This type of combined  
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32 thinking shows how a synergistic approach where statistical control concepts add value to the  
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34 process control concepts is better than attempting to replace the existing engineering controls.  
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## 42 6.3 Big Data Readiness in the (Bio)Chemical Industries

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44 In comparison to many other industries, the (bio)chemical industries have a proven track record  
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46 of having sensors embedded in its processes and collecting large amounts of data. However, the  
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48 data collected requires further structuring and pre-processing. Moreover, the use of data  
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50 compression reduces the quality and the quantity of available process data, which diminishes their  
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52 ability to identify relationships between phenomena of interest and potential process variables  
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3 behavior, since it can destroy potential multivariate features in the data <sup>87,88</sup>. As a result of these  
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5 deficiencies, a significant amount of pre-processing is required before these datasets can be used  
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7 for real-time data-driven process monitoring.  
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10 This problem is further exacerbated by recipe data as well as other key pieces of information,  
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12 which are sometimes only available as scanned documents or in paper form, which require an  
13  
14 additional digitalization step. This lack of digital data has been an area of active focus in the  
15  
16 (bio)chemical industry, where noticeable resources and personnel are devoted to continual data  
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18 reviews and internal programs focused on educating key stakeholders about the benefits of having  
19  
20 digital data. Furthermore, a few companies in the process industries are investing heavily in  
21  
22 making process data accessible in the cloud, such that process chemists are given the opportunity  
23  
24 to easily compare data across batches within one production site, but also across production sites.  
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26 However, many corporations still prefer to keep process data in dedicated internal historian servers  
27  
28 due to perceived cybersecurity concerns. This can, as a first benefit, yield a direct optimization  
29  
30 potential by comparing and adjusting batch or fed-batch process performance across sites.  
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32 Moreover, it finally results in a situation where ML and AI tools can be readily applied to the  
33  
34 collected process data. Undoubtedly, the next step should then be closing the loop, and adjusting  
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36 process set-points based on real-time information about the state of the process inferred from the  
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38 data.  
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#### 47 6.4 Convincing Key Stakeholders 48

49 In order for Big Data-based closed-loop controls to be implemented at any part of the control  
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51 hierarchy, there is the need to convince multiple stakeholders within an organization that the  
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53 solution does not just add value, but also provides an equal level of process safety as conventional  
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3 solutions do. From a plant operations perspective, the key stakeholders in a control changeover are  
4 management, (technical and field) engineers and operators with often conflicting expectations and  
5 requirements.  
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10 In today's economic environment, plant managers can be convinced to implement Big Data-  
11 based closed-loop control as there is support for Industry 4.0 and Big Data topics from corporate  
12 management. However, plant management is generally risk averse and might opt to invest time  
13 and resources on other (Big Data) applications, e.g., predictive maintenance, where risk can be  
14 better managed.  
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21 Technical and field engineers must be convinced that they can reasonably fix and alter the  
22 Big Data-based closed-loop controllers if needed, as their primary role is to act as operations  
23 support and ensure an implemented solution is kept in operation over time. One key benefit of  
24 Big Data-based concepts is their adaptability to changing process conditions, e.g., due to catalyst  
25 deactivation. This ability to cyclically re-identify or modify models promises a better  
26 representation of the plant for longer periods of time without intervention from operations support.  
27 Hence, it may be argued that Big Data-based control loops will require less operations support  
28 than classical ones. Although, whenever operational support is needed, the current technical  
29 engineers might require additional help in the form of either a dedicated Big Data control support  
30 engineer or IT support. An additional requirement is further support over the solution's lifetime.  
31 Finally, development of training and continuing education <sup>86</sup> in Big Data concepts and tools is also  
32 a necessary requirement to support such approaches.  
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49 One should keep in mind that the primary task of the operator is to ensure that the plant operates  
50 within the safety limits and Big Data control concepts must not distract the operators from this  
51 primary responsibility.  
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## 7. Conclusions

Even though researchers and engineers have been working on data-driven techniques to improve process monitoring and control for decades, the increase in computing power and recent algorithmic developments in other business areas make for exciting possibilities in the Big Data domain. Methods like predictive maintenance are on the verge of large-scale deployment to real world (bio)chemical facilities, which illustrates the underlying potential. However, methods aiming at closing the loop still require development work as well as education/training to ensure workforce acceptance and the high degree of automation that is required to add sufficient value to warrant the technical and organizational changes.

Further, not all methods (e.g., in SPC) are equally suited to handle complex time-dependent closed-loop systems, requiring targeted development work. The process industries exhibit specific characteristics that need to be dealt with. (Bio)Chemical processes continuously generate lots of data, but they are information-poor. Most data points are serially correlated; *a priori*-knowledge and first principles have to be incorporated as to leverage these vast amounts of data, which underlines the need for hybrid approaches. Otherwise, it is difficult to imagine that purely data-driven techniques can fully compensate for the low information-value of process data and instill confidence among operations and management.

Nevertheless, the greatest value addition is expected in the middle layers of the control structure hierarchy, where model development is time consuming and expensive and softly-constrained optimization requires further progress. Machine Learning techniques may overcome these drawbacks and may excel in slowly and continuously changing environments. Moreover, the creation and implementation of easy-to-use capabilities, such as processing of datasets of *any* size and integrated non-linear model fitting, may also provide lasting value. Finally, for Big Data

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3 techniques to materialize in an organization and to reap the benefits, a key element is the creation  
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5 of a data-centric organizational mindset. Only data of known value that is readily accessible will  
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7 provide the basis for successful and long-living Big Data applications throughout an organization.  
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